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Integration of carbon capture and sequestration and renewable resource technologies for sustainable energy supply in the transportation sector



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ABSTRACT

In this study, a new design for a sustainable energy system was developed by integrating two technology frameworks: the renewable resource-based energy supply and the conventional (fossil fuel) resource-based energy production coupled with carbon capture and sequestration. To achieve this goal, a new superstructure-based optimization model was proposed using mixed-integer linear programming to identify the optimal combination of these technologies that minimizes the total daily cost, subject to various practical and logical constraints. The performance of the proposed model was validated via an application study of the future transportation sector in Korea. By considering six different scenarios that combined varying crude oil/natural gas prices and environmental regulation options, the optimal configuration of the energy supply system was identified, and the major cost drivers and their sensitivities were analyzed. It was shown that conventional resource-based energy production was preferred if crude oil and natural gas prices were low, even though environmental regulation was considered. Environmental regulation caused an increase in the total daily cost by an average of 26.4%, mainly due to CO₂ capture cost.

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1. Introduction

Because CO_2 accumulation in the atmosphere has been identified as the most detrimental cause of climate change, reduction of CO_2 emissions has become a critical issue [1]. In particular, it is important to reduce CO_2 emissions, 95% of which are supplied from fossil fuels [2], in the transportation sector, a consumer of 25% of overall energy [3].

For the mitigation of CO_2 emissions, either carbon capture and sequestration (CCS) or renewable resource-based energy production can be employed. CCS is considered a practical means that can immediately address the CO_2 problem associated with conventional (fossil fuel) resource-based energy production [4], as it can be applied to any process and its relevant technologies are mature [5]. However, CCS cannot be a radical resolution to the CO_2 problem because it is an end-of-pipe technology [6]. Renewable resource-based energy production is a promising alternative for overcoming this issue [7] because it uses eco-friendly resources [8], thereby significantly reducing [9] or completely avoiding CO_2 generation [10]. However, the unit cost for this type of energy pro-

¹ Equally contributed.

duction is costly due to its immature technologies [11], and the technologies are only applicable to areas, where the renewable resources are abundant [12].

As a technological bridge for smooth transition of energy infrastructure from conventional resources to renewable resources, a combination of CCS and renewable resource technologies should be considered. However, the number of published works on this subject is limited. The majority of studies to date have focused on individual systems, including material [13] and process development [14] for CCS and unit operations [15] and supply chain management [16] for renewable technologies. Only a few researchers have developed integrated energy supply systems for specific types of energy demands [17] or resources [18].

Accordingly, the purpose of this study is to develop a new framework for the design and analysis of an integrated energy supply system that involves renewable resource-based energy production and conventional (fossil fuel) resource-based energy production coupled with CCS technologies. To achieve this goal, a technology superstructure that includes all possible technologies and energy/mass flows (from energy resources to the final energy demands) is generated (Section 2). Then, a superstructure-based optimization model is proposed using a mixed-integer linear programming (MILP) technique to identify the optimal configuration of technologies, which minimizes the total daily cost to meet the

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Nomenclature				
			10	officiency of facility f
			η_f	power output of a wind turbing in region g
	Index	G ₁ = -11:4:	σ_{fg}	maximum number of narallel ninelines
	J ∈ F ≈ ⊂ C	facilities	2	unit conversion factor
	g∈G	regions	Υ Π.	$\Omega_{\rm e}$ emission factor
	$m \in \mathbf{N}$	transportation modes	μ_f	
	$p \in P$		Continu	ous ustishis
	l ∈ k	resources	Continue	amount of CO captured by facility f in region g
	<i>C</i> /			amount of CO_2 captured by facinity f in region g
	Set		D _{pg} EC	fuel cost for railcar and truck
	\mathbf{F}_{p}^{r}	energy production facility	FCC	total capital cost of facility
	F_p^S	intermediate product storage facility	FOC	total operating cost of facility
	\vec{F}_{n}^{C}	CO_2 capture facility	CC	general cost for railcar and truck
	р М	transportation mode for product n	Lc.	$\frac{1}{1}$
	M.	transportation mode for product p	I Casilana (labor cost for railcar and truck
	nF		MC	muck maintenance cost for railcar and truck
	\mathbf{P}^{ε}	electricity	Perm	amount of product <i>n</i> produced by facility <i>f</i> in region g
	P ^{··}	H ₂	о От такит	amount of product <i>p</i> produced by identify <i>f</i> in region <i>g</i> to region
	P ^r	fuel	€pgg′m	<i>o</i> ' by transportation mode <i>m</i>
	P^{c}		0	amount of product <i>n</i> transported from region g' to re-
	R ²	DIOMASS	≪pg [,] gm	gion g by transportation mode m
	K⁼ n ^N		$0_{rag/m}$	amount of resource r transported from region g to re-
	ĸ	liatural gas	Cigg in	gion g' by transportation mode m
	_		Sng	amount of CO_2 sequestrated in region g
	Paramete	2r	TČČ	total capital cost of transportation mode
	BN	upper bound of the transportation capacity	TDC	total daily cost
	CCapa _{fp}	capacity of CO_2 capture facility f	ТОС	total operating cost of transportation mode
		capital charge factor	TOC _{electr}	icity/fuel operating cost of transportation mode for elec-
	$DD_{gg'}$	transportation distance between regions, g and g	ciccu	tricity and fuel
	DE_{pg}	driver were	<i>TOC</i> _{resou}	rces operating cost of transportation mode for resources
	DVV pm	driver wage	TPC	total primary resource cost
	FE _{pm}	capital cost of facility f	TSC	total CO ₂ sequestration cost
		fuel price for transportation mode m	U_{fpg}	amount of product p used in region g
	ΓΡ _{pm} CE	general expenses for transportation mode m	U_{fprg}	amount of resource r used by facility f in region g
	GL _{pm} UUV	high heating value of resource r		
		loading/unloading time	Integer	variable
	ME	maintenance expenses for transportation mode m	NFfng	number of facilities f in region g
	DCana	capacity of production facility f	$NP_{ngg'm}$	number of parallel pipelines that connect the regions, g
	SCana	capacity of intermediate storage facility f	100	and g'
	SH	solar heat in region g	NR _{pm}	number of railcars and trucks
	SI a	solar light in region g	-	
SN 1		lower bound of the transportation capacity Binary val		variable
	SP	average transportation speed	Xngg'm	1 if product <i>p</i> is transported from region <i>g</i> to region <i>g'</i> by
	TA _{nm}	availability of transportation mode m for product n	P88	transportation mode <i>m</i> , 0 otherwise
	TCana	capacity of transportation mode <i>m</i> for product <i>p</i>	Y_{ng}	1 if product p is exported from region g, 0 otherwise
	TMCnm	capital cost of transportation mode m for product p	Z_{ng}^{rs}	1 if product p is imported to region g, 0 otherwise
	UOCf	unit operating cost of facility <i>f</i>	F8	
	UPC _r	unit purchase cost of resource r	Abbrevia	ntion
	UTC _{nm}	unit transportation cost for transportation modes m for	CCS	carbon capture and sequestration
	- pm	product <i>p</i>	CO2	carbon dioxide
	UTC _{rm}	unit transportation cost for transportation modes <i>m</i> for	H_2	hydrogen
		resource r	MILP	mixed integer linear programming
	β	storage holding period		· · · · · · · · · · · · · · · · · · ·
	δ_{f}	capacity of photovoltaic and CO ₂ splitting facilities		
-				

final demands using limited energy resources and technology capacities (Section 3). The capability of the proposed model is illustrated through an application study on the transportation sector of future Korea with six different cases to examine the effect of fossil fuel (crude oil and natural gas) price volatility and environmental regulation options on the optimal configuration of the integrated energy supply system (Section 4). Resultantly, the features of the system configuration and the major costs breakdown are analyzed,

and the major cost drivers and their sensitivity regarding the total required cost are determined (Section 5).

2. Integrated energy supply system

Fig. 1 shows a schematic diagram of the integrated energy supply system. Two types of primary resources (conventional and renewable) and three types of energy demands (electricity for Download English Version:

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