INTERNATIONAL JOURNAL OF HYDROGEN ENERGY XXX (2017) 1–10



Available online at www.sciencedirect.com

#### **ScienceDirect**



journal homepage: www.elsevier.com/locate/he

# Respirometric evaluation of $S_0/X_0$ ratio effect on the kinetic and stoechiometric parameters of activated sludge

## Mahfoud Sakhraoui<sup>\*</sup>, R. Zamouche-Zerdazi, M. Bencheikh-Lehocine, A.-H. Meniai

Laboratoire de l'Ingénierie des Procédés d'Environnement (LIPE), Faculté de Génie des Procédés, Université Constantine 3, Constantine 25000, Algeria

#### ARTICLE INFO

Article history: Received 2 August 2016 Received in revised form 1 January 2017 Accepted 16 January 2017 Available online xxx

Keywords: Respirometry S<sub>0</sub>/X<sub>0</sub> ratios Stoechiometric-kinetic parametres Activated sludge

#### ABSTRACT

Respirometry has been used in this work to assess the effect of  $S_0/X_0$  ratio, knowing that this ratio is a very important operational parameter in the conduct of wastewater treatment plant. It affects its design and operation; part of the respirometry calculations, dissolved oxygen transfer coefficient  $K_La$  is calculate for each respirometric experiment, due to the fact that operational condition change. Under endogenous conditions OUR<sub>end</sub> is calculated using the linear portion of the variation of DO concentration under no aeration conditions. Then the OURend is used in the endogenous phase at a no oxygen concretion variation to calculate the  $K_La$ . Samples of wastewater, with different  $S_0/X_0$  ratios in the range between 0.01 and 0.23, containing sometimes ATU, a nitrification inhibitor, were injected in the respirometer with DO concentration variation recording. Exogenous OURexo were calculated from the DO data and they show that as  $S_0/X_0$  ratio increased total  $OUR_t$ increased too as well as total oxidation time. However when, COD is present alone the removal kinetics is more rapid than when both substrates (nitrogen and carbonaceous) are present. It has been shown that the use of respirometry in biomass activation assessment is a sound approach because of the celerity, the reliability and the limited cost. Consequently it has been extended in to the assessment of biomass activation when it is exposed to antibiotics.

© 2017 Hydrogen Energy Publications LLC. Published by Elsevier Ltd. All rights reserved.

#### Introduction

Activated sludge biomass activity has been studied in a batch respirometer [1-4] through DO consumption. This method is one of the most frequently used to optimize biological reactions and to evaluate kinetic and stoechiometric parameters [5-10] such as the substrate affinity constant (K<sub>s</sub>), the

maximum specific growth rate ( $\mu_{max}$ ), the yield ( $Y_{X/S}$ ) [11] etc. This technique consists of measuring biological oxygen consumption rate under well-defined conditions [12]. Particular thought has been paid to the influence of the initial substrate to biomass ratio  $S_0/X_0$  [13] on wastewater treatment performance [14–18]. This  $S_0/X_0$  ratio is an important [10,11] parameter in batch experiments because it reflects the initial energy level, to investigate the consumption of

Please cite this article in press as: Sakhraoui M, et al., Respirometric evaluation of  $S_0/X_0$  ratio effect on the kinetic and stoechiometric parameters of activated sludge, International Journal of Hydrogen Energy (2017), http://dx.doi.org/10.1016/j.ijhydene.2017.01.097

<sup>\*</sup> Corresponding author. LIPE, Constantine 3 University, 25000, Algeria.

E-mail address: mahfoudsakh@yahoo.com (M. Sakhraoui).

http://dx.doi.org/10.1016/j.ijhydene.2017.01.097

<sup>0360-3199/© 2017</sup> Hydrogen Energy Publications LLC. Published by Elsevier Ltd. All rights reserved.

Symbols used	
COD	Chemical Oxygen Demand, mg $L^{-1}$
BOD	Bio-Chemical Oxygen Demand, mg $L^{-1}$
DO	Dissolved Oxygen concentration, mg $L^{-1}$
OUR	Oxygen Uptake Rate, mg $_{O2}L^{-1}$ s $^{-1}$
TSS	Total Suspended Solids, mg ${ m L}^{-1}$
VSS	Volatile Suspended Solids, mg ${ m L}^{-1}$
V	Volume, L
SVI	Sludge Volume Index, mg ${ m L}^{-1}$
K <sub>L</sub> a	Oxygen Transfer Coefficient, ${ m h}^{-1}$
Ks	Substrate Affinity Constant, mg ${ m L}^{-1}$
$\mu$	Growth Rate, $d^{-1}$
Yx/s	Yield, mg $_{ m VSS}$ L $^{-1}$
$S_0/X_0$	Initial Substrate to Biomass Ratio, $g_{COD}/g_{VSS}$
ATU	AllulThioUrea
WWTP	Waste Water Treatment Plant
Index	
eff	Effluent
b	Sludge
t	Total
S	Soluble
end	Endogenous
exo	Exogenous
max	Maximum
30	After thirty minutes
5	After five days

substrate compounds [19,20] and it allows knowing of whether or not cell duplication can take place during the exogenous substrate removal, under given conditions, or if it is inhibited by a lack of substrate [21]. Many authors [2] were highlighted the importance of  $S_0/X_0$  ratio, this ratio key to affect the analysis and the respirometric response [10], first aerobic batch biodegradation testing and also on the relationship between preliminary acclimatization and biodegradation of different compounds (organic or refractory such as inhibitors) [14]. Moreover,  $S_0/X_0$  ratio, could also influence the OUR shape curve reliability and other kinetics parameters [9,39].

The initial substrate-to-biomass ratio will directly affect the growth patterns of microorganisms and the values of the kinetics and stoechiometric parameters [14,22]. However, there is no common agreement on this  $S_0/X_0$  ratio and the experimental procedures. Generally, testing at low ratios S<sub>0</sub>/X<sub>0</sub> (<0.2 g<sub>COD</sub>/g<sub>VSS</sub>) demonstrate the existence of a threshold below which the reactor performance is seriously affected. The stressed biomass can survive under lack of substrate condition better than unstressed biomass which cell duplication is strongly inhibited [7]. In addition, working under low ratio prevents possible variations in the composition and the physiological form of biomass population due to the different growth velocities of the various microorganisms present in the consortium [10,33]. Besides, several authors ascertain that it seems that only the kinetic parameters obtained at low  $S_0/X_0$ ratios, can be correctly used in the design and the study of activated sludge plants. Furthermore, it should be taken into account that in actual municipal wastewater treatment plants

 $S_0/X_0$  ratio is always kept very low: 0.01 for aerobic completely mixed systems and 0.13 for plug-flow systems [15]. When the ratio is sufficiently high ( $S_0/X_0 > 2 \text{ mg}_{COD}/\text{mg}_{VSS}$ ), biomass conditions itself to limitless growth, since it will be on the exponential growth phase, and the measured kinetic parameters can be independent of the retrospective feeding of the biomass [35–38]. Kinetic parameters obtained at these conditions show maximum activity [9].

This work aims at studying the influence of various  $S_0/X_0$  ratios (= 0.01, 0.02, 0.03, 0.04, 0.06, 0.09, 0.15 and 0.23) on the response of non acclimated biomass growth and synthetic COD substrate composed of sodium acetate removal [23,24] in a batch aerated respirometer [3–6]. Short-term Oxygen Uptake Rate, OUR, can provided much information about the treatment process, their determination is detailed in several studies [27–33]; it requires the Volumetric Oxygen Transfer Coefficient  $K_La$  determination in the solution which is necessary for the interpretation of respirometric data [34]. OUR experiments can be successfully used to measure the activated sludge response [25] and the determination of biological removal performance for Heterotrophic and Autotrophic biomass on the one hand; and on the other hand, the Heterotrophic biomass only.

Two series of batch experiments were carried out, using sodium acetate as a single source of carbon, in the presence or not of the nitrification inhibitor Allyl-Thio-Urea (ATU, in order to determine the optimal)  $S_0/X_0$  ratio to be used in the assessment of inhibitory effect of pharmaceutical products [24,26–29].

#### Materials and methods

#### The respirometer

The respirometer used in this experimental work is an open and aerated 0.5 L volume glass reactor (09). The air is supplied by an aquarium pump 'SHARK-RS-510' (10), with a maximum air flow of 150 L/h connected to a plastic air diffuser (06). The liquid phase is mixed by a magnetic bar (07) and a magnetic stirrer 'AGIMATIC-N' (08). A syringe is used to inject the substrate (02). The *p*H, DO and temperature were measured using a *p*H probe 'IDS-WTW' (03) and a WTW oxygen probe 'FDO-925 IDS' (04), which was connected to a WTW Oxymeter 'Multi-3430' (05). The system was maintained at a fixed temperature (20 °C  $\pm$  0.5 °C) (01) in a thermostatic enclosure of WTW (11). Fig. 1 represents the set up used during the test.

#### Synthetic effluent (substrate)

The composition of the synthetic wastewater used in this work is reproduced in Table 1.

The compositions of the synthetic wastewater was chosen so that its theoretical COD is of 2000 mg/L, stored at a temperature of 4 °C and allowed to reach 20 °C  $\pm$  1 °C before use.

#### Analytical methods

All analyses were done according to standard methods [24,27,40]. Soluble Chemical Oxygen Demand, CODs, was

Download English Version:

## https://daneshyari.com/en/article/5147816

Download Persian Version:

### https://daneshyari.com/article/5147816

Daneshyari.com