

Available online at www.sciencedirect.com



Journal of Biotechnology 125 (2006) 252-268

Journal of BIOTECHNOLOGY

www.elsevier.com/locate/jbiotec

Constant specific growth rate in fed-batch cultivation of *Bordetella pertussis* using adaptive control

Z.I.T.A. Soons^{a,b,*}, J.A. Voogt^a, G. van Straten^a, A.J.B. van Boxtel^a

^a Wageningen University, Agrotechnology and Food Sciences, Systems and Control Group, P.O. Box 17, 6700 AA Wageningen, The Netherlands
 ^b Netherlands Vaccine Institute, Antonie van Leeuwenhoeklaan 9-11, P.O. Box 457, 3720 AL Bilthoven, The Netherlands

Received 3 August 2005; received in revised form 8 February 2006; accepted 3 March 2006

Abstract

Monitoring and control of production processes for biopharmaceuticals have become standard requirements to support consistency and quality. In this paper, a constant specific growth rate in fed-batch cultivation of *Bordetella pertussis* is achieved by a newly designed specific growth rate controller.

The performance of standard control methods is limited because of the time-varying characteristics due to the exponentially increasing biomass and volume. To cope with the changing dynamics, a stable model reference adaptive controller is designed which adapts the controller settings as volume and biomass increase. An important asset of the design is that dissolved oxygen is the only required online measurement.

An original design without considering the dissolved oxygen dynamics resulted experimentally in oscillatory behaviour. Hence, in contrast to common believes, it is essential to include dissolved oxygen dynamics. The robustness of this novel design was tested in simulation.

The validity of the design was confirmed by laboratory experiments for small-scale production of *B. pertussis*. The controller was able to regulate the specific growth rate at the desired set point, even during a long fed-batch cultivation time with exponentially increasing demands for substrates and oxygen.

© 2006 Elsevier B.V. All rights reserved.

Keywords: Model-reference adaptive control; Biopharmaceuticals; Fed-batch cultivation; Specific growth rate; Dissolved oxygen; Bordetella pertussis

1. Introduction

* Corresponding author. Tel.: +31 30 274 2066; fax: +31 30 274 4426.

E-mail address: zita.soons@wur.nl (Z.I.T.A. Soons).

Monitoring and control of production processes for biopharmaceuticals have become standard requirements to support consistency and quality. Recently, FDA encourages with its view on process analytical

^{0168-1656/\$ -} see front matter © 2006 Elsevier B.V. All rights reserved. doi:10.1016/j.jbiotec.2006.03.005

a, b, c, d constants for dual substrate model of		
G	Bordetella pertussis	
C	nominal value of controller (mmol l^{-1})	
C_{G}	glutamate concentration (mmol l^{-1})	
$C_{\rm G0}$	initial glutamate concentration	
	$(\text{mmol } l^{-1})$	
$C_{\rm L}$	lactate concentration (mmol l^{-1})	
$C_{ m L0}$	initial lactate concentration (mmol l^{-1})	
C_{X}	biomass concentration (OD)	
$C_{\rm X0}$	initial biomass concentration (OD)	
$\hat{C}_{\mathbf{X}}$	software sensor biomass concentration	
21	(OD)	
$C_{\rm G}^{\rm in}$	glutamate concentration in the feed	
υG	$(\text{mmol } l^{-1})$	
$C_{ m L}^{ m in}$	lactate concentration in the feed	
c_{L}	$(\text{mmol}l^{-1})$	
DO	dissolved oxygen, oxygen concentration	
DO	in the medium (mmol l^{-1})	
DO		
DO _{set}	set point for oxygen concentration in the $11-1$	
DO	medium (mmol l^{-1})	
DO _{senso}	or oxygen concentration measured by the	
_	sensor (mmol l^{-1})	
Ε	objective function	
$E_{\rm DO}$	relative variation of DO	
E_{μ}	relative variation of μ	
f _G	Monod kinetics for glutamate	
$f_{\rm L}$	Monod kinetics for lactate	
F_{O_2}	(enriched) airflow through the	
	headspace $(l h^{-1})$	
F_1	"proportional" correction substrate feed	
	rate $(l h^{-1})$	
F_2	feed rate by prior calculation $(1h^{-1})$	
$\bar{F_3}$	integral correction substrate feed rate	
5	$(1h^{-1})$	
$F_{G+L}^{in} F_{tot}$ total substrate feed rate (glutamate		
- G+L- G	+ lactate) $(l h^{-1})$	
ISE	integral squared error (h^{-1})	
$k_{\rm L}a$	oxygen transfer coefficient (h^{-1})	
$K_{\rm C}$	gain for dissolved oxygen control	
K _G	Monod constant on glutamate	
nG	$(\text{mmol}l^{-1})$	
K.	Monod constant on lactate $(mmol l^{-1})$	
$K_{\rm L}$		
K_1, K_2	gains for specific growth rate control	
$K_{\rm C}^{\rm h}$	gain for headspace control	
LPS	lipopolysaccharide	

$m_{\rm G}$	maintenance coefficient on glutamate
	$(\text{mmol OD}^{-1} \text{h}^{-1})$
$m_{\rm L}$	maintenance coefficient on lactate
	$(\text{mmol}\text{OD}^{-1}\text{h}^{-1})$
$m_{\rm O}$	maintenance coefficient on oxygen $(\text{mmol OD}^{-1} \text{ h}^{-1})$
Oa	
O_2^a	auxiliary oxygen concentration $(\text{mmol } l^{-1})$
O_2^h	oygen concentration in the headspace
O_2	$(\text{mmol}1^{-1})$
O_2^{in}	oygen concentration in the incoming air
02	$(\text{mmol}l^{-1})$
OD	optical density at 590 nm (OD_{590} ml ⁻¹)
OTR	oxygen transfer rate (mmol $l^{-1} h^{-1}$)
OUR	oxygen uptake rate (mmol $l^{-1} h^{-1}$)
OUR _{no}	
	$(\text{mmol } l^{-1} h^{-1})$
PRN	Pertactin
rpm	rounds per minute
t	cultivation time (h)
v, w	constants for normalised Monod
	equations
\hat{V}	liquid volume (l)
Ŷ	software sensor liquid volume (l)
$V_{\rm h}$	volume of the headspace (l)
$Y_{\rm G1}$	yield on glutamate over pathway 1 (OD mmol ^{-1})
$Y_{\rm G2}$	yield on glutamate over pathway
I G2	$2 (OD \text{ mmol}^{-1})$
$Y_{\rm L}$	yield on lactate (OD mmol ^{-1})
Y_0	yield on oxygen (OD mmol ^{-1})
-0	,,gen (or,
Greek l	
β	ratio between normalised Monod equa-
	tions
β_1, β_2	convergence speed of reference model
γ_1, γ_2	tuning parameters for MRAC
μ	specific growth rate (h^{-1})
μ̂	software sensor specific growth rate (h^{-1})
$\mu_{ m enh}$	enhanced specific growth rate (h^{-1})
μ_{\max}	maximum specific growth rate (h^{-1})
$\mu_{ m set}$	set point specific growth rate (h^{-1})
$\hat{\mu}_0$	initial software sensor specific growth
	rate (h^{-1})

Download English Version:

https://daneshyari.com/en/article/25750

Download Persian Version:

https://daneshyari.com/article/25750

Daneshyari.com