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Design procedure for cooling ducts to minimise efficiency loss due to temperature rise in PV arrays

B.J. Brinkworth a,*, M. Sandberg b

^a Cotswold, 11 Wellesley Close, Waterlooville, Hants, UK ^b Department of Built Environment, KTH Research School, University of Gavle, Sweden

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Abstract

The principal variable to be fixed in the design of a PV cooling duct is its depth, and hence the hydraulic diameter of its cross-section D. Analysis of the flow and heat transfer in the duct under still-air (buoyant flow) conditions, when the temperature rise is greatest, is validated by measurements on a full-scale test rig. It is shown that there is an optimum value of this design variable, such that for an array of length L the minimum temperature occurs when the ratio L/D is about 20. The optimum value is not affected much by other quantities, including the slope of the array.

In practical situations, the flow is obstructed by devices across the duct inlet and outlet to exclude insects, birds and rain, and by structural support members crossing the duct interior. It is shown that the latter are no cause for concern, since the effect of the reduction in the flow-rate due to their presence is more than offset by an increase in heat transfer through additional turbulent mixing.

It is also shown that array temperatures are strongly reduced by wind effects, which increase both the heat lost from the front surface of the array and by enhancement of the flow in the duct. Though the trends are clear, limitations are encountered in the present state of knowledge in both areas.

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1. Introduction

The general arrangement of a PV array, with a cooling duct fitted behind it, is represented in Fig. 1. Most of the absorbed solar energy appears passively as heat, raising the temperature of the cells

and thus reducing the efficiency with which the active part is converted into electricity. Measured losses of peak output power of around 1/2% per K temperature rise have been reported for monocrystalline silicon cell arrays (Brinkworth et al., 1997). The raised temperature of the array causes heat to be lost from the front face into the surroundings, and from the rear face into the cooling duct. Buoyancy due to the warming of the air in the duct induces an upward flow, so that the inwardly-transmitted heat

^{*} Corresponding author. Tel.: +44 2392 266547. *E-mail addresses*: bjb@cots.freeserve.co.uk (B.J. Brinkworth), Mats.Sandberg@hig.se (M. Sandberg).

Nomenclature			
a c	constant in Eq. (23) (Wm ⁻² K ⁻¹) coefficient in Eq. (23) (Wm ⁻² K ⁻¹ per	q_0	convective heat flux at front heated wall (Wm^{-2})
	$m s^{-1}$)	$q_{ m s}$	solar heat flux incident on array (Wm ⁻²)
c_p	specific heat capacity of air (J kg ⁻¹ K ⁻¹)	Re_{D}	Reynolds number referred to duct
D	hydraulic diameter of duct cross-section		hydraulic diameter
_	(m)	R^+	roughness parameter for wall friction
$d_{ m h}$	distance from rough wall to plane of zero	R	coefficient in Eq. (16)
7	heat flux (m)	r	exponent in Eq. (16)
d_{m}	distance from rough wall to plane of zero shear stress (m)	S	air temperature stratification parameter, Eq. (2)
F	view factor of duct opening from point on wall of duct	$St_{\rm r}$	Stanton number for convection at rough wall
$f_{ m r}$	Darcy friction factor for rough wall	S	spacing between ribs, or pitch (m)
G^+	wall roughness coefficient for heat trans-	$T_{\rm a}$	temperature of ambient air (K)
	fer	T_{b}	temperature of rear adiabatic wall (K)
g	acceleration due to gravity (m s ⁻²)	$T_{ m m}$	bulk mean temperature of air in duct (K)
g	exponent in Eq. (20)	T_{i}	representative wall temperature (K)
H	height of duct (m)	T_0	temperature of front heated wall (K)
h	height of rib or cross-member (m)	U	mean velocity of air flow in duct (m s ⁻¹)
h_0	convective heat transfer coefficient at heated surface (Wm ⁻² K ⁻¹)	U_{a}	overall heat loss coefficient for array to ambient $(Wm^{-2} K^{-1})$
h_{b}	convective heat transfer coefficient at adiabatic surface (Wm ⁻² K ⁻¹)	V_{10}	meteorological wind speed, 10 m height (m s^{-1})
$h_{ m r}$	heat transfer coefficient for radiative heat	W	width of duct (m)
	transfer $(Wm^{-2} K^{-1})$	W	width of rib (m)
h_{ec}	external heat transfer coefficient due to	X	distance along duct from entrance (m)
	convection $(Wm^{-2} K^{-1})$	α	solar absorptance of array
h_{er}	external heat transfer coefficient due to	$\Delta p_{ m w}$	pressure difference between ends of duct
	radiation $(Wm^{-2} K^{-1})$		due to wind effects (Pa m ⁻²)
h^+	roughness Reynolds number for rough	3	thermal emittance of array/wall
	wall, Eq. (19)	$\epsilon_{ m eff}$	effective emittance for radiative heat ex-
k	thermal conductivity of air (Wm ⁻¹ K ⁻¹)		change between walls
$k_{ m h}$	hydraulic loss coefficient	η	energy conversion efficiency for array
L	length of duct (m)	θ	slope of duct (inclination to horizontal)
$Nu_{\rm c}$	Nusselt number for duct heated from one side	$ heta^*$	influence coefficient for convective wall heat flux
n	convective heat flux partition ratio q_b/q_0	ho	density of air $(kg m^{-3})$
q	total heat flux into duct air (Wm ⁻²)	σ	Stefan–Boltzmann constant (5.67×10^{-8})
$q_{ m b}$	convective heat flux at rear adiabatic wall		${\rm Wm^{-2}K^{-4}}$
	(Wm^{-2})	v	kinematic viscosity of air (m ² s ⁻¹)

is also removed into the surroundings, thus lowering the temperature of the array and restoring some of its efficiency. The induced flow may be assisted or opposed by pressure differences between the inlet and outlet apertures of the duct, due to local wind effects at those points. Several features of this situation have been analysed and modelled over the last decade or so, in which the treatment of the induced flow and the heat transfer at the duct surfaces has been progressively refined (Cross et al., 1994; Brinkworth et al., 1997, 2000; Brinkworth, 2000a,b, 2002; Sandberg

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