



Research Paper

A time and wavelength dependent heat and mass transfer model

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ARTICLE INFO

Article history:

Received 22 December 2016

Revised 18 June 2017

Accepted 5 August 2017

Available online 18 September 2017

Keywords:

Heat and mass transfer

Porous medium

Radiation heat transfer

Wavelength heat transfer

Greenhouse energy system

ABSTRACT

This work presents a representation of the heat and mass processes dependent on wavelength spectrum which acts in a radiative cavity filled with a fluid mixture and interfaced with a porous medium. The formulation mainly aims to account for the wavelength dependent response of the transparent solid material and all involving constituents in order to improve the simulation of their radiation interaction. The model is based on a set of governing equations of mass, momentums and energy balance approximated by a finite-difference scheme and some empirical relations. The model is validated against data measured in a field experimentation of a greenhouse. The reasonable agreement between numerical and experimental results, in term of temperature and water mass content of fluid and porous medium, demonstrate the effectiveness of the proposed numerical model.

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1. Introduction

Heat and mass transfer in a solid cavity filled with a fluid mixture and interfaced with a porous medium, concerns a wide variety of practical problems, agriculture greenhouses, engineering materials, industrial and food processing, energy storage [1–3]. Heat transfer in solid and porous medium [4] when radiation transfer is predominant over conduction and convection ones has been considered in scientific works, above all for high temperatures [5–7] or transparent-greenhouse systems [8–11].

Numerical modeling is a widely employed tool in heat flux and mass flux prediction of the response of a physical system although it remains complementary to experimental data. Numerical simulation of energy and mass exchange between physical components should account all the heat transfer modes: conductive, convective and radiative. Generally, the radiative mode transfer is approached by not effectively considering direction and diffuse wavelength variability of radiation participating elements. This approach can be around acceptable only when the elements are opaque not, instead, when the elements are semi-transparent.

The proposed model is physically based and split into its participating sub-systems, in a modular-type mode. This seems advantageous when wavelength-dependent and multiple scattering radiative variables deeply regulate energy gain. Other models such

as empirical ones use parameters with no physical inference and, being strongly dependent on input data, they can drop for applicability away from their strictly validation field.

This work proposes a representation of the physical processes dependent on wavelength spectrum which acts in a radiative cavity system. The present approach takes into account the monochromatic variability of absorptivity, transmissivity and reflectivity of all the involving constituents, semi-transparent and grey bodies [12–14]. The model is validated upon an experimental data set measured in field, from Sivoletta [15], for a case study of a greenhouse-soil system.

The model is based on a set of governing equations of mass, momentums and energy balance approximated by the Finite Difference Method (FDM) [16–17]. As starting point of the discretization process the FDM uses the strong or differential form of the governing equations, instead other available methods, Finite Volume Method (FVM) [18] and Finite Element Method (FEM) [19], use the weak or integral form of the governing equations, by reducing requirements on the regularity or smoothness of the solution. They can be advantageous, against FDM, to treat boundary conditions and discontinuity. However, the FDM has been chosen in this work mainly for its straightforwardness to implement in software code.

2. Materials and methods

The numerical model is applied to study the heat and mass behavior of a greenhouse as shown in Fig. 1a, under climate and

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Nomenclature

$\bar{a}_\lambda, a_\lambda$	monochromatic direct, diffuse absorptivity, dimensionless	Subscripts	
A	area of the surface, m^2	a	air phase
c_p	specific heat at constant pressure, $J\ kg^{-1}\ K^{-1}$	b	blackbody
d	characteristic dimension, geometrical distance, m	c	vegetation
D_{Tl}	thermal diffusivity for liquid phase, $m^2\ s^{-1}\ K^{-1}$	cri	critical
D_{Tv}	thermal diffusivity for vapor phase, $m^2\ s^{-1}\ K^{-1}$	d	dew point
D_{wv}	moisture diffusivity for liquid phase, $m^2\ s^{-1}$	e, h	e – th, h – th element, surface, node
D_{wl}	moisture diffusivity for vapor phase, $m^2\ s^{-1}$	f	fluid medium
D_w	diffusivity of water vapor, $m^2\ s^{-1}$	$f\gamma$	fluid phase
$\underline{e}_\lambda, e_\lambda$	direct, diffuse emissivity, dimensionless	i, j, k	indexes of grid nodes
$\underline{E}_\lambda, E_\lambda$	monochromatic direct and emissive power, Wm^{-2}	l	liquid phase
F	view factor, dimensionless	o	outside environment
\underline{f}	vector of body force for unit volume, $kg\ s^{-1}\ m^{-2}$	ot	windows
g	acceleration of gravity, $9.81\ ms^{-2}$	ow	open windows
$\underline{G}_\lambda, G_\lambda$	direct, diffuse received incident radiative heat flux, Wm^{-2}	p	porous medium
h	convective heat transfer coefficient, $Wm^{-2}\ K^{-1}$	$p\gamma$	porous phase
H	hydraulic conductivity of water in soil, $m\ s^{-1}$	ref	reference value at standard atmospheric pressure, $1.01325 \cdot 10^5\ Pa$, and at standard temperature, $273.15\ K$
k	conductivity heat transfer coefficient, $Wm^{-1}\ K^{-1}$	res	residual
i	internal energy per unit mass for the fluid, $J\ kg^{-1}$	s	transparent solid medium
l_i	leaf area index, dimensionless	sat	at saturation
L	latent heat of vaporization of water, $J\ kg^{-1}$	sky	sky
$\underline{\dot{m}}$	mass rate flow for unit area, $kg\ s^{-1}\ m^{-2}$	v	vapor phase
\dot{m}	specific rate of mass generation, $kg\ s^{-1}\ m^{-2}$	w	water
$\underline{\dot{q}}$	vector of the rate water mass generation per unit volume, kgm^{-3}	γ	phase
$\underline{\dot{m}}$	water liquid flux, $kg\ s^{-1}\ m^{-2}$	λ	monochromatic
$\underline{\dot{m}}_v$	water vapor flux, $kg\ s^{-1}\ m^{-2}$	0	initial value
\dot{m}_{ov}	mass rate flow of vapor phase, in the moist-air mixture, at open windows, $kg\ s^{-1}\ m^{-2}$	Greek symbols	
\dot{m}_{fv}	mass rate flow of vapor phase, in the moist-air mixture, at porous medium fluid interface, $kg\ s^{-1}\ m^{-2}$	α_c	corrective coefficient for evaporative mass flux, dimensionless
\dot{m}_{cv}	vapor phase mass flow rate, in the moist-air mixture, from vegetation, $kg\ s^{-1}\ m^{-2}$	β	thermal expansion coefficient, K^{-1}
Nu	Nusselt number, dimensionless	δ	volumetric transfer coefficient, $m^3\ s^{-1}$
\underline{n}	unit outward normal vector, m	δ_{fo}	volumetric transfer coefficient for forced evaporation, $m^3\ s^{-1}$
Pr	Prandtl number, dimensionless	δ_{fr}	volumetric transfer coefficient for free evaporation, $m^3\ s^{-1}$
p	partial pressure, Pa	φ	longitude angle, $^\circ$
p_t	atmospheric pressure, Pa	γ	water vapor resistance of vegetation, sm^{-1}
p_v	water vapor pressure, Pa	η_w	efficiency factor of the windows, dimensionless
p_{vsat}	saturation water vapor pressure, Pa	ϕ_{pv}	mass ratio of a phase, dimensionless
\dot{q}	specific rate of heat generation, Wm^{-2}	λ	wavelength, μm
$\underline{\dot{q}}$	heat flux vector per unit area, Wm^{-2}	μ	dynamic viscosity, $kg\ m^{-1}\ s^{-1}$
$\underline{r}_\lambda, r_\lambda$	monochromatic direct, diffuse reflectivity, dimensionless	ν	kinematic viscosity, $m^2\ s^{-1}$
$\underline{R}_\lambda, R_\lambda$	direct, diffuse radiosity, Wm^{-2}	θ	co-latitude angle, $^\circ$
R_g	gas constant, $J\ kg^{-1}\ K^{-1}$	ρ	phase density, $kg\ m^{-3}$
Re	Reynolds number, dimensionless	$\bar{\rho}$	medium bulk density, $kg\ m^{-3}$
\underline{S}, S	solar direct, diffuse irradiance, Wm^{-2}	ζ	shape factor, dimensionless
Sc	Schmidt number, dimensionless	ω	volumetric fraction of a phase, porous medium porosity, m^3m^{-3}
$\underline{t}_\lambda, t_\lambda$	monochromatic direct, diffuse transmissivity, dimensionless	Ψ	matric potential, m
t	time, s	Mathematical operators	
T	temperature, K	Φ	typical vector field
\underline{v}	fluid velocity vector, ms^{-1}	ψ	typical scalar field
$\underline{\bar{v}}$	bulk velocity vector, ms^{-1}	Δ	difference operator
\underline{x}	point position vector in a Cartesian system, m	∇	gradient operator
x, y, z	point position coordinates in a Cartesian system, m	$\nabla \cdot$	divergence operator
X	air humidity ratio, $kg^1\ kg^{-1}$		

control loads, in an unsteady regime. The physical system is geometrically discretized (Fig. 1b) into the following different type of volume elements, with suitable interfaces:

- shell of transparent material, modeled as a solid;
- inside-air, modeled as a multiphase fluid;
- soil, modeled as a multiphase porous medium.

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