



Investigations on thermal performance characteristics of wire screen packed bed solar air heater

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Abstract

This paper presents the theoretical investigations of thermal performance characteristics of solar air heater having its duct packed with blackened wire screen matrices. The heat transfer equations for two dimensional fully developed fluid flow under quasi-steady state conditions have been developed in order to analyze the thermal efficiency and temperature rise and to study the effect of system and operating parameters. Finite difference solution algorithm has been developed for obtaining numerical solutions of the governing equations for energy transfer. A computer programme is developed in C++ language to estimate the temperature rise of the entering air for evaluation of thermal efficiency by solving the governing equations numerically using relevant correlations for heat transfer coefficient for packed bed systems. Results of temperature distributions and other performance parameters obtained from analysis have been compared with available experimental results. The percentage deviation between the experimental and the analytical values of the dimensionless air temperatures of air and thermal efficiency have been found to be in the range of 7.18 to -9.83 and 7.20 to -9.65 respectively. This establishes the validity of proposed analytical model for the investigation of thermal performance characteristics of packed bed solar air heaters.

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Keywords: Solar energy; Packed-bed; Solar air heater; Plane collector

1. Introduction

Flat plate collectors are extensively used in low temperatures solar energy technology and have attracted the attention of large number of investigators. Several designs of solar air heaters have been developed over the years in order to improve their performance. There has been significant interest in packed-bed absorbers for air heating collector because of some distinct advantages over that of flat plate collectors. Packed-bed matrix absorbs solar radiation ‘in depth’ and has high ratio of heat transfer area to

volume and high heat transfer capability, resulting in relatively low absorber temperature. This will decrease the heat losses from absorber to ambient air and hence result in an increase in the efficiency of the collectors. Absorber having a bed packed with slit-and-expanded aluminum foils matrix (Shoemaker, 1961; Chiou, 1965), iron turnings (Cheema and Mannan, 1979), crushed glass (Collier, 1979), hollow spheres (Swartman and Ogunlade, 1966), iron chips, aluminum chips and pebbles (Mishra and Sharma, 1981), wire mesh screens (Sharma et al., 1991; Beckmann, 1968; Ahmad et al., 1996) have been reported. These studies indicate that such air heaters have superior performance as compared to that of plane collector. A packed-bed solar air heater having its bed packed with

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Nomenclature

A_c	collector plate area (m^2)	R	radiosity at the top surface of upper glass cover (W m^{-2})
A_p	surface area of packing material (m^2)	R_l	radiosity at the bottom surface of lower glass cover (W m^{-2})
A_f	frontal area of collector bed (m^2)	R_2	radiosity at the bottom plate (W m^{-2})
A_v	surface area per unit volume (m^{-1})	R_y	radiosity at a distance y from top surface (W m^{-2})
c_p	specific heat of air ($\text{J kg}^{-1} \text{K}^{-1}$)	\Re	Reynolds number ($= 4r_H G_0 / \mu$)
D	depth of the channel (m)	Re_m	modified Reynolds number ($= \frac{Re(1-Fp)}{Fp}$)
D_e	equivalent diameter of packing material ($= \frac{6V_p}{A_p}$) (m)	St	Stanton number ($= h_c / G_0 c_p$)
d	wire diameter of screen (m)	T_a, T_b, T_g, T_p, T_c	temperatures of surrounding, bed, air, packed material and cover glass respectively ($^{\circ}\text{C}$)
G	mass flow rate per unit collector area ($\text{kg s}^{-1} \text{m}^{-2}$)	T_i, T_o	inlet and outlet temperature of air respectively ($^{\circ}\text{C}$)
G_0	average mass velocity in matrix based on free flow area ($= m/pA_{fr}$) ($\text{kg s}^{-1} \text{m}^{-2}$)	ΔT	air temperature rise ($^{\circ}\text{C}$)
h_c	convective heat transfer ($\text{W m}^{-2} \text{K}^{-1}$)	\bar{u}	flow velocity in duct (ms^{-1})
h_{rs}	radiative heat transfer coefficient from solid surface to solid surface ($\text{W m}^{-2} \text{K}^{-1}$)	U_L	overall loss coefficient ($\text{W m}^{-2} \text{K}^{-1}$)
h_{rv}	radiative heat transfer coefficient from void to void ($\text{W m}^{-2} \text{K}^{-1}$)	V_p	volume of packing material (m^3)
h_v	volumetric heat transfer coefficient ($\text{W m}^{-3} \text{K}^{-1}$)	x	distance in horizontal direction from inlet (m)
h_w	wall heat transfer coefficient for glass cover ($\text{W m}^{-2} \text{K}^{-1}$)	\bar{x}	dimensionless distance ($= x/L$)
I	intensity of solar radiation (Wm^{-2})	$\Delta \bar{x}$	non-dimensional elemental thickness in x -direction
I_1	irradiation at the inner surface of lower glass cover (W m^{-2})	y	distance in vertical direction from top surface (m)
I_2	irradiation at the bottom plate of packed bed collector (W m^{-2})	\bar{y}	dimensionless depth ($= y/D$)
I_y	intensity of solar radiation at depth y from top surface of the bed (W m^{-2})	W	width of the channel
k_e	effective thermal conductivity of packed bed ($\text{W m}^{-1} \text{K}^{-1}$)	<i>Greek symbols</i>	
k_g, k_s	thermal conductivity of air, bed material respectively ($\text{W m}^{-1} \text{K}^{-1}$)	α	absorptivity of wire screen matrices
k_e^0	stagnant bed thermal conductivity ($\text{W m}^{-1} \text{K}^{-1}$)	α_c	absorptivity of cover glass
L	length of the channel (m)	τ	optical depth
l_v	effective thickness of fluid film in void (m)	τ_0	optical depth at $y = D$ ($= \beta D$)
m	mass flow rate of air (kg s^{-1})	$\Delta \tau$	non-dimensional elemental thickness in y -direction
n	refractive index of packing	ρ	density of air (kg m^{-3})
Nu	Nusselt number	σ	Stefan–Boltzmann constant
p	porosity of the bed	β	extinction coefficient of matrix (m^{-1})
p_l	longitudinal pitch (mm)	ε	emissivity of solid surface
p_t	transverse pitch (mm)	ε_w	emissivity of bottom plate
Pr	Prandtl number ($= \mu c_p / k_g$)	ϕ	angle factor i.e. the ratio of effective thickness of fluid film in the void in relation to thermal conduction to equivalent diameter of packing material ($= l_v / D_e$)
q_u	useful heat gain (W)	μ	dynamic viscosity of fluid (Ns m^{-2})
Q_r	radiative heat flux (W m^{-2})		
r_c	reflectivity of cover glass		
r_H	hydraulic radius $\left[= \frac{V_p}{A_p} \left(\frac{p}{1-p} \right) \right]$ (m)		

optically semi-transparent material was proposed and heat collection and storage characteristics were investigated theoretically and experimentally by Hastani et al. (1985). It was observed from the analysis of experimental data that

solar air heaters in which optically semi-transparent materials like glass beads or glass tubes were used for heat collection and storage material had higher efficiency of energy collection in comparison to a usual flat plate

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