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#### **ABSTRACT**

Hydrate-based  $CO<sub>2</sub>$  capture (HBCC) has received increasing attention, due to such advantages as the mild operating pressure and temperature, the ease of regeneration and its unique separation mechanism. This review paper is focused on the chemical additives and the mechanical methods that have been investigated to improve the CO2 separation efficiency and energy consumption through HBCC technology. Detailed comparisons of the effects of various chemical additives and mechanical methods on gas consumption, operating conditions, hydrate induction time and CO<sub>2</sub> recovery are critically reviewed. The limitations and challenges of HBCC, in comparison with the conventional methods for  $CO<sub>2</sub>$  capture also are discussed.

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## 1. Introduction

Carbon dioxide  $(CO<sub>2</sub>)$  capture is a continuous process which requires a significant amount of energy to operate. It contributes to around 70–90% of the total operating cost of the three-stage carbon capture and storage system that is commonly used for the reduction of  $CO<sub>2</sub>$  emissions ([Herzog and Golomb, 2004](#page--1-0)). Current  $CO<sub>2</sub>$ capture employs adsorption, absorption and membrane technologies which are low in efficiency and usually require multiple stages. Continuous efforts have been made to search for alternative methods in the area of  $CO<sub>2</sub>$  capture so that the overall operating cost of the carbon capture can be reduced.

 $CO<sub>2</sub>$  is captured from the effluent of power plants either post combustion or pre-combustion. Post-combustion capture refers to the treatment of flue gas before being released into the atmosphere. The flue gas consists of approximately  $15-20\%$  CO<sub>2</sub> and  $5\%$  O<sub>2</sub>, with the balance being  $N_2$ , and it is emitted from a full combustion process. Pre-combustion capture refers to the capture of  $CO<sub>2</sub>$  from the fuel gas, which is the partially combusted fuel containing approximately 40%  $CO<sub>2</sub>$  and 60% H<sub>2</sub>. The high  $CO<sub>2</sub>$  content in the fuel gas allows more efficient capture. However, it can only be employed in an integrated gasification combined cycle (IGCC) power plant where the fuel is pre-treated to produce  $CO<sub>2</sub>/H<sub>2</sub>$  syngas

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and the  $CO<sub>2</sub>$  is separated from the syngas while the H<sub>2</sub> is fed into the combustion process. Post-combustion  $CO<sub>2</sub>$  capture is less effective than the pre-combustion method. However, it can be retrofitted to any plant without much modification ([Spigarelli and Kawatra,](#page--1-0) [2013\)](#page--1-0). Regardless, the gas systems that are discussed in this paper are mostly  $CO<sub>2</sub>$ , or  $CO<sub>2</sub>/N<sub>2</sub>$ , or  $CO<sub>2</sub>/H<sub>2</sub>$ .

Hydrate-based  $CO<sub>2</sub>$  capture (HBCC) technology is a novel process that has received enormous attention, both from the industry and academic researchers, during the last two decades. The technology operates at mild pressures and temperatures, through a unique separation mechanism that is easy to regenerate and capable of separating gas mixtures, which might not be achievable via conventional technologies ([Englezos and Lee, 2005](#page--1-0)). A significant number of studies have reported on the potential application of gas hydrates technology in  $CO<sub>2</sub>$  capture. These include some early work that was mostly focused on phase equilibrium studies of pure CO2 hydrates, and more recent work that has focused closely on investigations of various chemical additives and mechanical methods for enhancement of the efficiency of  $CO<sub>2</sub>$  capture and separation. This paper will review the recent developments and research activities conducted on HBCC with a focus on chemical additives and mechanical approaches that are able to improve the selectivity, efficiency and kinetics of this technology. An introduction to the principles and significance of gas hydrates technology will be followed by detailed discussions of the current progress in technological improvements through the application of various chemical additives and mechanical methods. The key effects of the chemicals and mechanical methods, as well as the major outcomes





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of the research activities, will be summarised. In addition, the paper will give an account of the costs, limitations and challenges that are associated with HBCC, in comparison with the conventional technologies.

## 2. Hydrate-based CO<sub>2</sub> capture technology

#### 2.1. Gas hydrates

Gas hydrates are solid clathrates made up of gas molecules (guests), such as methane (CH<sub>4</sub>), CO<sub>2</sub>, N<sub>2</sub> and H<sub>2</sub>, that are caged within a cavity of hydrogen-bonded water molecules (host). They form under the favourable thermodynamic conditions of low temperature and high pressure, and they exhibit various structures depending on the size and chemical properties of the guest mole-cules ([Sloan and Koh, 2008\)](#page--1-0). Most small gas molecules, such as CO<sub>2</sub> and CH<sub>4</sub>, form structure I (S<sub>I</sub>). Structure II (S<sub>II</sub>) hydrates form with larger gas molecules such as  $N_2$  ([Davidson et al., 1986\)](#page--1-0) and propane. With the mixture of both small and large gas molecules, such as methane  $+$  cycloheptane, the structure H (S<sub>H</sub>) may form [\(Sloan,](#page--1-0) [2003](#page--1-0)). The crystal structures of these hydrates consist of different water cavities. The most common forms of water cavity include the irregular dodecahedron (4 $^{3}$ 5 $^{6}$ 6 $^{3})$  and the pentagonal dodecahedron (5<sup>12</sup>), as well as the tetrakaidecahedron (5 $^{12}6^2$ ), the hexakaidecahedron (5 $^{12}$ 6 $^{4}$ ) and the icosahedron (5 $^{12}$ 6 $^{8}$ ) that are often collectively described as  $5^{12}6^m$ , with  $m = 2, 4, 8$  [\(Sloan and Koh,](#page--1-0) [2008](#page--1-0)). The term " $5^{12}$ " is used to indicate that a relatively smaller cavity contains 12 pentagonal faces, whereas the term " $5^{12}6^{m}$ " denotes a larger cavity with 12 pentagonal and m hexagonal faces, while "4<sup>3</sup>5<sup>6</sup>6<sup>3</sup>" illustrates a medium cavity which contains 3 tetragonal, 6 pentagonal and 3 hexagonal faces. A combination of  $5^{12}$  and  $5^{12}6^2$  is more commonly seen in S<sub>I</sub>, while the combination of  $5^{12}$  and  $5^{12}6^4$  is more commonly seen in S<sub>II</sub>. In S<sub>H</sub>, a combination of 5<sup>12</sup>, 4<sup>3</sup>5<sup>6</sup>6<sup>3</sup> and 5<sup>12</sup>6<sup>8</sup> has been observed.

Formation of gas (in particular methane) hydrates has been a significant problem for the upstream oil and gas industry because they clog pipelines, valves, wellheads and processing facilities, thus reducing production and causing safety problems. Extensive research activities have been undertaken in order to prevent or mitigate the formation of gas hydrates ([Kelland, 2006](#page--1-0)). Research on the enhancement of gas hydrate formation began in the late 19th century after discovering the positive applications of gas hydrates for gas storage, separation, sequestration and desalination [\(Sloan](#page--1-0) [and Koh, 2008\)](#page--1-0).

## 2.2. Gas hydrate-based  $CO<sub>2</sub>$  capture

 $CO<sub>2</sub>$ , as a small nonpolar hydrocarbon, forms  $S<sub>I</sub>$  hydrates with a formula of  $CO_2 \cdot nH_2O$  ( $n = 5.75$ ) when coming into contact with water molecules below the equilibrium temperature and above the equilibrium pressure [\(Sloan and Koh, 2008](#page--1-0)). Upon dissociation, one volume of  $CO<sub>2</sub>$  hydrates can release 175 volumes of  $CO<sub>2</sub>$  gas at standard temperature and pressure conditions, which is potentially useful for the separation of the  $CO<sub>2</sub>$  from flue gas. The equilibrium phase diagram of  $CO<sub>2</sub>$  hydrates is presented in Fig. 1, which is constructed using an equation from experimental data reported by [Kamath \(1984\)](#page--1-0). The figure also shows that other gases, such as  $N_2$ ,  $H<sub>2</sub>$ , and  $O<sub>2</sub>$ , form hydrates under different equilibrium conditions. The equilibrium curve of  $H_2$  was obtained from [Dyadin et al. \(1999\).](#page--1-0)

As one can see from the equilibrium diagrams,  $CO<sub>2</sub>$  has the lowest hydrate-forming pressure in comparison with other components in flue gas. Separating  $CO<sub>2</sub>$  from the other gases can be achieved by first forming a solid hydrate phase that is enriched with CO<sub>2</sub>. Dissociating the hydrates, after separating the hydrate phase from the gaseous phase, leads to the recovery of  $CO<sub>2</sub>$  that is much higher in concentration than the initial feed. Studies have shown that the concentration of  $CO<sub>2</sub>$  in the hydrate phase is at least four times greater than that in the gas phase ([Duc et al., 2007](#page--1-0)). This hydrate-based  $CO<sub>2</sub>$  capture process is illustrated in a flow diagram displayed in [Fig. 2](#page--1-0). In brief, the gas mixture is sent to the hydrate formation reactor, in which  $CO<sub>2</sub>$  hydrates form as the pressure increases and temperature decreases. The hydrate slurry is separated from the  $CO<sub>2</sub>$ -lean gas in the separator and sent to a hydrates dissociation reactor, from which purified  $CO<sub>2</sub>$  is collected, and the CO2-rich gas is recycled for further processing.

### 2.3. Parameters describing the HBCC process

The efficiency of hydrate-based  $CO<sub>2</sub>$  separation is often described by such parameters as hydrate induction time, gas consumption, hydrate equilibrium pressure,  $CO<sub>2</sub>$  recovery or split fraction (S.Fr.) and separation factor (S.F.).



Fig. 1. The equilibrium phase diagrams of different hydrate formers.

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