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Original Research Paper

Effects of nanoparticles diameter and concentration on natural convection of the Al₂O₃-water nanofluids considering variable thermal conductivity around a vertical cone in porous media



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ABSTRACT

The effects of nanoparticles diameter and concentration on natural convection heat transfer of a nanofluid around a vertical cone embedded in a Darcy porous medium is theoretically investigated utilizing the drift-flux model. The thermal conductivity and the viscosity of the nanofluid are assumed as simultaneous functions of temperature and local volume fraction of nanoparticles using experimental correlations. In addition, the flux of nanoparticles on the surface of the cone is assumed to be zero. An efficient mathematical approach with a self-similar solution is utilized to theoretically analyze the boundary layer heat and mass transfer of an Al₂O₃-water nanofluid. The reduced system of ordinary differential equations are general and can be solved for any arbitrary functions of thermal conductivity and viscosity. The analysis of the nanofluid natural convection flow is accomplished for two cases of (i) $T_w > T_\infty$ and (ii) $T_w < T_\infty$. The results show that using nanoparticles would not (would) enhance the heat transfer from the cone for the case of a cone with a hot surface (cold surface). A decrease in the size of nanoparticles or an increase in the volume fraction of nanoparticles causes a decline in the heat transfer rate from the cone when the cone surface is hot. Finally, a comparison between the non-homogenous model (drift-flux model) and the homogenous model of nanofluids is performed. The results demonstrate that the driftflux model tends to the homogeneous model as the size and volume fraction of nanoparticles increase. © 2014 The Society of Powder Technology Japan. Published by Elsevier B.V. and The Society of Powder Technology Japan. All rights reserved.

1. Introduction

Natural convection flow and heat transfer over embedded bodies in porous media has various engineering applications such as thermal energy storage, groundwater systems, flow through filtering media, and crude oil extraction [1]. Such versatile applications have attracted extensive research on natural convection phenomena over embedded bodies within porous media.

Nanofluids are widely used in various thermal systems to boost the heat transfer rate and the thermal efficiency. Nanofluids have been employed in different fields of thermal engineering such as heat exchangers, nuclear reactors, and cooling of electronic devices [2]. Utilizing nanofluids as the working fluid may enhance the heat transfer because of the enhancement in the thermal conductivity. However, other thermo-physical properties also may affect the enhancement of heat transfer of nanofluids. Some of these factors are the thermal conductivity, viscosity, density, heat capacity, dispersion and amorphous movement of nanoparticles, Brownian motion, and thermophoresis effects.

There are two known models for theoretical study of convective heat transfer of nanofluids: (i) homogeneous models and (ii) nonhomogeneous models. In the homogeneous models, the nanofluid is uniform with no slip between the base fluid and nanoparticles. In the non-homogeneous models, the slip between nanoparticles and the base fluid is accounted for, and hence, the nanofluid would not be a uniform mixture of nanoparticles with a base fluid. Many researchers believe that the migration of nanoparticles within the base fluid is the significant reason behind the heat transfer enhancement of nanofluids. The migration of nanoparticles in the base fluid would transfer energy in the base fluid. Using scale analysis, Buongiorno [3] discussed seven possible mechanisms for drift flux of particles during convection of nanofluids. These are inertia, Brownian diffusion, thermophoresis, diffusion phoresis, Magnus effect, fluid

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Nomenclature

С	a constant	Greek s	Greek symbols	
Cp	specific heat (J/kg K)	(ρc)	heat capacity (J/m ³ K)	
D_{E}	Brownian diffusion coefficient (m ² /s)	μ	viscosity (Pa s)	
d_p	diameter of nanoparticle (m)	α	thermal diffusivity (m ² /s)	
D_1	thermophoretic diffusion coefficient (m ² /s)	β	volumetric expansion coefficient of fluid (1/K)	
f	rescaled nanoparticles volume fraction, nanoparticles	3	porosity	
	concentration	γ	cone half-angle	
g	gravitational acceleration vector (m/s ²)	η	dimensionless distance	
h	convective heat transfer coefficient	θ	dimensionless temperature	
k	thermal conductivity (W/m K)	κ	permeability of porous medium (m ²)	
k_B	Boltzmann's constant (1.3807 \times 10 ⁻²³ J/K)	ρ	fluid density (kg/m ³)	
Le	Lewis number	ϕ	nanoparticles volume fraction	
Nl	Brownian motion parameter	ψ	stream function	
Nı	buoyancy ratio			
Nt	thermophoresis parameter	Subscri	pts	
Nı	u Nusselt number	∞	ambient	
Р	pressure (Pa)	eff	effective property between porous medium as	
q_{M}	, surface heat flux	55	fluid	
Ra	l _x local Rayleigh number	f	the base fluid	
r	local radius of the cone	nf	nanofluid	
S	dimensionless stream function	p	nanoparticles	
Т	temperature (K)	ŝ	porous medium	
и,	v Darcy velocity components (m/s)	w	wall	
(<i>x</i>	y) Cartesian coordinates			

drainage, and gravity. However, only the thermophoresis and the Brownian diffusion effects were found to be important [3,4].

Nield and Kuznetsov [5] have extended the work of Buongiorno [3] to the heat transfer of nanofluids in porous media. They have analyzed the natural convection flow of nanofluids over an isothermal flat plate taking into account the Brownian motion and thermophoresis effects. They [5] found that the reduced Nusselt number is a decreasing function of the Brownian motion and thermophoresis parameters. Yih [6] numerically explored the effect of uniform lateral mass flux on natural convection around a cone embedded in a saturated porous medium using a similarity solution. Recently, Rashad et al. [7] have extended work of Yih [6] to the natural convection flow of nanofluids. They [7] have analyzed the heat transfer associated via migration of nanoparticles. They found that as the thermophoresis, Brownian motion and buoyancy ratio parameters increase, the reduced Nusselt number decreases. Natural convective boundary layer flow of a nanofluid over a horizontal plate embedded in a saturated porous medium has been examined by Gorla and Chamkha [8]. Chamkha et al. [9] presented a non-similar solution for natural convective boundary layer flow over a sphere embedded in a nanofluid-saturated porous medium. Rana et al. [10] analyzed the boundary layer heat transfer of nanofluids over an inclined plate embedded in a porous medium. In a recent work, Noghrehabadi et al. [11] have investigated non-Darcy flow and natural convection of nanofluids over a vertical cone embedded in a porous medium. They [11] have reported that the reduced Nusselt number decreases with an increase in the non-Darcy parameter. Noghrehabadi et al. [12] have studied natural convection heat and mass transfer of nanofluids over a vertical plate embedded in a porous medium by applying surface heat and nanoparticle fluxes as boundary conditions. Furthermore, Noghrehabadi and Behseresht [13] analyzed the flow and heat transfer of nanofluid over a cone placed in porous media. Considering the viscosity and thermal conductivity of nanofluids as a linear function of local volume fraction of nanoparticles, they studied the effect of variable properties on the flow and heat transfer of a nanofluid. The important outcome has shown that the reduced Nusselt number would increase with increase of viscosity parameter and decrease with an increase of thermal conductivity parameter [13]. In addition, Gorla et al. [14] have recently studied the nanofluid flow boundary layer for the natural convection over a non-dimensional vertical cone in a porous medium.

between porous medium and nano-

In the mentioned works [7–12], the effects of temperature and local volume concentration of nanoparticles on the thermal conductivity and viscosity of nanofluids were neglected. However, experiments demonstrate that the thermal conductivity and the dynamic viscosity of nanofluids strongly depend on both of the volume fraction of nanoparticles and temperature [4,15,16]. Indeed, although the effect of temperature on the thermal conductivity and the dynamic viscosity of conventional pure fluids can be neglected for small temperature differences, these effects cannot be neglected for nanofluids owing to the presence of nanoparticles [15]. Therefore, in the present study, experimental correlations as simultaneous functions of temperature and local volume fraction of nanoparticles are adopted to include the local effect of temperature and volume fraction of nanoparticles on the thermal conductivity and the dynamic viscosity of an Al₂O₃-water nanofluid.

Previous studies [7–12] have approximated the volume fraction of nanoparticles on the surface to be constant, but this constant is unknown and no effort was made to calculate it. Accomplishing a case study, however, requires the exact value of nanoparticles volume fraction on the surface. Furthermore, an approximation of constant value of nanoparticles volume fraction on the surface generally implies a non-zero value of particles mass flux at the surface. This is an unrealistic assumption since the particles cannot cross the surface. Hence, assuming a zero particle mass flux through the surface as a boundary condition makes a more physical sense.

In this paper, a zero particle flux through the cone surface is utilized as a new auxiliary boundary condition. Furthermore, using similarity variables, the governing partial differential equations are converted into a set of ordinary differential equations. A case study for an Al₂O₃-water nanofluid, as a typical nanofluid, is conducted. The experimental correlations in the literature are then used to evaluate the local values of the dynamic viscosity and the thermal conductivity. Moreover, the nanoparticles volume fraction at the cone surface is also evaluated.

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