



# Accurate finite volume investigation of nanofluid mixed convection in two-sided lid driven cavity including discrete heat sources



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## ABSTRACT

In the present work, two-dimensional mixed convection fluid flow and heat transfer of water–(Cu, Ag, Al<sub>2</sub>O<sub>3</sub> and TiO<sub>2</sub>) nanofluids in a two-sided facing lid-driven cavity partially heated from below have been investigated numerically. Two discrete heat sources are located on the bottom wall of the enclosure; however, the vertical moving walls and the ceiling are cooled at constant temperature. The remaining boundary parts of the bottom wall are kept insulated. The flow is driven by the moving two facing vertical walls in the same direction and the buoyancy force. The governing equations are solved using a second order accurate finite volume approach. The effects of the monitoring parameters in given ranges such as Reynolds ( $1 \leq Re \leq 100$ ) and Richardson numbers ( $1 \leq Ri \leq 20$ ), solid volume fraction ( $0 \leq \varphi \leq 0.2$ ), the nanoparticles materials as well as the two heat sources positions are investigated. The conducted benchmark study leads to excellent accordance with previous findings. The present study analyzes and discusses the flow patterns (streamlines structures and isotherms distributions) set up by the competition between the forced flow driven by the moving walls and the buoyancy force effects, and the heat transfer rate quantified by the averaged Nusselt number along the heat source. It was found that significant heat transfer enhancement can be obtained: (i) increasing  $Ri$  at high Reynolds number ( $Re = 100$ ) results in up-to 20% augmentation of heat transfer rate for all Cu volume fractions; (ii) increasing the volume fraction  $\varphi$ , a maximum heat transfer rate increase of 47.010% is reached with Cu suspensions for  $\varphi = 0.2$  and  $Ri = 1$ , while a minimum increase of 7.059% is observed for TiO<sub>2</sub>-water nanofluid at  $Ri = 10$  and  $\varphi = 0.05$ ; (iii) a highest heat transfer enhancement occurs when heat sources move toward the two vertical moving walls, while a lower heat transfer is obtained for heat sources located at bottom wall center.

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## 1. Introduction

Study of mixed convection and heat transfer problem in lid driven cavities was met with great interest by researchers and industrials due to its increasing applications in practical situations such as nuclear reactors, lubrication technologies, food storage processing, cooling of microprocessors and electronic components. Besides, to enhance the thermal conductivity

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**Nomenclature**

$C_p$	specific heat ( $\text{J kg}^{-1}\text{K}^{-1}$ )
$d_1$	distance of heat source from the left wall (m)
$d_2$	distance of heat source from the right wall (m)
$D_1$	dimensionless distance of heat source from the left wall $d_1/L$
$D_2$	dimensionless distance of heat source from the right wall $d_2/L$
$e$	length of the heat source (m)
$g$	gravitational acceleration
$Gr$	grashof number $g\beta\Delta TL^3/\nu_f^2$
$k$	thermal conductivity ( $\text{Wm}^{-1}\text{K}^{-1}$ )
$L$	enclosure width (m)
$Nu$	local Nusselt number along the heat source
$\overline{Nu}$	average Nusselt number along the heat source
$p$	pressure ( $\text{N m}^{-2}$ )
$P$	dimensionless pressure
$Pr$	Prandtl number $\nu_f/\alpha_f$
$q$	heat flux ( $\text{W m}^{-2}$ )
$Re$	reynolds number $V_w L/\nu_f$
$Ri$	Richardson number $Gr/Re^2$
$t$	times (s)
$T$	temperature (K)
$u, v$	velocity components in x and y direction ( $\text{m s}^{-1}$ )
$U, V$	dimensionless velocity components in X and Y direction
$V_w$	Lid velocity
$x, y$	cartesian coordinates (m)
$X, Y$	dimensionless coordinates

*Greek symbols*

$\alpha$	thermal diffusivity ( $\text{m}^2 \text{s}$ )
$\beta$	thermal expansion coefficient ( $\text{K}^{-1}$ )
$\Delta T$	temperature gradient $T_h - T_c$
$\tau$	dimensionless time
$\theta$	dimensionless temperature $(T - T_c)/\Delta T$
$\mu$	dynamic viscosity ( $\text{kg m}^{-1} \text{s}^{-1}$ )
$\rho$	density ( $\text{kg m}^{-3}$ )
$\nu$	kinematic viscosity ( $\text{m}^2 \text{s}^{-1}$ )
$\varphi$	volume fraction of the nanoparticles
$\varepsilon_1$	dimensionless length of left heater $e_{S1}/L$
$\varepsilon_2$	dimensionless length of left heater $e_{S2}/L$

*Subscripts*

$c$	cold
$f$	fluid
$h$	hot
$nf$	nanofluid
$s$	solid particles
$S1$	the left heater
$S2$	the right heater

of conventional fluids such as water, oil and ethylene glycol, new technique emerges; that consists of adding minor volume fraction of high thermal conducting nano-scale particles (<100 nm) in the base fluid. The product is called by Choi [1] nano-fluids. It is expected that the presence of the nanoparticles in the fluid really increases the effective thermal conductivity of the fluid and consequently enhances the heat transfer characteristics [1–12].

In the last several years, different researches concerning the problem of convection heat transfer in cavities filled with nanofluids have been carried out analytically, numerically and experimentally. For instance, Tiwari and Das [13] investigated numerically the problem of mixed convection in two-sided lid-driven differentially heated square cavity filled with Copper–water nanofluid. They found that for the Richardson number equal to unity, the average Nusselt number increased substantially with increase in the volume fraction of the nanoparticles. Sebđani et al. [14] used the finite volume method to investigate flow and heat transfer in a square cavity with a heat source on the bottom wall using  $\text{Al}_2\text{O}_3$ -water nanofluid. The

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