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Photocatalytic carbon oxidation with nitric oxide

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ABSTRACT

The photocatalytic oxidation of carbon black on TiO₂ using nitric oxide as an oxidizing agent was investigated. Layer-wise deposited carbon and $TiO₂$ powder was illuminated with UVA light in the presence of NO at parts per million concentrations in dry and hydrated carrier gas at a temperature of 150 ◦C. Carbon was photocatalytically converted mainly into $CO₂$, and NO mainly into $N₂$. Carbon oxidation rates of 7.2 μ g/h/mgTiO $_2$ were achieved in the presence of 3000 ppm NO. Under these experimental conditions in the absence of molecular oxygen, formation of surface nitrates causing $TiO₂$ photocatalyst deactivation is suppressed. Addition of water enhances surface nitrate formation and catalyst deactivation.

NO and carbon particulate matter are air pollutants emitted by diesel engines. Elimination of soot collected on a diesel particulate filter through oxidation is a demanding reaction requiring temperatures in excess of 250 ℃. The present study opens perspectives for a low-temperature regeneration strategy for the diesel particulate filter that simultaneously performs $DeNO_x$ reactions.

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1. Introduction

Particulate matter (PM) emissions generated in diesel engines have gained considerable attention due to the increasing number of diesel vehicles and due to their possible negative impacts on human health and environment $[1-3]$. There is increasing evidence on causal relationships between several diseases (e.g. cardiovascular and respiratory diseases) and chronic exposure to particulate matter $[4,5]$. The increasing concern has led to the introduction of more stringent exhaust emissions standards which necessitate the implementation of sophisticated exhaust gas purification systems in vehicles [\[6\].](#page--1-0)

Currently, PM is removed from exhaust gas using a diesel particulate filter (DPF) [\[7\]. P](#page--1-0)M trapped by DPF needs to be removed from the filter to avoid increasing backpressure which would degrade diesel engine performance. Periodic or continuous regeneration minimizes the risk of uncontrolled carbon burning in the filter $[6]$. Oxidation of retained PM to $CO₂$ in a diesel particulate filter is an evident way of filter regeneration. Oxidation of carbon using $O₂$ requires high temperatures of 500–550 °C [\[8\].](#page--1-0) Compared to O_2 , NO2 is a much more powerful oxidizing agent. In continuously

regenerated PM traps, NO emitted by the engine is oxidized to $NO₂$ over an oxidation catalyst positioned in front $[8]$. NO₂ is able to oxidize carbon at temperatures as low as $250^{\circ}C$ [\[9–13\]. R](#page--1-0)eaction mechanisms of the oxidation of carbon by $NO₂$ in the presence of water vapor and molecular oxygen are well documented [\[12–15\].](#page--1-0) In the carbon oxidation reaction, the $NO₂$ molecules are reduced mainly to NO:

$$
C + 2NO2 \rightarrow CO2 + 2NO
$$
 (1)

$$
C + NO2 + \frac{1}{2}O2 \rightarrow CO2 + NO
$$
 (2)

Since the DPF does not eliminate NO_x , an additional $DeNO_x$ system needs to be implemented to eliminate the NO downstream of the DPF [\[16,17\]. R](#page--1-0)eduction of NO_x using PM to $N₂$ instead of NO:

$$
C + 2NO \rightarrow CO_2 + N_2 \tag{3}
$$

would eliminate the need of a separate $DeNO_x$ system downstream of the DPF.

Selective formation of N_2 has been observed in the reaction of carbon with NO in the temperature range 600–1000 °C [\[18\]. T](#page--1-0)he formation of $CO₂$ and CO can be described globally by Eq. (3) combined with Eqs. (4) and (5) [\[19,20\]:](#page--1-0)

$$
2C + 2NO \rightarrow 2CO + N_2 \tag{4}
$$

$$
2CO + 2NO \rightarrow 2CO_2 + N_2 \tag{5}
$$

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The simultaneous elimination of two pollutants, viz. carbon particles and NO via reactions (3)–(5) is attractive in view of automotive applications, but the very high temperatures required for these reactions are impractical. The temperature of diesel exhaust gas in latest generation vehicles remains below the 250 ℃ threshold for regeneration, especially during urban driving conditions [\[21\]. R](#page--1-0)egeneration of a DPF often necessitates additional heating, which is achieved by combustion of fuel injected in the exhaust gas, representing a fuel penalty.

Photocatalytic processes could be an attractive alternative for accelerating depollution reactions at low temperature. Titanium dioxide is a popular photocatalyst for air as well as water treatment [\[22,23\],](#page--1-0) because of the large band gap energy of $TiO₂$ materials (anatase: 3.2 eV, rutile: 3.03 eV) these materials can only be activated by UVA light $[24]$. Application of TiO₂ on surfaces for pollutant removal through a solar-driven photocatalytic oxidation process in air is well documented [\[25,26\].](#page--1-0) Visual evidence of lateral and remote oxidation of soot by UVA-irradiated titanium dioxide thin films has been reported [\[27\].](#page--1-0) The elimination process of carbon particles on outdoor surfaces at ambient conditions is however quite slow [\[28\]. C](#page--1-0)hin et al. developed a kinetic model of photocatalytic soot oxidation and assumed two pathways of $CO₂$ formation [\[29,30\]:](#page--1-0) a direct soot oxidation to $CO₂$ and a multistep reaction for $CO₂$ generation from intermediate species of unknown nature. The oxidizing species generated by the photoactivation process are assumed to be superoxide anions $(O_2^{\bullet -})$ and hydroxyl radicals (HO•), derived from molecular oxygen and adsorbed water molecules, respectively [\[31–33\]. E](#page--1-0)vidence from EPR and FTIR spectroscopy hinted at an essential role of molecular oxygen-related radicals in photocatalytic soot degradation [\[33\].](#page--1-0) Photocatalysis with $TiO₂$ has already been shown to be active in the reduction of NO_x using ammonia (photocatalytic selective catalytic reduction or, in short, photo SCR), and in ammonia oxidation [\[34,35\].](#page--1-0) To our knowledge, no reports are available on the use of photocatalysis for performing the oxidation of carbon using nitric oxide as an oxidizing agent under conditions relevant to engine exhaust purification.

We investigated photocatalytic oxidation of carbon black in the presence of nitric oxide and water over commercial $TiO₂$ catalyst. We found that carbon can be photocatalytically oxidized into $CO₂$ under varied conditions. Furthermore, most of the NO is reduced to N_2 . Photocatalytic carbon oxidation with simultaneous NO_x reduction is an attractive concept for future photocatalysisassisted exhaust after treatment systems.

2. Experimental

2.1. Materials and sample preparation

Commercial TiO₂ photocatalyst (Cristal Global Millennium $PC500$) was used. This TiO₂ powder consists of anatase, has a surface area of 350 m²/g and a primary particle size of 9 nm [\[36\]. P](#page--1-0)rintex U is a popular model carbon black for evaluating carbon oxidation catalysis [\[37\]. A](#page--1-0)n amount of 5 mg of Printex U was deposited on a glass plate (300 mm \times 50 mm) by spreading and evaporating an isopropanol suspension. Subsequently, 50 mg of $TiO₂$ catalyst powder was spread over the soot-coated glass plate using isopropanol solvent as described earlier [\[35\].](#page--1-0)

2.2. Reactor set-up

The glass plate supporting the carbon and $TiO₂$ layer was placed in a flat photoreactor (Fig. 1).

The thermostatic support made of stainless steel is temperaturecontrolled and can be heated to 200 ◦C. The sample was illuminated

Reactor set-up

Fig. 1. Photograph (a) and schematic drawing (b) of the photoreactor.

from the top with a UVA-lamp (Rayonet) at a light intensity of 1.1 mW/cm^2 . The UVA lamp is mounted in an aluminum housing covering the reactor block. Sealing of the reactor is done by a borosilicate glass plate (430 mm \times 70 mm) and Viton O-ring (Eriks). The headspace between the glass plate with deposited sample and the borosilicate sealing plate is ca. 2 mm high, creating a gas volume of ca. 48 cm³. NO (5% in He) and N_2 are fed from gas cylinders using mass flow controllers (Bronkhorst). Water vapor is introduced in the N_2 stream via a temperature-controlled bubbler. Analysis of the gaseous reaction products is conducted via a UV detector for $NH₃$, NO and NO₂ (ABB Limas 11HW) and NDIR detector for N₂O, CO and $CO₂$ (ABB Uras 26 instrument). The detectors have specific filters for each gas compound, minimizing interference with other gases. After passing through the UV detector, the gas is led through an ABB SCC-C gas cooler for removal of water in the gas stream and lowering of the dew point to 3° C. All corrosive components $(SO₂, NH₃, NO₂)$ are transferred to the condensate for protection of the NDIR instrument. Both detectors are equipped with gas-filled cuvettes for autocalibration. The detection limits are less than 1% of the smallest measurement range [\(Table 1\).](#page--1-0) The selectivity for N_2 was estimated from the nitrogen atom balance. Based on the detection limits, the standard deviation value was estimated at $\pm 2\%$ using the formula of cumulative uncertainty.

2.3. Carbon photocatalytic oxidation experiments

In a preliminary experiment, photocatalytic carbon oxidation was investigated under continuous flow of a gas mixture with 1000 ppm NO and 3% $H₂O$ in N₂ at a flow rate of 150 ml/min, Download English Version:

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