



# Investigations on thermal-transfer characteristics of water based on stimulated Brillouin scattering

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## ABSTRACT

In this paper, we present a successful measurement of the thermal-transfer process of water in terms of stimulated Brillouin scattering (SBS) with a pulsed Nd:YAG laser as the light source. The temperature profiles between two different temperature layers can be determined through measuring the linewidth of SBS spectra. The measured results of thermal-transfer process of water are agree well with the theoretical simulation results based on the heat conduction equation. We have demonstrated that, the geometry width and temperature gradient of gradient layer depend on the temperature difference between  $T_1$  and  $T_0$  and different thermal-transfer times. This method presents an important step towards the practical application of a Brillouin lidar system, it could provide a potential technology for investigating the distribution characteristics of the thermocline in ocean.

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## 1. Introduction

The understanding of thermal conduction in liquids is a problem of great relevance in heat management applications, for instance, the dissipated heat of electronic devices can be efficiently transported through a liquid refrigerant recirculating system. The fundamental role that water plays in thermal management applications, since it presents the highest thermal conductivity observed in any molecular liquid. The thermal-transfer characteristics of water is also an important topic in hydrodynamic and biochemical processes, and have been subject to extensive theoretical and experimental investigations during the past decades [1–4]. Theoretically, the thermal conductivity of water can be computed by define suitable boundary conditions, for example, it is possible to estimate the thermal conductivity of water using the Green Kubo approach or by computing the fluid response to a distinct temperature gradient [5–8]. Most studies have focused on a specific temperature and density or a narrow range of thermodynamic states [9–11]. However, experimental studies on certain basic properties of thermal-transfer in water are still scanty, and some important characters during thermal-transfer process, such as geometrical width and temperature gradient at different time were seldom reported. In the present work, a new method for investigating the thermal-transfer characteristics of water based

on stimulated Brillouin scattering [12–16] at different temperature is proposed. Also, the temperature distribution between two different temperature layers is numerical simulated. Sequentially, distribution features of water temperature at different temperature differences are investigated experimentally and analyzed through analyzing the temperature dependence of the linewidth of SBS in water. The whole work is described as follows.

## 2. Theoretical consideration

In this work, the thermal-transfer process of water was considered based on the heat conduction equation:

$$\rho C_p \frac{\partial T}{\partial t} + \rho C_p u \cdot \Delta T = \nabla \cdot (\lambda \Delta T) + Q \quad (1)$$

where,  $C_p/C_v = 1$ ,  $\rho$  is the density of water,  $C_p$  is the thermo capacity at constant pressure,  $T$  is the thermodynamic temperature of water,  $u$  is the speed in the direction of  $\Delta T$ ,  $\lambda$  is the thermal conductivity of water and  $Q$  is the heat resource. For the general case in terms of experimental conditions, we have  $u = 0$ ,  $Q = 0$ . Then, the heat conduction equation can be simplified to the following expression:

$$\rho C_p \frac{\partial T}{\partial t} = \nabla \cdot (\lambda \Delta T) \quad (2)$$

Here, the temperature of water was varied from 5 °C to 40 °C in the natural environment. The thermal conductivity  $\lambda$ , the thermo capacity at constant pressure  $C_p$ , and the density  $\rho$  of water are the

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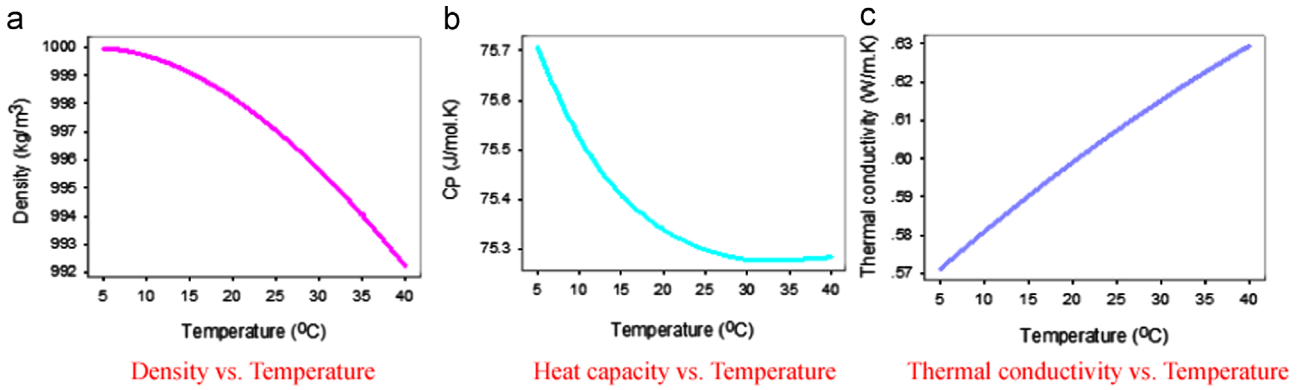


Fig. 1. Changes of density, heat capacity, and thermal conductivity of water with the change of temperature.

function of temperature  $T$ , and can be expressed respectively using:

$$\lambda = 0.561 + 0.002 \times T - (9.62 \times 10^{-6}) \times T^2 \quad (3)$$

$$C_p = 75.98 - 0.061 \times T + 0.002 \times T^2 - (1.755 \times 10^{-5}) \times T^3 \quad (4)$$

$$\rho = 999.86 + 0.058 \times T - 0.008 \times T^2 + (3.97 \times 10^{-5}) \times T^3 \quad (5)$$

Fig. 1 shows the changes of density, thermo capacity at constant pressure and thermal conductivity of water with the change of temperature. It can be seen that, they are neither constants nor linear change with temperature variation.

For simulating the thermal-transfer process, the first type boundary was chosen. Setting the lengths of the two layers are both 0.5 m, the temperature of the two layers are 5 °C and 40 °C, respectively:

$$T_0 = 40 \text{ °C} (0 \leq x \leq 0.5 \text{ m})$$

$$T_1 = 5 \text{ °C} (0.5 < x \leq 1 \text{ m})$$

Substituting the condition and (Eqs. (3)–(5)) into Eq. (2), the temperature distribution between the two layers can be numerical simulated, as shown in Fig. 2. The duration time for simulating the thermal-transfer process was 0–20 h, and Fig. 2 shows the simulated results at different time. One can see from the surface-temperature distribution that there is an obvious temporal variability of the thermal-transfer process of water, the thermal energy transferred gradually from high temperature layer ( $T_0$ ) to low temperature layer ( $T_1$ ). For comparison, the above evolution trait can also be observed from the line-temperature distribution. When the simulation time is 30 min, there is a remarkably thermocline between the high temperature layer and low temperature layer. With the increase of simulation time, the temperature distribution presents a gradient layer, and reaches steady state after 20 h and no stratification exists.

### 3. Experimental measurements and analysis

Basing on the theoretical simulations, we design the following experiments. The schematic diagram considered for experimental measurements is shown in Fig. 3. An injection-seeded, Q-switched and frequency-doubled Neodymium-doped Yttrium Aluminum Garnet (Nd:YAG) laser was used. The wavelength is  $\sim 532$  nm, the pulse duration is  $\sim 8$  ns, the repetition rate is 10 Hz. A narrow linewidth ( $0.003 \text{ cm}^{-1}$ ) can be achieved by switching on the seeder. A thermostatic water tank with the size of 2 m length, 30 cm width and 30 cm high was made. A thin spectralite plate with the size of

1 mm thick, 30 cm width and 30 cm high was glued just at the center of the water tank, so the water tank was divided for two parts with the length of 1 m respectively. Each part was filled up the distilled water. It should be stated that between the two parts there is no water exchange and only the heat exchange exists. In order to reduce the reflection influence from the optical surfaces of the water tank, the normal direction of the front, the middle and the rear surfaces of the water tank was slightly deviated from the direction of the pump laser beam with an angle of  $\sim 5^\circ$ .

The polarization of the pump laser is horizontal, and becomes a circularly polarization along the  $45^\circ$  direction after passing through the polarization beam splitter (PBS) and quarter-wave plate. The laser beam was firstly diverged by a concave lens, then was focused by a converge lens with the focus length of 900 mm. The water tank was placed on a translation stage, it can be moved along with its length direction so that the focus point of the laser just hits on the point close to the dividing glass at the center of the water tank. The water temperature in the part of  $T_1$  was set at 5 °C, while the water temperature in the part of  $T_0$  was set from 10 to 40 °C. When the water temperature in the both parts were stable (after about 30 min), the laser was switched on, and the stimulated Brillouin scattering (SBS) can be excited at the focus point. The data acquisition system consisting of collimating lens, F-P etalon, and ICCD camera. Through measuring the linewidth of SBS the water temperature can be simply determined based on the following empirical equation [14,15]:

$$T = 186.65 \exp(-3.98T_B) \quad (6)$$

Here,  $T_B$  represents the measured linewidth of SBS.

Fig. 4 shows the distribution of water temperature and linewidth of SBS using the SBS method, here “0 cm” in horizontal axis represents the position of spectralite plate. Fig. 4(a) shows the measured linewidth of SBS and corresponding temperature of water at different focus position. For each data point, 30 spectrums of SBS were recorded, and mean values of the linewidth of SBS and water temperature are presented with error bars. In order to show more visually the relationship between the temperature distribution and the water temperature of part  $T_1$  and  $T_0$ , Fig. 4(b) gives the temperature distribution in water tank when the temperature of part  $T_1$  was set at 5 °C and part  $T_0$  varied from 10 °C to 40 °C with the step of 5 °C. It can be seen that, the larger of the temperature difference between  $T_1$  and  $T_0$  is, the more obvious of the gradient layer in the middle position of water tank is. The measured results shown in Fig. 4 agree with the theoretical simulation results in Fig. 2.

For the purpose of expressing the thermal-transfer characteristics, two parameters that geometry width and temperature gradient are used in here. Geometry width denotes the width of gradient layer between  $T_1$  and  $T_0$ , it corresponding to the changes

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