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# Thermodynamically constrained averaging theory approach for modeling flow and transport phenomena in porous medium systems: 3. Single-fluid-phase flow

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#### Abstract

This work is the third in a series of papers on the thermodynamically constrained averaging theory (TCAT) approach to modeling flow and transport phenomena in multiscale porous medium systems. Building upon the general TCAT framework and the mathematical foundation presented in previous works in this series, we demonstrate the TCAT approach for the case of single-fluid-phase flow. The formulated model is based upon conservation equations for mass, momentum, and energy and a general entropy inequality constraint, which is developed to guide model closure. A specific example of a closed model is derived under limiting assumptions using a linearization approach and these results are compared and contrasted with the traditional single-phase-flow model. Potential extensions to this work are discussed. Specific advancements in this work beyond previous averaging theory approaches to single-phase flow include use of macroscale thermodynamics that is averaged from the microscale, the use of derived equilibrium conditions to guide a flux–force pair approach to simplification, use of a general Lagrange multiplier approach to connect conservation equation constraints to the entropy inequality, and a focus on producing complete, closed models that are solvable.

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Keywords: Porous medium models; Averaging theory; TCAT; Single-phase flow

#### 1. Introduction

This paper is the third in a series of efforts designed to yield complete, rigorous, closed models that describe transport phenomena in multiscale porous medium systems using the thermodynamically constrained averaging theory (TCAT) approach. Work to date has outlined a general TCAT approach that can be used to generate such models [20] and laid a mathematical foundation upon which these models can be constructed [25]. We will build on these results in the current and subsequent papers to construct closed models for important systems, to compare and contrast these models with conventional models in use for sim-

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ilar purposes, and to compare these new models with highly resolved sub-scale simulations and experimental observations. The present paper is focused on single-fluid-phase flow in porous media. This system has been chosen because it provides a relatively simple setting in which to demonstrate the application of the TCAT approach and to illustrate that putting even this well-studied system on firm theoretical footing illuminates some important intrinsic assumptions in conventional models.

The traditional model for single-phase flow is derived typically by (1) writing an equation of mass conservation for a fluid phase; (2) using Darcy's law as an approximate momentum equation to remove the superficial velocity vector from the conservation equation; (3) assuming a simple equation of state for the fluid phase that relates its density and pressure; (4) assuming that spatial gradients in density are small; and (5) approximating the compressibilities of

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Nomenclature			
Romar	n letters	$\overset{\kappa  o \imath}{M_{\eta}}$	exchange of entropy from the $\kappa$ to the $\iota$ entity
b	external entropy source per unit volume	,	resulting from mass transfer
С	Greens' deformation tensor	$\mathbf{n}_i$	outward normal vector from entity i
$\hat{c}$	compressibility parameter	$\mathcal{P}$	conservation of momentum equation
d	rate of strain tensor	$\mathscr{P}_i$	general microscale property
E	internal energy per unit volume	p	fluid pressure
$\hat{E}$	Young's modulus	$\overset{p}{\overset{\kappa  o \iota}{Q}}$	transfer of energy from the $\kappa$ to the $\iota$ entity
$E_{ m T}$	total energy per unit volume	Q	resulting from phase change, interfacial stress,
E	the set of entities in the model		and heat transfer
$\mathcal{E}$	conservation of energy equation	a	heat flux vector
€ <sub>c</sub>	connected set of entities	q Ř	symmetric, positive semi-definite second-rank
$\hat{E}_{v}$	variable grouping defined by Eq. (114)	11	momentum resistance tensor
е	solid-phase Eulerian strain tensor	Q	entropy balance equation
$e_{zz}^s$	macroscale solid-phase Eulerian strain tensor	$\mathscr{S} \hat{S}_{ extsf{s}}$	specific storage coefficient
22	diagonal component for the vertical direction	$\mathscr{T}$	CIT-based thermodynamic equation for mate-
F	thermodynamic force tensor		rial derivative of internal energy
F	thermodynamic force vector	$\overset{\kappa  o \imath}{\mathbf{T}}$	transfer of momentum from the $\kappa$ to the $\iota$ entity
F	thermodynamic force scalar	$\kappa \rightarrow \iota$	
F	set of all thermodynamic forces	$T_v$	transfer of energy from the $\kappa$ to the $\iota$ entity
G	geometric orientation tensor for an interface	_	resulting from interfacial stress
g	gravitational acceleration vector	t	stress tensor
g	magnitude of gravitational acceleration	t	time
H	hydraulic head	$\mathscr{V}$	the set of unknown variables requiring closure
h	heat source per unit volume		relations
ı	identity tensor	$\mathbf{v}$ $\mathbf{v}^{\overline{\imath},\overline{s}}$	velocity vector
I'	surface identity tensor	V	mass-averaged velocity of the <i>i</i> entity relative to
J	index set of entities		the mass-averaged velocity of the s entity
₽c	index set of connected entities	$\mathbf{X}$	weighting function in averaging operator position vector in the solid phase initially
$\mathscr{J}_{\mathrm{p}}$	index set of phase entities	X	position vector in the solid phase
J	thermodynamic flux tensor	A	position vector in the solid phase
J	thermodynamic flux vector	Grook	eletters
J	thermodynamic flux scalar	ά	Biot coefficient
ð	set of all thermodynamic fluxes	$\hat{\hat{eta}}$	compressibility parameter
j <b>K</b>	solid-phase Jacobian	$\Gamma$	boundary of domain of interest
^	hydraulic conductivity tensor		interfacial tension
$\mathbf{K}_q$	second-rank, symmetric, positive semi-definite	$\frac{\gamma}{\epsilon^i}$	specific measure of the $\iota$ entity
	heat conduction tensor	η	entropy per unit volume
$K_{\mathrm{E}}$	kinetic energy per unit mass due to microscale	$\overset{\prime }{ heta }$	temperature
ŵ	velocity fluctuations	$\Lambda$	entropy production per unit volume
$\hat{K}_{\mathbf{S}}$	bulk modulus of the solid phase	λ	vector of Lagrange multipliers
$K_{\mathrm{T}}$	bulk modulus of the skeleton	$\lambda$	Lagrange multiplier
k î	unit Cartesian vector oriented vertically upward	$\mu$	chemical potential
$\hat{k}_m$	non-negative interfacial mass transfer para-	î	Poisson's ratio
ŷ	meter	ρ	density
$k_q$	non-negative interfacial heat transfer parameter	σ	solid-phase Lagrangian stress tensor
$\mathcal{M}$	conservation of mass equation	τ	effective solid-phase stress tensor
$\stackrel{\kappa  o \iota}{M}$	transfer of mass from the $\kappa$ to the $\iota$ entity	$\stackrel{\kappa  ightarrow \iota}{oldsymbol{\Phi}}$	transfer of entropy from the $\kappa$ to the $\iota$ entity
$K \rightarrow i$ $M_{\Sigma}$	transfer of energy from the $\kappa$ to the $\iota$ entity	φ	entropy flux vector
$M_{\rm E}$	resulting from mass transfer	$\psi$	gravitational potential
$\mathbf{M}_v^{\kappa  o \imath}$	exchange of momentum from the $\kappa$ to the $\iota$	$\stackrel{arphi}{\Omega}$	spatial domain
1 <b>V1</b> <sub>U</sub>	entity resulting from mass transfer	$\frac{32}{\Omega}$	closed domain
I	charty resulting from mass transfer	22	Closes domain

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