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Thermal issues about Li-ion batteries and recent progress in battery thermal management systems: A review



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ABSTRACT

Electrical vehicles have the capability to lessen the severe threats of energy crisis and environment pollution. The Lithium ion battery as a promising solution for the energy storage in vehicular applications is briefly introduced in this paper. The adverse effects of improper temperature, including performance degradation, potential thermal runaway, temperature non-uniformity and low temperature performance are described afterwards. The thermal model, electrochemical model, equivalent circuit model and electrochemical/electrical-thermal coupling methods are also elaborated for the accurate battery modeling. More importantly, this review detailedly summarizes the progress on battery thermal management systems (BTMSs) including the air, liquid, boiling, heat pipe and solid-liquid phase change based strategies during recent years. Influence factors and development focus of different BTMSs are stated elaborately. Passive cooling systems utilizing the latent heat during the phase change process are more attractive options compared to the conventional single phase forced air and liquid cooling methods. However, there still exist some challenges to be addressed before commercializing. In addition, different methods could be combined to meet the requirements of various applications. The improvement of these existing BTMSs is supposed to be paid more attention to enhance Li-the performance and safety of Li-ion batteries.

1. Introduction

Nowadays, people all over the world are being posed to the threat of energy crisis and severe environment pollution. However, driven by the growing improvements in economic levels, the global demands for energy resources, especially for the fossil fuels (e.g. oil), are still rising rapidly. According to the statistics from BP Statistical Review of World Energy 2016 [1] and BP Energy Outlook 2016 [2], the global oil consumption grew by 1.9 million barrels per day, nearly two-thirds of which was attributed to the transportation sector. To reduce the emissions of pollutants and greenhouse gases, increasing attentions have been paid to the development of clean energy vehicles, including pure electric vehicles (EV), hybrid electric vehicles (HEV) and plug-in hybrid electric vehicles (PHEV), which are more energy-efficient and environment friendly than the traditional internal combustion engine systems [3]. Anderson et al. [4] indicated that the employment of EVs could bring about a remarkable reduction of greenhouse gas emissions by almost 40% if the electric power resources are renewable (e.g. solar, wind, etc.).

The key task of developing clean energy vehicles is to find a suitable

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energy storage system which can support high driving mileage and fast acceleration. Various power batteries have been proposed, such as leadacid (Pb-acid), nickel based, sodium based and lithium-ion (Li-ion) batteries [9]. Some key indicators for evaluating these battery systems are listed in Table 1. Among all these electrochemical systems, Li-ion batteries are the most promising choices for EVs and HEVs due to their superior characteristics of high specific energy and power, long cycling life, and low self-discharge rates, as indicated in Table 1. Therefore, Li-ion batteries have been widely employed in our daily lives, including wrist watches, smart phones, laptops and many other portable electronics [10].

However, in spite of its attractive prospect, Li-ion battery based EVs have not been widely adopted by consumers. The major hindrances in regard with the battery system include the high cost, limited calendar life, safety concerns, and the temperature-caused degradation [11]. Currently, extensive efforts have been made to find better electrode materials to enhance the specific energy, specific power and lifetime. However, the research in the thermal issues of Li-ion batteries under various conditions and the development of battery thermal management systems (BTMSs) have not been adequately addressed although

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| Nomenclature | | | velocity of solvent | | | |
|------------------------|---|--------------------|--|--|--|--|
| | | Т | temperature, K | | | |
| a_s | specific interfacial area of solid phase, $m^2 m^{-3}$ | U_L | load voltage, V | | | |
| Α | surface area of active material, m ² | U_{OC} | open-circuit potential, V | | | |
| A_s | cell surface area exposed to the convection coolant, m^2 | U_{RC} | voltage across the RC network, V | | | |
| B_i | Biot number | V | cell operating voltage, V | | | |
| Ce | concentration of lithium ions in electrolyte phase, | | | | | |
| | $mol m^{-3}$ | Greek s | ymbols | | | |
| c_s | concentration of lithium ions in solid phase, mol m^{-3} | | | | | |
| C_0 | battery capacity, A h | α_a | transfer coefficient of anode | | | |
| C_n | battery specific heat capacity, $J \text{ kg}^{-1} \text{ K}^{-1}$ | α_c | transfer coefficient of cathode | | | |
| D_s | mass diffusion coefficient of lithium in solid phase, $m^2 s^{-1}$ | σ | Stefan-Boltzmann constant, 5.67 $	imes$ 10 ⁻⁸ W m ⁻² K ⁻⁴ | | | |
| E_a | activation energy, J | $\sigma^{e\!f\!f}$ | effective electronic conductivity of the solid phase, S m^{-1} | | | |
| f. | molecular salt activity coefficient | ρ | battery density, kg m $^{-3}$ | | | |
| $\overset{J_{\pm}}{F}$ | faraday constant, 96,485 C mol ^{-1} | λ | thermal conductivity, $W m^{-1} K^{-1}$ | | | |
| h | heat transfer coefficient, W m^{-2} K ⁻¹ | ε | emissivity of the cell surface | | | |
| h_{s} | cell heat transfer coefficient, W m ^{-2} K ^{-1} | ε _e | volume fraction/porosity of electrolyte | | | |
| i | current per unit volume A m^{-3} | ø | angle in cylindrical-coordinate system, rad | | | |
| i, | current density in electrolyte phase. A m^{-2} | , Ø. | potential in the solid phase. V | | | |
| i, | transfer current density. A m^{-2} | ø, | potential in the electrolyte phase. V | | | |
| i | exchange current density. A m^{-2} | n | surface overpotential. V | | | |
| i. | current density in solid phase. A m^{-2} | Ψ | transport and kinetic parameters | | | |
| I | applied current density. A | - | a and part and millione parameters | | | |
| I. | current in the load circuit. A | Subscrit | nts | | | |
| i | pore-wall flux across interface mol $m^{-2} s^{-1}$ | Subscry | | | | |
| J_n | anodic reaction rate constant $m^3 s^{-1}$ | rof | with respect to a reference state | | | |
| k. | cathodic reaction rate constant $m^3 s^{-1}$ | amh | ambient environment or coolant | | | |
| k-eff | effective jonic conductivity $S m^{-1}$ | ana | with respect to average temperature | | | |
| T. | total thickness of the cell m | uvg rad | equivalent radiative coefficient | | | |
| L | thickness of negative electrode m | 1 uu t | equivalent coefficient which consists of the convection | | | |
| L _n I | thickness of separator m | ι | and radiation | | | |
| и | number of electrons participating in the reaction | ~ | and radiation | | | |
| Da | fluid pressure drop. Do | 0 X | with respect to temperature difference | | | |
| 1 fluid | rate of internal best generation per unit volume $W m^{-3}$ | х | x coordinate | | | |
| Ч О́ | heat generation rate of the battery W | <i>y</i> | | | | |
| Q r | distance in radial direction m | Z | z coordinate | | | |
| ' D | aquivalent resistance in the lead circuit. | r | radial coordinate | | | |
| R ₁ | universal as constant, $9.2145 \text{ Jmol}^{-1} \text{ K}^{-1}$ | C | | | | |
| л _g D | internal acuivalant resistance of unit volume. Ωm^{-2} | Supersc | Superscripts | | | |
| K _i | internal equivalent resistance of unit volume, s2 m | | | | | |
| K _s | radius of solid active material particle, m | тах | the maximum value in the particle of electrode | | | |
| Δ5 | entropy change, J mol K | surf | the value on the surface of the particle of electrode | | | |
| t t ⁰ | ume, s | avg | the average value in the particle of electrode | | | |
| ι_+ | transference number of the fitnium ions with respect to the | | | | | |
| | | | | | | |

they have a large impact on the performance, lifespan and security of battery. The acceptable operating temperature range for Li-ion batteries is $-\,20$ to 60 $^\circ C$ [12] and to maintain its optimal performance, a narrow

Table 1

Some properties of different electric vehicle batteries. adapted from [5-8]

temperature range between 15 $^\circ \mathrm{C}$ and 35 $^\circ \mathrm{C}$ is recommended by Pesaran et al. [13]. Temperatures outside the desired range will result in significant capacity loss. Motloch et al. indicated that every degree's

| Туре | Specific energy (W h kg^{-1}) | Specific power (kW kg^{-1}) | Nominal cell voltage (V) | Life cycles ¹ | Charge time (h) | Self-discharge rate ² (%) |
|-----------------------|----------------------------------|--------------------------------|--------------------------|--------------------------|-----------------|--------------------------------------|
| Lead-acid | 25-40 | 150-250 | 2 | 200–700 | 8 | 5 |
| Nickel-cadmium | 45-80 | 200 | 1.2 | 500-2000 | 1 | 20 |
| Nickel-metal hydride | 60–120 | 200 | 1.2 | 500-1000 | 1 | 30 |
| Nickel-iron | 50 | 100 | 1.2 | 2000 | / | 20-40 |
| Nickel-zinc | 70 | 150 | 1.7 | 300 | / | 20 |
| Sodium-sulphur | 100 | 150-200 | 2 | $\sim 1000^{3}$ | 8 | Quite low |
| Sodium metal chloride | 100 | 150 | 2 | $> 1000^4$ | 8 | 1 |
| Li-ion | 110-180 | 300 | 3.6 | > 1000 | 2–3 | 10 |
| Li-polymer | 100–130 | 300 | 3.6 | 300–500 | 2–4 | 10 |

1 Up to 80% capacity.

² Loss per month. ³ \sim 1000 means no more than 1000.

 4 > 1000 means no less than 1000.

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