



The continuous-flow synthesis of carbazate hydrazones using a simplified computer-vision controlled liquid–liquid extraction system



Matthew O'Brien*, Dennis A. Cooper, Panashe Mhembere

Lennard-Jones Laboratories, Keele University, Keele, Borough of Newcastle-under-Lyme, Staffordshire ST5 5BG, United Kingdom

ARTICLE INFO

Article history:

Received 9 September 2016
Revised 2 October 2016
Accepted 7 October 2016
Available online 10 October 2016

Keywords:

Continuous-flow
Computer-vision
Open-source
Liquid–liquid extraction
Hydrazone

ABSTRACT

A computer-vision controlled liquid–liquid extraction system was used in the continuous-flow synthesis of a series of carbazate hydrazones. The system uses open-source software components (Python, OpenCV) and is simpler and potentially more economical, in terms of hardware, than one we have described previously.

© 2016 Published by Elsevier Ltd.

In recent years, the emergence of continuous flow methodology has created new opportunities for chemical synthesis.¹ Compared with traditional batch processes, flow methods can often offer significant safety benefits, particularly for transformations involving hazardous conditions or reagents.² Additionally, the small dimensional scales involved lead to the efficient and scale-invariant interfacial transfer of energy and matter.³ A particularly attractive aspect of flow chemistry is the ability to incorporate inline purification stages. Solid-supported scavengers⁴ and phase-switching protocols have been extremely successful in this regard.⁵ However, solid-supported chemicals can often be much more expensive than their solution phase counterparts.⁶ In addition, they often give rise to significant and scale-dependent dispersion effects⁷ and become depleted over time, thus requiring replacement or regeneration. This can be a time consuming operation which usually necessitates halting of the flow process. As liquids can be continuously pumped through the system, inline liquid–liquid phase separation does not suffer from this problem and, whilst dispersion cannot be eliminated, it can be controlled and rendered scale invariant.

One general method of inline liquid–liquid separation used in continuous flow makes use of the selective wetting of certain materials, particularly expanded porous PTFE membranes, to separate aqueous and organic solutions.⁸ We have been interested,

however, in gravity-based separations of immiscible liquids based on their densities.⁹ This is essentially a continuous flow adaptation of the classical separating funnel. The basic concept is shown in Figure 1.

A biphasic stream of immiscible liquids with differing densities will, when passed into a suitable vessel, separate vertically. The dense phase will exit the vessel through a lower exit and the light phase will exit the vessel through an upper exit. In Figure 1 the organic phase is the dense phase and the aqueous extractant is the light phase, although these roles could be switched if less dense organic solvents, e.g. diethyl ether, were required. Obviously, it is important to maintain the interface within the separation vessel, otherwise liquids may leave through the wrong outlets. This

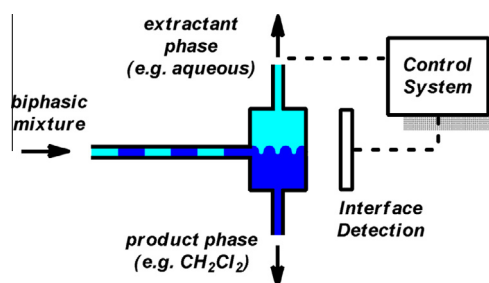


Figure 1. General schematic for inline separation.

* Corresponding author.

E-mail address: m.obrien@keele.ac.uk (M. O'Brien).

requires some kind of positional feedback system. Although several methods for determining the position of the interface could be used (including refractive index¹⁰ and electrical impedance),¹¹ in the growing context of camera-enabled synthesis technologies¹² we have focused on the use of computer-vision systems, in conjunction with inexpensive and readily available web-cams, to locate a coloured interfacial float. In our previously described system, the control computer used the determined interfacial position to dynamically adjust the flow rate of the extractant-out pump (Fig. 2A). Although we have used this successfully in a number of continuous flow reactions, we sought to develop a streamlined and more cost-efficient system by reducing the overall number of pumps involved.

In situations where a smoothly varying response to interface level perturbations is not necessary, the extractant-out pump could be replaced by a simple motor actuated valve providing a binary on/off response. If the open valve provides the path of least resistance to the liquid (which it will if there is any back-pressure downstream of other outlets) the extractant phase will leave through the valve. This is shown schematically in Figure 2B. Thus, if the extractant (i.e. aqueous phase) has a higher volumetric flow rate than the organic phase, the position of the interface will fall. If it falls below a lower bound, the valve can be opened, allowing liquid to leave through the upper (extractant) outlet. When the interface level reaches an upper bound, the valve can be closed again which will force liquid to exit via the lower (product) outlet. Thus, a hysteresis pattern will result, with the interface position oscillating between the two boundary points. The check-valve prevents any of the product stream siphoning back in when the aqueous-out valve is open. As this system uses one less pump than that shown in Figure 2A, it represents a significant economic benefit. HPLC pumps typically cost upwards of £1000, whereas a

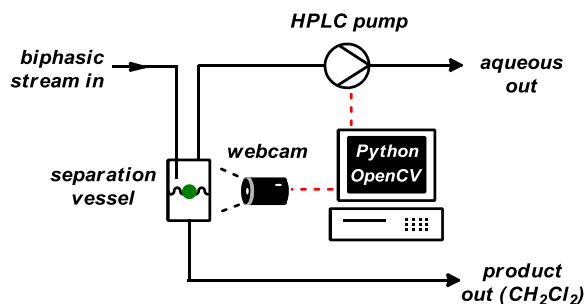
stepper motor and required ancillary components can be obtained for under £50.

For this work we used a simple luer PTFE stopcock which was actuated using a stepper motor (for technical details and images, see the ESI).

We were interested in applying this system to the formation of carbazate hydrazones¹³ **3a–j** using a condensation reaction, catalysed by pyridinium toluenesulfonate (PPTS), between *tert*-butyl carbazate **1** and a range of aromatic aldehydes **2a–j** (Scheme 1). In this case, excess carbazate was used to ensure reactions went to completion in a timely manner. Unreacted carbazate material, due to its basicity, could be extracted from the product stream, along with the PPTS catalyst, using an inline liquid–liquid extraction with aqueous phosphoric acid.

The flow setup is shown in Figure 3. Solutions of carbazate and aldehyde/PPTS (cat.) are introduced into the solvent flow streams (CH_2Cl_2) via separate injection loops. The carbazate solution was injected into the flow stream 30 s prior to the aldehyde/PPTS solution to ensure that the aldehyde was always accompanied by the carbazate. This corresponds to an overlap of 30 s at the injection front and 2 min at the tail. These meet at a T-piece and pass into a residence-loop where they react at room temperature. The reaction flow stream is then met by a flow stream of aqueous phosphoric acid. The phases are efficiently mixed together by passing through a magnetically stirred mixer (several tiny magnetic stirrer bars inside an omnifit column on the plate of a stirrer/hotplate).¹⁴ On exiting the mixer the phases rapidly revert to plug-flow. The

A) HPLC pump regulated system



B) motor driven valve regulated system

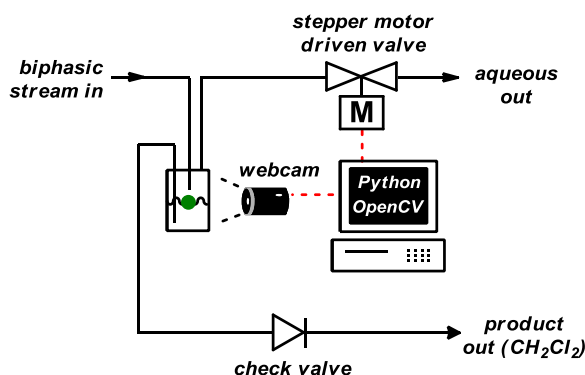
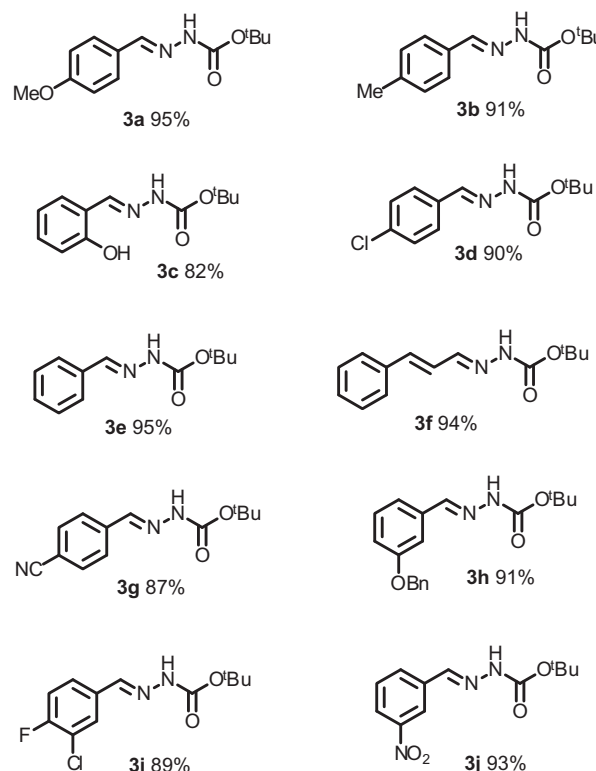
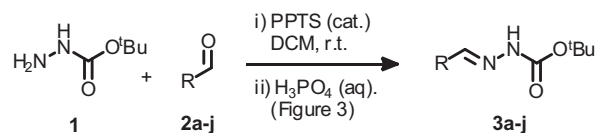


Figure 2. (A) HPLC pump regulated extraction system. (B) Motor driven valve regulated extraction system.



Scheme 1. Results for the synthesis of carbazate hydrazones **3a–j**.

Download English Version:

<https://daneshyari.com/en/article/5258266>

Download Persian Version:

<https://daneshyari.com/article/5258266>

[Daneshyari.com](https://daneshyari.com)