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An experimental investigation of flow structure and heat transfer in an impinging annular jet*

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ABSTRACT

The paper presents the results of an experimental study of flow and heat transfer in an impinging annular jet. 14 Using the PIV-system the distribution of average and pulsation velocities was measured; and heat fluxes and 13 their pulsations were detected using miniature heat flux sensors. The measurement results have been compared 16 at identical mass flow rate of air with similar data for a round jet with a diameter equal to the outer diameter of 17 the annular jet. It is shown that under these conditions of comparison the values of velocity and turbulent 18 pulsations in the annular jet are significantly higher than the same values in the round jet. The heat transfer 19 intensity of the impinging annular jet is also higher than that of the round jet, and the degree of heat transfer 20 enhancement depends on the annular gap size and distance from the nozzle to the obstacle. 21

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32 1. Introduction

The impinging jets are widely used in modern cooling systems. In 33 this regard, the issue of increasing their efficiency is important. One of 34the known ways to increase the intensity of heat removal by impinging 35jets is to change the geometry of the nozzle through which the cooling 36 medium is supplied. This problem is actively studied in a large number 37 of experimental and numerical works [1–3]. The goal of these studies is 38 the search for possible ways to expand the region of higher heat transfer 39 in the zone of jet stagnation and for a more uniform distribution of the 40 heat transfer coefficient. Such opportunities may be realized for the 41 annular impinging jets. This is evidenced by data of the first experimen-42 43 tal work [4], dedicated to the comparative analysis of heat transfer in the annular and round jets. The authors determined that at the same 44 coolant flow rate the impinging annular jets with the ratio of inner to 45outer diameter $d_2/d_0 = 0.3$ and 0.6 can give a more intense heat transfer 4647 than the round ones with an identical external diameter.

It should be noted that even free annular jets have complex flow structures. Even more complex are the impinging annular jets. This follows from the works [5–7], devoted to the experimental study of flow fields and mass transfer of the impinging annular jets at a close location of the nozzle and obstacle ($S/d_0 \le 2$, where S is the distance between the nozzle and the obstacle), when the vortex structures formed behind the nozzle interact directly with the streamlined wall.

The conditions of experiments [5] were the following: the ratio of the internal diameter of the ring to the outer one was $d_2/d_0 = 0.77$

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http://dx.doi.org/10.1016/j.icheatmasstransfer.2016.10.011 0735-1933/© 2016 Published by Elsevier Ltd. and 0.95, and the values of the Reynolds number, calculated based on 57 parameters at the nozzle outlet, were $Re = U_0 d_0 / \nu_0 = 5 \cdot 10^3 \div 10^4$. 58 This work showed that two alternative flow patterns (bistability) are 59 possible for the impinging annular jets in the studied conditions. In 60 one case, a rather small region of recirculation was formed behind the 61 central insert of the nozzle, and in the other case, the recirculation 62 region behind the nozzle became much larger and extended all the 63 way to the streamlined wall, forming therein an annular line of stagna- 64 tion. According to the results of [5,6], bistability occurred only for a nar- 65 row annular nozzle (in the experiments [5] it was observed when the 66 ratio of the inner to the outer diameter of the nozzle was $d_2/d_0 = 67$ 0.95) at low values of Reynolds number ($Re \leq 5 \cdot 10^3$) and small 68 distances between the nozzle and the wall ($S/d_0 \approx 1$). The instability 69 of the flow pattern in the regime of bistability led to a spontaneous 70 transition from one flow pattern to another and to stratification of the 71 pressure and heat transfer distributions. 72

Similar experimental studies were conducted by the authors of [7]. 73 Conditions of experiments were the following: the ratio of the 74 diameters was $d_2/d_0 = 0.8 \div 0.98$, the Reynolds number $Re = (d_0 - 75$ $d_2)U_0/2\nu = 1.2 \cdot 10^3 \div 3.6 \cdot 10^4$, and U_0 was the mean flow velocity at 76 the nozzle outlet. The authors noted an interesting phenomenon of 77 the impinging annular jets, namely an appearance of a reverse (against 78 the direction of the incident jet) flow in the frontal point. According to 79 the findings of [7], three different variants of the obstacle streamlining 80 are formed depending on the distance S/d_0 . They differ in the radial 81 position of the stagnation point on the obstacle and in the heat transfer 82 intensity. 83

When comparing the efficiency of cooling by the annular and round 84 jets, the conditions of comparison become vital. In terms of technical ap- 85 plication it is logical to compare the various nozzles provided at the 86

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T1.1	Nomenclature	
T1.2	r	Radial coordinate (mm)
T1.3	х	Distance from the nozzle to the considered cross-
T1.4		section (mm)
T1.5	x _p	Distance from the obstacle to the cross-section (mm)
T1.6	d_0	Diameter of the base round nozzle; the outer diameter
T1.7		of the annular nozzle (mm)
T1.8	d_2	Inner diameter of the annular nozzle (mm)
T1.9	S	Distance from the nozzle to the barrier (mm)
T1.10	T_0 , T_w	Flow temperature at the nozzle outlet and temperature
T1.11		of the barrier (°C)
T1.12	$q_{ m i}$, $q_{ m w}$	Local heat flux density: instantaneous and averaged on
T1.13		data array (W/m ²)
T1.14	U _{0r} , U _{0an}	5
T1.15		zles (m/s)
T1.16	<i>Re</i> _{0r} , <i>Re</i> _{0an} Reynolds number of the round and annular nozzles	
T1.17		$(U_{0r} d_0 / \nu_0 \text{ and } U_{0an} d_0 / \nu_0)$
T1.18	Pr	Prandtl number
T1.19	Nu_0	Nusselt number for the stagnation point of the obstacle
T1.20		$(lpha_0 d_0 / \lambda_0)$
T1.22	Greek	
T1.23	$lpha$, ($lpha_0$)	Heat transfer coefficient, (heat transfer coefficient in the
T1.24		frontal point of the obstacle) (W/m ² $^{\circ}$ C)
T1.25	λ_0	Coefficient of thermal conductivity of air at temperature
T1.26		$T_0 (W/m °C)$
T1.27	ν_0	Coefficient of kinematic viscosity at temperature T_0
T1.29		(m ² /s)
T1.30	Subscripts	
T1.31	0r	Corresponds to the output cross-section of the round
T1.32		nozzle
T1.33	0an	Corresponds to the exit section of the annular nozzle

same mass flow of refrigerant. If the areas of the outlet cross-sections of 87 the nozzle are the same as well, the velocities at their section and the 88 integral values of the jet pulses, respectively, are also equal. This situa-89 90 tion is possible only when the diameter of the round jet and the inner 91diameter of the annular jet are identical, while its outer diameter should be equal to $d_0 = \sqrt{2} \cdot d_2$. Identical impulses at the nozzle outlet were in-9293 vestigated in [8], where the annular and round impinging laminar jets were studied numerically. The distribution of friction and heat transfer 9495for the annular jet significantly differs from the same distribution for the round jet by the presence of a region of negative friction (the flow 96 is directed from the periphery to the center) and by a substantial 97 decrease in the heat transfer intensity in the axial region for the annular 98 jets. As a result, if the average heat transfer is compared under the above 99 100 conditions, then its intensity for the annular jet is \approx 20% lower than for 101 the round one. This conclusion, at first glance contradicting the data of 102work [4], where the heat transfer intensity for the annular jet is much higher than that for the round one, indicates the fundamental 103 importance of the conditions of comparison of the impact cooling 104 efficiency. It is appropriate to emphasize that the problem of choosing 105the governing parameters has not been completely solved even for the 106 classical axisymmetric jet that is noted in particular in [9]. 107

A detailed experimental study of characteristics of flow and heat transfer in the impinging annular jets at small distances from the nozzle to the obstacles $S/d_0 \le 1$ was made in [10] with the variation of parameter $d_2/d_0 = 0.51 \div 0.9$ with a fixed outer diameter. Measurements taken with thermal anemometer and liquid crystals showed that when reducing the height of the annular gap the intensification of heat transfer takes place. The obtained experimental results were generalized using correlations, describing the distribution of *Nu* along 115 the radius for different slit parameters. However, these relations are 116 valid only at small distances between the nozzle and the surface. 117

It should be noted that the problem of flow and heat transfer in the 118 impinging annular jets is of great practical interest to create the burner 119 spray, since the central stagnant zone is a good stabilizer of combustion 120 [11,12]. A special place in this problem belongs to the study of swirling 121 annular [13–15] and coaxial [16,17] jets. With jet swirling the 122 mechanisms of transfer processes become much more complicated, 123 and the intensity of heat and mass transfer largely depends on the 124 level of centrifugal forces. As a rule, an increase in the swirling leads to 125 the suppression of heat exchange due to more intense mixing of the 126 impinging jet with the ambient medium [18]. However, at small 127 distances between the nozzle and the obstacle, the swirl can cause the 128 enhancement of heat transfer as well [14]. In general, this research 129 area is of independent interest, and more details on the issue may be 130 found in several monographs and reviews [19–21].

This article presents the results of experimental studies of flow and 132 heat transfer in the impinging annular jet with variation of the ring pa-133 rameters, the Reynolds number and the distance from the nozzle to the 134 obstacle. As shown in [22], the annular jet is characterized by a number 135 of features in comparison with the round jets. The most important of 136 them are the presence of the axial separation zone, the development 137 of the internal mixing layer and the resulting global instability of the 138 entire jet.

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2. Description of setup and measurement methods

The experiments were carried out on the set-up, whose scheme is 141 shown in Fig. 1. Main elements of the set-up were the system of feeding, 142 adjustment and measurement of air flow, the test section, including the 143 nozzle forming a jet and the barrier, and two instrument units for 144 studying flow fields and heat transfer. The working medium was the 145 air coming from the high-pressure air net. In the experiments, the 146 impinging jets of round and annular cross-sections were studied. 147 Round jets were used to obtain "baseline". It served for comparison 148 with the data for the impinging annular jet that allowed identifying 149 the effects associated with the nozzle geometry. The round nozzle was 150 characterized by: the total length of the nozzle – 72 mm, the length of 151 the tapering part (L_1) – 67 mm, the height of the centering ring (L_2) – 152 5 mm, the diameter of the nozzle up to tapering (d_1) – 62 mm, tapering 153 of the nozzle 12.1, and the output diameter $d_0 = 17.8$ mm. For forming 154 an annular cross-section the cylindrical rod of varying diameter d_2 (see 155

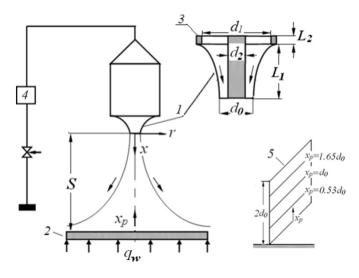


Fig. 1. The scheme of experimental set-up: 1 – nozzle; 2 – obstacle; 3 – centering insert; 4 – flowmeter; and 5 – the measuring plane.

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