Applied Thermal Engineering 125 (2017) 799-810

Contents lists available at ScienceDirect

Applied Thermal Engineering

journal homepage: www.elsevier.com/locate/apthermeng

Supercritical CO₂ as heat transfer fluid: A review

Luisa F. Cabeza^{a,*}, Alvaro de Gracia^b, A. Inés Fernández^c, Mohammed M. Farid^d

^a GREA Innovació Concurrent, Universitat de Lleida, Edifici CREA, Pere de Cabrera s/n, 25001 Lleida, Spain

^b Departament d'Enginyeria Mecànica, Universitat Rovira i Virgili, Av. Països Catalans 26, 43007 Tarragona, Spain

^c Department of Materials Science and Metallurgical Engineering, Universitat de Barcelona, Martí i Franquès, 1, 08028 Barcelona, Spain

^d Department of Chemical and Materials Engineering, The University of Auckland, New Zealand

HIGHLIGHTS

• Comprehensive review of correlations of heat transfer coefficient of supercritical CO2.

• Different applications of supercritical CO₂ are also reviewed and discussed.

• Correlations from experimental are presented for different geometries.

• There is a lack of a unique universal correlation for each geometry.

ARTICLE INFO

Article history: Received 30 September 2016 Revised 4 July 2017 Accepted 6 July 2017 Available online 8 July 2017

Keywords: Supercritical CO₂ Heat transfer fluid Heat exchanger Empirical correlation Cooling

ABSTRACT

This paper presents a comprehensive review of all correlations and experimental studies available in the literature to determine the heat transfer coefficient of supercritical CO_2 flowing in heat exchangers. The different applications in which it is used are also reviewed and discussed. The correlations obtained from extensive experimental measurements are presented for different geometries (horizontal, vertical and inclined tubes, closed-loop circular pipes, and mini-channels) and dimensions. The review shows that there is a lack of a unique universal correlation for each geometry, suggesting the need for more work in this area.

© 2017 Elsevier Ltd. All rights reserved.

Contents

| 1. | Introduction | 799 |
|----|---|-----|
| 2. | Applications of supercritical CO ₂ | 800 |
| 3. | scCO ₂ properties | 802 |
| 4. | Heat transfer improvement using supercritical CO ₂ | 802 |
| | 4.1. Heat transfer characteristics at supercritical pressures | 802 |
| | 4.2. Nusselt correlations | 803 |
| | 4.3. Experimental investigations | |
| 5. | Conclusions | 808 |
| | Acknowledgements | 808 |
| | References | 808 |
| | | |

1. Introduction

Supercritical fluid is a fluid state where it is held at or above its critical temperature and critical pressure. Carbon dioxide behaves

* Corresponding author. E-mail address: lcabeza@diei.udl.cat (L.F. Cabeza).

http://dx.doi.org/10.1016/j.applthermaleng.2017.07.049 1359-4311/© 2017 Elsevier Ltd. All rights reserved. as a supercritical fluid above its critical temperature (304.25 K) and critical pressure (72.9 atm or 7.39 MPa), expanding to fill its container like a gas but with a density like that of a liquid (Fig. 1). When fluids and gases are heated above their critical temperature and compressed above their critical pressure they enter a supercritical phase where some properties, such as solvent power, can be dramatically changed. Fig. 2 shows in images how CO₂ goes







| Nomenclature | | | | | |
|--|---|--|--|--|--|
| C _p Cp D f G r g h k L Nu P r P r q Re Rr T | specific heat at constant pressure [J/kg·K] average specific heat at constant pressure [J/kg·K] inner diameter [m] friction factor [-] mass flux [kg/m ² ·s] Grasshof number [-] gravity acceleration [m ² /s] specific enthalpy [J/kg] thermal conductivity [W/m·K] tube length [m] Nusselt number [-] pressure [Pa] Prandtl number [-] average Prandtl number [-] heat flux from tube wall to fluid [W/m ²] Reynolds number [-] channel relative roughness temperature [K] | Greek s α β Δ ϵ μ ρ Subscri ac b exp f in Iso Out Pc Pred W | symbols heat transfer coefficient [W/m ² ·K] thermal expansion coefficient [1/K] Increment channel roughness [m] dynamic viscosity [Pa·s] density [kg/m ³] ipts acceleration at fluid bulk temperature experimental at film temperature inlet isothermal outlet at pseudo-critical temperature predicted at inner wall temperature | | |
| | | | | | |

through different phases from behaving as a sub-critical fluid to a supercritical fluid.

Okamoto et al. [3] in 2003 successfully visualized the variation of scCO₂ under forced convective heat transfer using schlieren and shadowgraph techniques as research towards the precise characterization of supercritical fluid behaviour. For example, Fig. 3 presents scCO₂ imaging by infrared laser and its translation to an instantaneous vector map and the average velocity distributions.

Supercritical CO_2 is becoming an important commercial and industrial solvent due to its role in chemical extraction in addition to its low toxicity and being environmental friendly solvent. The relatively low temperature of the process and the stability of CO_2 also allow most compounds to be extracted with little damage or denaturing. In addition, the solubility of many extracted compounds in CO_2 varies with pressure, permitting selective extractions. $scCO_2$ has been used for fluid extraction in areas such as food science, pharmaceuticals, chemical residues, biofuels, and polymers [4].

The aim of this review is to summarize the literature on the use of $scCO_2$ as a heat transfer fluid (HTF), however its wider application of extraction will also be summarized in this review.

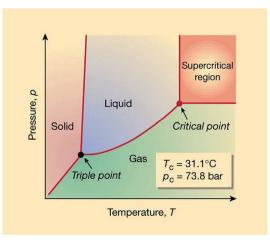


Fig. 1. Supercritical CO₂ p-T diagram [1]

2. Applications of supercritical CO₂

A short summary of supercritical CO_2 applications is presented here. Supercritical carbon dioxide (scCO₂) offers an acceptable combination of pressure and temperature to achieve supercritical conditions. scCO₂ is not a good solvent for most materials, which are scCO₂-phobic. However, both silicone and fluoro-products may be regarded as CO₂-philic and, therefore, potentially more soluble; such products are used in magnetic media production, one of the first applications of scCO₂ studied [5].

Another application investigated was supercritical extraction in petroleum refining and petrochemistry [6]. According to this publication, the advantages of carbon dioxide as solvent include; nonexplosiveness and incombustibility; chemical inertness; absence of toxic wastes; sufficiently low critical parameters (pressure and temperature); low polarity; availability and low cost; high extraction rate due to high diffusing power.

The food industry is always looking for the best separation technology to obtain natural compounds of high purity, healthy products of excellent quality with several industrial applications. The conventional extraction process for those compounds has some limitations regarding the solvent toxicity, flammability and wastefulness. Supercritical carbon dioxide is ideal for the food processing industry because of its non-flammable, non-toxic, non-polluting and recoverable characteristics [7,8]. Examples of applications in the food industry are extraction of cholesterol and other lipids from egg yolk; milk fat fractioning; extraction of lipids and cholesterol from meat and meat products; from fish; extraction of natural colourings from several foodstuffs (such as carrots, leaf protein concentrates, sweet potatoes, tomato paste waste and tomato skin, and rape grape skin); extraction, refining and fractioning of oils and vegetable fats; extraction and fractioning of natural flavourings; extraction of antioxidants; decaffeinating of coffee and tea; extraction of hop; and the alcoholisation of drinks.

 $scCO_2$ is also used in separation processes [9]. For example, Semenova and Ohya [10] studied the fractionation of SC CO₂/ethanol and $scCO_2/iso$ -octane mixtures using an asymmetric Kapton membrane. The investigators concluded that CO₂ transfer across was predominantly by convection rather than diffusion. At approximately the same time, Hsu and Tan [11] proposed the use of Download English Version:

https://daneshyari.com/en/article/4991230

Download Persian Version:

https://daneshyari.com/article/4991230

Daneshyari.com