



Dehydration of 1,4-butanediol over supported rare earth oxide catalysts

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ABSTRACT

Vapor-phase catalytic dehydration of 1,4-butanediol was investigated over rare earth oxides supported on ZrO₂. In the dehydration of 1,4-butanediol, 3-buten-1-ol was mainly produced, together with tetrahydrofuran (THF) and γ -butyrolactone. The heavy group of rare earth oxides, such as Dy₂O₃, Ho₂O₃, Er₂O₃, Tm₂O₃, Yb₂O₃, and Lu₂O₃, supported on monoclinic ZrO₂ showed higher selectivity to 3-buten-1-ol than pure monoclinic ZrO₂ and supported light rare earth oxides, such as La₂O₃ and Pr₆O₁₁. Supported Yb₂O₃ catalysts dispersed on other oxides, such as alumina, silica, and tetragonal ZrO₂ catalyze the formation of THF. X-ray diffraction (XRD) measurements reveal that cubic Yb₂O₃ crystallites dispersed on monoclinic ZrO₂ provide active sites in the dehydration of 1,4-butanediol to produce 3-buten-1-ol.

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1. Introduction

Unsaturated alcohols such as allylic and homoallylic alcohols are important chemicals as resources of aroma chemicals, medical drugs, agricultural chemicals and polymers. We have previously reported that CeO₂ catalyzes the dehydration of 1,3-diols into unsaturated alcohols [1–4]: 3-buten-2-ol and *trans*-2-buten-1-ol are produced from 1,3-butanediol at 325 °C with the selectivities of 57 and 36 mol%, respectively [1]. CeO₂ also catalyzes the dehydration of 1,4-butanediol into 3-buten-1-ol at 375–425 °C [2,4,5]: 3-buten-1-ol is produced with a maximum selectivity of 68 mol% at 400 °C [5]. Side reactions such as isomerization, dehydrogenation, hydrogenation and further dehydration of 3-buten-1-ol to produce 2-buten-1-ol, 2-butenal, 1-butanol, and 1,3-butadiene, respectively, and the cyclization of 1,4-butanediol into tetrahydrofuran (THF) and γ -butyrolactone (GBL) reduce the selectivity to 3-buten-1-ol at any temperature.

We have also found that ZrO₂ with monoclinic structure catalyzes the dehydration of 1,4-butanediol to produce 3-buten-1-ol together with THF at 300–375 °C [6,7]. The step-wise reactions, such as isomerization, dehydrogenation, hydrogenation, and further dehydration of 3-buten-1-ol, are completely suppressed over monoclinic ZrO₂ at a low temperature of 325 °C. In the formation of 3-buten-1-ol, the acid–base property of ZrO₂ plays an important role [7]: modification of ZrO₂ with sodium cation enhances the selectivity to 3-buten-1-ol to over 70 mol%.

Recently, we have reported that several rare earth oxides (REO), such as Tb₄O₇, Er₂O₃, and Yb₂O₃, are selective for the production of 3-buten-1-ol from 1,4-butanediol [8,9]. We have found an important issue that Yb₂O₃ shows different catalytic activities depending on the crystal structure [8]. The crystal structure of Yb₂O₃ varies from monoclinic to cubic structure at temperatures around 800 °C. Cubic Yb₂O₃ shows the selectivity to 3-buten-1-ol of higher than 80 mol%. In addition, cubic Yb₂O₃ as well as monoclinic ZrO₂ catalyzes the dehydration of 1,5-pentanediol into 4-penten-1-ol [10]: 4-penten-1-ol is produced with the selectivity of higher than 75 mol% over cubic Yb₂O₃. However, cyclic ethers such as THF and tetrahydropyran are produced over monoclinic Yb₂O₃ [8,10]. The surface character of REOs is basic rather than acidic [9].

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REOs, especially heavy rare earth oxides, are as expensive as noble metals. In this paper, we aimed to prepare effective catalysts by dispersing REO on ZrO₂ to improve the catalytic activity by weight of REO, and we examined the dehydration of 1,4-butanediol over the REOs supported on ZrO₂. We also discussed the catalytic property as correlated with the changes in the structure and basicity of ZrO₂-supported Yb₂O₃ catalysts.

2. Experimental

2.1. Catalyst preparation

SiO₂ (CARIAct Q10), Al₂O₃ (DC2282), monoclinic ZrO₂ (RSC HP), and tetragonal ZrO₂ were supplied from Fuji Silicia Chemical Ltd., Dia Catalyst, Daiichi Kigenso Kagaku Kogyo Co., Ltd., and SAINT-GOBAIN, respectively. They were used as supports as well as catalysts. The support materials were crushed and sieved in the granule size of 0.25–1.00 mm. Rare earth metal nitrates were purchased from Wako Pure Chemical Co. Ltd. Yb₂O₃ was purchased from Kanto Chemical Co. Ltd.

Loading of REO on support material was done by incipient wetness impregnation. Each aqueous solution of nitrate with the prescribed amount of rare earth metal was impregnated on monoclinic ZrO₂. The resulting samples were calcined in air at a prescribed temperature for 3 h. Hereafter, the ZrO₂-supported REO is expressed as Ln/ZrO₂, where Ln means the atomic symbol of each rare earth element. Ln loading (wt.%) is defined as the following equation: Ln/(Ln + ZrO₂) in weight percentage. Other catalysts were prepared in the same way as the Ln/ZrO₂ using SiO₂ and Al₂O₃, and tetragonal ZrO₂ instead of monoclinic ZrO₂.

2.2. Catalytic reaction

The dehydration of 1,4-butanediol was carried out in a fixed-bed flow reactor under atmospheric pressure of N₂ with a flow rate of 26 cm³ min⁻¹ at 325 °C. Prior to the reaction, a catalyst (0.574 g) was preheated in N₂ flow at 500 °C for 1 h. After the catalyst bed had been heated at the prescribed temperature, 1,4-butanediol was fed into the reactor at a liquid flow rate of 1.41 cm³ h⁻¹. An effluent collected hourly was analyzed by gas chromatography (GC-8A, Shimadzu, Japan) with a 30-m capillary column (TC-WAX, GL Science, Japan). Gaseous products such as 1,3-butadiene were analyzed by on-line gas chromatography (GC-8A) with a 1-m packed column (Porapak Q).

2.3. Characterization

The specific surface area (SA) of each catalyst was calculated by the BET method using the N₂ isotherm at –196 °C. X-ray diffraction (XRD) patterns were recorded on an XRD7000 (Shimadzu, Japan) using Cu Kα radiation (λ = 0.15 nm) to detect the crystal structure of the samples. The tube voltage and current were 40 kV and 30 mA, respectively.

Temperature-programmed desorption (TPD) profiles of NH₃ and CO₂ were measured to estimate the acidity and the basicity of the catalysts, respectively [7,9]. The numbers of acid and base sites were estimated from neutralization–titration curves of diluted H₂SO₄ and NaOH solution, respectively. A sample (ca. 50 mg) was preheated at 500 °C for 1 h under a reduced pressure. In NH₃-TPD, NH₃ at 13 kPa was introduced to the sample at room temperature for 1 h. In CO₂-TPD, CO₂ was adsorbed on the sample at room temperature for 72 h. Then, each sample was evacuated for 1 h. After no adsorbate had been observed in N₂ flow, the sample was heated from room temperature to 800 °C at a heating rate of 10 °C min⁻¹ under an N₂ flow of 15 cm³ min⁻¹. The desorbed adsorbate molecules, together with N₂ gas, were bubbled into an electric conductivity cell containing a dilute H₂SO₄ or NaOH solution (50 cm³). The conductivity of the solution was monitored, and the obtained conductivity curve was differentiated to provide a distribution curve of adsorbate desorbed from adsorbent.

3. Results

3.1. Dehydration of 1,4-butanediol over supported rare earth oxide catalysts

Table 1 lists the catalytic results of several supported Yb₂O₃ catalysts in the reaction of 1,4-butanediol at 325 °C. Over Al₂O₃, THF was dominantly produced regardless of Yb loading. Yb/SiO₂ completely converted 1,4-butanediol to THF, while pure silica was not active for the reaction of 1,4-butanediol under the present conditions. It is known that acids catalyze the formation of THF from 1,4-butanediol [11,12]. It is reasonable that Al₂O₃ enhances the THF formation since it is acidic [5,13]. Because Yb/SiO₂ is selective for the THF formation, acidic sites could be generated on the surface of Yb/SiO₂. On the other hand, 3-buten-1-ol was produced over Yb/ZrO₂, while THF was formed over pure ZrO₂. Particularly, Yb₂O₃ supported on monoclinic ZrO₂ catalyzed the selective dehydration of 1,4-butanediol into 3-buten-1-ol. Thus, the monoclinic ZrO₂ was selected as the catalyst support in the following research.

Table 1
Dehydration of 1,4-butanediol over several supported Yb₂O₃ catalysts at 325 °C^a.

Catalyst ^b	Yb loading (wt.%)	SA ^c (m ² g ⁻¹)	Conversion (%)	Selectivity (mol%) ^d			
				3-Buten-1-ol	THF	GBL	Others
Al ₂ O ₃	0	205	100	0.1	97.4	0.0	2.5
Yb/Al ₂ O ₃	30	115	99.8	1.3	96.4	0.5	1.8
SiO ₂	0	316	1.6	0.0	26.5	0.0	73.5
Yb/SiO ₂	30	149	100	0.2	98.3	0.1	1.4
m-ZrO ₂	0	56	94.4	34.1	65.9	0.0	0.0
Yb/m-ZrO ₂	20	40	50.8	86.5	4.3	1.1	8.1
t-ZrO ₂	0	91	99.9	0.7	96.8	0.2	2.3
Yb/t-ZrO ₂	20	43	77.1	39.4	50.7	0.8	9.1
Yb ₂ O ₃ ^e	0	30	57.8	84.8	1.4	1.1	12.7

^a Conversion and selectivity were averaged in the initial 5 h. $W/F = 0.407 \text{ g h cm}^{-3}$ where W and F are catalyst weight and flow rate of reactant fed, respectively, reaction temperature = 325 °C, N₂ carrier flow rate = 26 cm³ min⁻¹.

^b Calcined at 400 °C. m-ZrO₂ means monoclinic ZrO₂, and t-ZrO₂ means tetragonal ZrO₂.

^c SA, specific surface area.

^d THF, tetrahydrofuran; GBL, γ -butyrolactone. Others include 1,3-butadiene, 2-buten-1-ol, and 1-butanol.

^e Calcined at 800 °C.

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