### Energy 85 (2015) 221-235

Contents lists available at ScienceDirect

# Energy

journal homepage: www.elsevier.com/locate/energy

# Performance and profitability perspectives of a CO<sub>2</sub> based district energy network in Geneva's City Centre



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#### ARTICLE INFO

Article history: Received 3 September 2014 Received in revised form 28 February 2015 Accepted 14 March 2015 Available online 16 April 2015

Keywords: District energy Refrigerant CO<sub>2</sub> Urban energy systems Heat pump Thermoeconomics

## ABSTRACT

A new type of district energy network providing simultaneously heating and cooling services is being investigated. It is based on the use of  $CO_2$  as a heat transfer fluid by taking advantage of the latent heat of vaporization, to store and transfer heat across the network. The goal of the present study is to determine the performance of a  $CO_2$  network when applied to a real urban area. It focuses first on determining the requirements for the various thermal energy services for a part of Geneva's City Centre. The final energy consumption is first computed for the energy conversion technologies now in place in this area – namely heating oil boilers and air cooled compression chillers. Then the new final energy consumption is computed the  $CO_2$  network is used instead of boilers and air cooled compression chillers. For the area considered the  $CO_2$  network is variant leads to a final energy consumption of 10,968 MWh of electricity. It represents a reduction of 84.4% when compared to the boilers and chillers case. A comparative profitability analysis of the two cases is also presented. The analysis takes into account investment, heating oil and/or electricity, equipment replacement, operation, and maintenance costs, as well as the sales of energy services.

For an interest rate of 6%, a price of the delivered heating/cooling services at 0.108  $\in$  kW h<sup>-1</sup> and a lifetime of 40 years, the conventional technology does not reach profitability while the CO<sub>2</sub> network achieves a profit in present value of 69.59 million  $\in$  and the break-even point is reached after 5.5 years of operation.

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## 1. Introduction

District heating and cooling networks have been used to deliver energy in urban areas for many decades. Generally, these networks rely on centralized and efficient energy conversion technologies supplying heating and/or cooling to the users through a water network. In most of the cases, the supply temperature of such a network is selected according to the most demanding consumer connected. Thus all the other users are supplied at a temperature beyond their needs – often far beyond their needs. Furthermore, when heating and cooling have to be supplied, two independent water loops are needed. Finally, most of the time, heat discharged by the cooling users in the district cooling network is not transferred to the district heating network, and thus not recovered. A

new type of district energy network is being investigated. It is based on the use of refrigerant as a heat transfer fluid. It uses the latent heat of vaporization, instead of sensible heat, to store and transfer heat. The pressure of the network is selected such that evaporation/condensation takes place at a desired temperature usually around to 15 °C, but potentially up to the critical temperature of the refrigerant chosen. The level of temperature should be selected so as to allow for free cooling in most of the cooling applications, while decentralized heat pumps transfer heat from the network to each user at the specific required temperature level. Furthermore only two pipes are required by the network, thus allowing the waste heat from the cooling users to be recovered by the heating users. Obviously, the heat required by the heating users may, most of the time, not be strictly equal to the waste heat discharged by the cooling users. Hence, a central plant is needed to balance the overall network by taking or releasing heat into the environment, for instance a lake. A schematic view of a refrigerant based network using CO<sub>2</sub> as a working fluid is provided in Fig. 1 and



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| Nomenclature     |  | ε <sub>n</sub><br>ε <sub>n</sub> | Boiler first law efficiency at part load<br>Boiler first law efficiency at nominal load |  |
|------------------|--|----------------------------------|---|--|
|                  |  | η                                | Efficiency  |  |
| Acronyms         |  | λο                               | Boiler consumption at idling condition relative to                                      |  |
| ERA              | Energy reference area                                  |                                  | nominal load  |  |
| HX               | Heat exchanger   | ρ                                | Mass density, kg m <sup>-3</sup>  |  |
| LMTD             | Log mean temperature difference                        | au                               | Load factor   |  |
| MDAC             | Mechanical draught air-cooler                          |                                  |   |  |
| PLC              | Programmable logic controller                          | Subscrip                         | ubscripts   |  |
| YDD              | Yearly degree days                                     | а                                | Atmosphere  |  |
|                  |  | air                              | Cooling air   |  |
| Symbols          |  | AirCond                          | Air conditioning  |  |
| Α                | Area, m <sup>2</sup>                                   | cond                             | Condenser   |  |
| Ė                | Electric power, W                                      | data                             | Data centre cooling   |  |
| h                | Specific enthalpy, J kg <sup>-1</sup>                  | ERA                              | Energy reference area   |  |
| ṁ                | Massflow, kg s <sup>-1</sup>                           | evap                             | Evaporator  |  |
| <u></u>          | Heat rate, W   | Н                                | Space heating supply  |  |
| s                | Specific entropy, $I kg^{-1} K^{-1}$                   | heating                          | Space heating   |  |
| Т                | Temperature, °C  |                                  | HotWaterHot water preparation   |  |
| U                | Overall heat transfer coefficient, W m <sup>-2</sup> K | in                               | Inlet condition   |  |
|                  |  | liq                              | State in the liquid CO <sub>2</sub> line  |  |
| Greek symbols    |  | Ν                                | Network   |  |
| ∆h               | Specific enthalpy difference, J kg $^{-1}$             | out                              | Outlet condition  |  |
| $\Delta P$       | Pressure drop, N m <sup><math>-2</math></sup>          | refrig                           | Refrigeration   |  |
| $\Delta T$       | Temperature change, K                                  | S                                | Isentropic  |  |
| $\Delta T_{min}$ | Minimum approach temperature difference, K             | sat                              | Saturation state  |  |
| $\Delta T_{SC}$  | Subcooling, K  | vap                              | State in the CO <sub>2</sub> vapour line  |  |
| $\Delta T_{SH}$  | Superheat, K   | W                                | Water   |  |

a more detailed description of the concept is given by Weber and Favrat in Refs. [1,2]. Finally, a list of possible energy services and associated conversion technologies that can be included in a refrigerant based network was done by Henchoz et al. in Ref. [3]. The objective of the present study is to determine the benefits that

a refrigerant based district energy network, using  $CO_2$  as a working fluid, could have over a fully decentralized conversion technology using a combination of boilers and compression chillers. The comparison is done with respect to the final energy consumption and the economic viability of both systems. The present study



Fig. 1. Schematic representation of a CO<sub>2</sub> based district energy network. Side A – net cooling operation. Side B – net heating operation.

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