ARTICLE IN PRESS

ICHMT-03549; No of Pages 12

International Communications in Heat and Mass Transfer xxx (2016) xxx-xxx

Contents lists available at ScienceDirect



02.016

 International Communications in Heat and Mass Transfer

journal homepage: www.elsevier.com/locate/ichmt

Conjugate natural convection heat transfer in a partitioned differentially-heated square cavity

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ARTICLE INFO

Available online xxxx

Keywords: Conjugate natural convection Differentially-heated cavity Heat transfer Partition Numerical simulation

ABSTRACT

In this study numerical results for conjugate natural convection flow and heat transfer in a differentiallyheated square cavity divided by a partition with finite thickness and thermal conductivity are presented. A series of numerical simulation is carried out using the finite volume method over a wide range of the Rayleigh number (10^5-10^9) , with three dimensionless partition thicknesses (0.05, 0.1 and 0.2) and three dimensionless partition positions (0.25, 0.5 and 0.75), both are non-dimensionalized by the cavity width. The results show that the average Nusselt number increases with the Rayleigh number but decreases with partition thickness. It is also found that the partition position has a negligible effect on the average Nusselt number for the whole range of Rayleigh number considered.

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1. Introduction

Conjugate natural convection in a differentially-heated, partitioned cavity with heat-conducting partition wall is present in various situations in nature and engineering, such as in solar thermal systems, electronic equipment, chemical reactors and buildings, and has attracted extensive research interest (see, e.g., [1–6]). The majority of the early studies have focused on the steady-state behaviour and assumed either a very thin partition (in particular a partition without thickness) or a partition with infinite thermal conductivity. The neglect of or the over-simplified assumptions about the coupling of the fluids on either side of the heat-conducting partition have been shown to lead to significant inaccuracy in prediction of the heat transfer coefficients (see, e.g., [7, 8]).

The numerical results of Ho and Yih [9] show that heat transfer in an air-filled partitioned rectangular cavity is considerably lower than that in a non-partitioned cavity, while the numerical study of Acharya and Tsang [10] shows that inclination angle also has a strong influence on the maximum Nusselt number. Turkoglu and Yücel [11] numerically simulated the flow and conjugate natural convection heat transfer in cavities with multiple conducting partitions and

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http://dx.doi.org/10.1016/j.icheatmasstransfer.2016.12.003 0735-1933/© 2016 Elsevier Ltd. All rights reserved.

conducting side walls and found that the increase of number of par-titions leads to the decrease of heat transfer whereas on the other hand the increase of the Rayleigh number results in increased heat transfer. However, they also found that the cavity aspect ratio has no significant bearing on heat transfer within the range considered. Cuckovic-Dzodzo et al. [12] made a numerical and experimental study on the laminar conjugate natural convection flow and heat transfer in a cubic enclosure with and without a heat conducting partition with glycerol as the working medium and the partition placed in the middle of the enclosure. Their results also show that the convective heat transfer in the partitioned cavity is reduced in comparison to that in the cavity without a partition, from 59.1% to 63.6% for the Rayleigh number in the range of 38,000 to 369,000. Sim-ilarly, Nishimura et al. [13] conducted a numerical and experimental study on the laminar conjugate natural convection in a rectangular enclosure divided by multiple vertical partitions. In this study, the thickness of the partitions was neglected in the numerical simula-tion and the partitions were equally spaced in the enclosure. Their numerical results reveal that the Nusselt number was inversely pro-portional to (1 + N), where N is the number of partitions, which was in agreement with their experimental results as well as the results obtained by Cuckovic-Dzodzo et al. [12].

Transient laminar natural convection in a partitioned enclosure with an adiabatic baffle and with the enclosure heated by uniform heat flux from left wall and cooled from right wall has been studied numerically by Fu et al. [14, 15]. They observed that for the Rayleigh number in the range of 10^4 to 10^6 the adiabatic baffle and the

Please cite this article as: M. Khatamifar et al., Conjugate natural convection heat transfer in a partitioned differentially-heated square cavity, International Communications in Heat and Mass Transfer (2016), http://dx.doi.org/10.1016/j.icheatmasstransfer.2016.12.003

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Rayleigh number have significant influence on the transient heat 133 134 transfer mechanism, with the largest effect occurring mainly in the first one-third of the transient stage, regardless of the presence or 135 136 location of a baffle. A numerical simulation of unsteady natural con-137 vection in a differentially heated cavity with a thin fin of different lengths on a sidewall at the Rayleigh number of 3.8×10^9 was 138 performed by Xu et al. [16]. They reported that the fin length signifi-139 140 cantly influences the transient thermal flow around the fin and heat transfer through the finned sidewall in the early stage. Xu [17] also 141 investigated the unsteady coupled thermal boundary layers induced 142 by a fin on the partition of a differentially heated cavity and demon-143 strated that the fin may induce a transition to unsteady coupled 144 thermal boundary layers and the critical Rayleigh number for the 145 occurrence of the transition was between $3.5 \times 10^8 - 3.6 \times 10^8$. 146

Xu et al. [18] classified unsteady natural convection flows in a 147 148 partitioned cavity into three distinct stages: the initial, transient 149 and steady-state stages. They examined the transient start-up char-150 acteristics of unsteady natural convection flows on both sides of 151 the partition, and found that the temperature distribution on the partition surrounded by the coupled convection boundary layers 152 is like that in a differentially heated cavity with isothermal side 153 154 walls. However, due to the presence of the partition, the volumetric 155 flow rate and heat transfer is reduced by 37% and 50%, respectively. A numerical study on the natural convection heat transfer in an 156 157 isosceles triangular enclosure having a vertical infinite conductivity 158 wall at the center was carried out by Saha and Gu [19]. Their results 159 support the flow classification of Xu et al. [18], and show that the 160 temperature distribution on the partition is similar to the isothermal cavity case at the transition stage and to the isoflux cavity case 161 at the steady state stage. Williamson et al. [20] investigated the 162 163 time-dependent oscillatory flow in a differentially heated rectangular cavity with an infinitely conducting vertical partition. They found 164 that the critical Rayleigh number for flow to become unstable is 165 dependent on the aspect ratio. 166

167 The effect of partition characteristics have been examined in 168 some previous studies. Ghosh et al. [21] examined the effect of 169 the partition position on the flow structure and heat transfer in a 170 rectangular cavity with a single thin partition, and found that for the Rayleigh number in the range of $10^3 - 10^7$, the partition loca-171 172 tion does not have a significant effect on the heat transfer. Tong and 173 Gerner [22] investigated the effect of the position of vertical partition in an air-filled rectangular enclosure. In the study, the partition 174 was assumed to have negligible thermal resistance and the Rayleigh 175 number was in the range of $10^4 - 10^5$. The results show that placing 176 177 the partition in the middle will result in the largest reduction in heat 178 transfer. Kahveci [23] extended the investigation by making more 179 realistic assumptions on the conducting partitions and examined the 180 effect of partition thickness, conductivity and position on the Nusselt 181 number of the steady-state laminar natural convection heat transfer 182 at relatively low Rayleigh numbers, over the range of 10^4 – 10^6 . It 183 is found that when the distance of the partition is increased from 184 the left wall towards the middle of the cavity, the average Nusselt number decreases asymptotically towards a constant value and the 185 partition thickness has negligible effect on the heat transfer. It is 186 also found that the variation of the thermal resistance of the par-187 188 tition leads to substantially different heat transfer changes, which was also found by Kangni et al. [24], who studied the effect of the 03 189 190 thermal resistance of the partition in a divided tall cavity with a finite thickness partition. Additionally, Kahveci [25] examined the effect 191 192 of aspect ratio on natural convection heat transfer in a partitioned 193 cavity and reported that the increase in the aspect ratio will result in 194 enhanced heat transfer.

From the literature review, it is revealed that the studies on 195 196 the effect of the partition on natural convection have been focused 197 on the centrally placed or thin partition or partition with infinite 198 thermal conductivity and at relatively low Rayleigh numbers over

narrow ranges. This motivates the current study which aims to 199 examine the effects of partition position and thickness on the 200 unsteady conjugate natural convection heat transfer in a differen-201 tially heated partitioned enclosure over a wide range of Rayleigh 202 203 numbers.

The remainder of this paper is organized as follows. The physical 204 system under consideration, the computational domain, the govern-205 ing equations, the initial and boundary conditions, the numerical 206 solution technique, and the benchmark results of the numerical solu-207 tions against the available solutions are briefly described in Section 2. 208 In Section 3, the major results of this study and the pertinent discus-209 sion are detailed. Finally, the conclusions are drawn in Section 4. 210

2. Numerical methodology

The physical system under consideration is a two-dimensional 215 partitioned rectangular cavity (with height H and width L and the 216 aspect ratio A = H/L), as illustrated in Fig. 1. The top and bottom 217 walls of the cavity are adiabatic and the left and right vertical walls 218 are isothermal fixed at T_h and T_c respectively ($T_h > T_c$, with the 219 dimensionless temperatures $\theta = 1.0$ and $\theta = 0.0$, respectively, 220 where $\theta = (T - T_c)/(T_h - T_c)$). A partition of thickness T_p is placed 221 at the location X_p from the left wall (both T_p and X_p are dimen-222 sionless, made dimensionless by L). The working fluid is assumed 223 to be air (Pr = 0.71, where Pr is the Prandtl number as will be 224 defined by Eq. (5)), which is initially quiescent and at a temperature 225 of $(T_h + T_c)/2$ (*i.e.*, at the dimensionless temperature $\theta = 0.5$). All 226 the interior walls and the partition surfaces are rigid and no-slip. The 227 partition wall is heat conducting, with finite thermal conductivity k_s . 228

The transient flow of fluid within the cavity is governed by 229 the two-dimensional Navier-Stokes equations with the Boussinesq 230 approximation for buoyancy which, together with the temperature 231 equation, can be written in dimensionless forms in Cartesian coordi-232 nates as follows, 233

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0,$$



Fig. 1. Schematic of the physical system under consideration, the computational domain and the initial and boundary conditions.

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