

# The influence of tube wall on fluid flow, permeability and streaming potential in porous transducer for liquid circular angular accelerometers

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## ABSTRACT

The effects of the tube wall on the fluid flow, permeability and streaming potential are reported for a porous transducer for use in a liquid circular angular accelerometer. Fluid flow and pressure near the surface of the transducer are modeled and validated numerically. We show that the differential pressure across the transducer is not affected by the tube wall. A capillary bundle model is employed to represent the transducer to obtain the radial porosity, permeability and streaming potential distributions due to wall effects. A simulated spherical packing is generated from measured particle parameters to specify the model by calculating the radial porosity distribution. The theoretical permeability and streaming potential coupling coefficient are located within one standard deviation from the mean of measurements. Due to the radial distribution of streaming potential, the electrode can be configured into a large streaming potential region to measure the signal more efficiently. Three electrode configurations are described based on these results, which can be applied to increase the signal of the sensor.

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## 1. Introduction

Angular accelerometers play an important role in angular acceleration measurement, which can be used in navigation, robotics and industrial machines [1–7]. To obtain no-delay and accurate angular acceleration, different angular accelerometers have been designed and investigated [8–18]. Traditional solid-based angular accelerometers yield great precision, but their bandwidth and range are limited [8,9]. Novel micro-electro-mechanical systems (MEMS) technologies bring new possibilities to this field because of the miniaturization of the angular sensor [10]. The reduced inertia of the sensor produces improvements in bandwidth and range but with unsatisfactory accuracy. New categories of angular accelerometer have been investigated recently, employing electromagnetics [11], heat transfer [12], and fluidics [13–18]. Compared to other angular accelerometers, fluidic accelerometers have attracted much attention owing to their good accuracy, bandwidth, range, size, and insensitivity to linear acceleration [13–18].

The design and operating principle of a liquid circular angular accelerometer (LCAA) have been recently reported [15–19].

The LCAA has a structure typical of fluidic angular accelerometers (Fig. 1(a)). A viscous fluid flows in a circular tube made of glass, and a porous transducer sintered by glass microspheres is fixed in the circular tube. In theory, signal generation of an LCAA can be divided into fluidic and electrokinetic processes (Fig. 1(b)) [15]. Owing to the fluid motion, the angular acceleration input,  $\beta$ , is transformed into differential pressure across the transducer,  $\Delta P$ . In the electrokinetic process, owing to the existence of the electrical double layer at the interface between the transducer and the fluid, a differential pressure results in the movement of the electrical charge and the generation of a streaming potential signal,  $E_s$ , [20,21]. Electrodes mounted on the two sides of the transducer measure the streaming potential.

In [15], a transfer function of the fluidic process has been investigated, which performs accurate prediction in low-frequency gain,  $\Delta P/\beta$ , but shows large deviation in bandwidth. The transient fluid in the circular tube was then modeled with the consideration of fluid compressibility [16], which can be used to obtain the frequency response of the fluidic process. This model has been improved, and the influence of structural parameters on the frequency and transient responses of the fluidic process have been reported [17]. The electrokinetic process in the porous transducer is modeled with a streaming potential coupling coefficient (SPCC),  $C_{sp} = E_s/\Delta P$ , and is illustrated by Helmholtz-Smoluchowski (HS) equation in steady flow [20,22–24]. Because the SPCC shows great

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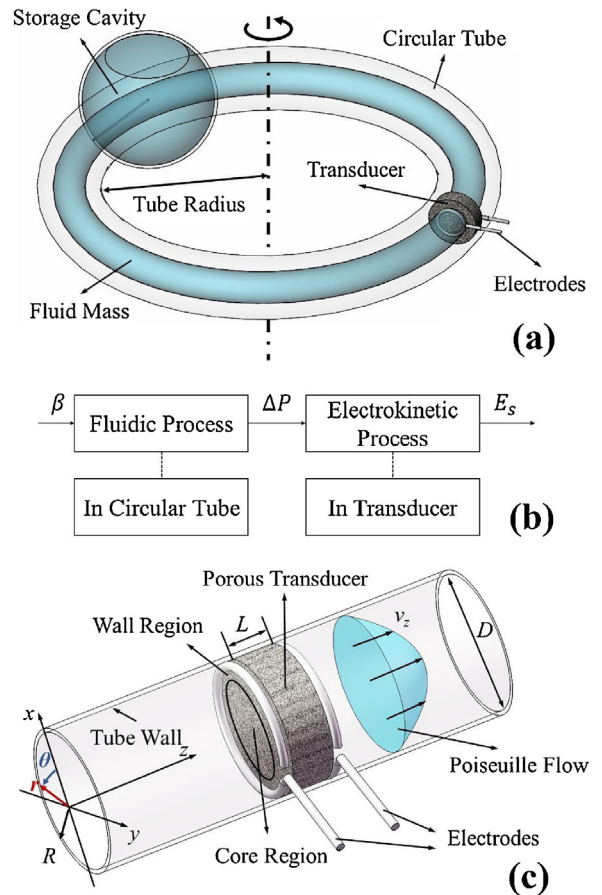
**Nomenclature**

$A$	Cross-section area of the transducer ( $\text{m}^2$ )
$C_f$	Factor of viscous resistance in the transducer (1/s)
$C_j$	Factor inertial resistance in the transducer (1/m)
$C_{sp}$	Streaming potential coupling coefficient (V/Pa)
$C_{sp\_core}$	Streaming potential coupling coefficient in core region (V/Pa)
$d$	Diameter of the microspheres (m)
$\bar{d}_p$	Average diameter of the microspheres (m)
$d_{ij}$	Distance between the centers of the $i$ th and $j$ th spheres (m)
$d_{ik}$	Distance between the $i$ th sphere and the $k$ th wall (m)
$D$	Diameter of the circular tube (m)
$E_s$	Streaming potential (V)
$E(r_c^2, r)$	Second original moment of $rc$ on every $r$ ( $\text{m}^2$ )
$\bar{f}_p$	Permeation resistance ( $\text{m/s}^2$ )
$F$	Formation factor (non-dimensional)
$F_{ij}^c$	Elastic force between the $i$ th and $j$ th spheres (N)
$F_{ik}^b$	Elastic force from the wall (N)
$I_s$	Streaming current (A)
$I_c$	Conduction current (A)
$I_i$	Moment of inertia of the $i$ th sphere ( $\text{kg}\cdot\text{m}^3$ )
$K$	Bulk permeability ( $\text{m}^2$ )
$K_{core}$	Bulk permeability in core region ( $\text{m}^2$ )
$l_{ij}^c$ and $l_{ik}^b$	The distance between $F_{ij}^c$ as well as $F_{ik}^b$ and their contact points on the sphere surface (m)
$L$	Axial length of the transducer (m)
$L_c$	Path length of the capillaries (m)
$m$	Cementation exponent (non-dimensional)
$m_i$	Mass of the $i$ thth sphere (kg)
$n(r_c, r)$	Number density of capillary tubes with radius $r_c$ at $r$ ( $1/\text{m}^2$ )
$N_c$	Number of the capillary tubes on every $r$ ( $1/\text{m}$ )
$p$	Pressure (Pa)
$\Delta P$	Differential pressure across the transducer (Pa)
$Q$	Volumetric flow rate ( $\text{m}^3/\text{s}$ )
$r_c$	Capillary radius (m)
$r_{min}$	Minimal radii of the capillaries (m)
$r_{max}$	Maximal radii of the capillaries (m)
$r_i$	Radii of the $i$ th sphere (m)
$R$	Cross-sectional radius of the circular tube (m)
$R_0$	Coefficients of fitting function, Eq. (29) (non-dimensional)
$Re = \rho v_z D / \eta$	Reynolds number
$r, \theta, z$	Cylindrical coordinates, Fig. 1
$\vec{v} = (v_r, v_\theta, v_z)$	Superficial velocity (m/s)
$V(r)$	Total volume at $r$ in transducer ( $\text{m}^3$ )
$V_f(r)$	Fluid volume at $r$ in transducer ( $\text{m}^3$ )
$\alpha_i$	Acceleration of the $i$ th sphere ( $\text{m/s}^2$ )
$\sim\alpha_1 - \sim\alpha_6$	Coefficients of fitting function, Eq. (29), (non-dimensional)
$\beta$	Angular acceleration input ( $\text{rad/s}^2$ )
$\beta_i$	The angular acceleration of the $i$ th sphere ( $\text{rad/s}^2$ )
$\epsilon_0, \epsilon_r$	Vacuum and relative dielectric constants of liquid (F/m, non-dimensional)
$\zeta$	Zeta potential on liquid-solid interface (V)
$\Theta$	Transform value from $d$ to $r_c$ (non-dimensional)
$\mu_d, \sigma_d$	Mean and variance of particle size distribution (non-dimensional)
$\mu_c, \sigma_c$	Mean and variance of capillary radius distribution (non-dimensional)

$\rho$	Density of liquid ( $\text{kg/m}^3$ )
$\Sigma$	Total conductance of capillary tubes (S)
$\Sigma_s$	Specific surface conductance of capillary tubes (S)
$\sigma_0$	Bulk electrical conductivity of liquid (S/m)
$\eta$	Dynamic viscosity of liquid (Pa·s)
$\tau = L_c/L$	Capillary tortuosity
$\varphi$	Porosity (non-dimensional)
$\varphi_0$	Coefficients of fitting function, Eq. (29), (non-dimensional)
$\bar{\varphi}$	Average porosity

dependence on permeability [21,22,24], the permeability of the transducer in the LCAA has been investigated in [18,19]. However, when a porous medium is fixed in a small diameter tube, as in the LCAA, the inner wall of the tube (tube wall) creates a radial distribution of porosity and permeability [25,26], which can further influence the electrokinetic process which is the focus of our investigation. We consider flow in a neighborhood of the transducer and regard the tube as straight (Fig. 1(c)), because the tube radius (Fig. 1(a)) is much larger than the diameter of transducer,  $D$ , and the asymmetry of the flow caused by the curvature of the tube can be ignored due to the low Reynolds number [27].

Two factors must be investigated to study the influence of the tube wall. First, the flow in the tube can be modeled as Poiseuille flow [28]. The velocity distribution possibly produces a distribution of the differential pressure across the transducer [29], which will affect the streaming potential. Secondly, because the transducer is essentially a granular porous medium fixed in the tube, the



**Fig. 1.** (a) Sensor structure. (b) Signal generation in LCAA. (c) Fluid flow in the tube with cylindrical coordinates.

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