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[Mathematics](dx.doi.org/10.1016/j.matcom.2013.04.021) and Computers in Simulation 99 (2014) 28–36

www.elsevier.com/locate/matcom

## Gas phase appearance and disappearance as a problem with complementarity constraints $\vec{x}$

Original article

Ibtihel Ben Gharbia <sup>a</sup>*,*b*,*∗, Jérôme Jaffré <sup>b</sup>

<sup>a</sup> *Eddimo, Ceremade, University of Paris-Dauphine, 75775 Paris, France* <sup>b</sup> *INRIA-Paris-Rocquencourt, team-project Pomdapi, BP 105, F-78153 Le Chesnay, France* Received 14 November 2011; received in revised form 26 September 2012; accepted 3 April 2013 Available online 6 August 2013

#### **Abstract**

The modeling of migration of hydrogen produced by the corrosion of the nuclear waste packages in an underground storage including the dissolution of hydrogen involves a set of nonlinear partial differential equations with nonlinear complementarity constraints. This article shows how to apply a modern and efficient solution strategy, the Newton-min method, to this geoscience problem and investigates its applicability and efficiency. In particular, numerical experiments show that the Newton-min method is quadratically convergent for this problem.

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*Keywords:* Porous media; Two-phase flow; Nuclear waste underground storage; Nonlinear complementarity problem; Newton-min

### **1. Introduction**

The Couplex-Gas benchmark [\[22\]](#page--1-0) was proposed by Andra (French National Inventory of Radioactive Materials and Waste) [\[3\]](#page--1-0) and the research group MoMaS (Mathematical Modeling and Numerical Simulation for Nuclear Waste Management Problems) [\[21\]](#page--1-0) in order to improve the simulation of the migration of hydrogen produced by the corrosion of nuclear waste packages in an underground storage. This is a system of two-phase (liquid–gas) flow with two components (hydrogen–water). The benchmark generated some interest and engineers encountered difficulties in handling the appearance and disappearance of the phases. The resulting formulation [\[15\]](#page--1-0) is a set of partial differential equations with nonlinear complementarity constraints. Even though they appear in several problems of flow and transport in porous media like the black oil model presented in [\[8\]](#page--1-0) or transport problems with dissolution–precipitation [\[7,17,19\],](#page--1-0) complementarity problems are not usually identified as such in hydrogeology and, to circumvent the solution of complementarity conditions, problems are often solved by reformulating the problem as in  $[1,2,6]$ . However the solution of complementarity problems is an active field in optimization [\[5,10,13\]](#page--1-0) and we draw from the know-how of this scientific community. A similar path is followed bin papers like [\[12,18,20\].](#page--1-0) The application of a semi-smooth Newton method [\[14,16\],](#page--1-0) sometimes called the Newton-min algorithm, to solve nonlinear complementarity problem is

<sup>-</sup>This work was partially supported by the GNR MoMaS (PACEN/CNRS, ANDRA, BRGM, CEA, EDF, IRSN).

<sup>∗</sup> Corresponding author at: INRIA-Paris-Rocquencourt, team-project Pomdapi, BP 105, F-78153 Le Chesnay, France. Tel.: +33 617635032. *E-mail addresses:* [ibtihel.ben-gharbia@inria.fr](mailto:ibtihel.ben-gharbia@inria.fr) (I. Ben Gharbia), [Jerome.Jaffre@inria.fr](mailto:Jerome.Jaffre@inria.fr) (J. Jaffré).

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described. We will demonstrate through a test case, the ability of our model and our solver to efficiently cope with appearance or/and disappearance of one phase.

In Section 2, we introduce the formulation of the problem and in Section [3](#page--1-0) we describe the numerical method. In Section [4,](#page--1-0) we present and discuss a numerical experiment.

### **2. Problem formulation**

This section gives a precise formulation of the mathematical model for the application that was outlined in the introduction. We consider a problem where the gas phase can disappear while the liquid phase is always present.

#### *2.1. Fluid phases*

Let  $\ell$  and  $g$  be the respective indices for the liquid phase and the gas phase. Darcy's law reads

$$
\mathbf{q}_i = -K(x)k_i(s_i)(\nabla p_i - \rho_i g \nabla z), \quad i = \ell, g,
$$
\n(1)

where *K* is the absolute permeability. For each phase  $i = \ell$ , *g*, *s<sub>i</sub>* is the saturation and  $k_i = k_{ri}(s_i)/\mu_i$  is the mobility with  $k_{ri}$  the relative permeability and  $\mu_i$  the viscosity (assumed to be constant). The mobility  $k_i$  is an increasing function of  $s_i$  such that  $k_i(0) = 0$ ,  $i = \ell$ , g. Assuming that the phases occupy the whole pore space, the phase saturations satisfy

 $0 \le s_i \le 1, \quad s_\ell + s_g = 1.$ 

The phase pressures are related through the capillary pressure law

$$
p_c(s_\ell) = p_g - p_\ell \geq 0,
$$

assuming that the gas phase is the non-wetting phase. The capillary pressure is a decreasing function of the saturation *s-*.

In the following, we will choose  $s_{\ell}$  and  $p_{\ell}$  as the main variables since we assume that the liquid phase cannot disappear for the problem under consideration.

#### *2.2. Fluid components*

We consider two components, water and hydrogen, identified by the indices  $j = w, h$ . The mass density of the phase is

$$
\rho_i = \rho_w^i + \rho_h^i, \quad i = \ell, g.
$$

From *M<sup>w</sup>* and *Mh*, the water and hydrogen molar masses, we define the molar concentration of phase *i*:

$$
c_i = c_w^i + c_h^i, \quad c_j^i = \frac{s_i \rho_j^i}{M^j}, \quad j = w, h, \quad i = \ell, g.
$$
 (2)

The molar fractions are

$$
\chi_h^i = \frac{c_h^i}{c_i}, \quad \chi_w^i = \frac{c_w^i}{c_i}, \quad i = \ell, g. \tag{3}
$$

Obviously,

$$
\chi_w^i + \chi_h^i = 1, \quad i = \ell, g. \tag{4}
$$

We assume that the liquid phase may contain both components, while the gas phase contains only hydrogen, that is the water does not vaporize. In this situation we have

$$
\rho_w^g = 0
$$
,  $\rho_g = \rho_h^g$ ,  $\chi_h^g = \frac{c_h^g}{c_g} = 1$ ,  $\chi_w^g = 0$ .

*g*

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