



## Novel methods of oil fouling inhibition on surface of plate heat exchanger in simulated oilfield geothermal water



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### ABSTRACT

Crude oil fouling on heat transfer surface (HTS) is a very troublesome problem for the utilization of oilfield geothermal water in which slight crude oil exists. The deposition of crude oil on HTS will decrease heat transfer efficiency, increase the pressure drop of fluid flow, and even block flow channel. In this study, surface hydrophilization via anodization, flow velocity enhancement and chemical addition three measures were adopted to solve the problem of crude oil soiling via weakening the adhesion force between crude oil and HTS as well as intensifying the interaction between water and crude oil. Contact angle measurement and microscopic morphology study were conducted on the highly-hydrophilic surface fabricated via anodization. Oil-soiling experiments accompanied with three mentioned techniques were carried out in plate heat exchanger (PHE) apparatus, and obvious oil-fouling inhibition effects were presented. The effect was reflected by the decrease of fouling thermal resistance. For 110 °C simulated oilfield geothermal water, which contained approximate 1 vol.% crude oil soiling, with 0.24 m/s flow velocity, the fouling induction period extended to 500 min from 0 min when surface hydrophilization was applied through anodization. In anodized PHE with titanium plates, the value of fouling thermal resistance decreased by about 77.8% when the flow velocity of 110 °C hot fluid without chemical additive increased from 0.24 m/s to 0.72 m/s, and the value could be reduced by around 62.5% after the addition of 0.29 g/L chemical additive LIUXU-10 mainly composed of sodium dodecyl sulfonate (SDS), when the flow velocity of 110 °C hot fluid was 0.12 m/s. Compared with PHE with titanium plates (Ti-PHE) at 0.24 m/s hot fluid flow velocity, the fouling thermal resistance decreased by approximate 93.3% when the Ti-PHE was anodized to be highly hydrophilic, the hot fluid flow velocity increased to 0.6 m/s and 0.87 g/L chemical additive was added.

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### 1. Introduction

Due to the excessive exploitation of fossil energy such as petroleum and natural gas, people start to seek newer substituted energy source. With the advantages of wide distribution, abundant reserves, low cost and low contamination, geothermal energy gradually becomes a kind of potential new energy [1]. While scaling or fouling in heat exchanger is a ubiquitous problem existing in the utilization of geothermal source. Fouling problems, which cause severe decrease of heat transfer coefficient in heat

exchanger, exist in about 90% heat exchangers [2] and bring economic loss which takes up to 0.25% of GNP (Gross National Product) at developed country [3]. Therefore, it is very necessary to understand the process of fouling deposition and exploit new methods to solve the heat exchanger fouling problems.

Plenty of researches have been focused on the fouling behaviors through experiments or modelling [4–8]. Besides, many antifouling methods have also been attempted to mitigate the fouling attachment on HTS. These methods include electromagnetism antifouling technology [9–11], ultrasonic antifouling technology [12,13], optimizing operation parameters or HTS textures [5,14,15], physical or chemical addition [16–19], and surface coating [20–34]. For electromagnetism antifouling technology, the scaling will become fragmented and loose under electric field, which contributes to the fouling mitigation on HTS [11]. For ultrasonic antifouling

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## Nomenclature

$A_0$	effective heat transfer area (m <sup>2</sup> )	$\Delta P$	pressure drop between hot fluid outlet and hot fluid inlet (kPa)
$A'$	projected heat transfer area (m <sup>2</sup> )	$\Delta P_f$	friction pressure drop of hot fluid (Pa)
$C_p$	fluid specific heat capacity at constant pressure (J/(kg·K))	$\Delta P_h$	flow channel pressure drop of hot fluid in PHE without fouling deposition (Pa)
$C_{p,h}$	hot fluid specific heat capacity at constant pressure (J/(kg·K))	$\Delta P'_h$	flow channel pressure drop of hot fluid in PHE with fouling deposition (Pa)
$C_{p,c}$	cold fluid specific heat capacity at constant pressure (J/(kg·K))	$\tau_f$	friction shear stress (N)
$C, K_p, z$	constants	$\Delta G_{SWO}^T$	interfacial free energy between solid surface and oil surface in aqueous medium (mJ/m <sup>2</sup> )
$D_p$	port diameter (mm)	$\Delta G_{SO}^T$	interfacial free energy between solid surface and oil surface (mJ/m <sup>2</sup> )
$d_e$	equivalent diameter of fluid channel in PHE (m)	$\Delta G_{OO}^T$	interfacial free energy between oil surface and oil surface (mJ/m <sup>2</sup> )
$f_p$	mean cross-sectional flow area per channel (m <sup>2</sup> )	$\theta_1$	water contact angle on substrate (°)
$f$	friction coefficient	$\theta_2$	glycerol contact angle on substrate (°)
$H$	corrugation amplitude or mean channel spacing (mm)	$\theta_3$	diiodomethane contact angle on substrate (°)
$h$	mean flow channel spacing (m)	$\theta_{OW}$	intersection angle between solid-oil interfacial tension and oil-water interfacial tension (°)
$L_v$	vertical distance between centers of ports (mm)	$\theta_{PTFE}$	contact of water with the addition of LIUXU-10 on PTFE (°)
$L_h$	horizontal distance between centers of ports (mm)	$\theta_{PMMA}$	contact of water with the addition of LIUXU-10 on PMMA (°)
$L_w$	plate width inside gasket (mm)	$\gamma_S^{LW}$	Lifshitz-van der Waals component of surface energy for substrate (mJ/m <sup>2</sup> )
$L_{eff}$	effective flow length in PHE (m)	$\gamma_W^{LW}$	Lifshitz-van der Waals component of surface tension for water (mJ/m <sup>2</sup> )
$l$	length of fluid flow (m)	$\gamma_O^{LW}$	Lifshitz-van der Waals component of surface tension for oil soiling (mJ/m <sup>2</sup> )
$M$	number of passes in PHE	$\gamma_S^+$	electron-acceptor component of surface energy for substrate (mJ/m <sup>2</sup> )
$P$	corrugation pitch (mm)	$\gamma_W^+$	electron-acceptor component of surface tension for water (mJ/m <sup>2</sup> )
$Pr_f$	fluid Prandtl number	$\gamma_O^+$	electron-acceptor component of surface tension for oil soiling (mJ/m <sup>2</sup> )
$Pr_h$	hot fluid Prandtl number	$\gamma_S^-$	electron-donor component of surface energy for substrate (mJ/m <sup>2</sup> )
$Pr_c$	cold fluid Prandtl number	$\gamma_W^-$	electron-donor component of surface tension for water (mJ/m <sup>2</sup> )
$Q_c$	heat transfer load of cold fluid (W)	$\gamma_O^-$	electron-donor component of surface tension for oil soiling (mJ/m <sup>2</sup> )
$R_f$	fouling thermal resistance ((m <sup>2</sup> ·K)/W)	$\gamma_S^{\bar{}}$	electron-donor component of surface energy for substrate (mJ/m <sup>2</sup> )
$Re_f$	fluid Reynolds number	$\gamma_W^{\bar{}}$	electron-donor component of surface tension for water (mJ/m <sup>2</sup> )
$Re_h$	hot fluid Reynolds number	$\gamma_O^{\bar{}}$	electron-donor component of surface tension for oil soiling (mJ/m <sup>2</sup> )
$Re_c$	cold fluid Reynolds number	$\gamma_{SW}$	solid-water interfacial tension (mN/m)
$R_a$	arithmetical mean deviations of profile (μm)	$\gamma_{SO}$	solid-oil interfacial tension (mN/m)
$T_{h,i}$	hot fluid inlet temperature (°C)	$\gamma_{OW}$	oil-water interfacial tension (mN/m)
$T_{h,o}$	hot fluid outlet temperature (°C)	$\gamma_{water}^{LW}$	Lifshitz-van der Waals component of surface tension for water with the addition of LIUXU-10 (mJ/m <sup>2</sup> )
$T_{c,i}$	cold fluid inlet temperature (°C)	$\gamma_{water}^+$	electron-acceptor component of surface tension for water with the addition of LIUXU-10 (mJ/m <sup>2</sup> )
$T_{c,o}$	cold fluid outlet temperature (°C)	$\gamma_{water}^-$	electron-donor component of surface tension for water with the addition of LIUXU-10 (mJ/m <sup>2</sup> )
$U$	overall heat transfer coefficient (W/(m <sup>2</sup> ·K))	$\gamma_{water}$	surface tension for water with the addition of LIUXU-10 (mN/m)
$U_0$	initial overall heat transfer coefficient (W/(m <sup>2</sup> ·K))	$\gamma_{PTFE}^{LW}$	Lifshitz-van der Waals component of surface energy for PTFE (mJ/m <sup>2</sup> )
$V$	volumetric flow rate of fluid (m <sup>3</sup> /s)	$\gamma_{PMMA}^{LW}$	Lifshitz-van der Waals component of surface energy for PMMA (mJ/m <sup>2</sup> )
$V_h$	volumetric flow rate of hot fluid (m <sup>3</sup> /s)	$\gamma_{PMMA}^{\bar{}}$	electron-donor component of surface energy for PMMA (mJ/m <sup>2</sup> )
$v_h$	flow velocity of hot fluid (m/s)		
$V_c$	volumetric flow rate of cold fluid (m <sup>3</sup> /s)		
<b>Greek symbols</b>			
$\delta$	plate sheet thickness (mm)		
$\Phi$	enlargement factor		
$\rho$	fluid density (kg/m <sup>3</sup> )		
$\rho_h$	density of hot fluid (kg/m <sup>3</sup> )		
$\rho_c$	density of cold fluid (kg/m <sup>3</sup> )		
$\eta$	experimental relative error of overall heat transfer coefficient (%)		
$\alpha$	convective heat-transfer coefficient (W/(m <sup>2</sup> ·K))		
$\alpha_h$	convective heat-transfer coefficient of hot fluid (W/(m <sup>2</sup> ·K))		
$\alpha_c$	convective heat-transfer coefficient of cold fluid (W/(m <sup>2</sup> ·K))		
$v$	fluid flow velocity in PHE channel (m/s)		
$v_h$	hot fluid flow velocity in PHE channel (m/s)		
$\mu_f$	fluid viscosity in flow channel of PHE (Pa·s)		
$\mu_w$	fluid viscosity at wall temperature in PHE (Pa·s)		
$\mu_h$	hot fluid viscosity in flow channel of PHE (Pa·s)		
$\mu_c$	cold fluid viscosity in flow channel of PHE (Pa·s)		
$\lambda_f$	fluid thermal conductivity (W/(m·K))		
$\lambda_h$	hot fluid thermal conductivity (W/(m·K))		
$\lambda_c$	cold fluid thermal conductivity (W/(m·K))		
$\lambda$	thermal conductivity of titanium (W/(m·K))		
		<b>Subscripts</b>	
		$c$	cold fluid
		$p$	constant pressure
		$e$	equivalent
		$v$	vertical
		$h$	horizontal/hot fluid

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