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S. Baghdar Hosseini, R. Haghighi Khoshkhoo, S.M. Javadi Malabad

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Numerical Study on Polydisperse Particle Deposition in a Compact Heat Exchanger

S. Baghdar Hosseini¹, R. Haghighi Khoshkhoo^{2*}, S. M. Javadi Malabad³

^{1,2}Department of Mechanical and Energy Engineering, Shahid Beheshti University, Tehran – Iran ³Department of Mechanical Engineering, Quchan University of Advanced Technology, Quchan-Iran

* Corresponding author E-mail: <u>r haghighi@sbu.ac.ir</u> Telephone No: (+98) 912 564 49 02

Abstract

In this paper, the effect of particle size on deposition in a compact heat exchanger is investigated numerically. The effect of flow velocity and particle mass on the deposition for different particle size is also studied and discussed. Particle motions are simulated using the Lagrangian approach and discrete particle model (DPM). The deposition is modeled applying user defined function (DEFINE DPM EROSION). Flow simulation is performed using the Eulerian approach by solving Reynolds-Averaged Navier-Stokes (RANS) equations. Turbulence is simulated with the Realizable kepsilon model applying the Discrete Random Walk (DRW) model to account turbulent velocity fluctuations. Also, enhanced wall treatment is used with turbulence model. A computational study is done on a 3D five fin channels of a compact heat exchanger. The air flow is entered from upstream with velocity over a range from 1 m/s to 5 m/s and six polydisperse particles groups with various diameters from 1 µm to 1500 µm, are introduced into the computational domain. The results show that most of the particles deposited on the front of channels and also on the first, second and last edges of fin channels. Besides, deposition ratio increased with the increase of particle diameter, up to a maximum value, and then it decreased. The effect of injecting small particles with larger size particles is also studied, and their results showed an increase in particle deposition. Results show that velocity increase can promote or hinder particle deposition.

Keywords

Compact heat exchanger, CFD analysis, DPM, Particle deposition, Polydisperse, Pressure drop

Nomenclature

- C_c Cunningham correction
- d Diameter (m)
- d_{ij} the deformation tensor
- e_r Coefficient of restitution
- \vec{g} gravitational acceleration (m/s²)
- *k* turbulent kinetic energy (J/kg)

- v' Turbulent fluctuation in y direction (m/s)
- w' Turbulent fluctuation in *z* direction (m/s)
- U_p Particle velocity (m/s)
- V Volume (m³)
- v_{rel} The relative velocity of particle-fluid (m/s)
- *X* Position (m)

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