

CO₂ abatement by co-firing of natural gas and biomass-derived gas in a gas turbine

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Abstract

In this work, a possible way for partial CO₂ emissions reduction from gas turbine exhausts by co-firing with biomass is investigated. The basic principle is the recirculation of a fraction of the exhausts (still rich in oxygen) to a gasifier, in order to produce syngas to mix with natural gas fuel. As biomass is a CO₂ neutral fuel, the fraction of replaced natural gas is a measure of CO₂ removal potential of the powerplant.

The investigated solution considers the conversion of solid fuel to a gaseous fuel into an atmospheric gasifier, which is blown with a recirculated fraction of hot gas turbine exhausts, typically still rich in air. In this way, the heat content of the exhausts may be exploited to partially sustain the gasification section.

The produced syngas, after the tar removal into the high temperature cracker, is thus sent to the cooling section, consisting of three main components: (I) gas turbine recuperator, (II) heat recovery steam generator and (III) condensing heat exchanger to cool down the syngas close to the environmental temperature before the subsequent recompression and mixing with natural gas fuel into the combustion chamber. The water stream produced within the condensing heat exchanger upstream the syngas compression is vaporised and sent back to the gasifier.

If very limited modification to the existing gas turbine has to be applied in order to keep the additional costs limited, only a relatively reduced fraction of the low calorific value syngas may be mixed with natural gas. The analysis at different levels of co-firing has shown that no appreciable redesign has to be applied to the target GE5 machine up to 25–30% (heat rate based) renewable fraction. With an accurate heat recovery from the cooling/cleaning system of the syngas, the same levels of efficiency of the original machine have been achieved, in spite of the relatively large power consumption of the syngas recompression. Very interesting results have been obtained within the 10–30% range of biomass co-firing, with CO₂ removal levels between 30% and 50% with reference to the values of the base GE5 gas turbine powerplant.

The economic analysis has shown that, in spite of the high investment required for the syngas fuel production chain (gasifier, coolers, cleaners and fuel compressor), approximately at the same level of gas turbine itself, there is an interesting attractiveness due to the possibility of selling high-value green certificates and CO₂ allowances, which reduce the payback time to 2–4 years.

The uncertainty on the calculated economic parameters are greatly influenced by the uncertainty on actual biomass availability and yearly working time of powerplant, whereas off design operation, which affects mainly the uncertainty of compressor and turbine efficiency, is mainly reflected on the uncertainty of electric power output and efficiency.

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1. Introduction

The Kyoto Protocol subscription led many countries to make efforts toward the research and proposal of systems

and techniques for CO₂ capture and sequestration from powerplants. Most of these studies investigate the field of massive CO₂ emissions capture (80% plus), by applying pre or post combustion technologies [1–11]. The proposed solutions often imply relevant changes in existing turbo-machinery equipment, which are highly expensive and generally discourage the electricity providers in taking

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Nomenclature

AF_{st}	actual air/fuel ratio	h_Y	yearly number of working hours (years)
AF_{act}	stoichiometric air/fuel ratio	LHV	generic lower heating value (kJ/kg)
a_{GT}	sound speed at inlet turbine (m/s)	LHV _{CC}	lower heating value of fuel mixture at combustion chamber inlet (kJ/kg)
α	moles of H per mole of biomass	LHV _{syn}	lower heating value of syngas (kJ/kg)
β	moles of O per mole of biomass	Lp _{GAS}	relative pressure loss ($\Delta p/p$) at the gasifier + tar cracker
$\Delta\Phi_{GE5}$	variation of dimensional flow coefficient at turbine inlet relative to the nominal GE5 design value	Lp _{PHRSG}	relative pressure loss ($\Delta p/p$) at the heat recovery steam generator (HRSG) + baghouse filter
η_{GT}	GT efficiency	Lp _{REC}	relative pressure loss ($\Delta p/p$) at the GT recuperator
η_{EL}	net electric efficiency	Lp _{SEP}	relative pressure loss ($\Delta p/p$) at the condensing heat exchanger (SEP) + scrubber
η_{film}	film cooling effectiveness	m_{bio}	biomass flowrate (kg/s)
η_{GEN}	electric generator efficiency	m_{IG}	mass flowrate of exhausts recirculated to the gasifier (kg/s)
C_{quota}	price of CO ₂ allowance per ton of CO ₂ avoided	m_{GT}	inlet turbine mass flowrate (kg/s)
ER	equivalence ratio = AF_{act}/AF_{st}	\underline{m}_{steam}	mass flow of reinjected steam into the gasifier (kg/s)
ε_H	blade cooling effectiveness	m_{syn}	syngas flowrate (kg/s)
f	fraction of exhausts recirculated to the gasifier	PBT	payback time (years)
Φ_{GE5}	nominal dimensional flow coefficient of the target GE5 gas turbine (m ²)	PR	compressor pressure ratio
Φ_{GT}	dimensional mass flow coefficient at turbine inlet (m ²)	Q	heat added or released to gasifier (kW)
F_{ren}	fraction of gas turbine heat rate provided with syngas fuel	R	powerplant size scale coefficient
GC	price of green certificates (€/kWh)	ρ_{GT}	gas density at turbine inlet (kg/m ³)
G_{green}	yearly incomes from sale of green certificates (€)	T_0	reference temperature (K)
G_{CO_2}	yearly incomes (or missed outcomes) due to CO ₂ quota (€)	T_g	gasification temperature (K)
G_{CH_4}	yearly savings, over the basic GT, due to reduced natural gas consumption (€)	T_{in}	gasifier inlet temperature (K)
H_P	total energy of products (kW)	T_{OSEP}	syngas temperature at the SEP outlet (K)
H_R	total energy of reactants (kW)	W_{emain}	main compressor power consumption (kW)
		W_{csyn}	power demand for syngas fuel recompression (kW)

some measures against CO₂ emissions [10,11]. Even the cheapest solutions, aimed to reduce, as far as possible, the redesign of existing equipment (i.e. semi-closed gas turbine cycles SCGT), have shown additional costs of electricity around 60–70% compared to traditional layouts with no CO₂ removal [12,13], even if most recent studies promise to reach the low 30–40% levels [14]. Further unknowns connected to costs of transportation and storage of liquid compressed CO₂ and the related environmental safety made application of CO₂ capture systems unattended [15].

It is well known that renewable fuel sources have, globally, zero CO₂ emissions to the environment, thus they might have an interesting potential to approach the greenhouse issue. On the other hand, their extensive application to existing powerplants often involves deep and expensive modifications to current technologies. The most mature are those involving IGCC, the largest fraction of which are currently fed with coal but might be converted (at least partially) to biomass fuels with no appreciable changes in equipment. They are, anyway, applicable in the field of large power generation, of the order of few hundred MW electric power [16].

The upcoming 2006 CO₂ emissions trading into the European Community should encourage all Member States to provide substantial investments for tackling CO₂ emissions. The market of CO₂ allowances is planned to start by April 2006. Companies covered by the Emissions Trading Scheme need to record and report their CO₂ emissions as of January 2005. They also need to deliver for the first time in April 2006 a sufficient number of allowances to cover emissions during 2005. If a company delivers no allowances—or not enough allowances—a sanction of €40 per non-delivered allowance will be imposed by the Member State. In this way, the adoption of systems with even partial CO₂ emissions reduction potential (15–50%) might lead to a consistent reduction in electricity production costs and encourage companies to make investments for CO₂ abatement. The partial integration of biomass fuels with natural gas implies a proportional reduction of CO₂ emissions, playing, globally, an important role if its application was extended to several powerplants. The co-firing of gas turbines with natural gas and biomass-derived fuel has been a largely investigated

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