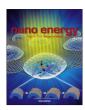
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CO₂ removal from flue gas with amine-impregnated titanate nanotubes



Liping Guo^a, Jie Yang^a, Gengshen Hu^b, Xin Hu^{a,*}, Herbert DaCosta^c, Maohong Fan^{d,**}

- ^a College of Chemistry and Life Sciences, Zhejiang Normal University, Jinhua 321004, PR China
- b Zhejiang Key Laboratory for Reactive Chemistry on Solid Surfaces, Institute of Physical Chemistry, Zhejiang Normal University, Jinhua 321004, PR China
- ^c Math, Science, and Engineering Division, Illinois Central College, 1 College Drive, East Peoria, IL 61635, USA
- d Department of Chemical and Petroleum Engineering, University of Wyoming, Laramie, WY 82071, USA

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ABSTRACT

The purpose of this work was to develop a new high-capacity CO₂ sorbent. Protoned titanate nanotube (PTNT) with different porous textures were synthesized by a hydrothermal method and further modified with different types and amounts of amines including triethylenetetramine (TETA), tetraethylenepentamine (TEPA) and polyethyleneimine (PEI) for CO2 adsorption. Scanning electron microscopy, transmission electron microscopy, nitrogen adsorption, Fourier transform infrared spectroscopy and thermogravimetric analysis were used to characterize PTNT supports or amine composite sorbents. The CO₂ adsorption performances of sorbents were evaluated in a fixed-bed reactor coupled with an online gas chromatograph using a gaseous mixture that resembled realistic flue gas. Experimental results revealed that pore volume rather than surface area of the supports is the dominant factor that determines the CO₂ sorption capacities of the composite sorbents. Furthermore, the CO₂ uptake capacities of the PTNT composite decreased as the size of the impregnated amines increased. The highest CO2 sorption performance attained with the sorbents is 4.33 mmol/g for a PTNT with 60 wt% TETA loading under simulated flue gas condition. It is also found that enhanced contact between CO2 and the impregnated amine was obtained when there was a small space left within the pores of the composite sorbent after amine impregnation. Besides high capacity for CO₂ adsorption, the amine-impregnated PTNTs also display positive effect of moisture, good stability and reusability indicating their great potential in CO2 removal from flue gas.

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1. Introduction

CO₂ emission has caused serious environmental concerns, since CO₂ is the major contributor to greenhouse gas and its consequent global warming effect [1]. To mitigate the CO₂ emission, different CO2 capture techniques have been explored, among which absorption using aqueous amine solution is a state-of-the-art process [2]. This method, however, has high energy penalty, causes corrosion of equipment, in addition to solvent loss, and has high toxicity. In order to circumvent these problems, adsorption with the use of sorbents is proposed as an attractive alternative that can avoid the disadvantages of amine absorption [3–5]. The key of this technology is to find sorbents with superior CO₂ capture capacity under conditions similar to flue gas, which only comprises 10-15% CO₂ with the temperature around 75 °C [6]. Efficient capture of CO₂ under such low CO₂ partial pressures is still a challenge.

E-mail addresses: huxin@zjnu.cn (X. Hu), mfan@uwyo.edu (M. Fan).

Presently, most actively researched solid sorbents include porous carbons [7-12], metal oxide [13-15], zeolites [16,17], metal-organic frameworks (MOFs) [18,19], and porous polymer [20]. These materials possess highly developed porosity and can adsorb large amounts of CO₂ by physisorption under low temperature and high pressure. However, these sorbents show rather low CO₂ capacity and selectivity because of the decreased interaction between sorbent and CO₂ under the condition of flue gas. To improve the CO₂ capture capacity, solid-supported amine sorbents have been developed and show great promise [21-27]. In these composite sorbents, the strong interaction between amine and CO₂ molecules results in high CO₂ uptake at the low pressures of CO₂. Of all kinds of porous materials, silica is the most common used substrate. For example MCM-41 [28,29], MCM-48 [30], SBA-15 [31,32], KIT-6 [33], and silica foam [34-36] were explored as supports for development of amine modified composite sorbents. The results of these studies reveal that the pore volume, pore size, and surface area of the supports determine the CO₂ sorption capacity of the composite sorbents [37]. Generally speaking, support with larger pore volume, pore size and surface area can accommodate a larger

^{*} Corresponding author.

^{**} Corresponding author.

amount of amine for CO2 capture, which is beneficial for the enhancement of CO₂ sorption capacity of the composite sorbents. On the other hand, some works have reported that the surface properties of the supports also played a significant role in creating more effective CO₂ sorbents [14,15,38,39]. For example, protonated titanate nanotube (PTNT) has been used as supports and amineimpregnated protonated titanate nanotube (PTNT) composite sorbents have shown great potential in capture of CO₂ from flue gas i.e. ca. 4 mmol/g CO₂ uptake capacity under conditions of simulated flue gas [40–42]. However, to find the PTNT-based sorbent with higher CO₂ capacity and further understand the CO₂ adsorption mechanism for this system, more systematic studies are needed. With that in mind, this study was designed to enhance our understanding of the characteristics of PTNT-based composite CO₂ sorbents that are synthesized with PTNT having multiple porous structures and various amines, such as triethylenetetramine (TETA), TEPA and polyethyleneimine (PEI). The effects of porous properties of the support and character of the amines on the CO₂ uptake of the resulting composite sorbents are investigated to give more insights in developing new amine/support sorbents for effective CO₂ removal from combustion flue gas.

2. Experimental

2.1. Materials

Anatase Titanium (IV) Oxide (325 mesh) was supplied by Aldrich. This study included the following organic amines: TETA (technical grade), TEPA (technical grade), and PEI (branched, M. W.=600, 99%), supplied by J&K Scientific. NaOH and ethanol was obtained from Sinopharm Chemical Reagent Co., Ltd. Hydrochloric acid (HCl) was supplied by Quzhou reagent Juhua Co., LTD. All experiments used distilled water. All these chemicals were used as obtained, without additional purification.

2.2. Synthesis of protonated titanate nanotube

Three PTNTs with different porous texture were synthesized using a hydrothermal method described elsewhere [41]. Anatase titanium(IV) oxide (2 g) was mixed with 40, 75 or 100 mL 10 mol/L NaOH solution, respectively. After stirring and ultrasonic oscillation, the mixture was transferred to a stainless steel autoclave with Teflon liner and heated at 130 °C for 24 h. After cooling to room temperature, the collected precipitate was firstly washed with 0.1 M HCl solution until the pH value reached about 1.6 and then washed with deionized water to pH=7. The suspension was filtered by suction filtration, and the resulting white solid were put into a vacuum oven at 100 °C overnight. The final product were obtained and designated as T1, T2 and T3, respectively.

2.3. Synthesis of PTNT composite sorbents

Amine functionalized PTNTs were prepared with the wet impregnation method. The typical preparation begins with dissolving the desired amount of amine (TETA, TEPA or PEI) into $10.0\,\mathrm{g}$ ethanol, following by stirring for 30 min, and adding 1 g Tx. The slurry that resulted was then stirred and refluxed at 80 °C for 2 h, and dried at 80 °C until it reached complete volatilization of ethanol. The resulting samples were labeled as n-amine/Tx in which n represents the weight percentage of amine in the composites. For example, 50-TETA/T1 represents the sorbent contains $50\,\mathrm{wt}\%$ TETA and $50\,\mathrm{wt}\%$ T1 support.

2.4. Characterization

The morphology of PTNT support was obtained by field emission scanning electron microscopy (FE-SEM, Hitachi S-4800) and a JEOL-2100F transmission electron microscope operated at 200 KV. The pore characteristics of the sorbents were determined with nitrogen adsorption at -196 °C using Beishide 3H-2000PS2 analyzers. The PTNT and amine functionalized composite sorbents were degassed at 150 °C and 80 °C under vacuum at 1×10^{-3} Torr for a period of at least 12 and 4 h, respectively. The surface area was obtained from calculations using the multipoint Brunauer-Emmett-Teller (BET) method. The total pore volume (V_{total}) was obtained as the volume of liquid nitrogen adsorbed at a relative pressure of 0.98. The pore size distributions of sorbents were derived from the desorption branches of isotherms based on Barrett-Joyner-Halenda (BJH) theory. Thermogravimetric Analysis (TGA) was carried out with a NETZSCH STA 449 C thermal graphic analyzer using a heating rate of 10 K/min in N2. Attenuated Total Reflection Infrared (ATR-IR) spectrum of TETA was determined on a Nicolet 670 FTIR spectrometer equipped with an ATR-IR accessory. Fresh PTNT and TETA-impregnated sorbents were additionally characterized by transmission infrared spectroscopy carried out on the pellets. The ¹³C CP/MAS NMR experiment was conducted on a Bruker AVANCE 400. The spinning frequency was set to 8 kHz. The contact time was 14.85 ms, with recycle delays of 3 s.

2.5. CO₂ adsorption and sorbents regeneration

The CO₂ adsorption capacities of the sorbents were carried out in a fixed-bed reactor system as shown in Fig. S1 (supplementary materials). The adsorption process was done at atmospheric pressure and the outlet gases were monitored online by using an Agilent 7820A gas chromatograph with a thermal conductivity detector (TCD). The online GC can automatically do continuous measurement even with up to 300 data points per minute. Based on the signal changing on the TCD detector, CO2 breakthrough curve was achieved. About 0.5 g dried adsorbent was packed into the middle of the quartz-tube reactor (6 mm inner diameter) and heated by heating tapes. Before each adsorption test, the adsorbent was activated by heating it to 100 °C and maintained in N₂ stream for 1 h with a flow rate of 20 mL/min. After the sorbent cooling to the desired adsorption temperature (e.g., 75 °C), a mixture of 10% CO₂ balanced with N₂ stream at a total flow rate of 10 mL/min was introduced and passed through the adsorbent bed until it reached adsorption saturation. The CO2 breakthrough capacity of adsorbents was calculated by integrating the breakthrough curve along with the subtraction of blank.

In the multiple cyclic adsorption-desorption test, each sample was first activated at 100 °C for 1 h in N_2 . Then, it was cooled down to 75 °C, at which temperature CO_2 adsorption was performed under 10% CO_2/N_2 flow (10 mL/min). Following that, the sorbent regeneration was carried out under N_2 (20 mL/min) through the bed at 100 °C for 1 h. The same adsorption-desorption procedure was conducted for 6 cycles in order to test the stability of the sorbent.

3. Results and discussion

3.1. Characterization of sorbents

The morphology of PTNT (T2 as the representative case) was examined by SEM and TEM, respectively. We can see many irregular aggregations of PTNTs in Fig. 1a. On close observation, Fig. 1b and c reveal that the surfaces of these aggregations contain a large number of scattered and overlapped one-dimensional structures.

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