

# Investigation of reaction between $\text{LiNH}_2$ and $\text{H}_2$

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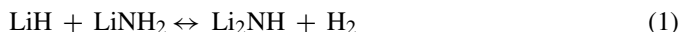
## Abstract

The reactions for  $\text{LiNH}_2$  under a  $\text{H}_2$  and an Ar flow were investigated, respectively. The results showed that  $\text{LiNH}_2$  can be converted into LiH and  $\text{NH}_3$  by reacting with  $\text{H}_2$  under a  $\text{H}_2$  flow condition, whereas  $\text{LiNH}_2$  is converted into  $\text{Li}_2\text{NH}$  and  $\text{NH}_3$  by decomposition under an Ar flow. Moreover, the reaction between  $\text{LiNH}_2$  and  $\text{H}_2$  can be accelerated by mixing  $\text{LiNH}_2$  with LiH as well as doping  $\text{LiNH}_2$  with  $\text{TiCl}_3$ . The confirmation of reaction between  $\text{LiNH}_2$  and  $\text{H}_2$  is helpful for the deeper insight in the systems of Li–N–H and Li–Mg–N–H for hydrogen storage materials.  
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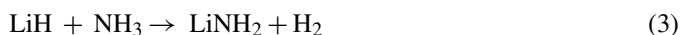
**Keywords:** Hydrogen storage materials; Gas–solid reaction; X-ray diffraction

## 1. Introduction

In order to develop high-performance solid-state hydrogen storage materials for on-board application, recently, much attention has been paid to complex metal hydride [1–4]. Since the Li–N–H system was reported by Chen et al. to be one of the most promising hydrogen storage materials [3], many efforts have focused on the development of this novel hydrogen storage system. Ichikawa et al. [5] has first reported that by doping with 1 mol%  $\text{TiCl}_3$ , the ball-milled mixture of  $\text{LiNH}_2$  and LiH reversibly desorbs/absorbs a large amount of  $\text{H}_2$  (5.5–6 mass%) between 150 and 250 °C according to the following reaction:



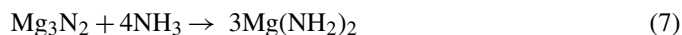
Subsequently, it has been clarified that the above hydrogen desorption reaction proceeds through the following two elementary reaction steps [6,7]:



On the basis of the above mechanism model, we have successfully designed and developed a novel Li–Mg–N–H system, which reversibly stores ~7 mass%  $\text{H}_2$  according to the following reaction [8]:



Similar to the mechanism of the hydrogen desorption reaction (1), it has been proved that the hydrogen desorption reaction (4) was also possible to be mediated by  $\text{NH}_3$  [8,9]. Furthermore, the mechanism of the hydrogenation process of reaction (4) has been investigated as well, indicating that  $\text{Li}_2\text{NH}$  is first hydrogenated into LiH and  $\text{LiNH}_2$ , and then the mixture of  $\text{LiNH}_2$  and  $\text{Mg}_3\text{N}_2$  is hydrogenated into LiH and  $\text{Mg}(\text{NH}_2)_2$ . Finally, the following reactions were proposed as the hydrogenation process [10]:

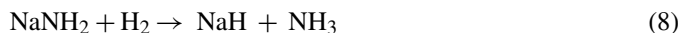


The reactions (5) and (7) have been proved before, but the reaction (6) has not been confirmed yet [10]. On the other hand, a direct molecule–molecule reaction model due to the strong affinity between  $\text{H}^{\delta+}$  in metal amides and  $\text{H}^{\delta-}$  in metal hydride was proposed for understanding a hydrogen desorption mechanism in the Li–N–H and Li–Mg–N–H systems [11,12]. Therefore, the

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study on the reaction between  $\text{LiNH}_2$  and  $\text{H}_2$  seems to be helpful to understand the dominant mechanism of hydrogen storage in this system and provides clues for future research on hydrogen storage materials.

Previously, our results showed that the LiH phase was not detected in the XRD profile after heating  $\text{LiNH}_2$  at  $200^\circ\text{C}$  under a static hydrogen pressure in a closed space [10]. On the other hand, a similar reaction between  $\text{NaNH}_2$  and  $\text{H}_2$  was already investigated one century ago [13,14]. Miles [13] reported that  $\text{NaNH}_2$  was partially converted into NaH in a stream of hydrogen at temperatures between 200 and  $300^\circ\text{C}$ . Therefore, he thought that the following reaction took place:



However, Titherley [14] could not find the proceeding of the reaction (8) when  $\text{NaNH}_2$  was heated under a hydrogen gas atmosphere in an enclosed space up to  $300^\circ\text{C}$ . These results suggest that the equilibrium pressure of  $\text{NH}_3$  for the decomposition of  $\text{NaNH}_2$  is too low and/or the activation energy for the desorbing  $\text{NH}_3$  from the surface of the sample is too high for proceeding of the reaction (8). Motivated by the above results, we planned in this work to investigate the reaction between  $\text{LiNH}_2$  and  $\text{H}_2$  under a  $\text{H}_2$  flow in an open space, which can lead the  $\text{NH}_3$  partial pressure to almost zero on the surface of  $\text{LiNH}_2$  and can progress the reaction (6) even if the equilibrium pressure of  $\text{NH}_3$  is low. In addition, we also studied the doping effect of  $\text{TiCl}_3$  and the mixing effect with LiH on the reaction between  $\text{LiNH}_2$  and  $\text{H}_2$ , since the hydrogen storage properties of the mixture of  $\text{LiNH}_2$  and LiH were significantly improved by doping with 1 mol%  $\text{TiCl}_3$ . As comparison, the two contrastive experiments under a close static hydrogen pressure (close space) as well as an Ar gas flow (open space) were carried out in this work.

## 2. Experimental

The starting material  $\text{LiNH}_2$  (95%), LiH (95%) and  $\text{TiCl}_3$  (98%) were purchased from Sigma–Aldrich. Four kinds of samples, i.e.  $\text{LiNH}_2$ , 1 mol%  $\text{TiCl}_3$ -doped  $\text{LiNH}_2$ , the mixture of  $\text{LiNH}_2$  and LiH, and the mixture of  $\text{LiNH}_2$  and LiH doped with 1 mol%  $\text{TiCl}_3$ , were prepared by ball milling the mixtures for 2 h under a 1 MPa  $\text{H}_2$  atmosphere. The thermal analyses of their samples were carried out by differential scanning calorimetry (DSC) equipment (Q10 PDSC, TA Instruments) under a  $\text{H}_2$  or Ar flow with a flow rate of 100 ml/min. The DSC equipment was especially installed in a glovebox filled with purified argon, so that the samples were never exposed to air. The samples were first heated up to  $200^\circ\text{C}$  at a rate of 5 K/min and kept at  $200^\circ\text{C}$  for 4 h. A temperature of  $200^\circ\text{C}$  was chosen to be the same temperature as the hydrogenation temperature of reaction (4) [10]. The pressure of  $\text{H}_2$  flow was employed to be 1 MPa, and that of Ar to be 0.25 MPa. The identification of structure was carried out by the X-ray powder diffraction (XRD) method with a Cu  $\text{K}\alpha$  radiation (Rigaku, RINT-2100). In addition, Fourier transform infrared spectroscopy measurement (FT-IR, Spectrum One, Perkin-Elmer) was employed to check the identification of products obtained under an Ar flow as well.

## 3. Results and discussion

As shown in Fig. 1a, there are small amount of  $\text{LiOH}$  and  $\text{Li}_2\text{O}$  in the ball-milled  $\text{LiNH}_2$  sample, which are the main impurities of the starting material  $\text{LiNH}_2$ . In the following XRD profiles, although the relative intensity of these impurities looks stronger comparing with the very poor scatterer of LiH, these impurities

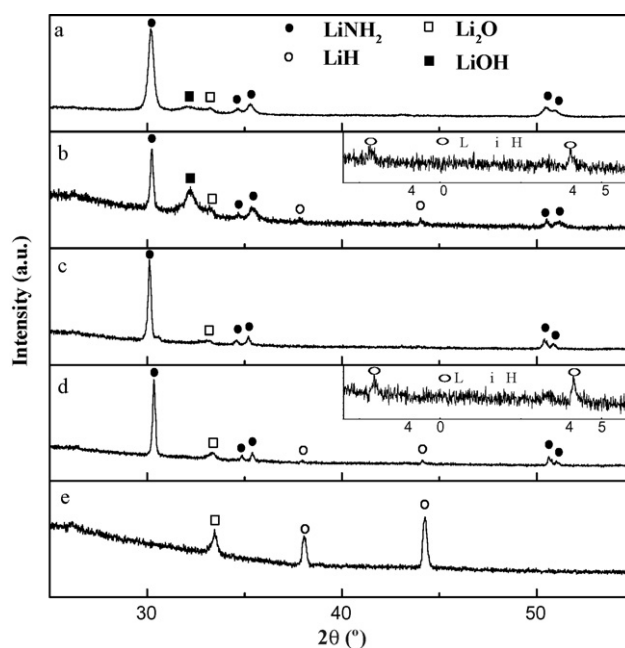


Fig. 1. XRD profiles of the ball-milled  $\text{LiNH}_2$  (a) before heat treatment, (b) after heat treatment at  $200^\circ\text{C}$  for 4 h under a 1 MPa  $\text{H}_2$ -gas pressure flow with a rate of 100 ml/min, (c) after heat treatment at  $200^\circ\text{C}$  for 4 h under 1 MPa  $\text{H}_2$  in a close space, (d) after heat treatment at  $300^\circ\text{C}$  for 4 h under 1 MPa  $\text{H}_2$  in a close space and (e) after heat treatment at  $300^\circ\text{C}$  for 4 h under 1 MPa  $\text{H}_2$  with a flow rate of 100 ml/min, respectively.

have no noticeable effect on the results and our discussion. In order to compare the most intense  $\text{LiNH}_2$  peaks with the tiny LiH ones, the smaller inserts have been added in the corresponding XRD figures which show the poor diffraction peaks of LiH in the narrow region from  $37^\circ$  to  $46^\circ$ . As shown in Fig. 1b,  $\text{LiNH}_2$  is partially converted into LiH after the heat treatment at  $200^\circ\text{C}$  for 4 h under a 1 MPa  $\text{H}_2$  flow, indicating that reaction (6) takes place in an open system, i.e. the  $\text{LiNH}_2$  is hydrogenated into LiH and  $\text{NH}_3$ . However, in a close space even at the same temperature and pressure, reaction (6) does not proceed (Fig. 1c), which is consistent with our previous results [10]. When the temperature is further increased up to  $300^\circ\text{C}$ ,  $\text{LiNH}_2$  is partially converted into LiH even in a close space (Fig. 1d), while under a  $\text{H}_2$  flow (in an open space) it is completely converted into LiH (Fig. 1e). The above results indicate that the equilibrium pressure of  $\text{NH}_3$  for the decomposition of  $\text{LiNH}_2$  is too low for reaction (6) to progress at low temperature of  $200^\circ\text{C}$  and/or the activation energy for releasing  $\text{NH}_3$  from the surface of  $\text{LiNH}_2$  is too high for proceeding of reaction (6) at  $200^\circ\text{C}$  in a close space. However, when  $\text{NH}_3$  is taken away from the system by flowing  $\text{H}_2$ -gas, reaction (6) can easily proceed (Fig. 1b and e). The confirmation of the reaction between  $\text{LiNH}_2$  and  $\text{H}_2$  is helpful for the deeper insight in the systems of Li–N–H and Li–Mg–N–H for hydrogen storage materials. In our previous work [10], we claimed that the mixture of  $4\text{LiNH}_2$  and  $\text{Mg}_3\text{N}_2$  was able to be hydrogenated into  $4\text{LiH}$  and  $3\text{Mg}(\text{NH}_2)_2$  at  $200^\circ\text{C}$ , because  $4\text{NH}_3$  and  $4\text{LiH}$  could be formed by reacting  $4\text{LiNH}_2$  with  $4\text{H}_2$ , and then the produced  $4\text{NH}_3$  is consumed by reacting with  $\text{Mg}_3\text{N}_2$  to form  $3\text{Mg}(\text{NH}_2)_2$ . These results well suggest that the  $\text{NH}_3$  mediated reaction mechanism is acceptable

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