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Effect of supply/exhaust diffuser configurations on the contaminant distribution in ultra clean environments: Eulerian and Lagrangian approaches

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ABSTRACT

In this research, the airflow pattern and particle dispersion in a contaminated full-scale cleanroom are investigated numerically using both Eulerian and Lagrangian approaches. Three different supply diffuser configurations namely (1) central, (2) horizontal and (3) vertical and three different exhaust grille configurations namely (4) vertical symmetric, (5) asymmetric and (6) horizontal symmetric are selected for the analysis. The presented results reveal that the supply/exhaust openings arrangement has a significant influence on the particulate contaminant dispersion in the cleanrooms. The comparison of the above different supply diffuser configurations shows that the vertical and horizontal supply diffuser configurations lead to a more escaped particles and less deposited particles on the room walls and installed working table in the room than the central one. It is also found that for different exhaust grille arrangements, the performance of the ventilation system in the horizontal symmetric case is higher than asymmetric and vertical symmetric ones. At the same time, it is observed that the variations of contaminant concentration in both Eulerian and Lagrangian approaches are almost the same. The results of the velocity and particle concentration show good agreement with the available experimental data in the literature.

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1. Introduction

Indoor air quality (IAQ) is crucial for both human health and manufacturing processes. In many industries such as pharmaceutical, food processing, biotech, aerospace, optics, microelectronics and operating rooms, particulate contamination has a significant effect on IAQ. In recent decades, cleanrooms have been extensively used to decrease particulate contamination, as well as to control other environmental parameters such as temperature, humidity and pressure to provide an appropriate comfort level [1,2]. Better dilution of dispersed contaminant from cleanrooms is a fundamental factor for the cleanroom ventilation system design. The dispersion of the contaminant directly depends on the type of airborne particles and the airflow pattern within the cleanrooms. The airborne particles are transported with a large volume of air that enters from supply diffusers and away from critical zones such as working table. The airflow pattern and the turbulence

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http://dx.doi.org/10.1016/j.enbuild.2016.06.028 0378-7788/© 2016 Elsevier B.V. All rights reserved. can be the most efficacious factor on particle transportation [3]. Therefore, based on the cleanroom flow field, the investigation of airborne contaminant concentration and developing a new method to reduce this effect is essential.

Since the 90s, with significant improvement in the computational capacity, computational fluid dynamics (CFD) has become a powerful and efficient tool to study engineering problems including airflow and airborne contaminant distribution in enclosures. It is known that there are two main particle transport approaches in CFD simulations: (1) the Eulerian-Eulerian (E-E), and (2) the Eulerian-Lagrangian (E-L) approach. Considering computational cost, the E-L approach is more suitable for particle concentration modeling for transient state whereas for steady state, the E-E approach simulates concentration in less computational time than E-L approach [4]. Several investigations have been made to explore the effect of different factors that influence the contaminant concentration in cleanrooms with two aforementioned approaches. The main factors such as airflow pattern, particle characteristics, the location of obstacles [5], contaminant source location [4–6], supply/exhaust openings arrangement [7–9] are reported in the literature.







Nomenclature

Ahhrevia	tions
CED	Computational fluid dynamics
	Discrete rendem wells
E-E	Eulerian-Eulerian
E-L	Eulerian-Lagrangian
IAQ	Indoor air quality
RANS	Reynolds averaged Navier-Stokes
RNG	Renormalization group
LIDE	User defined function
ODI	oser denned function
Crook sw	mbols
GIEEKSyl	Energy discipation rate
ε	Ellergy dissipation fale
ρ	Density of the fluid
$ ho_p$	Density of the particle
μ_{eff}	Air effective viscosity
μ_1	Laminar viscosity
μ _t	Turbulent viscosity
τ	Particle relaxation time
τ^*	Dimensionless time
τ	Particle eddy crossing time
•c	Lifetime of the turbulent energy
le	
λ	Mean free path
η	Ratio of turbulent to mean strain time scale
$\sigma_k, \sigma_{arepsilon}$	Model constants in the RNG k- ε model
β	Volumetric expansion coefficient
Subscript	ts
i.i	Spatial coordinates
in	Inlet
I	Lagrangian
L D	Lagialigiali
P	Particle
1	
Latin syn	ndois
A _{in}	Inlet area
Cc	Cunningham slip correction factor
C_{1}	
$c_{1\varepsilon}, c_{2\varepsilon}$	Model constants in the RNG k- $arepsilon$ model
$C_{1\varepsilon}, C_{2\varepsilon}$ C_{μ}	Model constants in the RNG k-ε model Model constant in the RNG k-ε model
$C_{1\varepsilon}, C_{2\varepsilon}$ C_{μ} c	Model constants in the RNG k-ε model Model constant in the RNG k-ε model Contaminant concentration
$C_{1\varepsilon}, C_{2\varepsilon}$ C_{μ} C_{i}	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell
$C_{1\varepsilon}, C_{2\varepsilon}$ C_{μ} C_{j} D	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate
$C_{1\varepsilon}, C_{2\varepsilon}$ C_{μ} C_{j} D d	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter
$C_{1\varepsilon}, C_{2\varepsilon}$ C_{μ} C_{j} D d_{p} d_{t}	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Darticle regidence time
$C_{1\varepsilon}, C_{2\varepsilon}$ C_{μ} C_{j} D d_{p} $dt_{(i,j)}$	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time
$C_{1\varepsilon}, C_{2\varepsilon}$ C_{μ} C_{j} D d_{p} $dt_{(i,j)}$ F_{a}	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces
$C_{1\varepsilon}, C_{2\varepsilon}$ C_{μ} C_{j} D d_{p} $dt_{(i,j)}$ F_{a} G	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number
$C_{1\varepsilon}, C_{2\varepsilon}$ C_{μ} C_{j} D d_{p} $dt_{(i,j)}$ F_{a} G g_{i}	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction
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$C_{1\varepsilon}, C_{2\varepsilon}$ C_{μ} C_{j} D d_{p} $dt_{(i,j)}$ F_{a} G g_{i} k Kn	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number
C_{1e}, C_{2e} C_{μ} C_{j} D d_{p} $dt_{(i,j)}$ F_{a} G g_{i} k Kn L_{e}	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number Eddy length scale
C_{1e}, C_{2e} C_{μ} C_{j} D d_{p} $dt_{(i,j)}$ F_{a} G g_{i} k Kn L_{e} \dot{M}	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number Eddy length scale Flow rate
C_{1e}, C_{2e} C_{μ} C_{j} D d_{p} $dt_{(i,j)}$ F_{a} G g_{i} k Kn L_{e} \dot{M} p	Model constants in the RNG k-ε model Model constant in the RNG k-ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number Eddy length scale Flow rate
C_{1e}, C_{2e} C_{μ} C_{j} D d_{p} $dt_{(i,j)}$ F_{a} G g_{i} k Kn L_{e} \dot{M} P P	Model constants in the RNG k-ε model Model constant in the RNG k-ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number Eddy length scale Flow rate Turbulent energy production rate
C_{1e}, C_{2e} C_{μ} C_{j} D d_{p} $dt_{(i,j)}$ F_{a} G g_{i} k Kn L_{e} \dot{M} P p	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number Eddy length scale Flow rate Turbulent energy production rate Pressure
C_{1e}, C_{2e} C_{μ} C_{j} D d_{p} $dt_{(i,j)}$ F_{a} G g_{i} k Kn L_{e} \dot{M} P p S	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number Eddy length scale Flow rate Turbulent energy production rate Pressure Particle to fluid density ratio
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c_{1e}, c_{2e} C_{μ} c c_{j} D d_{p} $dt_{(i,j)}$ F_{a} G g_{i} k Kn L_{e} \dot{M} P p S Sc_{t} T_{L}	Model constants in the RNG k-ε modelModel constant in the RNG k-ε modelContaminant concentrationMean particle concentration in a cellMolecular diffusion rateParticle diameterParticle residence timeAdditional forcesGaussian random numberGravitational constant in <i>i</i> directionTurbulent kinetic energyKnudsen numberEddy length scaleFlow rateTurbulent energy production ratePressureParticle to fluid density ratioSchmidt numberTurbulent lagrangian time scale
c_{1e}, c_{2e} C_{μ} c c_{j} D d_{p} $dt_{(i,j)}$ F_{a} G g_{i} k Kn L_{e} \dot{M} P p S Sc_{t} T_{L} t	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number Eddy length scale Flow rate Turbulent energy production rate Pressure Particle to fluid density ratio Schmidt number Turbulent lagrangian time scale Time
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C_{1e}, C_{2e} C_{μ} C_{μ} C_{j} D d_{p} $d_{(i,j)}$ F_{a} G g_{i} k Kn L_{e} \dot{M} P p S Sc_{t} T_{L} t U_{in} u_{i}	Model constants in the RNG k-ε modelModel constant in the RNG k-ε modelContaminant concentrationMean particle concentration in a cellMolecular diffusion rateParticle diameterParticle residence timeAdditional forcesGaussian random numberGravitational constant in <i>i</i> directionTurbulent kinetic energyKnudsen numberEddy length scaleFlow rateTurbulent energy production ratePressureParticle to fluid density ratioSchmidt numberTurbulent lagrangian time scaleTimeInlet velocityFluid mean velocity components
C_{1e}, C_{2e} C_{μ} C_{μ} C_{j} D d_{p} $d_{(i,j)}$ F_{a} G g_{i} k Kn L_{e} \dot{M} P p S Sc_{t} T_{L} t U_{in} u_{i} u_{P}^{P}	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number Eddy length scale Flow rate Turbulent energy production rate Pressure Particle to fluid density ratio Schmidt number Turbulent lagrangian time scale Time Inlet velocity Fluid mean velocity components Particles velocity components
C_{1e}, C_{2e} C_{μ} C_{j} D d_{p} $d_{t(i,j)}$ F_{a} G g_{i} k Kn L_{e} \dot{M} P p S Sc_{t} T_{L} U u_{i} u_{i}^{p} u' u'	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number Eddy length scale Flow rate Turbulent energy production rate Pressure Particle to fluid density ratio Schmidt number Turbulent lagrangian time scale Time Inlet velocity Fluid mean velocity components Particles velocity components
C_{1e}, C_{2e} C_{μ} C_{j} D d_{p} $dt_{(i,j)}$ F_{a} G g_{i} k Kn L_{e} \dot{M} P p S Sc_{t} T_{L} t U_{in} u_{i} u_{i} V	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number Eddy length scale Flow rate Turbulent energy production rate Pressure Particle to fluid density ratio Schmidt number Turbulent lagrangian time scale Time Inlet velocity Fluid mean velocity components Particles velocity components Turbulent fluctuating velocity components
C_{1e}, C_{2e} C_{μ} C_{j} D d_{p} $d_{t_{(i,j)}}$ F_{a} G g_{i} k Kn L_{e} \dot{M} P p S Sc_{t} T_{L} t U_{in} u_{i} u_{i}^{P} V V	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number Eddy length scale Flow rate Turbulent energy production rate Pressure Particle to fluid density ratio Schmidt number Turbulent lagrangian time scale Time Inlet velocity Fluid mean velocity components Particles velocity components Turbulent fluctuating velocity components Cleanroom volume
C_{1e}, C_{2e} C_{μ} C_{j} D d_{p} $d_{(i,j)}$ F_{a} G g_{i} k Kn L_{e} \dot{M} P p S Sc_{t} T_{L} t U_{in} u_{i} u_{i}^{P} V V_{j}	Model constants in the RNG k- ε model Model constant in the RNG k- ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number Eddy length scale Flow rate Turbulent energy production rate Pressure Particle to fluid density ratio Schmidt number Turbulent lagrangian time scale Time Inlet velocity Fluid mean velocity components Particles velocity components Turbulent fluctuating velocity components Cleanroom volume Volume of a computational cell
C_{1e}, C_{2e} C_{μ} C_{μ} C_{j} D d_{p} $d_{t_{(i,j)}}$ F_{a} G g_{i} k Kn L_{e} \dot{M} P p p S Sc_{t} T_{L} t U_{in} u_{i} u_{i}^{P} V V_{j} x, y, z	Model constants in the RNG k-ε model Model constant in the RNG k-ε model Contaminant concentration Mean particle concentration in a cell Molecular diffusion rate Particle diameter Particle residence time Additional forces Gaussian random number Gravitational constant in <i>i</i> direction Turbulent kinetic energy Knudsen number Eddy length scale Flow rate Turbulent energy production rate Pressure Particle to fluid density ratio Schmidt number Turbulent lagrangian time scale Time Inlet velocity Fluid mean velocity components Particles velocity components Turbulent fluctuating velocity components Cleanroom volume Volume of a computational cell Rectilinear orthogonal coordinates

One of the main parameters which may impact the contaminant concentration, especially in ultra-clean environments, is the configurations of supply and exhaust diffusers [10]. Zhao et al. [11] numerically studied the aerosol particle concentration and deposition in displacement and mixing ventilation rooms. Their results showed that a displacement-ventilated room had a lower particle deposition rate and larger escaped particle mass than the mixing one, while the average particle concentration of displacement case was higher than the mixing case. Sadrizadeh et al. [12] investigated the effectiveness of vertical and horizontal ventilation system on the particle distribution in the surgical zone. They found that the preferred selection between vertical and horizontal ventilation scenario in an operating room was highly dependent on internal constellation of obstacles, work practice, and the supply airflow rate.

Although, some researchers have studied the particle movement, deposition and distribution in indoor airflow, few investigations have been found in the literature to explore the effectiveness of different supply/exhaust configurations in reducing contaminant in the cleanroom.

In the present paper, the effect of supply diffuser and exhaust grille configurations on the contaminant transport in cleanrooms is studied numerically using both E-E and E-L approaches. To compare the contaminant distribution, particles are supposed to be uniformly distributed in the model cleanroom and the ventilation system removes contaminant from the model room. The following questions will be investigated:

- 1) What is the effect of different supply/exhaust opening arrangements on the contaminant distribution in a model cleanroom?
- 2) Which configuration has better effectiveness to discharge contaminant from the cleanroom? Is there any significant difference between the percentages of escaped and deposited particles for different configurations?
- 3) Is there difference between E-E and E-L approaches to predict the contaminant concentration distribution for a model cleanroom?

The goal of this study is to provide detailed knowledge and engineering guidelines for better design in future cleanrooms.

2. Analysis of numerical method

This investigation compares the two modeling approaches with an emphasis on their performance of predicting particle concentration distributions in ventilated spaces. Both the E-E and E-L models under examination are performed based on the same airflow field calculated by solving the Reynolds Averaged Navier–Stokes (RANS) equations with the Renormalization Group (RNG) $k - \varepsilon$ turbulence model.

2.1. Flow model

2.1.1. Governing equations

As the contaminant concentration in cleanrooms is very low, the airflow hydrodynamics is not affected by the contaminant phase. Therefore the interaction between continuous airflow phase and particle discrete phase are treated as one-way coupling [4]. Considering Boussinesq's turbulent viscosity hypothesis [13], the flow governing equations are as follows [14]:

Continuity equation:

$$u_{i,i} = 0$$

where u_i are the mean velocity components.

(1)

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