



Short communication

Preparation of Pd/(Ce_{1-x}Y_x)O₂/γ-Al₂O₃/cordierite catalysts and its catalytic combustion activity for methane

Hengcheng Liao*, Miaomiao Liu, Peiyuang Zuo

School of Materials Science and Engineering, Southeast University, Jiangsu Key Laboratory for Advanced Metallic Materials, Nanjing 211189, China



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ABSTRACT

A series of (Ce_{1-x}Y_x)O₂ ($x = 0, 0.15, 0.35, 0.5$) coatings on γ-Al₂O₃ pre-coated cordierite honeycomb were prepared by sol-gel method, and then palladium was loaded by aqueous solution impregnation deposition with Pd(NO₃)₂ as precursor. The structure and morphology of samples were evaluated and the catalytic combustion activity for methane was also discussed. (Ce_{1-x}Y_x)O₂ synthesized by sol-gel has a single-phase cubic fluorite structure. Increasing the Y/Ce ratio can significantly improve the inner surface morphology of the honeycomb channels and also the coating mechanical stability, and leads to a considerable improvement in the catalytic activity of the prepared catalysts for methane.

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1. Introduction

With increasingly stringent requirements for protecting our environment, catalytic combustion of nature gas (methane) has attracted more and more attention [1]. Monolithic catalysts are widely used for catalytic combustion of methane and other organics. As a supporter, cordierite ceramic honeycomb (abbreviated to COR) has very small specific surface area (usually <1 m²/g) [2], thus γ-Al₂O₃ coating is usually used as a transition layer to create a higher surface area [3], however, at high temperature, it is prone to transform into the θ-phase, finally into the α-form, which has a low specific surface area.

In order to prevent the transformation of γ-Al₂O₃ and also to enhance catalytic activities, some rare-earth element oxides (such as CeO₂, La₂O₃, and Y₂O₃) are commonly used as additives [4–6]. CeO₂ has been widely studied in recent years for catalytic application. CeO₂ has many advantages, such as: strong ability to store/release oxygen [7,8], high thermal and structure stabilities [9], and good ability to disperse the noble metal active component [10,11]. Doping divalent or trivalent ions in CeO₂ could improve its oxygen storage capacity [12,13]. Addition of Y to (Ce,Zr)O₂ solid solution could improve oxygen vacancies and promote the reduction of Ce⁴⁺ [14], and also improved the reduction–reoxidation properties of the active PdO species [15].

In this paper, (Ce_{1-x}Y_x)O₂ solid solution coatings were prepared by sol-gel method. The effect of Y/Ce ratio on the phase constitution, surface morphology, and mechanical stabilities was investigated and the catalytic performance of the prepared Pd/(Ce_{1-x}Y_x)O₂/γ-Al₂O₃/COR catalysts for methane was also discussed.

2. Experimental

2.1. Preparation of (Ce_{1-x}Y_x)O₂/γ-Al₂O₃/COR

A commercial honeycomb ceramic was cut into cuboid samples (6 mm × 6 mm × 30 mm) which were pretreated by conventional process. Then they were immersed in the γ-Al₂O₃ transition sol for 5 mins and the excess γ-Al₂O₃ sol inside the honeycomb channels was blown off, and then they were dried at 120 °C for 2 h and roasted at 550 °C for 2 h in a muffle furnace with flowing air. The amount of the loaded γ-Al₂O₃ coating can reach 12 wt.% – 15 wt.% after double repeating. The prepared samples above were labeled as γ-Al₂O₃/COR.

Ce and Y nitrates were used as Ce- and Y- precursors, and the mole ratios of Ce and Y was 1:0, 0.85:0.15, 0.65:0.35, and 0.5:0.5. The mixed aqueous solution of Ce- and Y- nitrates and citric acid was prepared with distilled water. Citric acid was added as a complexing agent in 1:2 M ratio with respect to the sum of the metal salts. The mixed solution were heated at 70 °C in a water bath and constantly stirred until a stable sol was obtained. The γ-Al₂O₃/CORs were impregnated in this sol for 5 min. The excess sol inside the channels need blow off.

* Corresponding author at: School of Materials Science and Engineering, Jiangning Campus of Southeast University, Nanjing 211189, China.
E-mail address: hengchengliao@seu.edu.cn (H. Liao).

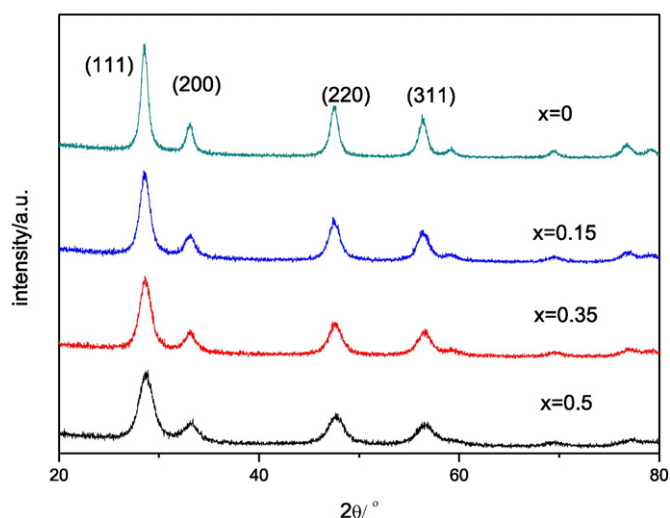


Fig. 1. XRD patterns of $(\text{Ce}_{1-x}\text{Y}_x)\text{O}_2$ ($x = 0, 0.15, 0.35, 0.5$) powders after calcination.

Table 1

Lattice constant and crystallite size of $(\text{Ce}_{1-x}\text{Y}_x)\text{O}_2$.

x	Lattice constant a/nm	Crystallite size D/nm
0	0.5413	11.8
0.15	0.5402	9.5
0.35	0.5395	8.8
0.5	0.5378	8.4

Subsequently, they were dried at 120 °C for 2 h in air and roasted at 550 °C for 2 h. This processed sample is labeled as $(\text{Ce}_{1-x}\text{Y}_x)\text{O}_2/\gamma\text{-Al}_2\text{O}_3/\text{COR}$.

2.2. Preparation of catalysts

Catalysts were prepared by a classical aqueous solution impregnation method, in which $\text{Pd}(\text{NO}_3)_2$ is as precursors. The $(\text{Ce}_{1-x}\text{Y}_x)\text{O}_2/\gamma\text{-Al}_2\text{O}_3/\text{COR}$ s were completely impregnated in the Pd-solution for 30 min, and the excess aqueous solution inside the channels was blown off. Then they were dried at 120 °C for 2 h in air and roasted at 450 °C for 2 h. The final sample is labeled as $\text{Pd}/(\text{Ce}_{1-x}\text{Y}_x)\text{O}_2/\gamma\text{-Al}_2\text{O}_3/\text{COR}$.

2.3. Characterization

The XRD patterns of $(\text{Ce}_{1-x}\text{Y}_x)\text{O}_2$ dried gel powder were collected on a Bruker apparatus (D8-Discover), using $\text{Cu K}\alpha$ radiation ($\lambda = 1.5418 \text{ \AA}$). The X-ray tube was operated at 40 kV and 30 mA and the scanning rate was 0.02°/step in the range of $20^\circ \leq 2\theta \leq 90^\circ$. The specific surface area was measured by N_2 adsorption at 77 K on ASAP 2000 M with the Brunauer–Emmet–Teller (BET) method. The surface morphology of the $(\text{Ce}_{1-x}\text{Y}_x)\text{O}_2$ coating was examined by XL30 environmental SEM.

Ultrasonic oscillating test was performed, to evaluate the cohesive strength of coating on the cordierite substrate, in a KQ-250B ultrasonic bath with a power of 220 W for 30 min. Before test, the dry sample was weighted as m_{before} , and after test, the sample was dried again, and then weighted as m_{after} . The mass losses of the coating was calculated using $\Delta W\% = (m_{\text{before}} - m_{\text{after}}) / m_{\text{before}} \times 100\%$.

Inductively coupled plasma-optical emission spectroscopy (ICP-OES) was performed to measure the loading amount of palladium, cerium and yttrium in the prepared monolithic catalysts.

2.4. Catalytic activity evaluation

The catalytic combustion of methane on the $\text{Pd}/(\text{Ce}_{1-x}\text{Y}_x)\text{O}_2/\gamma\text{-Al}_2\text{O}_3/\text{COR}$ catalysts was carried out in a conventional fixed-bed flow quartz micro-reactor (length = 400 mm, i.d. = 10 mm). A gas mixture

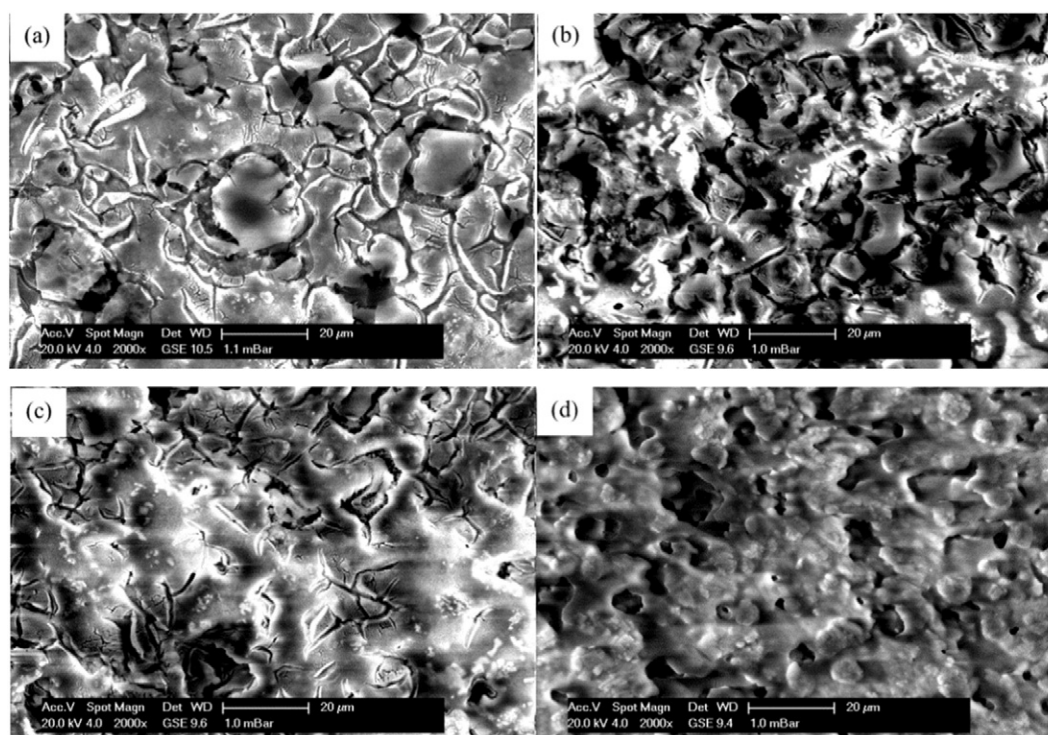


Fig. 2. The inner surface morphology of $(\text{Ce}_{1-x}\text{Y}_x)\text{O}_2/\gamma\text{-Al}_2\text{O}_3/\text{COR}$ s (a) $x = 0$; (b) $x = 0.15$; (c) $x = 0.35$; (d) $x = 0.5$.

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