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A Novel Approach for Operational Optimization of Multi-Stage Refrigeration Cycles in Gas Refineries

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Highlights

- A novel approach for optimization of in-use refrigeration cycles is proposed.
- The performance limitations of components are considered in this approach.
- The independent variables of multi-stage refrigeration cycles are introduced.

Abstract

The efficient use of energy in refrigeration cycles of gas liquefaction plants is a contemporary topic of interest. The previous optimization studies on refrigeration cycles have not considered the components' operational limitations. By considering the fact that in operating plants, all constraints must be thoroughly taken into account, this paper presents a novel approach for operational optimization of in-use refrigeration cycles which takes into account the operational limitations of the components as well as the interaction between the refrigeration cycle and the core process. This novel approach exploits a combination of thermodynamic principles and pinch technology to express the multi-stage refrigeration cycles' power consumption as a function of several independent variables. To examine the applicability of the proposed approach, it is used to optimize a three-stage refrigeration cycle in a propane liquefaction plant. About 15.4% reduction in the specific power consumption is achieved.

Keywords:

Multi-stage refrigeration cycle, gas liquefaction plants, operational limitations of components, optimization, independent variables.

Nomenclature			
η_{ex}	exergetic efficiency	<i>MIX</i>	mixer
η_c	Carnot factor	<i>AC</i>	air condenser
η_s	isentropic efficiency	<i>D</i>	drum
$A_{ECC \text{ or } EGCC}$	enclosed area in the ECC or EGCC (kW)	<i>EV</i>	expansion valve
T_0	ambient temperature (K)	<i>E</i>	evaporator
T	temperature (K)	Base case	denote the refrigeration cycle before optimization
H	enthalpy (kJ)	Case A	denote the refrigeration cycle after optimization by the CPEA
h	specific enthalpy (kJ.kg ⁻¹)	Case B	denote the refrigeration cycle after optimization by the presented approach
ΔT	temperature difference (K)		
ΔT_{min}	minimum temperature difference approach (K)	Subscripts	
\dot{m}	mass flow rate (kg.h ⁻¹)	<i>evp</i>	evaporator
$\eta_{s,comp}$	isentropic efficiency of compressor	<i>s</i>	isentropic
\dot{W}	power consumption (kW)	<i>cond</i>	condenser
X	vapor quality	<i>comp</i>	compressor
\dot{Q}_{evp}	cooling rate of evaporator (kW)	<i>U</i>	upper stage
h_{fg}	enthalpy of vaporization (kJ.kg ⁻¹)	<i>L</i>	lower stage
<i>CRS</i>	compressor rotational speed (rpm)	<i>max</i>	maximum
<i>PR</i>	pressure ratio		
\dot{w}	specific power consumption (kJ.kg ⁻¹)		

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