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#### Short communication

## Bioelectrocatalytic formate oxidation and carbon dioxide reduction at high current density and low overpotential with tungsten-containing formate dehydrogenase and mediators



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#### ABSTRACT

We show a great possibility of mediated enzymatic bioelectrocatalysis in the formate oxidation and the carbon dioxide (CO<sub>2</sub>) reduction at high current densities and low overpotentials. Tungsten-containing formate dehydrogenase (FoDH1) from *Methylobacterium extorquens* AM1 was used as a catalyst and immobilized on a Ketjen Black-modified electrode. For the formate oxidation, a high limiting current density ( $j_{lim}$ ) of ca. 24 mA cm<sup>-2</sup> was realized with a half wave potential ( $E_{1/2}$ ) of only 0.12 V more positive than the formal potential of the formate/CO<sub>2</sub> couple ( $E^{\circ\prime}_{CO2}$ ) at 30 °C in the presence of methyl viologen (MV<sup>2+</sup>) as a mediator, and  $j_{lim}$  reached ca. 145 mA cm<sup>-2</sup> at 60 °C. Even when a viologen-functionalized polymer was co-immobilized with FoDH1 on the porous electrode,  $j_{lim}$  of ca. 30 mA cm<sup>-2</sup> was attained at 60 °C with  $E_{1/2} = E^{\circ\prime}_{CO2} + 0.13$  V. On the other hand, the CO<sub>2</sub> reduction was also realized with  $j_{lim} \approx 15$  mA cm<sup>-2</sup> and  $E_{1/2} = E^{\circ\prime}_{CO2} - 0.04$  V at pH 6.6 and 60 °C in the presence of MV<sup>2+</sup>.

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#### 1. Introduction

Electro-enzymatic devices have received considerable attention in view of clean technology to produce electricity and useful materials from renewable fuel sources. An interconversion system of the formate/carbon dioxide (HCOO $^-$ /CO $_2$ ) couple is one of the promising objects for such devices (strictly speaking, CO $_2$  exists as hydrogen carbonate (HCO $_3^-$ ) around neutral pH, but we may simply use "CO $_2$ " in this paper). HCOO $^-$  is an energy-rich compound and can be used as a fuel of energy conversion systems such as HCOO $^-$ /O $_2$  biofuel cells, which are comparable to H $_2$ /O $_2$  biofuel cells in terms of the theoretical standard electromotive force (ca. 1.2 V [1–3]). On the other hand, an efficient bioelectrochemical system of the CO $_2$  reduction may help us to produce energy-rich products or useful organic chemicals [4] and to reduce the atmospheric CO $_2$  level under mild conditions [5].

Recently, we have electrochemically characterized tungstencontaining formate dehydrogenase from *Methylobacterium extorquens* AM1 (FoDH1; EC 1.2.1.2) as a heterodimeric soluble enzyme [6]. It has been shown that FoDH1 produces mediated bioelectrocatalytic currents for both of the HCOO<sup>-</sup> oxidation and the CO<sub>2</sub> reduction. From the viewpoint of the kinetics between the enzyme and the mediators, 9,10-phenanthrenequinone (PQ) is the most effective mediator for the HCOO $^-$  oxidation. From the thermodynamic viewpoint, methyl viologen (MV $^{2+}$ , 1,1′-dimethyl-4,4′-bipyridinium ion) is a useful mediator for the reversible catalytic reaction of FoDH1 because the midpoint potential of the MV $^{2+}$ /MV $^{+*}$  couple ( $E_{\rm m,MV}$ ) is very close to the formal potential of the HCOO $^-$ /CO $_2$  couple ( $E^{\circ}$ /<sub>CO2</sub>) around neutral pH. FoDH1 is expected to be applied to the construction of efficient electro-enzymatic devices utilizing the interconversion between HCOO $^-$  and CO $_2$ .

In such bioelectrochemical devices, a large current density (j) should be realized at potentials close to  $E^{\circ}_{CO2}$ . A promising approach to increase j is to immobilize enzymes and mediators on an electrode surface. For this purpose, Heller's group has developed osmium polymers to successfully immobilize enzymes and mediators on electrodes for a mediated electron transfer (MET)-type bioelectrocatalytic system [7]. By using this method, Tsujimura et al. recorded 100 mA cm $^{-2}$  of limiting current density ( $j_{lim}$ ) at 25 °C for a glucose oxidation [8]. However, very large overpotentials ( $\approx 1$  V) are required in such bioelectrochemical glucose oxidation systems to get large  $j_{lim}$  because of a large formal potential difference between the substrate and the enzyme and of a large kinetic hindrance between the enzyme and the Os polymers. Development of a new mediated bioelectrocatalytic system with small overpotentials is needed.

In this paper, we attempt to construct a MET-type bioelectrocatalytic system for the HCOO $^-$  oxidation and the CO $_2$  reduction with high  $j_{\rm lim}$  and very small overpotentials by using FoDH1. PQ, MV $^2+$ , and a viologen-functionalized polymer (VP) were used as mediators. In

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addition, we focused on Ketjen Black (KB) as an electrode material to effectively immobilize FoDH1. The high  $j_{\rm lim}$  of ca. 145 mA cm $^{-2}$  was realized at 60 °C without the overpotential in practice for the HCOO $^{-}$  oxidation by using free MV $^{2+}$ . Co-immobilization of FoDH1 and mediators was also attempted for practical purpose. The bioelectrochemical CO $_{2}$  reduction with high  $j_{\rm lim}$  was also realized.

#### 2. Experimental

#### 2.1. Chemicals

KB was kindly donated from Lion Co. (Japan). Poly(tetrafluoroethylene) fine powder (PTFE, 6-J) was obtained from DuPont Mitsui Fluorochemicals (Japan). MV<sup>2+</sup> dichloride and PQ were obtained from Tokyo Chemical Industry (Japan). Poly(vinylpyrrolidone) (PVP) and poly(ethylene glycol) diglycidyl ether (PEGDGE) were obtained from Sigma-Aldrich Co. (USA). Other chemicals were obtained from Wako Pure Chemical (Japan). FoDH1 was purified according to the literature [6].

#### 2.2. Preparation of FoDH1-modified electrodes

KB slurry (KB:PTFE = 8:2 (w/w) in 2-propanol) was applied on a glassy carbon electrode (GCE) for rotating disk voltammetry, and a KB-modified GCE (KB/GCE) was prepared according to the literature [9]. The projective surface area of the GCE was 0.071 cm². FoDH1 was immobilized on the KB/GCE by immersing the electrode in 40  $\mu$ L of an FoDH1 solution (50  $\mu$ M of FoDH1 solution in 100 mM potassium phosphate buffer (KPB) of pH 6) containing 0.5% (v/v) glutaraldehyde for 24 h at 4 °C. The bioelectrode is called FoDH1/KB/GCE.

#### 2.3. Preparation of FoDH1/PQ co-immobilized KB/GCEs

A PQ-modified KB/GCE (PQ/KB/GCE) was prepared by immersing the KB/GCE in DMSO containing 100 mM of PQ for 12 h at room temperature. After washing the electrode with 100 mM KPB (pH 7.0), FoDH1 was immobilized on the PQ/KB/GCE in a manner similar to that described in Section 2.2. The bioelectrode is called FoDH1/PQ/KB/GCE.

#### 2.4. Preparation of VP and FoDH1/VP co-immobilized KB/GCEs

N-(4-bromobutyl)-N'-methyl-4,4'-bipyridinium dibromide was synthesized according to the literature [10]. VP was prepared by dissolving N-(4-bromobutyl)-N'-methyl-4,4'-bipyridinium dibromide (1.1 g, 3 mmol) and PVP (0.5 g, 10  $\mu\text{mol}$ ) in 100 mL of DMF, and the solution was stirred for 4 d at 45 °C. The product (VP) was precipitated in diethyl ether and dried. 4  $\mu\text{L}$  of 100 mM KPB (pH 7.0) reaction solution containing 90 mg mL $^{-1}$  VP, 20 mg mL $^{-1}$  PEGDGE, and 18 mg mL $^{-1}$  FoDH1 was cast onto the surface of the KB/GCE. The electrode was dried at 4 °C for 3 h. The bioelectrode is called FoDH1/VP/KB/GCE.

#### 2.5. Electrochemical measurements

All electrochemical measurements were carried out in 1.0 M KPB at various pHs and at various temperatures under a complete argon atmosphere on an electrochemical analyzer BAS CV-50W. The working electrodes were rotated with a RDE-1 (BAS, USA). A homemade Ag/AgCl/sat.KCl electrode and a Pt-wire were used as the reference electrode and the counter electrode, respectively. All of the potentials are referred to the reference electrode in this paper.

#### 3. Results and discussion

#### 3.1. HCOO oxidation at FoDH1-modified KB/GCEs

Fig. 1A shows rotating disk cyclic voltammograms (RDVs) at FoDH1/ KB/GCEs in the presence of HCOO<sup>-</sup> and MV<sup>2+</sup>. The  $E_{\rm m,MV}$  was -0.63 V. The sigmoidal curves represent the catalytic oxidation of HCOO<sup>-</sup>, in which FoDH1 and MV<sup>2+</sup> work as a catalyst and a mediator, respectively. The catalytic current completely disappeared by HCl-treatment of the bioanode. The current reached the limiting value at potentials more positive than -0.45 V and the half-wave potential  $(E_{1/2})$  was -0.58 V, which is only 0.12 V more positive than  $E^{\circ}{}'_{CO2}$  (-0.70 V at pH 8.0 [11]). The  $j_{lim}$  value increased with the bulk concentration of  $MV^{2+}$  ( $c_{MV}$ ) in a manner of Michaelis Menten-type saturation curve (Fig. 1A, inset). The apparent Michaelis constant against MV<sup>2+</sup> was estimated to be 1.0  $\pm$  0.2 mM, the error being an asymptotic standard one in non-linear regression. The  $j_{lim}$  value was almost independent of the rotation rate ( $\omega$ ) at  $\omega$  > 600 rpm (Fig. 1B), indicating that  $j_{lim}$  is predominantly governed by the enzymatic kinetics. Under the conditions,  $j_{\rm lim}$  of the HCOO $^-$  oxidation reached 24  $\pm$  3 mA cm $^{-2}$  at 30 °C and at  $\omega = 1000 \text{ rpm } (\sqrt{\omega} = 10.23 \text{ s}^{-1/2}).$ 

When the solution temperature was increased up to 60 °C to improve the enzymatic kinetics,  $j_{\rm lim}$  showed a clear dependence on  $\omega$  and was enhanced to  $145 \pm 6$  mA cm $^{-2}$  at  $\omega = 6000$  rpm (Fig. 1C). This is the highest  $j_{\rm lim}$  reported so far for the HCOO $^-$  oxidation at enzymatic bioanodes. The inset in Fig. 1C shows the Koutecký–Levich plot based on: [12]

$$\frac{1}{j_{\text{lim}}} = \frac{1}{j_{\text{D}}} + \frac{1}{j_{\text{cat}}} \tag{1}$$

where  $j_{\rm D}$  is the Levich-type diffusion-controlled current density and  $j_{\rm cat}$  is the enzymatic kinetics-controlled current density. The non-linear regression analysis by Gnuplot® with Eq. (1) provided a result that  $j_{\rm cat}=294\pm52\,{\rm mA\,cm^{-2}}$  and  $j_{\rm D}/\omega^{1/2}=11\pm1\,{\rm mA\,s^{1/2}\,cm^{-2}}$ . The large value of  $j_{\rm cat}$  indicates that this FoDH1-based system is very useful for the HCOO $^-$  oxidation.

Since PQ is a better electron acceptor than the natural one (NAD<sup>+</sup>) from the kinetic viewpoint [6], we tried to use PQ as a mediator and prepared FoDH1/PQ/KB/GCEs to construct a useful bioelectrocatalytic system for the HCOO<sup>-</sup> oxidation. PQ adsorbed on a KB/GCE in a manner of Langmuir isotherm (data not shown). The absorbed PQ gave a pair of redox peaks (Fig. 2; b0) at  $E_{\rm m}=-0.20$  V. The electrodes produced large anodic currents of the catalytic oxidation of HCOO<sup>-</sup> (Fig. 2; b1, b2). The  $j_{\rm lim}$  value was almost independent of  $\omega$  at 30 °C, indicating the characteristics predominantly controlled by the enzymatic kinetics. The  $j_{\rm lim}$  that increased up to ca. 35 mA cm<sup>-2</sup> at 60 °C, however, is much smaller than that expected from the bimolecular rate constant (which is 1000 times larger than that of MV<sup>2+</sup> [6]), in spite of a rather large overpotential. Most probably, the restricted movement of the adsorbed PQ interferes with the enzymatic reaction between the adsorbed PQ and the immobilized FoDH1.

Although the MV<sup>2+</sup>-system shows very small overpotential, MV<sup>2+</sup> is very soluble and it is difficult to immobilize MV<sup>2+</sup> on electrodes. Therefore, we synthesized VP and immobilized it on KB/GCEs. The  $E_{\rm m,VP}$  was -0.52 V (Fig. 2; a0) and slightly more positive than  $E_{\rm m,MV}$ , probably due to the repulsion between the positive charges in the oxidized polymer. In the presence of HCOO<sup>-</sup>, the FoDH1/VP/KB/GCEs produced large anodic j (Fig. 2; a1, a2) comparable with that of FoDH1/PQ/KB/GCEs. The  $j_{\rm lim}$  value reached ca. 30 mA cm<sup>-2</sup> at 60 °C and at  $\omega=1000$  rpm. The  $E_{1/2}$  was -0.57 V and only 0.13 V more positive than  $E^{\rm o}{}'_{\rm CO2}$ . These results suggest that the VP-immobilized system can well mediate the electron transfer between the immobilized FoDH1 and the KB/GCE compared with the PQ-adsorbed system. Such a polymer system seems to retain some extent of the mobility, which is essential in MET-type bioelectrocatalysis. The flexibility seems to increase at

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