Contents lists available at ScienceDirect



International Journal of Heat and Mass Transfer

journal homepage: www.elsevier.com/locate/ijhmt

A novel, net-shape polymer electrolyte fuel cell: Higher power density, smaller stack size and less bipolar plate required



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ARTICLE INFO

Article history: Received 29 August 2017 Received in revised form 14 October 2017 Accepted 16 October 2017

Keywords: Polymer electrolyte membrane fuel cell Netlike fuel cell Stack size Bipolar plate cost Performance Three-dimensional non-isothermal simulation

ABSTRACT

Cost, power density and durability are still major challenges to the large-scale commercialization of polymer electrolyte membrane fuel cells (PEMFCs). Most of these issues could be addressed by changing the conventional architecture of PEMFCs. The present work introduces a novel, net-shape flat architecture with unique capabilities. This netlike design increases the active area dramatically by bringing each channel in contact with three different electrodes. These capabilities are further investigated through a wellvalidated three-dimensional non-isothermal model in ANSYS Fluent.

Comparing the polarization curves shows that, per unit active area, the net-style design has a performance significantly better than that of conventional (classical) PEMFCs. In addition, it shows more uniform distribution of oxygen, water, current and temperature. Moreover, it provides remarkably higher current and power densities. Owing to its netlike shape, the proposed multi-channel PEMFC is also considerably smaller and requires less bipolar plates per unit active area. As a result, the state-of-the-art design introduced in this work can enhance the performance of PEMFCs remarkably while reducing their size and the bipolar plate cost. The net-type stack can therefore be considered one of the promising designs for the next generation of PEMFCs.

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1. Introduction

Although polymer electrolyte membrane fuel cells (PEMFCs) have been considered the best replacement to internal combustion engines, the technology is still immature for widespread commercialization. Critical prerequisites for PEMFCs commercialization are improvements in power density, reliability and durability as well as reductions in production costs [1]. Over the past decade, materials characterization [2,3] and interfacial phenomena [4,5] have been the focus of the most of industrial and academic research projects. Less attention has been to date devoted to the *stack architecture* and the component arrangement, which play crucial roles in PEMFC performance, cost and durability [6–8]. The current capability of conventional (classical) PEMFC stacks has to date led to a few major breakthroughs in reducing their cost and size. The breakthrough improvements have to consider well-designed novel

architectures, with precisely-controlled domain sizes and patterns. (*i*) The high cost [9] of the brittle graphite bipolar plates, (*ii*) the temperature and current distribution non-uniformity that intensifies degradation, (*iii*) the maldistribution of reactants inside the cells, and (*iv*) the relatively large and heavy PEMFC stacks have still been considered key priorities to be addressed in fuel cell industry. A number of these issues can be resolved by changing the architecture of PEMFC stacks.

Table 1 summarizes the new designs and architectures ever proposed to improve the conventional PEMFC performance, cost and size. Some of these designs, which comprise non-rectangular channels, have shown the capability of producing higher current density in comparison with the conventional (classical) PEMFCs. Specifically, the tubular multi-channel architectures [4] have recently shown promising potential for the reduction of the stack size and the amount of the bipolar plates required. However, the manufacturing of the graphite plates and membrane electrode assemblies (MEAs) in tubular shapes is indeed hard and highly costly. This point highlights the importance of having novel stacks and bipolar plates in a flat shape.

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Nomenclature

а	water activity	β	a modified heat transfer coefficient accounting for both
Α	area (m ²)		convective heat transfer and the specific surface area of
С	molar concentration (mol m^{-3})		the porous medium
CCM	catalyst-coated membrane	ζ	stoichiometric ratio
Cell	fuel cell	η	overpotential (V)
D	diffusion coefficient $(m^2 s^{-1})$	λ	water content in the membrane
F	Faraday constant (C mol ⁻¹)	μ	viscosity (kg m ^{-1} s ^{-1})
GDL	gas diffusion layer	ρ	density (kg m ^{-3})
Н	channel height (mm)	σ	ionic or electrical conductivity (ohm ⁻¹ m ⁻¹)
Ι	local current density (A m^{-2})	ψ	humidity
i	local current density (A m^{-2})	3	effective porosity
J	exchange current density (A m^{-2})		
K	permeability (m ⁻²)	Subscri	ints and Superscripts
k	thermal conductivity (W m ⁻¹ K ⁻¹)	а	anode
L	channel length (mm)	act	activation
Μ	molecular weight (kg mol ⁻¹)	ave	average
MEA	Membrane Electrode Assembly	6	cathode
n_d	electro-osmotic drag coefficient	ch	channel
P	pressure (Pa or atm)	eff	effective value
PEMFC	Polymer Electrolyte Membrane Fuel Cell	GDL	gas diffusion laver
R	universal gas constant (J mol ⁻¹ K ⁻¹)	i	hydrogen at the anode side and oxygen at the cathode
Т	temperature (K)		side
и	velocity (m s ^{-1})	in	at the channel inlet
t	thickness (µm or m)	i	water
V	cell voltage (V)	k	chemical species
V _{OC}	open-circuit voltage (V)	land	land (rib)
W	channel width (mm)	MEA	membrane electrolyte assembly
Χ	mole fraction	Mem	membrane
Y,y	mass fraction	ref	reference value
		sat	saturated
Greek letters		W	water
Ø	potential (V)		
α	water transfer coefficient		

In the present study, an unprecedented, net-shape flat architecture with specific capabilities is proposed for air-cooled (<5 kW [18]) PEMFCs. As shown in Fig. 1a and b, this unique, netlike design brings each channel in contact with *three* MEAs, which leads to a larger active area per unit volume. It also connects each anode to the cathode of different MEAs and vice versa. These special features offer the possible capability of enhancing the current density while reducing the stack size and the bipolar plates required. This may remarkably enhance all of areal, volumetric and gravimetric power densities. The architecture shown in Fig. 1 is the first version of the net-shape PEMFC and can therefore be further improved for its next-generation designs.

Using a well-validated numerical code in ANSYS Fluent, the present study investigates the possible advantages of the new architecture over the conventional or classical PEMFCs currently available in the market (the base model shown in Fig. 1c). The study further explores the capabilities that the new design could offer in terms of higher current and power densities, uniform current, temperature and reactant distributions inside the cell and any possible reduction in the stack size or in the amount of the bipolar plates required.

2. Design description

In the net-form configuration introduced, each channel is innovatively connected to three MEAs. This is one of the best designs ever introduced, especially in terms of its potential for enhancing the active area and the power density as well as its capacity for

Table 1

New stack designs and architectures capable of improving the PEMFC performance

Authors	Architecture shape	Advantages over the classical PEMFCs
Pourmahmoud and Torkavannejad [10,11]	Elliptical and circular architectures	Slightly better performance
Mohammadi-Ahmar et al. [12]	Cylindrical circle-, triangle- and	An enhanced power density
	square-shape architectures	
Walckzy et al. [13]	Ribbon-shape MEA	More uniform current distribution
Khazaee and Ghazikhani [14]	Multi-connected-duct architectures	Higher current densities
Torkavannejad et al. [4]	Annular circular-duct architectures	Higher current and power densities
Osanloo et al. [15]	Square duct-shaped PEMFCs	Higher current density and more uniform temperature and reactant distributions
Pourmahmoud et al. [16]	Nesting tubular architecture	Higher current density and more uniform temperature and reactant distributions
Liu et al. [17]	Coupled metal hydride containers	Noticeably larger surface-to-volume ratio

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