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## Indicated diagrams of low temperature differential Stirling engines with channel-shaped heat exchangers

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#### A R T I C L E I N F O

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#### ABSTRACT

The low temperature differential Stirling engine with channel-shaped heat exchangers and regenerators achieved approximately 5 times the indicated power per a stroke volume of displacer of the cases using flat-shaped heat exchangers. The ratio of the maximum fluctuation of ensemble averaged working fluid temperatures, which is the ratio of the internal energy fluctuation to the heat capacity of the working fluid, to the temperature difference between the two heat exchangers in cases using flat-shaped heat exchangers was 0.08–0.09, that in cases using channel-shaped heat exchangers was 0.10–0.17, and that in case using channel-shaped heat exchangers and regenerators was 0.21. The improvement in the experiments is lower than the estimation by the CFD. In terms of the polytropic index, low temperature differential Stirling engines with channel-shaped heat exchangers and regenerators obtained a higher value than low temperature differential Stirling engines with flat-shaped heat exchangers before the displacer reached the dead center.

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#### 1. Introduction

The aim of this study is the development of a low temperature differential (LTD) Stirling engine (SE) with a heat source temperature below 100 °C for a personal-use application. A LTDSE can generate brake power from a low-exergy heat source. A non-fuel combustion heat source is available, although LTDSEs can receive only part of the energy from such a heat source. Therefore, it is difficult to define the energy supply in the discussion of thermal efficiency. However, the problem to solve is power, not thermal efficiency. The poor power output discourages the practical use of LTDSEs.

The first low-temperature differential Stirling engine was presented at the International University Center in Dubrovnik in 1983 [1]. Ohyagi et al. [2] reported experimental data from a LTDSE that utilized atmospheric air as the working fluid and operated with an approximately 18 °C temperature difference between the heat source and the heat sink. Kongtragool and Wongwises [3] reported the experimentally determined effect of some parameters on brake power. Karabulut et al. [4] reported that a beta configuration SE reports that practical LTDSEs have generated watt-level power with a heat source temperature of approximately 100 °C. Schleder and Zoppke [5] developed a practical LTDSE called "Sunwell50". This SE worked as a water pump, and the energy source was sunlight. Hoshino and Yoshihara [6] developed two free piston beta SEs with an expansion space temperature of 100 °C. One of the engines that Hoshino and Yoshihara developed is based on the test models of a free piston SE converter, which was developed for the demonstration of solar heat energy utilization for future aerospace applications. In another engine that they developed, the working fluid was helium with a mean pressure of 0.5 MPa. According to their report, the piston power output, the difference between the indicated power and the work required to move the displacer, was 11.8 W, although the electrical power output from the mismatched linear alternator was approximately 1 or 2 W. In this case, the frequency of the piston and the displacer may be 35 Hz with strokes of 8 mm; the expansion space temperature was 100 °C, and the coolant temperature was 20 °C. These reports suggest that LTDSEs for practical use can be realized.

could operate with a hot end temperature of 93 °C. There are some

Table 1 shows the evaluations of LTDSEs from previous works. Takeuchi et al. [7] reported their SE operated by 300 °C- oil as a LTDSE. Tavakolpour et al. [8] reported LTDSE heated by solar collector. Kato [9] reported indicated diagrams. The West number  $W_N$ [10] is defined by Eq. (1), where The Beale number  $B_N$  is expressed



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Abbreviations: CFD, Computational fluid dynamics; LTD, Low temperature differential; SE, Stirling engine; MFEAWFT, the maximum fluctuation of ensemble averaged working fluid temperature.

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Nomenclature		$\overline{T_{C}}$	Ensemble averaged temperatures of the cold side section in the displacer chamber [K]		
B <sub>N</sub>	Beale number [W/(bar·cc·Hz)]	T <sub>Cin</sub>	Temperature of the working fluid flowing into the cold		
C	Specific heat $[J/(kg \cdot K)]$	<sup>4</sup> Cin	side section in the displacer chamber [K]		
$C_1$	Coefficient	T <sub>Cw</sub>	Heat exchanger temperature of the cold side section in		
$C_2$	Coefficient	- CW	the displacer chamber [K]		
$\tilde{C_{\mu}}$	Coefficient	$T_{\rm h}$	The hot side temperature [K]		
Ĕ	Coefficient	$\frac{T_{\rm H}}{T_{\rm H}}$	Ensemble averaged temperatures in the hot side		
h	Ratio of temperature differences	•н	section of the displacer chamber [K]		
h <sub>C</sub>	Ratio of temperature differences in cold side	T <sub>Hin</sub>	Temperature of the working fluid flowing into the hot		
$h_{ m H}$	Ratio of temperature differences in hot side	- 1 1111	side section in the displacer chamber [K]		
k	Turbulent kinetic energy	T <sub>Hw</sub>	Heat exchanger temperature of the hot side section in		
т	Mass of working fluid [kg]		the displacer chamber [K]		
п	Engine speed[Hz]	U	Time averaged velocity in the horizontal direction [m/		
р	Pressure [Pa]		s]		
$p_1$	Pressure [Pa]	$u_{ au}$	Friction velocity [m/s]		
$p_2$	Pressure [Pa]	ΔU	Internal energy fluctuation of the working fluid during		
<i>p</i> <sub>3</sub>	Pressure [Pa]		one cycle [J]		
P'm	Mean pressure used for the estimation by the Beale	V	Volume [m <sup>3</sup> ]		
C C	number [bar]	$V_1$	Volume [m <sup>3</sup> ]		
Q <sub>Cin</sub>	Internal energy contained by the working fluid flowing	$V_2$	Volume [m <sup>3</sup> ]		
6	from the cold side to the regenerator	$V_3$	Volume [m <sup>3</sup> ]		
Q <sub>Cout</sub>	Internal energy contained by the working fluid flowing	V'	Volume used for the estimation by the Beale number		
0	from the regenerator to the cold side		[cc]		
$Q_{\rm Hin}$	Internal energy contained by the working fluid flowing	$W_{\rm N}$	West number		
0	from the hot side to the regenerator	Wout	Brake power used for the estimation by the Beale		
Q <sub>Hout</sub>	Internal energy contained by the working fluid flowing from the regenerator to the hot side		number [W]		
P	from the regenerator to the hot side	x <sub>stD</sub>	Stroke of the displacer [m]		
R S-	Gas constant [J/(kg·K)] Cross-sectional area of the displacer chamber [m <sup>2</sup> ]	$y^+$	Dimensionless length [–]		
$S_{\rm D}$ $T_1$	Temperature [K]	α	Phase angle, which is difference between the phase		
$T_1$ $T_2$	Temperature [K]		angle of a displacer oscillation and the phase angle of a		
$T_2$ $T_3$	Temperature [K]		power piston oscillation		
13 T <sub>average</sub>	Ensemble averaged temperatures in the section below	$\eta_{ m R}$	Regenerator efficiency [–]		
* average	the displacer [K]	$\varphi$	Phase angle of power piston oscillation in a calculation.		
( <i>AT</i>	$_{\rm ge}$ max Maximum fluctuation of ensemble averaged	-	The volume is minimum when $\varphi = 0$		
working fluid temperature [K]		$\sigma_{\varepsilon}$	Coefficient [-]		
T <sub>c</sub>	The cold side temperature [K]	$\sigma_k$ $\sigma$	Coefficient [-]		
-L		au	$T_{\rm c}/T_{\rm h}$ [–]		

by Eq. (2). The performance difference shown in Table 1 is significant. In terms of West number  $W_N$ , the maximum value is 83 times of minimum value in Table 1. The difference of West number  $W_N$ causes the difference of power, as engine speed, mean pressure and stroke volume effect on an engine power. However, the reason for the difference is not clarified. Therefore, a discussion based on a basic mechanical engineering is required.

$$W_{\rm N} = 10B_{\rm N}\frac{1+\tau}{1-\tau} \tag{1}$$

Table 1	
West numbers of LTDSEs	from previous works.

	W <sub>N</sub>	Wout	n	$V = S_{\rm D} x_{\rm stD}$	P'm	$T_{\rm h}$	T <sub>c</sub>
		[W]	[Hz]	$[\times 10^{-3} m^3]$	[kPa]	[°C]	[°C]
Ref. [7]	$1.2 \times 10^{-1}$	$1.0 \times 10^4$	15	28.51	600	300	20
Ref. [3]	$1.5 \times 10^{-2}$	$9.0 \times 10^{-1}$	0.7	6.39	100	126	34
Ref. [8]	$1.8 \times 10^{-3}$	$1.5  imes 10^{-1}$	0.5	14.52	100	110	25
Ref. [2]	$1.4 \times 10^{-3}$	$1.0 \times 10^{-3}$	0.2	1.15	100	22	4
Ref. [9]	$4.1 \times 10^{-3}$	$3.3  imes 10^{-3}$	0.8	0.24	100	56	28
Ref. [9]	$5.2  imes 10^{-3}$	$2.2  imes 10^{-3}$	0.6	0.24	100	44	25

$$W_{\rm out} = B_{\rm N} P'_{\rm m} V' n$$

(2)

Kato [9] suggested that the indicated work of a conventional LTDSE was much lower than the thermodynamic upper limit. Fig. 1 shows the schematic views of the tested LTDSE, a conventional LTDSE. The shape of the heat exchangers was flat. The heat exchangers are installed on both the top and bottom of the displacer

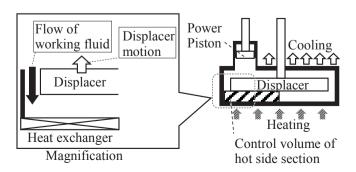


Fig. 1. Schematic views of a LTDSE with flat-shaped heat exchangers.

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