



# Development of extended release multiple unit effervescent floating drug delivery systems for drugs with different solubilities



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## ABSTRACT

The purpose of this study was preparation and evaluation of extended release multiple unit floating drug delivery systems based on CO<sub>2</sub> formation with rapid and extended floating and good control over the release for drugs with different solubilities. The pellet systems were prepared by fluidized bed layering/coating techniques and evaluated by floating, drug release, medium uptake and swelling studies in 0.1 N HCl. Two different pellet systems were evaluated; the first consisted of drug-layered sugar cores, NaHCO<sub>3</sub>-layer and a polymeric top-coating, which ideally controlled both floating and release properties. The second, modified system consisted of drug-containing Eudragit® RS 30 D coated extended release pellets coated with NaHCO<sub>3</sub>-layer and Eudragit® RL 30 D top-coating. The Eudragit® RL coating resulted in sufficient medium penetration, a prerequisite for CO<sub>2</sub> formation, and in high CO<sub>2</sub> entrapment efficiency. Floating was maintained over a wide range of Eudragit® RL/RS combinations. Extended release from the first system could be achieved only for low solubility, high dose drugs because of high Eudragit® RL permeability. For high solubility drugs, separating floating and release “functions” was successful. Extended release pellets were used to achieve better drug release control, while floating was achieved by an Eudragit® RL top-coat.

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## 1. Introduction

Gastroretentive dosage forms are interesting extended release delivery systems for drugs with a narrow window of absorption in the upper intestine, for drugs with pH-dependent solubility [12], for drugs degraded by higher pH intestinal fluids [2,24] or for drugs with local action in the proximal part of the GI tract, such as antibiotic administration for *Helicobacter pylori* in the treatment of peptic ulcer [16,26].

Several approaches to prolong gastric retention have been investigated: Magnetic systems [8], high density systems [18], mucoadhesive systems [4], swelling [6,19] and expanding systems [14] as well as floating systems [1,21].

Floating systems are either based on an inherently low density or on effervescence. Non-effervescent systems have their inherent low density due to the entrapment of air, as with low density hollow microspheres [2,13], incorporation of low density material (sponges) [21] or due to swelling [7,20]. In contrast, effervescent

systems, have an initially high density, which decreases upon contact with the acidic environment due to CO<sub>2</sub> formation [11].

Besides frequently investigated single unit dosage forms, which have a high variability in GI transit time due to their all-or-nothing emptying process [22], multiple unit floating systems have been developed to overcome this problem due to their more uniform emptying from the stomach [5], as well as reducing the risk of dose dumping [10]. Multiple unit effervescent systems utilizing ion exchange resins beads [1], matrix minitablets [9], as well as extruded-spherized pellets [23] have been previously developed.

In the present study, floating reservoir-type pellets based on CO<sub>2</sub> formation were developed for drugs with different solubilities, characterized in vitro and their stability under various conditions was evaluated.

## 2. Materials and methods

### 2.1. Materials

Non-pareils 710–850 μm (Suglets sugar spheres NF, NP Pharm S.A., Bazainville, France), propranolol HCl, theophylline anhydrous (BASF SE, Ludwigshafen, Germany) and micronized carbamazepine

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(Fabrica Italiana Sintetici, Alto de Monte Vecchio, Italy) as model drugs, sodium hydrogen carbonate ( $\text{NaHCO}_3$ ) (Merck KGaA, Darmstadt, Germany) as effervescent agent, polyvinyl acetate aqueous dispersion (Kollicoat<sup>®</sup> SR 30 D; BASF AG, Ludwigshafen, Germany), methacrylic copolymers with varying ratios of trimethylammonioethyl methacrylate as functional group, Type A and B (Eudragit<sup>®</sup> RL 30 D and Eudragit<sup>®</sup> RS 30 D respectively; Evonik Industries AG, Darmstadt, Germany), triethyl citrate (TEC) (Morflex, Greensboro, NC, USA), talc (Luzenac Europe, Toulouse, France), hydroxypropyl methylcellulose (HPMC) (Methocel E5; Colorcon, Orpington, UK), polyethylene glycol 6000 (Lutrol E 6000, BASF AG, Ludwigshafen, Germany), and silicon dioxide (Aerosil 200; Evonik Industries AG, Darmstadt, Germany) were used as received. All other reagents were of analytical grade and were used without further purification.

## 2.2. Preparation of pellets

### 2.2.1. Preparation of the three-layer pellet system

Drug loaded pellets were prepared by layering drug suspensions in isopropyl alcohol: water (88: 12 w/w) for carbamazepine and theophylline and solution in ethanol: water (70: 30 w/w) for propranolol HCl using HPMC E5 as binder (10%, w/w, based on drug) onto sugar pellets in a fluidized bed coater GPCG1 (Glatt Process Technology GmbH, Binzen, Germany) to achieve a 10% (for all drugs) or 50% (for carbamazepine) drug content based on the initial pellet weight. The layering conditions were, batch size: 900 g, inlet temperature: 38–44 °C (carbamazepine), 32–36 °C (theophylline) and 42–46 °C (propranolol HCl); product temperature: 32–36 °C (carbamazepine), 30–32 °C (theophylline) and 38–42 °C (propranolol HCl); air flow: 80–90 m<sup>3</sup>/h; nozzle diameter: 1.2 mm; spray pressure: 1.2 bar; spray rate: 9–12 g/min (carbamazepine), 8–10 g/min (theophylline and propranolol HCl); final drying at 40 °C for 15 min.

The drug-loaded pellets were coated with  $\text{NaHCO}_3$ , as the gas-generating agent, suspended in aqueous HPMC solution, which was plasticized with Lutrol E 6000 (10%, w/w, based on the solids content of HPMC). The ratio of  $\text{NaHCO}_3$  to HPMC was 2:8 w/w, the solids content of the coating suspension was kept constant at 12% w/w and coating was performed in a fluidized bed coater, Glatt GPCG-1 to a weight gain of 15%. The layering conditions were: batch size: 900 g; inlet temperature: 44–48 °C; product temperature: 36–40 °C; air flow: 80–90 m<sup>3</sup>/h; nozzle diameter 1.2 mm; spray pressure: 1.2 bar; spray rate: 6–6.5 g/min and final drying at 40 °C for 15 min.

As top-coat, Eudragit<sup>®</sup> RL 30 D, RS 30 D or Kollicoat<sup>®</sup> SR 30 D were coated from an aqueous polymer dispersion, plasticized with 20% TEC (w/w, based on the total dry polymer weight of Eudragit<sup>®</sup> RL 30 D and Eudragit<sup>®</sup> RS 30 D and their combination) or 10% TEC (w/w, based on the dry Kollicoat<sup>®</sup> SR 30 D weight). 35% Talc (w/w, based on polymer content) was used as antitacking agent. The polymer content was adjusted to 15% (w/w) with purified water and the coating was done in a fluidized bed coater Mini Glatt (Glatt GmbH, Binzen, Germany) to a weight gain of 10–20% (w/w). The coating conditions were: batch size: 100 g; inlet temperature: 32–34 °C (Eudragit<sup>®</sup> RL 30 D; RS 30 D) and 34–38 °C (Kollicoat<sup>®</sup> SR 30 D); product temperature: 28–30 °C; air flow: 0.2 bar; nozzle diameter 0.5 mm; spray pressure: 0.9 bar; spray rate: 1 g/min and final drying at 40 °C for 15 min. 1% Aerosil was added to the coated pellets, which were oven-cured at 60 °C directly after the coating step using dry heat, with no controlled humidity for 2 h (Table 1). The samples were put into a desiccator until further tested.

### 2.2.2. Preparation of the modified multiple unit drug delivery system

Propranolol HCl loaded pellets were prepared by layering drug-

binder solution in ethanol: water (70: 30, w/w) using HPMC E5 as binder (10%, w/w, based on drug) onto drug free sugar pellets in a fluidized bed coater GPCG1 (Glatt Process Technology GmbH, Binzen, Germany) to achieve a 10% drug content based on the initial pellet weight. The layering conditions were, batch size: 900 g, inlet temperature: 42–46 °C; product temperature: 38–42 °C; air flow: 80–90 m<sup>3</sup>/h; nozzle diameter: 1.2 mm; spray pressure: 1.2 bar; spray rate: 8–10 g/min; and final drying at 40 °C for 15 min (Table 2).

The propranolol HCl loaded pellets were further coated with an aqueous colloidal polymeric dispersion of Eudragit<sup>®</sup> RS 30 D in a fluidized bed coater Glatt GPCG-1 to a predetermined weight gain. The dispersion was plasticized with 20% TEC (w/w, based on the dry Eudragit<sup>®</sup> RS 30 D weight). 35% Talc (w/w based on the dry polymer weight) was used as antitacking agent. The polymer content was adjusted to 15% (w/w) with purified water. The coating conditions were batch size: 900 g, inlet temperature: 38–42 °C, product temperature: 30–34 °C, air flow: 70–80 m<sup>3</sup>/h, nozzle diameter 1.2 mm, spray pressure: 1.2 bar, spray rate: 8–10 g/min and final drying at 40 °C for 15 min. Samples of the coated pellets were oven-cured directly at 60 °C after the coating step using dry heat, with no controlled humidity for 2 h, after adding 1% Aerosil and put into a desiccator until further tested.

The extended release uncured pellets were further coated with  $\text{NaHCO}_3$  (15 or 20%, w/w, based on the initial pellet weight) and finally with Eudragit<sup>®</sup> RL 30 D (to a predetermined weight gain) as top-coat, using the same procedure as previously mentioned. 1% Aerosil was added to the coated pellets, which were oven-cured at 60 °C for 2 h directly after the coating step (Table 2). The samples were put into a desiccator until further tested.

## 2.3. Floating properties

The floating abilities of the pellets was determined in 50 ml prewarmed 0.1 N HCl or deionized water at 70 rpm,  $37 \pm 0.2$  °C for 18 h, using a shaker apparatus (GFL shaking incubator 3033; GFL GmbH, Burgwedel, Germany) ( $n = 2$ ). One hundred pellets ( $n_{\text{initial}}$ ) were placed in the medium; the number of floating pellets ( $n_t$ ) over the tested time range was measured by visual observation. The percentage of floating pellets was calculated as follows:

$$\text{Floating pellets(\%)} = \frac{n_t}{n_{\text{initial}}} * 100$$

Alternatively, the floating lag time (time at which all pellets started floating) and the% floating pellets at 18 h was determined.

## 2.4. Drug release

The drug release was investigated in a USP paddle apparatus (VK 700, Vankel Industries, Edison, NJ, USA), 900 ml of 0.1 N HCl, deionized water, deionized water + 0.01 N  $\text{NaHCO}_3$  or + 0.1 N  $\text{NaHCO}_3$  (100 rpm, 37 °C,  $n = 3$ ). The weight of pellets used was equivalent to about 50 mg of propranolol HCl, and 20 mg for theophylline and carbamazepine. At predetermined time intervals, 3 ml samples were withdrawn and analyzed with UV spectrophotometry (UV-2101 PC, Shimadzu Scientific Instruments, Columbia, MD, USA), propranolol HCl,  $\lambda = 290$  nm; theophylline,  $\lambda = 270$  nm and carbamazepine,  $\lambda = 283$  nm.

## 2.5. Medium uptake and mass loss of pellets

One hundred pellets were weighed ( $\text{weight}_{\text{initial}}$ ), put into 50 ml prewarmed 0.1 N HCl, and shaken at  $37 \pm 0.2$  °C, 70 rpm for 18 h, using a shaker apparatus (GFL shaking incubator 3033; GFL GmbH,

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