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Overexpression of secreted sucrose isomerase in *Yarrowia lipolytica* and its application in isomaltulose production after immobilization



Peng Zhang ^a, Zhi-Peng Wang ^{b,*}, Song Liu ^c, Yi-Lin Wang ^d, Zhong-Feng Zhang ^a, Xin-Min Liu ^a, Yong-Mei Du ^a, Xiao-Long Yuan ^a

^a Tobacco Research Institute, Chinese Academy of Agricultural Sciences, Qingdao, Shandong 266101, China

^b Key Laboratory of Sustainable Development of Polar Fishery, Ministry of Agriculture and Rural Affairs, Yellow Sea Fisheries Research Institute, Chinese Academy of Fishery Sciences, Qingdao, Shandong 266071, China

^c Coordination Office in Qingdao Huanghai, Qingdao, Shandong 266000, China

^d College of Science, China University of Petroleum, Qingdao, Shandong 266580, China

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ABSTRACT

Isomaltulose production by bacterial fermentation was limited, due to generation of undesirable products and reduced yields. Isomaltulose production using sucrose isomerase (Slase) catalyzed methods was expected to be more applicable, but was hampered by low Slase activity and lack of a secreted Slase producer. Here, we aimed to obtain high levels of secreted Slase by overexpressing the Slase gene from *Pantoea dispersa* UQ68J in *Yarrowia lipolytica*, a successful host for efficient secretory expression, with a newly characterized strong constitutive promoter. After optimization of the culture medium, the engineered strain JD secreted Slase with an activity of 49.3 U/mL. The recombinant Slase was effectively immobilized onto polyvinyl alcohol-alginate, and the enzymatic activity recovery rate was up to 82.4%. The stability of the Slase was significantly improved by immobilization. Batch production of isomaltulose catalyzed by the immobilized Slase was performed under optimal conditions, generating 620.7 g/L isomaltulose with a yield of 0.96 g/g. The conversion rate of sucrose after 13 batches remained above 90%. These results demonstrated that the proposed Slase expression and immobilization method was promising in the industrial production of isomaltulose.

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1. Introduction

Sucrose (α D glucopyranosyl 1,2 D fructofuranose) is a commonly used sweetener. Upon ingestion, sucrose is degraded into glucose and fructose, thus elevating blood glucose levels [1]. Excessive sucrose intake can easily cause obesity and is associated with health problems, such as heart disease and type 2 diabetes [1]. Increases in the standard of living and health consciousness have led to a focus on healthier functional sweeteners that can replace sucrose [2,3]. Isomaltulose is an ideal functional sweetener that has been approved as a safe substitute for sucrose by the United States Food and Drug Administration [4]. This compound also possesses health advantages, including prolonged energy release, slower digestion, higher stability, lower carcinogenicity, and reduced insulin levels [5].

In industry, isomaltulose is mainly produced from sucrose by bacterial fermentation. Those isomaltulose producing strains can synthesize sucrose isomerase (Slase), which is responsible for isomerizing sucrose into isomaltulose and other by-products, such as trehalulose, fructose,

* Corresponding author. E-mail address: wangzp@yasfri.ac.cn (Z.-P. Wang). and glucose [6–11]. But the concentration of sucrose substrate was limited and the isomaltulose yield was reduced during the fermentation, as sucrose serves as both substrate of the Slase and carbon source for cell growth [11–13]. Even using free cells or immobilized cells to produce isomaltulose can't avoid the extra sucrose consumption via cell utilization [6–12]. Additionally, those isomaltulose producing strains lack a food-grade genetic background. The existence of various uncertified extracellular products complicated isomaltulose recovery process [11].

Implementing the isomerization reaction using pure Slase was expected to be more applicable for isomaltulose production, for the increased substrate concentration and separated products from strains [11]. Immobilization of Slase has been tried to achieve repeated use of enzymes and improved stability, reducing enzyme demand [14,15]. Generally, wild strains secrete Slases with low activity, not meeting the demand of isomaltulose production [7,9–11]. High Slase activity was obtained by expressing Slase genes in *Escherichia coli*; but the intracellular localization of Slases and endotoxin generation necessitate expensive and difficult downstream isolation processes [11,16,17]. Secretory expression of the Slase gene has been tried in *Lactococcus lactis*. However, the activity was below 3.0 U/mL, far from meeting industry requirements [13]. Accordingly, lack of a suitable secreted Slase

producer should be a significant obstacle to isomaltulose production using enzymatic methods. Thus, a more suitable host should be identified for secretory expression of Slase.

The yeast *Yarrowia lipolytica* is classified as a "generally recognized as safe" microbe and has been shown to be a successful host for efficient secretory expression of many bacterial and fungal genes [18]. TEF promoter with intron (TEFin) is a newly characterized strong constitutive promoter in *Y. lipolytica*, inducing a 5-fold increase in expression over the traditional promoter [19]. In this study, we aimed to obtain high levels of secreted Slase and achieve isomaltulose production by enzymatic methods. To this end, the Slase gene from *P. dispersa* UQ68J with highest product specificity, was ligated into the expression vector pM06 carrying TEFin promoter, and transformed into *Y. lipolytica* host. Then the secreted Slase was immobilized onto polyvinyl alcohol (PVA), a support of low cost and nontoxicity [20], to implement isomaltulose production using enzymatic methods.

2. Materials and methods

2.1. Strains, plasmids, and media

The uracil mutant *Y. lipolytica* XY strain was kindly provided by Dr. Xiao-Yan Liu (Huaiyin Normal University). The expression vector pM06 was kindly provided by Ji-Ming Wang (Qingdao Institute of Bioenergy and Bioprocess Technology); the plasmid and accessory DNA elements were shown in Fig. S1. *E. coli* DH5 α (TaKaRa Biotechnology, China) was used for plasmid amplification. *E. coli* was cultured at 37 °C in LB medium supplemented with 30.0 µg/mL kanamycin or 100.0 µg/mL ampicillin. Yeast strains were cultivated in YPD medium (20.0 g/L glucose, 20.0 g/L peptone, 10.0 g/L yeast extract) [18]. *Y. lipolytica* JD transformants were screened on YNB plates (1.7 g/L yeast nitrogen base without amino acids, 10.0 g/L glucose, 5.0 g/L (NH4)₂SO₄, 25.0 g/L agar) [18].

2.2. DNA manipulation

Restriction endonuclease digestion and DNA ligation were performed according to Thermo Scientific protocols. DNA polymerase was used as recommended by the manufacturer (New England BioLabs, USA). Digested DNA fragments were recovered and purified using a TaKaRa MiniBEST Agarose Gel DNA Extraction Kit Ver.4.0. *E. coli* was transformed was performed as previously described [21]. *E. coli* transformants were screened on LB agar containing 30.0 µg/mL kanamycin or 100.0 µg/mL ampicillin. Genomic DNA from corresponding *Y. lipolytica* transformants was extracted using a TIANamp Yeast DNA Kit (TIANGEN BIOTECH, China).

2.3. Slase expression in Y. lipolytica

The Slase gene from *P. dispersa* UQ68J (accession no.: AY223549) was used for recombinant Slase expression. After codon redesign and optimization, the coding sequence of the Slase gene with or without a 6× His tag was synthesized (Synbio Technologies, China), named PDSIH and PDSI, respectively. The synthesized PDSIH and PDSI DNA fragment with Sfil and BamHI restriction sites was ligated into pMD19-T, forming pMD19-T-PDSIH, pMD19-T-PDSI (Synbio Technologies). The plasmids pMD19-T-PDSIH, pMD19-T-PDSI, and pM06 were digested by Sfil and BamHI. After purification, the fragment containing PDSIH or PDSI, and linearized pM06 were ligated to construct the final recombinant expression plasmid pM06-PDSIH and pM06-PDSI. The two expression plasmids were linearized following NotI digestion. The purified fragments carrying Slase gene were separately transformed into Y. lipolytica URA⁻ cells using the LiAc method [22]. The linearized fragment of pM06 not carrying any genes was transformed into the host as a control. Positive transformants were grown on YNB agar at 30 °C. To confirm integration of the Slase coding gene, genomic DNA from the transformants and control strain was extracted and verified by polymerase chain reaction (PCR) using the following primers: SIR (5'-AACCATTGTCGGTGTTAGGAGAC-3') and URAF (5'-AAGAAACCGTGCTT AAGAGC-3').

2.4. Purification of the recombinant Slases

Based on PCR detection, a transformant named strain JD carrying *PDSIH* gene was picked, the gene coding Slase with a $6 \times$ His tag. And a transformant named strain JW carrying *PDSI* gene was also picked, the gene coding Slase without a $6 \times$ His tag. Strain JD and strain JW were separately cultivated in YPD liquid seed medium for 20 h and then switched to 100 mL YPD liquid fermentation medium for 60 h. Cultures were centrifuged at 5000 ×g, and supernatants were collected for analysis of Slase activity. The fermentation broth of strain JD and strain JW were concentrated 10 times using a 10-kDa ultrafiltration membrane. These concentrated supernatants containing the Slase enzyme were dialyzed overnight.

The concentrated supernatant of strain IW containing the Slase enzyme PDSI was adjusted to pH 6.0 in phosphate buffer (50 mM), and then applied to a DEAE Sepharose™ Fast Flow column (GE Healthcare, USA). The Slase enzyme PDSIH was attached to the gel and then eluted with a linear gradient NaCl solution (0–1 M) at a flow rate of 1 mL/min. The concentrated supernatant of strain JD containing the Slase enzyme with $6 \times$ His tag was adjusted to pH 5.0 using in phosphate buffer (50 mM), then applied to a Ni-chelating affinity gel column (GE Healthcare, USA). The Slase enzyme PDSIH was attached to the gel and were eluted stepwise, each time with 20 mL of elution buffer (20 mM Tris, pH 8.0, 500 mM NaCl, imidazole), with imidazole concentrations ranging from 10 to 500 mM. The Slase enzyme solutions were dialyzed and stored at -80 °C. The protein concentration was determined by the Bradford method with bovine serum albumin (BSA) as standard. The purity and molecular mass of the enzymes were verified by SDS-PAGE.

2.5. Enzymatic activity assay and sugar concentration determination

Slase activity was detected as described previously [16]. Briefly, 100 g/L sucrose was prepared in phosphate buffer (50 mM, pH 6.0). Then, 100 µL Slase solution or immobilized Slase was added, and the total volume was adjusted to 1.0 mL after incubation at 30 °C for 10 min. The final reaction solutions were filtered through a 0.22-um membrane and diluted for high performance liquid chromatography (HPLC) analysis. The samples were injected onto an amino column (Thermo Scientific, USA) fitted on an Agilent 1200 system (Agilent Technologies, USA). Sugar concentrations were determined using a refractive index detector. The mobile phase was acetonitrile: water (88:12) with the flow rate of 1.5 mL/min at 30 °C. The amounts of isomaltulose, trehalulose, glucose, fructose, and sucrose were calculated according to peak areas and retention time. One unit of Slase activity was defined as the amount of enzyme releasing 1 µmol isomaltulose or trehalulose in 1 min under the catalyzing conditions mentioned above.

2.6. Optimization of culture medium for Slase production in flasks

Initial Slase producing YPD medium contained 20.0 g/L glucose, 20.0 g/L peptone, and 10.0 g/L yeast extract (pH 6.0). All batch fermentations in flasks were conducted for 72 h at 30 °C and 180 rpm. Different nitrogen sources and nitrogen source concentrations were evaluated. Remaining glucose was detected by HPLC as described above; cell dry weight was evaluated as described previously [23].

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