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Thermophoretically driven capillary transport of nanofluid in a microchannel

Soumya Bandyopadhyay, Suman Chakraborty*

Department of Mechanical Engineering, Indian Institute of Technology, Kharagpur, West Bengal 721302, India

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ABSTRACT

We investigate the interplay of thermophoretic force and interfacial tension on the capillary filling dynamics of a Newtonian nanofluid in a microchannel. In our model, we also consider an intricate thermofluidic coupling by taking the temperature dependence of viscosity aptly into account. This, in turn, determines the evolution of the viscous resistive force as the capillary front progresses, and presents an involved inter-connection between the driving thermophoretic force and the viscous resistive force. The two distinct regimes of particle transport in a fluid medium, delineated by particle size, are expounded to peruse the impact of imposed thermal gradients and particle size on particle retaining propensity of the nanofluid. Additionally, we witness a significant reduction in particle bearing proclivity of the nanofluid with enhancement in a thermal gradient. The results demonstrate the efficacy of the thermophoretic actuation towards the filling of narrow capillaries under the influence of a thermal gradient.

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43 1. Introduction

Capillary-driven systems are ubiquitous in this physical world, 44 with implications in diverse applications ranging from the trans-45 port of blood in the cardio-vascular pathways to the ascent of 46 47 sap in plants occurring through the xylem and phloem tissues. Capillary transport has also been a widely pursued problem in 48 the field of microfluidics [1-7]. Microfluidic transport has wide-49 spread importance, encompassing biomedical engineering [8-11] 50 51 to flow-modulated cooling of electronic components [12,13] and 52 also in chemical engineering [14,15]. Pressure-driven microfluidic transport has several disadvantages which include the paucity of 53 precise experimental control, high pumping power requisites, 54 and ample dispersion. This has led to the emergence of various 55 other modes of transport which include electrosmosis [16-19], 56 57 electrocapillarity [20], and electrokinetics [21]. Various state of the art models is available in this regard with an attempt to 58 59 understand the physics of flow of Newtonian [22–25] as well as 60 Non-Newtonian fluids [16,17]. Because of the immense diversity 61 of the environments where capillary flows prevail, they are sub-62 jected to different physical forcing conditions arising from their 63 surroundings. In this context, the detailed analysis of the physics

of capillary flows attains paramount importance as it not only provides extremely useful theoretical insights to intricacies of the physical phenomenon by eliciting valuable scientific implications but also leads to the development of devices with widespread practical applications.

When there is a temperature gradient in a particle-laden fluid 69 subjected to capillarity, the particles suspended in the fluid experi-70 ence a force on account of thermophoresis, as expounded by Talbot 71 et al. [26]. This thermophoretic force has been a driving factor 72 behind the deposition of particles in a gaseous medium leading to 73 commonly observed phenomena like blackening of a lantern. Based 74 on particle sizes, different particles will experience different forces 75 in presence of thermal gradients in a given flow field. As a conse-76 quence, thermophoresis results in varied migration rates of the par-77 ticles, as delineated by Malvandi and Ganji [27], Guha and Samanta 78 [28]. Hence, such thermal gradients which are prevalent in most of 79 the modern day lab-on-a-chip devices may be pertinently utilized 80 to regulate the resultant capillary dynamics. Additionally, temper-81 ature gradients existing in a system can be employed to separate 82 different particles in a suspension. In the context of such systems, 83 migration of nanoparticles eventually results in their preferential 84 deposition determined by existing thermal fields. The separation 85 of nanoparticles attains utmost importance not only in the context 86 of achieving homogeneous suspensions but also in the design of 87

* Corresponding author. *E-mail address:* suman@mech.iitkgp.ernet.in (S. Chakraborty).

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particle retrieval systems essential for minimizing operationalcosts.

90 Choi and Eastman [29] coined the term "nanofluid" as a dilute 91 mixture of particles, varying in size from 1 nm to 100 nm, 92 suspended in a base fluid. Compared to base fluids, nanofluids 93 inimitably possess superior thermophysical attributes like thermal 94 conductivity [29]. Previously, Malvandi et al. [30] studied 95 thermophoretic effects in nanofluids with a motivation to explore 96 critical heat fluxes in boiling condition. Shiekholeslami et al. [31] 97 delineated magnetohydrodynamic effects on natural convection 98 with Cu-water nanofluid. Additional studies [32-34] have been 99 conducted to expound intricate and interesting physics of nanofluids. Furthermore, researchers have investigated the enhancement 100 of heat transfer in the convective flow of nanofluids in different 101 102 geometries [35–37]. In microscale engineering systems like heat 103 pipes and cooling components of electronic devices, where appre-104 ciable thermal gradients prevail, nanofluids can be utilized for their 105 enhanced thermophysical properties. Consequently, the study of 106 thermophoretic effects on the capillary transport of nanofluids in microfluidic confinements becomes immensely important. 107

108 This paper deals with the effects of thermophoresis on the cap-109 illary filling dynamics of nanofluids. The primary focus is to mathematically investigate the dynamics of capillary flow of nanofluids 110 111 in the presence of thermal gradients, using a reduced order model, 112 addressing the following: (a) effect of particle size, (b) influence of 113 thermal gradient. Furthermore, the work is motivated by the 114 requirement to achieve nanoparticle separations accompanied by 115 a critical exegesis of the influence of pertinent parameters on 116 nanoparticle deposition in microfluidic confinements. To the best of authors' knowledge, no comprehensive study thus far has been 117 118 conducted to explore capillary dynamics in presence of ther-119 mophoretic effects. The present theoretical findings are expected 120 to impel the researchers in performing experiments with nanoflu-121 ids to explicate thermophoretic effects in microscale confinements. 122 In the following section, the mathematical model used to illustrate 123 the above-mentioned physical aspects is discussed in detail, along 124 with the relevant fundamental parameters that implicitly influence 125 the interaction of the various important facets controlling the phy-126 sics of flow.

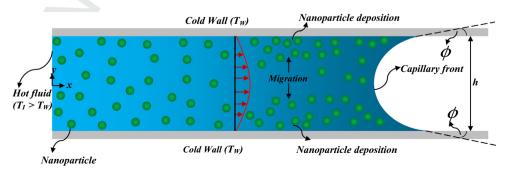
127 2. Mathematical formulation and numerical procedure

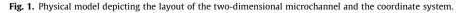
128 2.1. Physical problem

129 We consider parallel plate microchannel geometry, with the 130 two plates being separated by a distance *h* which is equal to 131 500 μ m. The channel is assumed to have a width *b* perpendicular 132 to the plane of the diagram, such that $b \gg h$. The fluid has initially 133 traversed a perfectly insulated section which is long enough for the 134 flow to become hydro-dynamically fully developed. We set our 135 origin at the center of the channel in the beginning of the noninsulated section (see Fig. 1), with y axis running along the trans-136 verse direction and x axis along the length of the channel. The sta-137 tic contact angle at the solid-liquid-gas (air) interface is denoted by 138 ϕ . There will be a transition of the fully developed velocity profile 139 to a meniscus traction regime near the interface via a transition 140 region. However, the length of the meniscus traction regime is very 141 small compared to the length of the fully developed region and 142 hence, is neglected in this model. 143

At the inlet of the non-insulated section, we have a uniform temperature (T_I) , concentration (C_o) and fully developed velocity field. The walls are cooled to a constant temperature (T_w) . The nanofluid under consideration conceived as a suspension of nanoparticles comprises two discrete phases-1) The liquid phase (water) 2) The particle phase (SiO₂). One of the most important considerations of the present model is that there is unidirectional coupling (i.e. the particle motion is determined by the flow field not the other way around) and there will be no mutual interaction between the particles. A similar model has been adopted by Guha and Samanta [28], Chein and Liao [38]. The potency of this assumption is attributed to the fact that we will be dealing with nanofluids of extremely dilute concentrations $(C \sim 10^{-3} \text{ M})$ and nanoparticles of sizes $(d \sim 1 \text{ nm})$, resulting in low volume fraction ($\phi \sim 0.001\%$). In the current study, gravity, inter-particle forces, magnetic and electrostatic forces on the particle are all neglected. The temperature dependence of viscosity is suitably taken into account in the present model through its dependence on the mean temperature at a given cross-section. Consequently, it is a function of the axial coordinate (x) only. Except for viscosity, other thermo-physical properties of the fluids are evaluated at the average of the maximum and minimum temperatures. The temperature dependence of thermophysical properties of the fluid is given by Eqs. (A.1)–(A.4). The thermophysical property of a given nanofluid like thermal conductivity, heat capacity, dynamic viscosity was computed as a function of the particle volume fraction (ϕ) by He et al. [39]. Later, Ganguly et al. [31] incorporated established models to obtain pertinent thermophysical properties of the nanofluids in their study. However, in the limit of low volume fractions, the thermophysical property of a nanofluid becomes equivalent to the corresponding property of the fluid phase. Hence, in the present analysis, the nanofluid properties have been replaced by the analogous properties of the fluid phase.

Here, we apply a reduced order model [40] that is commonly 177 used for evaluating the capillary filling distance as a function of 178 time. This model has its inception from the early works of Lucas 179 [41] and Washburn [42]. By dynamics of the capillary transport fol-180 lowing this model, what we intend to study is the average position 181 (x) of the capillary front at a time t. The equation of motion for the 182 capillary advancement taking the appropriate direction of the 183 forces, following Newton's second law of motion, may be expressed 184 as (neglecting inertial forces consistent with a microfluidic 185 186 paradigm):





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