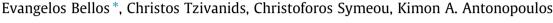
Energy Conversion and Management 137 (2017) 34-48

Contents lists available at ScienceDirect

Energy Conversion and Management

journal homepage: www.elsevier.com/locate/enconman

Energetic, exergetic and financial evaluation of a solar driven absorption chiller – A dynamic approach



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ARTICLE INFO

Article history: Received 12 October 2016 Received in revised form 8 January 2017 Accepted 14 January 2017

Keywords: Solar cooling ETC Exergetic analysis Financial analysis Dynamic simulation

ABSTRACT

In this study, a solar cooling system of 100 kW is analyzed parametrically in dynamic basis for the city of Athens, Greece. The objective of this study is the design of a sustainable system, using energetic, exergetic and financial criteria. The examined system includes evacuated tube collectors, storage tank and a single stage absorption chiller operating with LiBr-H₂O working pair. Different combinations of collecting areas and storage tank volumes are tested in order to determine the most suitable cases exergetically. These optimum cases are evaluated financially and finally the system with the higher financial indexes is selected as the most suitable. More specifically, the collecting area is analyzed from 150 m² to 600 m² and the storage tank from 6 m³ to 16 m³. Finally, 450 m² of evacuated tube collectors with a 14 m³ storage tank was proved to be the optimum solution financially with 15 years payback period and 67 k \in net present value.

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1. Introduction

The role of renewable and sustainable energy sources in our society becomes more and more important because of the environmental threats, the fossil fuel depletion and the increasing price of electricity [1]. Solar energy is the most abundant and easily utilized energy source, especially for countries with high solar potential, as Greece [2]. Solar energy can be utilized in domestic water heating applications, for space heating, for space cooling with sorption machines, for industrial heat production and for electricity production with solar power plants and with photovoltaics collectors [3]. Among these applications, solar cooling seems to have the best compatibility between source supply and load demand [4]. Moreover, solar cooling technologies aid the decrease of high peaks of electricity consumption is summer which creates severe problems in the grid energy distribution [5].

Up today, solar cooling technologies are based on sorption machines, with absorption chillers to be the most mature technology. The most usual working pairs in the absorption chillers are lithium bromide-water (LiBr-H₂O) for temperature levels greater than 5 °C and water-ammonia (H₂O-NH₃) for producing cooling in extremely low temperature levels [6]. Alternative working pairs have been examined [7–9], as lithium chloride-water (LiCl-H₂O), lithium nitrate-ammonia (LiNO₃-NH₃), ammonia-calcium chloride

(NH₃-CaCl₂) and ammonia/sodium thiocyanate (NH₃-NaSCN), with the first to be the most promising solution in the future [10]. According to the literature, LiBr-H₂O is the most usual working fluid for solar cooling applications, because of stability and efficiency reasons [11].

In the literature, many solar collectors' types have been tested in solar cooling applications; flat plate collectors (FPC), evacuated tube collectors (ETC), compound parabolic collectors (CPC) and parabolic trough collectors (PTC). The most usual absorption machines are single effects absorption machines, while there are systems with double or triple effect absorption chillers coupled with PTC or ETC [12–13]. The majority of these studies are focused on countries with high irradiation level as the Mediterranean countries and the Middle-East countries, while there are fewer studies for the Nordic countries [13-14].

Flat plate collectors have been analyzed in many studies with single effect absorption chillers. Tsoutsos et al. [15] examined this configuration for Crete (Greece) with TRNSYS and they concluded that 500 m² of FPC is able to lead to 70% solar coverage and to investment payback period of 12 years. Balghouthi et al. [16] proved that 30 m² of FPC with a storage tank of 800 l are able to cover the cooling load of a Tunisian building with a satisfying way. Angrisani et al. [17] compared FPC and ETC coupled with a single effect absorption chiller for the climate of southern Italy. They proved that ETC lead to higher yearly solar thermal efficiency and to higher solar fraction for the examined system. The use of ETC for producing cooling in Italy was also examined by Vasta







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Nomenclature

А	collecting area, m ²	n	efficiency
A A _{st}	storage tank outer area, m ²	η	water density, kg m^{-3}
CF	cash flow, €	ρ Φ	latitude, °
CP COP _m	mean COP for the conventional refrigerator, –	Ψ	latitude,
COPs	solar coefficient of performance, –	-	ots and superscripts
с _р	specific heat capacity, J kg ⁻¹ K ⁻¹	А	absorber
C ₀	capital cost, €	am	ambient
d	diameter, m	С	condenser
D	daily energy, kWh	ch	chiller
DD	number of the day in the year, –	col	collector
E	exergy flow, kW	D	daily
GT	solar radiation, W m^{-2}	E	evaporator
h	specific enthalpy, kJ kg ⁻¹	ex	exergy
Н	daily total irradiation in the collector level, kWh m ⁻²	h	hot
i	counter, –	HEX	heat exchanger
j	counter, –	in	inlet
Kch	chiller specific cost, $\in kW^{-1}$	G	generator
Kel	cost of electricity, \in kWh ⁻¹	loss	heat losses
K _{ETC}	specific cost of the ETC, $\in m^{-2}$	m	mean
K _{O&M}	cost of operation and maintenance, %	max	maximum
K _{ref}	cost of refrigeration, \in kWh ⁻¹	min	minimum
K _{tank}	specific cost of the storage tank, $\in \mathrm{m}^{-3}$	net	net gain
L	length, m	opt	optimum
m	mass flow rate, kg s ^{-1}	out	outlet
Μ	project life, years	r	refrigerant
M _{st}	water mass in storage tank, kg	ref	refrigeration
Ν	storage tank zones	S	solar
N _D	day duration, hours	st	storage tank
Q	heat rate, W	str	strong solution
r	discount factor, %	sys	system
t	time, s	th	thermal
t _{max}	time for the maximum ambient temperature, s	u	useful
Т	temperature, °C	w	weak solution
T _{SUN}	sun temperature, K		
UA	heat transfer coefficient, W K ⁻¹	Abbroui	ations
UT	tank total heat loss coefficient, W m^{-2} K ⁻¹	Abbrevi COP	
v	tank volume, m ³	COP	coefficient of performance
Wp	pump power, W	ETC	compound parabolic collector
X	LiBr mass concentration in mixture, %	FPC	evacuated tube collector
Y	yearly refrigeration production, kWh		flat plate collector
Z	daily exergy, kWh	IRR	internal rate of return
		NPV	net present values
Greek symbols		PP	payback period
δ	solar declination, ^o	PTC	parabolic trough collector
Δt	time step, s	SCOP	seasonal coefficient of performance
Δι	time step, s	SPP	simple payback period

et al. [18] and they concluded that the financial support policy is vital for these investments; something that is also has been stated by Angrisani et al. [17].

Al-Alili et al. [19] examined a solar powered absorption chiller with ETC for Abu Dhabi and they proved that the electricity consumption can be reduced to the half, compared to the conventional cooling systems. They stated that the falling cost of the solar equipment and the increasing rate of electricity are the key factors for the financial viability of solar cooling systems. Muye et al. [20] studied a solar absorption power-cooling system with ETC for Spain, while in India. They proved that this system produces greater amounts of cooling in the Spain, while India solar potential is higher. The reason for this interesting result is the higher ambient temperature in India which has a negative impact on the coefficient of performance (COP) of the chiller. Buonomano et al. [21] analyzed the use of a new ETC by TVP Solar in a solar cooling system with double stage absorption chiller. They also compared this configuration with the respective with PTC. According to the final results, ETC is the best solution because higher solar fraction can be achieved, because there are high optical losses in the case of PTC.

As it has been stated, the use of PTC can lead to satisfying results with double effect absorption chillers. These systems have been analyzed in the climate of Italy [22], Tunisia [23] and Greece [24]. A recent study [25] which compared FPC, ETC, CPC and PTC energetically and financially proved that ETC is the best solution because this technology utilizes also the diffuse solar energy.

According to the previous studies and their results, ETC is the most appropriate solar device for coupling with single effect absorption chillers. In majority of the studies, the systems are compared energetically and financially. In recent years, the exergetic analysis of absorption chillers [26–28] and of solar cooling systems [29,30] becomes more and more attractive, because this analysis

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