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Physical modelling and advanced simulations of gas-liquid two-phase jet flows in atomization and sprays

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ABSTRACT

This review attempts to summarize the physical models and advanced methods used in computational studies of gas-liquid two-phase jet flows encountered in atomization and spray processes. In traditional computational fluid dynamics (CFD) based on Reynolds-averaged Navier-Stokes (RANS) approach, physical modelling of atomization and sprays is an essential part of the two-phase flow computation. In more advanced CFD such as direct numerical simulation (DNS) and large-eddy simulation (LES), physical modelling of atomization and sprays is still inevitable. For multiphase flows, there is no model-free DNS since the interactions between different phases need to be modelled. DNS of multiphase flows based on the one-fluid formalism coupled with interface tracking algorithms seems to be a promising way forward, due to the advantageous lower costs compared with a multi-fluid approach. In LES of gas-liquid two-phase jet flows, subgrid-scale (SGS) models for complex multiphase flows are very immature. There is a lack of well-established SGS models to account for the interactions between the different phases. In this paper, physical modelling of atomization and sprays in the context of CFD is reviewed with modelling assumptions and limitations discussed. In addition, numerical methods used in advanced CFD of atomization and sprays are discussed, including high-order numerical schemes. Other relevant issues of modelling and simulation of atomization and sprays such as nozzle internal flow, dense spray, and multiscale modelling are also briefly reviewed.

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Contents

| 1. | Introduction | |
|----|---|--|
| 2. | Physical modelling of atomization and sprays | |
| | 2.1. The spray equation in the Lagrangian approach | |
| | 2.2. Liquid atomization modelling | |
| | 2.3. Droplet kinematics, droplet/droplet and spray/wall interactions, and liquid-fuel evaporation | |
| 3. | LES of spray flow and combustion | |
| | 3.1. Scale range separation, space filtering and mathematical formulation | |
| | 3.2. Subgrid-scale models and linear eddy mixing model for combustion | |
| | 3.3. Numerical issues for LES of spray flow and combustion | |
| 4. | . DNS-like simulations of gas-liquid two-phase flows for atomization and sprays | |
| | 4.1. Overview of multiphase flow modelling for a DNS-like simulation of atomization and sprays | |
| | 4.2. Interface tracking and reconstruction techniques | |
| | 4.2.1. VOF-type methods | |
| | 4.2.2. Level-set methods | |
| | 4.3. Modelling surface tension | |
| | 4.4. High-order numerical schemes for DNS of atomization and sprays | |
| 5. | . Other relevant issues of modelling and simulation of atomization and sprays | |

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| | 5.1. | Modelling nozzle internal flow, hollow-cone sprays, dense sprays, and electrohydrodynamic (EHD) atomization | . 159 |
|----|--------|---|-------|
| | 5.2. | Multiscale modelling of atomization and sprays | . 160 |
| 6. | Concl | uding remarks | 162 |
| | Refere | ences | . 164 |
| | | | |

| Nomenclature | | | Sherwood number |
|----------------------------|---|-----------------|---|
| | | t | time |
| а | parent droplet or blob radius | Т | Taylor parameter; gas temperature |
| Α | surface area | T_A | activation temperature |
| A_f, A_p | droplet/particle frontal area | T_d | droplet temperature |
| A_R | Arrhenius kinetics constant | Ťď | time rate of change of temperature |
| b | collision impact parameter | u | gas-phase velocity vector |
| b₽ | Arrhenius kinetics constant | U | gas velocity at the liquid surface |
| B_0, B_1 | "wave" breakup model constants | ν | particle velocity |
| BM | mass transfer number | v | droplet velocity vector |
| C C | specific heat | V | droplet volume: domain: diffusion velocity |
| C | constant | Vol | volume of the cell |
| Cn | drag coefficient | w | weighting |
| $C_{\rm D}$ | specific heats at constant pressure and volume | w | local relative velocity between the droplet and the |
| C_{p} | Smagorinsky constant | | surrounding gas $(\mathbf{v} - \mathbf{u})$ |
| | constants in the subgrid turbulent kinetic energy | W/ | molecular weight |
| C_{ν}, C_{ε} | equation | ۷۷ ۱۸/۶ | subgrid turbulence effects due to spray |
| d | particle cloud diameter | Wo | Wohor number |
| u D | diffusion coefficient: energy dissination rate: droplet | VVE | droplet position voctor |
| D | diameters distribution function | x | mole fraction, random number |
| Ð | uldifield, distribution function | л | nore fraction, faildoin fulfiber |
| D | | x_p | particle certificiti desplot transient le setion |
| e | specific total energy | X _i | dropiet transient location |
| E | error for stiene flavor service 1 | y V | droplet distortion from sphericity |
| J | function; flow variable | Y | mass fraction |
| J | arbitrary vector field | У | time rate of change of the droplet distortion |
| F | fuel; force | | (oscillation velocity) |
| F | force | <i>y</i> | time rate of change of oscillation velocity |
| g C | specific body force (gravitational acceleration) | Ζ | Ohnesorge number |
| h | heat flux: heat transfer coefficient: grid size | Greek | |
| h _u s | evaporated enthalpy at droplet surface | α | (laminar) thermal diffusivity: linking parameter: |
| H | heaviside function | | droplet variable |
| I | specific internal energy: indicator function | в | heat transfer correction coefficient |
| k | turbulent kinetic energy | Ŷ | molar fraction |
| k _P | reaction rate | δ | Kronecker delta function |
| 1 | eddy size | δ | smoothed delta function |
| L | large (integral) length scale | Δ | incremental amount |
| L., | latent heat for vaporization | _ ∇ | gradient operator |
| 2 v m | mass | ۶ | dissipation rate of turbulent kinetic energy |
| mn | unit normal vector | ~ | drop radius ratio (r_1/r_2) ; ratio of specific heats |
| n N | number | Γ | Fickian diffusion coefficient: interface |
| Nu | Nusselt number | n _v | Kolmogorov scale |
| 0 | oxidizer | ηκ κ | von Karman constant: curvature |
| n | probability | A | diffusive mass flux |
| Р D | product: probability density function: weighted | 2 | frequency of subgrid stirring: thermal conductivity |
| 1 | projection | 1 | wavelength |
| Dr | Projection Prondtl number | 21 | dynamic viscosity |
| ri a | random number between (0, 1): random scalar | μ | kinomatic viscosity |
| y O | hand transfer rate, storage locations | V | |
| Ų Ċ | heat release source form | ^v 12 | donsity |
| ų " | droplot radius | μ σ | uensity |
| ľ D | utopiet faulus | 0 П | surface tension |
| К D D | contribution and vanor and constants | | velocity-pressure gradient correlation |
| K_c, K_v | carrier gas and vapor gas constants | | VISCOUS WOIK |
| ке | keynolds number | τ | Dreakup time; wall snear stress; time scale |
| S C- | strain rate tensor; source term; surface area | φ | area nux |
| SC | Schiniat number | Ψ | species mass flux; volume fraction |

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