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Zn-Fe-CNTs catalytic in situ generation of H₂O₂ for Fenton-like degradation of sulfamethoxazole



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HIGHLIGHTS

- Zn-Fe-CNTs was capable of converting O₂ to H₂O₂ and further to OH.
- The Fenton-like degradation of sulfamethoxazole (SMX) using Zn-Fe-CNTs as catalyst was studied.
- The removal efficiency of SMX and TOC was 100% and 51.3%, respectively.
- The possible reaction mechanism of Zn-Fe-CNTs/O₂ process was tentatively proposed.

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ABSTRACT

A novel Fenton-like catalyst (Zn-Fe-CNTs) capable of converting O_2 to H_2O_2 and further to *OH was prepared through infiltration fusion method followed by chemical replacement in argon atmosphere. The catalyst was characterized by SEM, EDS, TEM, XRD and XPS. The reaction between Zn-Fe-CNTs and O_2 in aqueous solution could generate H_2O_2 in situ, which was further transferred to *OH. The Fenton-like degradation of sulfamethoxazole (SMX) using Zn-Fe-CNTs as catalyst was evaluated. The results indicated that Zn-Fe-CNTs had a coral porous structure with a BET area of 51.67 m^2/g , exhibiting excellent adsorption capacity for SMX, which enhanced its degradation. The particles of Zn^0 and Fe^0/Fe_2O_3 were observed on the surface of Zn-Fe-CNTs. The mixture of Zn^0 and CNTs could reduce Zn^0 0 through Fenton-like process. When initial Zn^0 1 process could catalyze in-situ generation of Zn^0 2 produce *OH through Fenton-like process. When initial Zn^0 3 process were detected and the possible pathway of SMX degradation and the mechanism of Zn^0 4 process were tentatively proposed.

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1. Introduction

Advanced oxidation processes (AOPs) have been widely used for the degradation of toxic organic contaminants in water and wastewater in the past decades [1]. The classic Fenton- and related reactions are convenient, economical, and green ways to generate *OH for the removal of non-biodegradable and/or toxic compounds [2]. Fenton-like process, using solid iron compounds/complexes as heterogeneous catalysts [3,4], has received increasing atten-

tion in recent years. It is also attractive to develop Fenton process which can spontaneously generate H_2O_2 in situ, such as electro-Fenton system and photo-Fenton process [5,6]. However, the low and hardly regulated concentration of H_2O_2 generated insitu decreased the degradation efficiency of organic contaminants [7–9]. Therefore, it is necessary to increase the concentration of H_2O_2 in solid iron compounds/ O_2 system.

The generation of H_2O_2 in-situ by the reaction between Zn^0 and O_2 was investigated, but the productivity was low [10–12]. According to the theory of electrochemical corrosion, the rate of oxidation-reduction reaction on the surface of metal can be accelerated in the galvanic-type corrosion cell without external power supply. Therefore, the in-situ generation of H_2O_2 can be improved by the electrode reaction in the corrosion cell using Zn^0 as anode. Cathodic H_2O_2 could be produced on the surface of carbon materi-

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als through the electrochemical process [13,14]. Carbon nanotubes (CNTs) may offer significant advantages for the two-electron reduction of O_2 due to their good electrical conductivity, high surface activity and mechanical strength [15]. Thus, high concentration of H_2O_2 can be possibly produced by the reduction of O_2 in the micro-electrolysis system of Zn^0 -CNTs, which formed numerous corrosion cells between the particles of Zn^0 and CNTs in aqueous solution. Moreover, the redox potential of Fe^{2+}/Fe^0 ($-0.44\,V$) is higher than that of Zn^{2+}/Zn^0 ($-0.76\,V$), the Fe^0 can be deposited on $Zn^0/CNTs$ via chemical replacement. Therefore, when the composite of Zn^0 , CNTs and Fe^0 reacts with O_2 , H_2O_2 can be continuously supplied through the micro-electrolysis reaction between O_2 and $Zn^0-Fe^0/CNTs$, which can catalyze the generated H_2O_2 to produce O_2 0. In this system, O_2 0 or the reaction with O_2 0.

The release of antibiotics into the aquatic environment caused by extensive use of antibiotics is receiving increasing attention in recent years [16–18]. Sulfamethoxazole (SMX), an antibiotic used worldwide for treatment of urinary infection, has been identified in many wastewater treatment plants (WWTPs) effluents [19]. It is required to develop effective approaches for SMX removal.

In this study, Zn-Fe-CNTs composite was synthesized, characterized and used as catalyst for Fenton-like degradation of SMX. The effect of initial pH, Zn-Fe-CNTs dosage, and initial SMX concentration on the removal efficiency of SMX was determined. The intermediates were detected by LC-MS and IC, and the possible degradation pathway of SMX was tentatively proposed.

2. Materials and methods

2.1. Materials and chemicals

Sulfamethoxazole (SMX) ($C_{10}H_{11}N_3O_3S$) was a sigma Aldrich product (≥99.0% purity). Multi-walled CNTs (d<8 nm, l=10–30 μ m) were produced by Beijing Deke Daojing Nano-Company, China. Zinc powders (size: 120 meshes, specific surface area: 0.72 m²/g, purity: >99.8%) were obtained from Shandong Xiya Corporation Ltd., China. Commercial iron powders (≥98.0% purity) with specific surface area of 1.26 m²/g were purchased from Tianjin Jinke Fine Chemical Industry Research Institute., China. H_2SO_4 , NaOH, FeSO $_4$ ·7 H_2O and H_2O_2 were all of analytical grade. De-ionized water was used in all experiments.

2.2. Preparation and characterization of Zn-Fe-CNTs

The Zn-Fe-CNTs preparation was as follows. Firstly, 1.5 g Zinc powder was mixed with 0.5 g multi-walled CNTs. 2 mL 40% w polyethyleneglycol 4000 was dropped into the mixture, stirred for 30 min, then dried at room temperature, sintered in the tube furnace at 550 °C for 120 min with a N₂ flow speed of 60 mL/min and cooled into room temperature to obtain Zn-CNTs. Secondly, FeSO₄·7H₂O (0.5 g) were dissolved in 200 mL of aqueous sulfuric acid solution (pH=3), and Zn-CNTs (1g) were added in argon atmosphere. After 1 h, Zn-Fe-CNTs composites were obtained. The formation of Zn-Fe-CNTs was based on the following principles: polyethyleneglycol 4000 was used as binder and to bind zinc powder and multi-walled CNTs. When the mixture of zinc powder, multi-walled CNTs and polyethyleneglycol 4000 was heated into 550 °C, zinc powder with melting points of 419.5 °C was melted into liquid and polyethyleneglycol 4000 was decomposed into volatile gases. When the heated mixture was cooled into room temperature, liquid zinc was solidified on the surface of multi-walled CNTs and form Zn-CNTs. When as-prepared Zn-CNTs were put into the Fe²⁺ solution, the chemical replacement between Fe²⁺ and Zn⁰ in Zn-CNTs resulted in the formation of Zn-Fe-CNTs composites.

Scanning electron microscopy (SEM) and energy dispersive spectrometer (EDS) analyses were performed on emission scanning electron microscope (SEM, SU8010, Hitachi). Transmission electron microscopy (TEM) images were recorded on a transmission electron microscope (HRTEM, JEM 2100 and JEOL). BET-surface areas were measured using a NOVA 3200e bath at 77 K and degassing at 373 K. The pore size distribution was determined by the BJH method. Powder X-ray diffraction (XRD) measurement was performed with Cu K α radiation (MiniFlex 600, Rigaku, 40 kV and 15 mA) at a scanning rate of 0.5°/min. X-ray photoelectron spectroscopy (XPS) was measured by an AXIS-Ultra instrument (Kratos Analytical, UK).

2.3. Fenton-like degradation of SMX

Experiments were conducted at room temperature in a glass bottle (500 mL) containing a 250 mL solution. The real effluent of wastewater was collected at a local municipal wastewater treatment plant. The sample had an initial content of TOC of 9.77 ± 0.36 mg/L and pH of 7.0 ± 0.2 .

2.4. Analytical methods

H₂O₂ concentration was measured by a photometric method on an UV-vis spectrometer (PerkinElmer Lambda 25) at 385 nm using potassium titanium oxalate as chromogenic reagent. SMX concentration was determined by HPLC (Agilent 1200) equipped with a diode array detector (DAD) and a C18 reversed-phase column $(4.6 \, \text{mm} \times 150 \, \text{mm})$. The mobile phase used for SMX was a mixture of distilled water and acetonitrile (55:45 (v/v)) at a flow rate of 1.0 mL/min with a column temperature of 30 °C, and the analytical wavelength was 255 nm. SMX had a retention time of 3.0 min under these conditions. HPLC-MS equipped with the above-mentioned column coupled to a Shimadzu 2010EV mass spectrometer with ESI ion source (LC-MS 2010, Columbia, USA) was used to analyze organic intermediates. It equipped with a photo diode array (PDA) detector, and operated in a negative mode. The aforementioned solvent conditions were used for the analysis of the intermediates. The injected volume was 30 µL. Total organic carbon (TOC) content was measured by a Multi TOC/TN Analyzer (2100, Analytik Jena. Germany). The concentration of dissolved zinc and iron generated from the reaction process was determined with a flame atomic adsorption spectroscopy (AAS, HITACHI ZA-3000, Japan).

3. Results and discussion

3.1. Characterization of Zn-Fe-CNTs

The $\rm N_2$ adsorption-desorption isotherms and pore size distributions of Zn-Fe-CNTs and Zn-CNTs were given in Fig. 1. The Zn-Fe-CNTs sample provided the IV type isotherm, which are typical for the highly ordering mesoporous material with narrow size distribution. The isotherm of Zn-CNTs was identified as type an III/IV mixed type isotherm, which was characteristic of co-existence of microporous and mesoporous. Zn-Fe-CNTs had a larger BET specific surface area (51.67 m²/g) than that of Zn-CNTs (26.99 m²/g). The pore size distribution was calculated using the Barrett-Joyner-Halenda (BJH) method (Fig. 4b). The result showed that the average pore sizes of Zn-Fe-CNTs and Zn-CNTs were 16.89 nm and 13.52 nm, respectively.

TEM image and SEM micrograph of Zn-Fe-CNTs were shown in Figs. 2 and 3.

The samples exhibited coral porous structure and large dispersive metal nano-particles were adhered to the surface of CNTs in the Zn-Fe-CNTs. In order to confirm the element distribution and relative element content in Zn-Fe-CNTs, EDS spectra and element

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