



## Improvement of hydrogen production from glucose by ferrous iron and biochar



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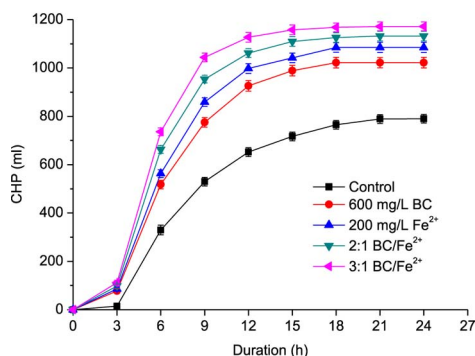
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### GRAPHICAL ABSTRACT

Effects of biochar (BC) and ferrous iron ( $\text{Fe}^{2+}$ ) additions on hydrogen ( $\text{H}_2$ ) production from glucose were investigated. Results showed that suitable  $\text{Fe}^{2+}$  concentration could enhance [Fe-Fe]-hydrogenase activity, while BC addition could facilitate hydrogen-producing bacteria growth. Both of them could synergistically improve  $\text{H}_2$  production, indicating a simple, cost effective and practical process.

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### ABSTRACT

Effects of biochar (BC) and ferrous iron ( $\text{Fe}^{2+}$ ) additions on hydrogen ( $\text{H}_2$ ) production from glucose were investigated using batch experiment. The glucose with both BC and  $\text{Fe}^{2+}$  additions were incubated at 37 °C for  $\text{H}_2$  production. As compared with the control group (without BC and  $\text{Fe}^{2+}$  additions), the synergic effects of BC and  $\text{Fe}^{2+}$  make the lag phase time decrease from 4.25 to 2.12 h, and  $\text{H}_2$  yield increase from 158.0 to 234.4 ml/g glucose. Moreover, suitable concentrations of BC and  $\text{Fe}^{2+}$  serve to enhance volatile fatty acid generation during  $\text{H}_2$  evolution. These results indicate that  $\text{H}_2$  production is improved by BC and  $\text{Fe}^{2+}$  regulations, where synergic mechanisms are described as follows: BC acts as support carriers of anaerobes and system pH buffers, which promotes the biofilm formation and maintains suitable pH environment; Appropriate  $\text{Fe}^{2+}$  concentration can improve hydrogenase activity in  $\text{H}_2$  production.

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## 1. Introduction

The combustion of fossil fuel has been predominated approximately 80% of the global energy consumption since the industrialized era (Chen et al., 2008). Besides, in the last decade the huge increase in world energy consumption has taken place, which will continue to occur in the next fifty years (Lucas et al., 2015), due to modernization and population increase (Lucas et al., 2015). Hydrogen ( $H_2$ ) has been widely considered as an available alternative energy carrier due to its effectiveness and cleanness. However, over 96% of world  $H_2$  production relies on fossil fuels, resulting in environmental pollution and energy crisis (Zhang et al., 2015a). Thus, it is urgent to develop other techniques for  $H_2$  production in a sustainable, cost effective and eco-friendly way. Among various  $H_2$  production methods, biological processes like photosynthesis microbial electrolysis cells and fermentation can provide  $H_2$  from abundant and cheap sources like organic wastes from biorefinery industries (Zhang et al., 2015a). Moreover, dark fermentation for  $H_2$  production requires less energy compared to other  $H_2$  processes. Bio- $H_2$  techniques mainly include dark fermentation process and photosynthetic  $H_2$  production. Compared to photosynthetic  $H_2$  production, dark fermentation process has evolved to the cutting-edge technology due to its economic efficiency, operation simplicity, and its independence on the availability of solar irradiation. Bio- $H_2$  production via dark fermentation also reveals the advantages of sustainable energy and carbon balance. Nonetheless, the major drawbacks of this technique are lower microbial conversion efficiency of substrate into  $H_2$  and large amounts of  $CO_2$  emissions.

Dark fermentation for  $H_2$  has been established for several decades, but it still needs to be optimized in the case of process stability, inhibition problems and higher  $H_2$  yields (Bundhoo and Mohee, 2016). Theoretically, the complete bioconversion of glucose into  $H_2$  could give 1493 ml  $H_2$ /g glucose (12-mol  $H_2$ /mol glucose). However, during the practical conversion there are no known existing anaerobes and metabolic pathways that may be capable of doing that and practical  $H_2$  yields appear to be limited to 4-mol (498 ml)  $H_2$ /mol glucose (Hallenbeck, 2009). A well-known issue concerning  $H_2$  fermentation from carbon-rich organic materials such as food waste, cane molasses, starch wastewater, fruit and vegetable wastes, is inhibition due to the vulnerability of fermentation micro-ecology. Many efforts have aimed to enhance the enrichment and activity of anaerobic microbes, and the additions of carrier and some trace elements are regarded as necessary measures (Mumme et al., 2014; Luo et al., 2015; Zhang et al., 2013). In addition, to improve  $H_2$  yield by dark fermentation, previous reports have focused on metabolic bioengineering (e.g., over-expression of hydrogenase) and key parameter optimization such as microbial selection and pH regulation (Zhang et al., 2011).

Recently, considerable attention has been paid to the potential application of carbon-rich material as carbon sequestration, soil amendment and pollutant remediation (Ahmad et al., 2014). The material is produced by thermal decomposition and recognized as biochar (BC) that is expected to improve crop productivity and reduce greenhouse gas emission. However, the broad application of BC is impeded due to relatively high costs (Roberts et al., 2010). It is necessary to overcome this major drawback in order to obtain economic benefits via expanding the BC value chain. For example, BC was served as an additive that increased biogas production in anaerobic digestion due to its ability to promote bio-film formation and mitigate acid and ammonia inhibition (Gong et al., 2011; Mumme et al., 2014). 10 g/L of BC addition to mesophilic anaerobic bioreactor inoculated with anaerobic granules and fed with 4 g/L glucose significantly increased maximum methane ( $CH_4$ ) production rate by 86.6% and decreased methanogenic lag phase time by 30.3% than the control test without BC (Luo et al., 2015). Another similar report about the improvement of  $H_2$  production from organic fraction of municipal solid waste by BC addition showed that BC addition shortened lag phase time from  $12.5 \pm 0.6$  h at control without BC to  $8.1 \pm 0.5$  h with 12.5 g/L BC and harvested maximum

$H_2$  yield of  $96.63 \pm 2.8$  ml  $H_2$ /g carbohydrates (Sharma and Melkania, 2017). There was a slight difference in optimal concentrations of BC, which was likely due to the main differences in substrate, inoculum and their metabolic pathways. Sunyoto et al. (2016) also found that BC addition could reduce the lag phase time of bio- $CH_4$  by 21.4–35.7%, and it further increased the subsequent  $H_2$  production potential by 14.2–31.0%. These reports indicated that porous BC would provide a relatively big surface area for the adhesion and growth of anaerobes and reduce the inhibition behavior by absorbing inhibitors (Wang and Han, 2012). However, there have been limited investigations on the application of BC for the fermentative production of organic acids or  $H_2$ .

Besides, some elements such as sodium (Na), magnesium (Mg), zinc (Zn) and iron (Fe) are essential micronutrients for bacterial metabolism, affecting hydrogen production. Among them Fe is a vital micronutrient, which acts as the co-factor for Fe-S protein and hydrogenase (Junelles et al., 1998). Wide varieties of prokaryotes contain hydrogenase that functions in the treatment of excess electrons by  $H_2$  formations. The Fe-S protein in ferredoxin serves as an electron carrier during pyruvate oxidation into  $CO_2$  and acetyl CoA (Schonheit et al., 1979). The addition of zero-valent iron ( $Fe^0$ ) was shown to obtain 38.2% more  $H_2$ , and the coupled system of activated carbon and  $Fe^0$  could further improve  $H_2$  yield (50.2%) (Zhang et al., 2015a). The maximum  $H_2$  yields of 140.6 ml and 145 ml/g glucose were observed at 50 mg/L of  $Fe^{2+}$  by Karadag and Puhakka (2010) and Wu et al. (2017), respectively, while the maximum  $H_2$  yield of 131.9 ml/g glucose was obtained at 352 mg/L of  $Fe^{2+}$  in another previous study (Lee et al., 2001). Although the optimal  $Fe^{2+}$  concentrations for different bio- $H_2$  production processes were not the same, these studies showed that shortage of iron could limit the activities of hydrogen-producing bacteria (HPB). Moreover, a suitable concentration of iron in batch process can help to raise  $H_2$  yield at various temperatures (Zhang and Shen, 2006). Li et al. (2009) compared the  $H_2$  yield from glucose by supplementing  $Fe^0$  and  $Fe^{2+}$ , respectively. They found that  $Fe^0$  played a better role in promoting bio- $H_2$  production than  $Fe^{2+}$ , and the inhibition of high concentration of  $Fe^0$  to HPB was lower than that of  $Fe^{2+}$  (Li et al., 2009). The maximum  $H_2$  conversion efficiency of 353.5 ml  $H_2$ /g COD was harvested under the optimized conditions of 7000 mg COD/L, 150 mg  $Fe^0$ /L and pH of 5.5 (Yogeswari et al., 2016).  $Fe^0$  is essential for enriching the dominant HPB (Yogeswari et al., 2016). However, the corrosion of  $Fe^0$  strongly depends on solution pH, and ferrous oxides formed on  $Fe^0$  surface may lower the activity of iron (Zhang et al., 2015a). Furthermore, it is difficult to treat the fermentation residue containing  $Fe^0$ . Multiple lines of evidences indicate that the application of BC or Fe in anaerobic fermentation might be beneficial. Nonetheless, related studies are largely unavailable, and some essential mechanisms are unclarified, especially the synergic effects of  $Fe^{2+}$  and BC.

To the best of our knowledge, there has been no report on the synergic behaviors of BC and  $Fe^{2+}$  in  $H_2$  fermentation until date. Hence, this study was conducted to assess the performances of BC/ $Fe^{2+}$  system in bio- $H_2$  process and to investigate the mechanism of improving  $H_2$  production in such eco-system. To achieve this aim, the effects of  $Fe^{2+}$  and BC concentrations on  $H_2$  fermentation from glucose medium were firstly investigated. Then the improvement of  $H_2$  production by BC/ $Fe^{2+}$  system was evaluated, which was compared with adding BC and  $Fe^{2+}$ , respectively. Finally, the possible mechanisms of increase in  $H_2$  yield and process stability were clarified.

## 2. Materials and methods

### 2.1. Anaerobic sludge and materials

Corn-bran residue (CBR) was obtained from a cornstarch plant in Shandong, China. The CBR was dried and crushed in order to keep its sizes ranging from 60 to 120 mesh (Zhang and Zheng, 2015). After that, it was used to produce BC at 600 °C with heating rate of 5 °C/min. Both

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