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# Reduction of $H_xMoO_3$ with different amounts of hydrogen to high surface area molybdenum oxides

Hirotoshi Sakagami, Yoko Asano, Tomoya Ohno, Nobuo Takahashi, Hidenobu Itoh, Takeshi Matsuda\*

Department of Materials Science, Kitami Institute of Technology, 165 Koen-cho, Kitami, Hokkaido 090 8507, Japan

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#### Abstract

The effect of the amounts of hydrogen in molybdenum bronze on the surface area of its reduction product was studied. H<sub>2</sub> reduction of molybdenum bronze induced an increase in the surface area. Molybdenum bronze with the larger amount of hydrogen exhibited the higher surface area after H<sub>2</sub> reduction. The reduction process varied with the amount of hydrogen in molybdenum bronze. The formation of MoO<sub>2</sub> was suppressed and that of molybdenum oxyhydride, MoO<sub>x</sub>H<sub>y</sub>, was promoted by an increase in the amount of hydrogen. Molybdenum bronze decomposed to Mo<sub>4</sub>O<sub>11</sub> and MoO<sub>2</sub> on thermal treatment at 400 °C in a flow of N<sub>2</sub>. The surface area of the thermally treated bronze changed very little with H<sub>2</sub> reduction. We conclude from these results that the reduction of molybdenum bronze to MoO<sub>x</sub>H<sub>y</sub>, of which the formation was dominated by the amount of hydrogen in molybdenum bronze, involved an enlargement in the surface area. (C) 2005 Elsevier B.V. All rights reserved.

Keywords: Hydrogen molybdenum bronze; H2 reduction; Surface area; Molybdenum oxides

## 1. Introduction

Inorganic materials with high specific surface area have a great utility as catalysts and adsorbents. Synthesis and characteristics of Mo- and W-based materials with high specific surface area have been reported. Volpe and Boudart [1] have reported that temperature-programmed reaction between MoO<sub>3</sub> or WO<sub>3</sub> with NH<sub>3</sub> provided a new way to prepare Mo<sub>2</sub>N and  $W_2N$  powders with surface areas as high as 220 and 91 m<sup>2</sup>/ g, respectively. The Mo<sub>2</sub>N and W<sub>2</sub>N were transformed to  $MoC_x$ and WC<sub>x</sub> with surface areas of 185 and 55 m<sup>2</sup>/g, respectively, by temperature-programmed carburization in a mixture of CH<sub>4</sub> and H<sub>2</sub> [2,3]. Temperature-programmed carburization of MoO<sub>3</sub> in a  $CH_4$ - $H_2$  mixture also led to the formation of  $MoC_x$  with high surface area [4]. Ledoux and co-workers have shown that the reaction of MoO<sub>3</sub> with a mixture of H<sub>2</sub> and hydrocarbon at  $350 \,^{\circ}\text{C}$  yielded molybdenum oxycarbide, MoO<sub>x</sub>C<sub>y</sub>, with a surface area of about  $150 \text{ m}^2/\text{g}$  [5–7].

We showed in previous papers [8,9] that  $H_2$  reduction of  $MoO_3$  at 350 °C was accompanied by a significant increase in

the surface area. The reduced  $MoO_3$  exhibited a surface area of 180 m<sup>2</sup>/g when its average valence of Mo was in the range of 2.5–3.5. The enlargement of surface area was found to result from the formation of pores with diameters of 0.6–3.0 nm.  $MoO_3$  became an active and selective catalyst for heptane isomerization after H<sub>2</sub> reduction at 350 °C [10,11]. Furthermore, the reduced MoO<sub>3</sub> catalyzed the dehydrogenation and the dehydration of propan-2-ol simultaneously [11,12]. We have suggested from these results that  $MoO_3$  reduced at 350 °C is a porous transition metal oxide with the bifunctional property.

The physical and catalytic properties of H<sub>2</sub>-reduced MoO<sub>3</sub> were strongly dependent on reduction temperature [13,14]. When the samples reduced at different temperatures were compared at a certain average valence of Mo, MoO<sub>3</sub> reduced at 350 °C had much higher surface area than MoO<sub>3</sub> reduced at 400 °C and above. Similar results were obtained in heptane isomerization. Since the formation of hydrogen molybdenum bronze, H<sub>x</sub>MoO<sub>3</sub>, was observed during reduction at 350 °C, but not at 400 °C, we have suggested that the surface area and the isomerization activity can be enlarged when reduction involves the formation of H<sub>x</sub>MoO<sub>3</sub>. Wehrer et al. reported the strong influence of reduction conditions of MoO<sub>3</sub> on its isomerization be the precursor of the active phase for alkane isomerization

<sup>\*</sup> Corresponding author. Tel.: +81 157 26 9448; fax: +81 157 26 4973. *E-mail address:* matsutk@mail.kitami-it.ac.jp (T. Matsuda).

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[15–17]. The important role of  $H_xMoO_3$  was also observed in preparation of molybdenum oxycarbide;  $MoO_xC_y$  was formed as a pure phase without the presence of  $MoO_2$  by starting from  $H_xMoO_3$ , while carburization of  $MoO_3$  yielded a mixture of  $MoO_xC_y$  and  $MoO_2$  [18].

The dependency of the surface area on reduction temperature was not observed when temperature-programmed reduction of MoO<sub>3</sub> was conducted in the presence of noble metal, such as Pt and Pd [19–21]. It is well known that MoO<sub>3</sub> with a noble metal absorbs a large amount of atomic hydrogen at room temperature without an equivalent amount of water being generated [22–24]. This phenomenon is understood as follows: H<sub>2</sub> molecules are dissociatively adsorbed on noble metal, and the dissociated species migrate onto MoO<sub>3</sub>, and then insert into the MoO<sub>3</sub> lattice, leading to the formation of  $H_xMoO_3$ . When reduction of Pt/MoO<sub>3</sub> was performed at 400 °C after heating in a stream of N<sub>2</sub>, the reduction proceeded without the formation of  $H_xMoO_3$ . In this case, the surface area did not change at all [25]. We reported in previous papers [26,27] that the effects of  $H_2$  reduction on the surface area of  $H_xMoO_3$  that were prepared from a mixture of MoO<sub>3</sub>, Zn, and HCl solution was similar to those on  $Pt/MoO_3$ , but differed from those on  $MoO_3$ . We have suggested from these results that the enlargement of surface area can originate from reduction of  $H_xMoO_3$ . However, the roles of H<sub>x</sub>MoO<sub>3</sub> in the enlargement of surface area are still under investigation. The main purpose of this paper is to describe the effect of the amounts of hydrogen in  $H_xMoO_3$  on the surface area of its reduction product.

## 2. Experimental

#### 2.1. Materials

H<sub>2</sub>, N<sub>2</sub>, and Ar were purified by passage through a molecular sieve and an Mn/SiO<sub>2</sub> oxygen trap. H<sub>2</sub>MoO<sub>4</sub> of purity 98% was purchased from Kanto Chemical Co. Inc. The MoO<sub>3</sub> used in this study was obtained by calcination of H2MoO4 at 400 °C for 3 h. Hydrogen molybdenum bronze, H<sub>x</sub>MoO<sub>3</sub>, was prepared at room temperature according to the method described by Glemser and Lutz [28]. MoO<sub>3</sub> powder (10 g) was mixed with chips of Zn, and then an aqueous solution of 4 M HCl was added. H<sub>x</sub>MoO<sub>3</sub> with the different amounts of hydrogen was obtained by changing the amounts of Zn and HCl solution, namely the molar ratio of MoO<sub>3</sub> and H<sub>2</sub> that was evolved from the reaction of Zn and HCl. H<sub>x</sub>MoO<sub>3</sub> samples were prepared at the H<sub>2</sub>/Mo ratios of 0.5, 1.0, and 2.0. The reaction mixture was filtered and washed many times in water to eliminate ZnCl<sub>2</sub> and HCl. After filtration, the product was dried in vacuo, and was then stored under Ar atmosphere.

## 2.2. Reduction and characterization methods

A sample weighing 0.1 g was heated to 200–500 °C at a rate of 5 °C/min in a stream of H<sub>2</sub> (60 mL/min), and was kept for 12 h. For comparison, H<sub>2</sub> reduction was conducted at 400 °C for a desired period, typically for 12 h, on H<sub>x</sub>MoO<sub>3</sub> that was treated in a flow of N<sub>2</sub> at 200–400 °C for 2 h prior to reduction.

After reduction and evacuation at room temperature, the adsorption isotherm of  $N_2$  was measured at -196 °C using a conventional high vacuum static system to determine the surface area. After the adsorption measurement, the sample was heated in vacuo to 500 °C, and then was oxidized by introducing prescribed amounts of  $O_2$ . The average valence of Mo was calculated from the amounts of  $O_2$  consumed in the reoxidation to MoO<sub>3</sub>. The pore-size distribution and the pore volume were determined with an automatic gas adsorption apparatus (Sorpmatic 1990, Carlo Erba) using the Horvath–Kawazoe method.

X-ray diffraction analyses were carried out on a Rigaku Model Rint 1200 diffractometer with the Ni-filtered Cu K $\alpha$  radiation. H<sub>2</sub>-reduced samples for XRD measurements were obtained as follows: a sample was subjected to H<sub>2</sub> reduction at temperature in the range of 200–500 °C for a desired period, followed by flowing N<sub>2</sub> for 0.5 h at the same temperature. After cooling to room temperature under a flow of N<sub>2</sub>, the reduced sample was transferred to a glove box without exposure to air, and was dispersed in a solution of heptane to avoid any bulk oxidation.

Temperature-programmed reduction (TPR) was conducted to study the reduction process of  $H_xMoO_3$ . A sample weighing 0.4 g was heated from 25 to 900 °C at a rate of 5 °C/min in a stream of 20% H<sub>2</sub>–Ar (20 mL/min). The concentrations of H<sub>2</sub> and H<sub>2</sub>O were monitored with TCD gas chromatography using a Porapak N separation column at 140 °C. Temperatureprogrammed decomposition (TPD) was carried out using Ar as a carrier gas to determine the amounts of hydrogen in H<sub>x</sub>MoO<sub>3</sub> samples.

# 3. Results and discussion

## 3.1. Characteristics of $H_x MoO_3$

Fig. 1 demonstrates the XRD patterns of  $H_xMoO_3$  samples prepared using Zn metal and an aqueous solution of HCl. The  $H_xMoO_3$  prepared at the H<sub>2</sub>/Mo molar ratio of 0.5 provided no diffraction lines due to the MoO<sub>3</sub> phase; the lines corresponding to the H<sub>0.34</sub>MoO<sub>3</sub> phase were observed at  $2\theta = 12.6^{\circ}$ , 23.7°, 27.0°, 29.8°, 33.8°, and 38.5°, and those to the H<sub>0.93</sub>MoO<sub>3</sub> phase appeared at  $2\theta = 12.2^{\circ}$ , 24.2°, 25.5°, 37.2°, and 39.1°. The mixture of the H<sub>0.34</sub>MoO<sub>3</sub>, the H<sub>0.93</sub>MoO<sub>3</sub>, and the H<sub>1.68</sub>MoO<sub>3</sub> phases was obtained at the H<sub>2</sub>/Mo ratio of 1.0. The H<sub>x</sub>MoO<sub>3</sub> prepared at the H<sub>2</sub>/Mo ratio of 2.0 gave no diffraction lines due to the H<sub>0.34</sub>MoO<sub>3</sub> and H<sub>0.93</sub>MoO<sub>3</sub> phases; the lines were observed at  $2\theta = 12.7^{\circ}$ , 24.4° and 38.7°, which were assigned to  $d(2 \ 0 \ 0)$ ,  $d(1 \ 1 \ 0)$ , and  $d(6 \ 0 \ 0)$  diffraction of the H<sub>1.68</sub>MoO<sub>3</sub> phase.

Temperature-programmed decomposition (TPD) and reoxidation of  $H_xMoO_3$  were performed to determine the *x* value of  $H_xMoO_3$ . Results are summarized in Table 1. TPD of  $H_xMoO_3$ in an Ar flow yielded  $H_2O$  only. The amounts of  $H_2O$  evolved from  $H_xMoO_3$  prepared at the  $H_2/Mo$  ratios of 0.5, 1.0, and 2.0 in temperatures of 25–500 °C were  $5.63 \times 10^{-2}$ ,  $6.88 \times 10^{-2}$ , and  $9.34 \times 10^{-2}$  g/g  $H_xMoO_3$ , respectively, from which the *x* values of the  $H_xMoO_3$  samples were determined to be 0.9, 1.1, Download English Version:

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