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# Effect of coal ash on the performance of alloys in simulated oxy-fuel environments



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#### HIGHLIGHTS

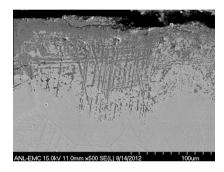
- Long-term performances of alloys in oxy-fuel environment with ash at 750 °C were evaluated.
- Two stages were found for ash corrosion: incubation stage and rapid corrosion stage.
- Mo, W, and Nb in alloys reduce the incubation time.
- Severe carburization was observed after incubation time in oxy-fuel environment with high CO<sub>2</sub> content.
- The corrosion rates in an oxy-fuel environment were higher than or close to the rates in an air combustion environment.

#### ARTICLE INFO

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#### G R A P H I C A L A B S T R A C T



#### ABSTRACT

Oxy-fuel combustion can increase efficiency and reduce pollution from coal power plants. To study material performance in an oxy-fuel environment, both Fe- and Ni-based alloys were exposed to simulated oxy-fuel environments at 750 °C for long terms up to 6300 h. The effects of ash and gas compositions (SO<sub>2</sub>, CO<sub>2</sub>, H<sub>2</sub>O and O<sub>2</sub>) on the performance of alloys were studied. Results from these tests are used to address the role of CO<sub>2</sub>, steam, and ash in the long-term corrosion performance of alloys. Detailed results are presented on weight change, scale thickness, internal penetration, microstructural characteristics of corrosion products, and cracking of scales for the alloys. Oxide scales were studied by synchrotron nanobeam X-ray diffraction.

An incubation period and a propagation period were observed for ash corrosion. Before incubation time, alloys gain weight. After incubation time, localized corrosion damages the protective scales, alloys lose weight and corrosion rates dramatically increase. Since the incubation time can be over 4000 h, long-term test results are more helpful in evaluating the alloy performance in an oxy-fuel combustion environment with ash than the results from a short-term test. The mechanism of ash corrosion is also discussed. © 2013 Elsevier Ltd. All rights reserved.

#### 1. Introduction

Electricity is the world's fastest-growing form of energy consumption. Coal provides the largest share of world electricity generation. Since coal is plentiful, its share of the global energy mix

\* Corresponding author. Tel.: +1 630 252 9842. *E-mail address:* zeng@anl.gov (Z. Zeng). continues to rise, and it could surpass oil as the world's top energy source. However, it is well known that coal combustion to produce a given amount of electricity produces more  $CO_2$  than oil or natural gas. The U.S. Department of Energy's Office of Fossil Energy is intensely promoting research and development of oxy-fuel combustion systems that employ oxygen, instead of air, for burning the fuel. The oxy-fuel combustion systems (without the diluent nitrogen gas) can enable recycling of the carbon dioxide to the



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compressor, the use of novel gas turbines, and advance reuse. The resulting flue gas consists primarily of H<sub>2</sub>O and CO<sub>2</sub>, which facilitates sequestration of CO<sub>2</sub> or its use in a turbine to generate electricity, thereby leading to reduction in CO<sub>2</sub> emissions. Also, because the oxidant is bereft of N<sub>2</sub>, NO<sub>x</sub> emissions are minimized in the exhaust gas. Studies at National Energy Technology Laboratory have indicated that oxy-fuel combustion can increase efficiency in the power plants from the current 30-35% to 50-60%. However, the presence of  $H_2O/CO_2$  and trace constituents such as sulfur and chlorine in the gas environment and coal ash deposits including alkalis at the operating temperatures and pressures can have adverse effects on the corrosion and mechanical properties of structural alloys [1]. The concentration of CO<sub>2</sub>, SO<sub>2</sub>, and H<sub>2</sub>O in oxy-fuel environments are higher than under air combustion conditions, because of the absence of airborne N<sub>2</sub>. Alloy corrosion behaviors of steel materials in H<sub>2</sub>O and CO<sub>2</sub> environments have been studied [2–7]. Increasing steam content can lead to breakaway oxidation [3]. Carburization was observed when alloys were exposed to CO<sub>2</sub> at elevated temperature [4]. High CO<sub>2</sub> and H<sub>2</sub>O concentrations also assist in partially oxidizing SO<sub>2</sub> to SO<sub>3</sub> [8]. The concentration of SO<sub>3</sub> in oxy-fuel environment is typically three or more times higher than under air combustion condition. SO<sub>3</sub> and steam can react to form sulfuric acid through the following reaction:

$$SO_3 + H_2O = H_2SO_4$$
 (1)

Higher  $SO_3$  and  $H_2O$  concentrations lead to higher concentration of corrosive  $H_2SO_4$  under oxy-fuel conditions. Thus there is a critical need to evaluate the response of structural and turbine materials in simulated oxy-fuel environments in an effort to select materials that have adequate high-temperature mechanical properties and long-term environmental performance.

Sulfur can be transported through oxide scale and increase the oxidation rates of alloys. Radiometric analysis indicated that the inward transport of sulfur is primarily due to the SO<sub>2</sub>/S<sub>2</sub> molecular transport. Sulfides were observed in the inner scale layer [9]. However, the effect of sulfur on corrosion in oxy-fuel system has scarcely been studied [10]. Coal ash can also lead to severe corrosion at high temperature [11–20]. The corrosion of alloys in the oxy-fuel and ash environments has also been scarcely reported [21,22]. Since coal power plants should be operated for long time, it is important to study the long-term performance of alloys. However, recent studies usually show only short-term test results. If the oxidation follows the parabolic law, short-term test results can provide useful information. However, if the oxide scale breaks down after the incubation period, the corrosion rate can dramatically increase. Short-term test results below the incubation time will not be enough to evaluate the alloy performance for coal power plants.

Table 1	l
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Nominal composition	(in wt%	) of alloys	selected f	or corrosion study.	

Therefore, this paper provides a study of long-term performance of alloy materials in oxy-fuel environments.

### 2. Experimental

#### 2.1. Materials

The compositions of the alloys selected for the study are listed in Table 1. Several alloys, both ASME-coded and uncoded, were selected for corrosion evaluation. Fe-based alloys and Ni-based alloys (333, 617, 625, 602CA, 230, 693, 740, and 718) were included in the study, especially for application at temperatures above 700 °C. MA956 is a Fe–Cr alloy produced via mechanical alloying and subsequent extrusion. Apart from fireside and steam-side corrosion resistance, the alloy selected for application in steam superheaters and reheaters should possess adequate strength at elevated temperatures for the duration of service.

#### 2.2. Gas compositions

To understand the effect of gas composition on alloy corrosion, the alloys were exposed to seven different gas compositions (see Table 2). Gas 1 and 2 were used to model the effect of gas composition on the corrosion of alloys in gas environments without ash. Gases 3 to 7 were used to study the corrosion of alloys in these gas environments in the presence of ash. Gas 3 simulates the gas environment under oxy-fuel combustion conditions when Gatling coal is used with  $\sim$ 4% oxygen excess. Gas 5 is used to compare the effect of the partial pressure of oxygen on alloy corrosion. The partial pressure of oxygen in Gas 5 is 6 times higher than it is in Gas 3. The partial pressures of steam and SO<sub>2</sub> remain similar between Gas 3 and Gas 7. Gases 4 and 6 do not contain steam, but the partial pressures of  $O_2$  and  $SO_2$  in Gas 4 are the same as in Gas 3. Gas 7 does not contain CO<sub>2</sub> and steam. The effect of steam and CO<sub>2</sub> on the corrosion of the alloys is studied by comparing their performance in the gas environments both with and without steam.

#### 2.3. Experiments

Oxidation experiments without ash were conducted in an experimental system that consists of a horizontal, tubular, high-temperature furnace capable of operation up to 1000 °C. The reac-tion chamber consisted of a quartz chamber (104-cm length, 5-cm OD, 0.32-cm thick), which was centered in a 30-cm-diameter resistive heating furnace. Type 316 stainless steel (SS) flange caps with an O-ring seal were used to close the ends of the quartz tube. The flange caps provided port fittings for the gas flow, steam/vapor

Material	С	Cr	Ni	Mn	Si	Mo	Fe	Other
153MA	0.05	18.4	9.5	0.6	1.4	0.2	Bal	N 0.05, Nb 0.07, V 0.2
304	0.08	18.0	8.0	1.6	0.6	-	Bal	
253MA	0.09	20.9	10.9	0.6	1.6	0.3	Bal	N 0.19, Ce 0.04
800H	0.08	20.1	31.7	1.0	0.2	0.3	Bal	Al 0.4, Ti 0.3
333	0.05	25.0	45.0	-	1.0	3.0	18.0	Co 3.0, W 3.0
617	0.08	21.6	53.6	0.1	0.1	9.5	0.9	Co 12.5, Al 1.2, Ti 0.3
625	0.05	21.5	Bal	0.3	0.3	9.0	2.5	Nb 3.7, Al 0.2, Ti 0.2
602CA	0.19	25.1	62.6	0.1	0.1	-	9.3	Al 2.3, Ti 0.13, Zr 0.19, Y 0.09
230	0.11	21.7	60.4	0.5	0.4	1.4	1.2	W 14, Al 0.3, La 0.015
693	0.02	28.8	Bal	0.2	0.04	0.13	5.8	Al 3.3, Nb 0.67, Ti 0.4, Zr 0.03
740	0.07	25.0	Bal	0.3	0.5	0.5	1.0	Co 20.0, Ti 2.0, Al 0.8, Nb + Ta 2.0
718	-	19.0	52.0	-	-	3.0	19.0	Nb 5.0, Al 0.5, Ti 0.9, B 0.002
MA956	-	20.0	-	-	-	-	Bal	Al 4.5, Ti 0.5, Y2O3 0.6
WASP	0.02	20	Bal	0.5	0.75	4.3	2.0	Co 12-15, Ti 2.6-3.25, Al 1.0-1.5, Zr 0.
ANL5	0.2	25	71.1	-	_	-	-	Al 3.3, Ti 0.3, Zr 0.2, Y 0.1

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