



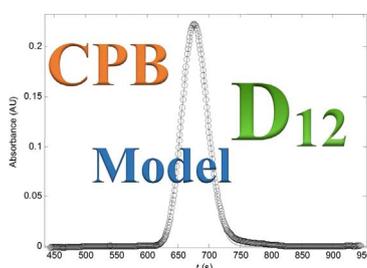
Measurement and modelling of tracer diffusivities of gallic acid in liquid ethanol and in supercritical CO₂ modified with ethanol



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GRAPHICAL ABSTRACT



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ABSTRACT

The tracer diffusion coefficients, D_{12} , of gallic acid in liquid ethanol and in supercritical carbon dioxide (SC-CO₂) modified with 16 mol.% ethanol were measured using the chromatographic peak broadening technique of Taylor-Aris. The diffusivity in ethanol ranged 0.485×10^{-5} – 0.905×10^{-5} cm² s⁻¹ (303.15–333.15 K and 1–100 bar) and in SC-CO₂/ethanol 3.256×10^{-5} – 4.978×10^{-5} cm² s⁻¹ (313.15–333.15 K and 150–250 bar). The dependencies of D_{12} upon temperature, pressure and Stokes–Einstein coordinates were examined in detail. With respect to modelling, lower deviations were achieved in both systems by: four 2-parameter correlations of Magalhães *et al.* (error 0.9–3.0%); the 1-parameter TL_{SM}₄ model (5.8% and 2.9% of error); and the 2-parameter Dymmond-Hilbrand-Batchinski (DHB) expressions (5.7% and 1.6% of error). The Wilke-Chang correlation cannot be applicable, due to consistent overpredictions of 133.0% (gallic acid/ethanol) and 114.0% (gallic acid/SC-CO₂/ethanol).

1. Introduction

The diffusivity can be defined in terms of a system response to a concentration disturbance, and relates the flow of particles with the resulting concentration gradients [1,2]. It is a transport property of great interest not only to study the structure and thermophysical behaviour of fluids, to capture information at microscopic level with regard to the interactions between molecules, but also for practical engineering applications [1–6]. The design of equipment depends on the physical properties of fluids, since an appropriate knowledge of

equilibrium data together with viscosity, thermal conductivity and diffusion coefficients is required for modelling processes involving momentum, heat and mass transfer [2,7], such as separation units and chemical reactors, particularly in the case of multiphase systems.

Gallic acid (3,4,5-trihydroxybenzoic acid) is a natural compound obtained from the hydrolysis of tannins [8], and possesses anti-inflammatory [9], antioxidant [10], antifungal [11] and carcinogenic [8] properties. It has proven to be one of the components with the highest bioactivity, enabling the fight against amyloid fibrils (fibril protein), which result from the aggregation of misshapen proteins that

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Nomenclature			
AARD	Average absolute relative deviation	\bar{u}	Average linear velocity
B_{DHB}	Parameter of the interaction solute-solvent in the DHB model	V_c	Critical molar volume
BPR	Back pressure regulator	V_D	Maximum packaging volume of the solvent in the DHB model
$C^{\text{app}}(z,t)$	Calculated average concentration of solute	V_m	Molar volume
$C^{\text{exp}}(t)$	Solute concentration at exit column	$V_{\text{TC,bp},2}$	Molar volume of the solute at its normal boiling point estimated by the method of Tyn and Calus
CO_2	Carbon dioxide	$W_{0.607}$	Peak half-width measured at 60.7% of total peak height
CPB	Chromatographic Peak Broadening method	y_i	Molar composition of the component i
D	Dispersion coefficient	z	Axial coordinate
D_{12}	Tracer diffusion coefficient of solute 2 through solvent 1		
De	Dean number, $De = Re/\sqrt{\xi}$		
DHB	Dymond-Hildebrand-Batchinski	<i>Greek letters</i>	
H	Height of the theoretical plate	ε	Root mean square deviation (rms)
k_B	Boltzmann constant, $k_B = 1.380658 \times 10^{-23} \text{J}\cdot\text{K}^{-1}$	λ	Wavelength
$k_{12,d}$	Binary interaction diameter	μ_1	Solvent viscosity
L	Length of the column	ξ	Curvature ratio
m	Total mass of solute injected	ρ_1	Solvent density; solvent number density
M	Molecular weight	σ_i	Molecular diameter of component i
M_{12}	Reduced molar mass	$\sigma_{L,i}$	Lennard-Jones diameter of component i
N_{av}	Avogadro's number, $N_{\text{av}} = 6.022 \times 10^{23} \text{mol}^{-1}$	ϕ	Dimensionless solvent association factor in the Wilke-Chang equation
NDP	Number of data points	ω	Acentric factor
NP	Number of parameters		
P	Pressure	<i>Subscripts</i>	
P_c	Critical pressure	1	Solvent
r	Radial coordinate	2	Solute
R	Inner column radius	12	Binary
R_c	Tube coil radius	bp	Property evaluated at normal boiling point
Re	Reynolds number	c	Critical property
R_g	Universal gas constant, $R_g = 8.3144 \text{J}\cdot\text{mol}^{-1}\cdot\text{K}^{-1}$	eff	Effective hard sphere diameter
Sc	Schmidt number	i	Component i
S_{10}	Asymmetric factor (ratio between peak half-widths at 10% peak height)	LJ	Lennard-Jones
SC-CO ₂	Supercritical carbon dioxide	mix	Mixture
t_i	Time at 10% peak height in the fitting method		
T	Absolute temperature	<i>Superscripts</i>	
T_{bp}	Normal boiling temperature of the component i	*	Reduced quantity
T_c	Critical temperature	calc	Calculated value
TLSM	Tracer diffusion coefficient model of Liu, Silva and Macedo	exp	Experimental value

deposit up in the tissues of the human body organs. Hence it plays an important role in treating diseases like Alzheimer and Parkinson [12].

Gallic acid is present in plants such as green tea and black tea [13], pomegranate peel [14], oak bark [15], and grape seed extracts [11]. This compound and its ester derivatives are important chemicals used in both pharmaceutical and food industries [14,16], from which one may cite the synthesis of *trimethoprim* (antibiotic used for infections) and propyl gallate, respectively [14].

In this work, tracer diffusion coefficients, D_{12} , of gallic acid in pure ethanol and in supercritical CO₂ (SC-CO₂) modified with ethanol were measured and modeled. The usage of ethanol as SC-CO₂ modifier is important under the context of biorefinery, taking into account that small amounts of a polar entrainer are frequently introduced to increment solubility and improve selectivity in separations [17]. However it is recognized the lack of diffusivity data in the case of multicomponent mixtures [18].

The diffusivities of the binary system gallic acid/ethanol were determined at 303.15, 313.15, 323.15 and 333.15K, and pressures of 1, 20, 40, 60, 80 and 100bar. In the case of the supercritical ternary system gallic acid/CO₂/ethanol, the measurements were carried out at 313.15, 323.15 and 333.15 K, and pressures of 150, 200 and 250 bar. In both cases the chromatographic peak broadening (CPB) method of

Taylor-Aris [19–21] was applied. A preliminary study of the most adequate detection wavelength was performed, and the influence of temperature, pressure, and viscosity on the obtained diffusion coefficients is also discussed.

The structure of the article is as follows: In Section 2, a brief theoretical background of the lab methodology and modelling approaches is presented; in Section 3, the chemicals, equipment and experimental procedure are described; Section 4 is devoted to discuss the experimental and calculated results, while the main conclusions are compiled in Section 5.

2. Theoretical background

2.1. Chromatographic peak broadening (CPB) method

The CPB method originally derived by Taylor and Aris [22–25] can be applied to measure diffusion coefficients (D_{12}) of solutes (component 2) at infinite dilution in pure or mixed solvents (component or pseudo-component 1) [21,26–29]. When a pulse of a solute is injected into a laminar flow of solvent through a capillary tube of circular cross section, that pulse will broaden due to the combined action of axial convection and radial molecular diffusion. The approximate average

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