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# Studies on the faradaic efficiency for electrochemical reduction of carbon dioxide to formate on tin electrode

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### HIGHLIGHTS

• pH value in CO<sub>2</sub>-saturated KHCO<sub>3</sub> solution has an effect on CO<sub>2</sub> reduction.

• Oxidation of formate is main reason for efficiency decreasing with time lasted.

• Formate oxidization accelerates as formate concentration in electrolyte increases.

• Faradaic efficiency is >91% when formate concentration is <0.01 mol  $L^{-1}$ .

## A R T I C L E I N F O

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#### 1. Introduction

The transformation of  $CO_2$  into value-added chemicals and fuels has attracted much attention in recent years. Up to now, many chemical, photochemical, electrochemical and photoelectrochemical methods have been investigated for the purpose [1–5]. Among these routes, electrochemical reduction of  $CO_2$  is a promising process because the product can be selectively controlled by changing the electrolysis condition, such as electrode [6–10] and electrolyte [11,12]. To date, formic acid [13], carbon monoxide [14], methanol [15], and oxalic acid [16] have been prepared by this way. Electrochemical reduction of  $CO_2$  also supplies a route that makes full use of the renewable photovoltaic, wind and marine energies that depend seriously on weather [17,18].

The electrode materials include various pure metals, coordination compounds or alloys, which play very important roles in

### ABSTRACT

The electrochemical reduction of carbon dioxide ( $CO_2$ ) on Sn electrode has been investigated in aqueous KHCO<sub>3</sub> solution by cyclic voltammetry and controlled potential electrolysis. The results show that the faradaic efficiency for producing formate is affected by the electrolysis potential, the concentration and pH value of KHCO<sub>3</sub> solution; the reason for the decrease of faradaic efficiency as the electrolysis time lasts is the oxidation of formate on the Pt anode. When the concentration of the formate in the electrolyte is less than 0.01 mol L<sup>-1</sup>, the faradaic efficiency can reach above 91%.

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determination of the products [19–26]. For example, Sn, Pb, Hg and In electrodes tend to produce formate in aqueous solution with high faradaic efficiency [27,28]. It is very interesting that faradaic efficiency for formic acid production in electrochemical reduction of  $CO_2$  in aqueous KHCO<sub>3</sub> solution in a fixed-bed reactor was 90% at 30 min, but it decreased to 30% after 2 h. The reason for this decrease was suggested to be the oxidation of formic acid [29]. However, another report revealed that the decrease should be resulted from the deposition of Zn on the surface of Sn electrode during electrolysis [30]. These two reports have provided different explanations for the decrease of faradaic efficiency.

Agarwal et al. discussed the engineering and economic feasibility of large-scale electrochemical reduction of  $CO_2$  to formate, and suggested that this process can be operationally profitable [31]. Therefore, it is important to find out what exactly determines the faradaic efficiency of the electrochemical reduction of  $CO_2$ .

In this paper, Sn was chosen from the metals with high faradaic efficiency for producing formate because of its low cost and relatively low toxicity. The influences of key variables like the electrolysis







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potential, the concentration and pH value of the KHCO<sub>3</sub> solution on the faradaic efficiency for producing formate were studied to obtain the optimal electrolysis condition. The most importantly, it is to find out the reason why the faradaic efficiency decreases.

## 2. Experimental

All the materials were purchased ( $\geq$ 99.5%) from commercial companies, and used without further treatments.

Scanning electron microscope (SEM) images were taken with a Hitachi S-4800 microscope at an acceleration voltage of 15 kV. The pH values of all the electrolytes were determined by a pen-like pH meter (CT-6022, Shanghai Rentong Meter Co., Ltd., China).

The products in the electrolyte were directly analyzed by ion chromatography (ICS-900 Dionex). The column was an IonPac AS11-HC anionic column using 0.02 mol  $L^{-1}$  KOH as the mobile phase at the rate of 1 mL min<sup>-1</sup>. 10 µL of the electrolyte were used for each time. The amount of formate in the electrolyte was also determined by titration (see Supporting information for details).

The cell used here is an airtight and undivided glass cell equipped with a gas inlet and outlet which is able to pass the either N<sub>2</sub> (99.99%) or CO<sub>2</sub> (99.99%) through the solution. A conventional three-electrode system was used during the measurements. The working electrode was always a Sn plate with a geometric surface area of 1 cm<sup>2</sup>. To obtain repeatable results, each Sn plate electrode is used only once. A Pt plate ( $1 \times 1$  cm<sup>2</sup>) and an Ag/AgCl electrode (sat. KCl) were used as counter and reference electrodes, respectively. The electrolyte used was 40 mL of KHCO<sub>3</sub> aqueous solution. All experiments were performed under room temperature and ambient pressure.

Cyclic voltammetry (CV) experiments were carried out using a CS350 electrochemical workstation (Wuhan CorrTest Instrument Co., Ltd., China) after purging the solution with either  $N_2$  or  $CO_2$  for 30 min for the actual determinations. The current density (*j*) is determined on the geometrical area of the electrode.

Controlled potential electrolysis was carried out using a LAND CT2001C cell performance-testing instrument (Wuhan Electronics Co., Ltd., China) in the same three-electrode electrochemical cell. The electrolyte was saturated with  $CO_2$  before each electrolysis process, and  $CO_2$  gas was continuously aerated at a flow rate of 10 mL min<sup>-1</sup> during the electrolysis process. The electrolysis experiments were terminated when the total charge passed reached a certain value. The average current density ( $j_a$ ) is expressed as the total current divided by the geometric surface area of the Sn electrode (1 cm<sup>2</sup>) for all cells.

The faradaic efficiency for the formation of formate (*f*) is determined by Equation (1):

$$f = n_{\rm formate} n F/Q \tag{1}$$

where  $n_{\text{formate}}$  is the moles of the formate produced; *n* represents the number of electrons required for the formation of one molecule of formate from CO<sub>2</sub> (*n* = 2 here); F is Faraday's constant (96485 C mol<sup>-1</sup> of electrons); and Q is the total charge in Coulomb passed across the electrode during the electrolysis.

#### 3. Results and discussion

#### 3.1. CV measurements

Fig. 1 depicts the voltammograms of the Sn electrode in 0.1 mol  $L^{-1}$  KHCO<sub>3</sub> solution after being bubbled with N<sub>2</sub> or CO<sub>2</sub> for 30 min. The anodic peaks between -0.3 and -0.6 V and the cathodic peak between -0.8 and -1.1 V in CV curves can be attributed to the formation and the reduction of tin oxides in basic



**Fig. 1.** Cyclic voltammograms on the Sn electrode in 0.1 mol  $L^{-1}$  KHCO<sub>3</sub> solution after being bubbled with N<sub>2</sub> (a) and CO<sub>2</sub> (b) for 30 min. The inset is the same cyclic voltammograms based on the RHE reference scale. The scan rate was 0.05 V s<sup>-1</sup>.

media respectively [32]. On the cathodic end of the voltammograms, sharp increases of the current densities can be observed under both  $N_2$  and  $CO_2$  (curves a and b in Fig. 1), which should be most probably caused by the reduction of water (under  $N_2$ ) and  $CO_2$ (under  $CO_2$ ).

Theoretically, it can be predicted that the pH value of the  $KHCO_3$  solution will be lowered if the solution is saturated with  $CO_2$  because of the reaction (2):

$$CO_2 + H_2O \rightleftharpoons HCO_3^- + H^+$$
(2)

Experiments did show that the pH value of the KHCO<sub>3</sub> solution increases continuously if it is bubbled with N<sub>2</sub> because of the dissipation of CO<sub>2</sub>, but it decreases if it is saturated with CO<sub>2</sub> (see Tables S1 and S2 in Supporting information for details). If the KHCO<sub>3</sub> solution has been bubbled with N<sub>2</sub> and CO<sub>2</sub> for 30 min, the pH values are 8.69 and 6.98 respectively.

As the pH value seriously affects the electrode potentials for the reduction of  $H_2O$  and  $CO_2$ :

$$2H^+ + 2e \rightleftharpoons H_2 \tag{3}$$

$$\mathrm{CO}_2 + \mathrm{H}^+ + 2\mathrm{e} \rightleftharpoons \mathrm{HCOO}^- \tag{4}$$

the CV curves should be adjusted to exclude the effect of pH. By converting the reference scale from Ag/AgCl to RHE using E (vs. RHE) = E (vs. Ag/AgCl) + 0.1988 V + 0.0591 V × pH, the cyclic voltammograms is re-plotted in the inset of Fig. 1. It can be seen that peaks related to the formation and the reduction of tin oxides almost overlapped [32]; and in the left end, the potential at the same current under  $CO_2$  is 0.1 V higher than that under  $N_2$ , and the current density at the same potential for the latter is about twice of that for the former. The increase of cathodic current can only be caused by the reduction of water under N<sub>2</sub>, but the enhanced current can be caused by both the reduction of CO<sub>2</sub> and H<sub>2</sub>O under CO<sub>2</sub>. We tried to find out if there is any substance that can reduce KMnO<sub>4</sub> in strong alkaline solution, and found that the solution after 5 circles of the CV scan under CO<sub>2</sub> contained the substance that made the color change from purple, characteristic of KMnO<sub>4</sub>, to the green color of K<sub>2</sub>MnO<sub>4</sub> in a few minutes; however, that under N<sub>2</sub> did not. Therefore, a small amount of formate formed.

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