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Toward a predictive model for estimating viscosity of ternary mixtures containing ionic liquids

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ABSTRACT

Ionic liquids (ILs) are widely under research and being more and more used in many industrial fields due to their 17 unique properties. The knowledge of physicochemical properties of ILs is vital for their applications. Viscosity is 18 one of the most important physical properties of ILs. Since the experimental measurement of viscosity is expen-19 sive, time consuming and cumbersome, seeking for a reliable and accurate model for predicting the viscosity of IL 20 mixtures is essential. To this end, a large data bank, covering a wide range of ternary mixtures containing ILs, was 21 collected from open literature sources. Afterwards, a rigorous modeling approach, namely least square support 22 vector machine (LSSVM) was employed to predict the viscosity of ternary mixtures. The parameters of the 23 model were optimized using coupled simulated annealing (CSA) optimization tool. The inputs of the model 24 are boiling point temperature, molecular weight and composition of mixture compounds. Statistical and graph- 25 ical error analyses indicated that the developed model can satisfactorily predict ternary mixture viscosity. More- 26 over, it was demonstrated that the proposed model is able to predict the actual physical trend of viscosity with 27 variation of molecular weight and boiling point of ILs, ethanol content and water content. Furthermore, the rel- 28 evancy factor demonstrated that the average boiling point of the ternary mixture has the greatest impact on the Q2 viscosity. Finally, the Leverage approach was performed, in which the statistical Hat matrix, Williams Plot, and 30 the residuals of the model results led to recognition of the probable outliers. All the experimental data seem to 31 be reliable except five data points. Thus, the developed model could be reliable for the prediction of ternary mix- 32 ture viscosity in its applicability domain. 33

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39 1. Introduction

Ionic liquids (ILs) are defined as salts that have melting points under 40 100 °C and are liquid in a wide range of temperature [1,2]. Ionic liquids 41 42 have the features of classical salts such as high polarity, chemical and thermal stability, flame resistance [3–7], recyclability, high solubility, 43nonvolatility, heat hardiness and conduction properties [8–14], while 44 they are liquid in ambient temperature, leading to draw considerable at-4546 tention from many fields such as electrolytes in batteries [14], lubricant agents [14], catalysts [15,16], liquid-liquid extraction media [16] and 47 separation processes [14,17]. Moreover, ILs are introduced as "solvent 48 49 designers" [1,18], because they can be designed to have desired properties by suitable selection of the anion and cation or by manipulation of 50branching length during ILs' synthesis. The cation part of ILs is organ-5152ic such as imidazolium, quaternary ammonium, phosphonium and 53pyridinium, while the anion part can be organic/inorganic such as 54tetrafluoroborate, hexafluorophosphate, trifluoromethanesulfonate Q3 and bis (trifluoromethylsulfonyl) amide [1,19–25].

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Physical and chemical properties of ILs are important for their design 56 and use in the aforementioned applications [26]. Viscosity is one of the 57 most significant properties, which has been widely used to study ILs and 58 their purity [27–31]. Viscosity is a transport property which is caused by 59 the friction among neighboring particles in a fluid that are moving at 60 different velocities. In other words, this property provides a measure 61 of fluid resistance to gradual deformation by shear stress or tensile 62 stress. The viscosity plays a crucial role in fluid flow, mass transfer and 63 heat transfer calculations [32-34]; therefore, in order to deal with a 64 fluid in industrial processes (such as heat-transfer equipment, piping, 65 liquid-liquid extractors, reactors, stripping columns, crystallization 66 equipment, and distillation columns), knowing viscosity value is of a 67 great importance [20]. One of the disadvantages of ILs is their higher vis- 68 cosity compared to conventional organic solvents, because it adversely af- 69 fects mass transfer and power requirements [1,35,36]. Since the ILs can be 70 custom designed, their viscosity covers a wide range. The viscosities of ILs 71 are strongly dependent on the amount of dissolved water [37]. Pure ILs 72 may have some limitations. In order to achieve more or various proper-73 ties, ILs may be mixed with other compounds. Thus, binary and ternary 74 IL mixtures which extend ILs' applications are more interesting [38]. 75

Although since the last decade many researchers have measured 76 physicochemical properties of ILs, experimental measurements have 77

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not been adequate [36,39–41]. Experimental measurements in many 78 79 cases are costly, time consuming and cumbersome. These difficulties are greater for ILs due to the diversity of anion-cation combinations 80 81 [35,42] (about 10¹⁸ potential anion–cation combinations [43]). Therefore, searching for a quick and accurate method for the determination 82 of ILs properties is inevitable. To this end, several researchers have 83 attempted to develop reliable and accurate models for predicting the 84 85 properties of IL mixtures.

IL mixtures are not analytically described in the literature as thor-86 87 oughly as their pure state [44,45]. Many analytical techniques have 88 been employed to predict thermo-physical properties. In semiempirical methods such as group contribution, enough experimental 89 data is required. Moreover, molecular dynamics simulation has been 90 91used in several papers to calculate viscosity [39,40,46,47]. Furthermore, group contribution method has been applied to predict viscosity by sever-92 al researchers [20,48–50]. Gharagheizi et al. [48] used a group contribu-93 tion method for 46 sub-structures to estimate the viscosity of ILs. The 94 proposed model produces a low average relative deviation (AARD) of 95less than 6.4%. Daniel et al. [49] proposed a group contribution method 96 to predict the viscosity at different temperatures of magnetic ionic liquids 97 (MILs). Their model exhibited a good agreement with the experimental 98 results and presented a percentage deviation of 7.64%. Bajić et al. [30] 04 100 used two different approaches, group contribution models (UNIFAC-VISCO and ASOG-VISCO) and correlations (Seddon, Grunberg-Nissan, 101 McAlister, Eyring-UNIQUAC and Eyring-NRTL models) to calculate viscos-102 ities of ten binary liquid mixtures consisting of ILs and organic compounds 103 in a wide temperature range. 104

105Some researchers have developed quantitative structure property relationships (QSPR) as prediction models for thermo-physical proper-106 ties such as melting point [43,51], density [52], viscosity [3,35,36,53,54], 107and conductivity [3,54] of ILs. Chen et al. [35] developed a correlation 108 109and simplified QSPR coupled with the descriptors of group contribution 110for viscosity of imidazolium-based ILs. They obtained a relationship between the descriptive parameters and the viscosity of imidazolium-111 based ILs. Yu et al. [36] obtained eight QSPR correlations for viscosities 112 of bis (trifluoromethylsulfonyl) imide-based ILs at 283 K, 293 K, 298 K, 113 303 K, 313 K, 323 K, 333 K and 343 K. 114

In recent years, few studies have been carried out to predict viscosity 115 of IL mixtures [30,42,55,56]. Unlike pure ILs, very few works have stud-116 ied the thermo-physical properties of ternary mixtures of ILs. Diaz-117 Rodriguez et al. [55] employed an artificial neural network multilayer 118 119 perceptron (MLP) model to estimate viscosity of ILs. They reported mean prediction errors around 1.5% for a k-fold cross-validation and 120 121about 2.3% for three blind tests. Fatehi et al. [56] estimated the viscosity 122of binary mixtures of ILs and solvents based on the structure groups of the ionic liquid using an artificial neural network. They concluded that 123124their result was capable to estimate the viscosity of binary mixtures, including a range of ionic liquids and solvents, with an average relative 125error of 0.6%. The main objective of this study is to propose a robust soft 126 computing modeling approach, namely least square support vector ma-127chine (LSSVM) for accurate viscosity prediction of ternary mixtures 128129contacting ILs. The parameters of the LSSVM model are optimized using 130 a novel feature selection mechanism based on coupled simulated annealing (CSA). To this end, the following are the objectives of this study: 131

- To acquire a comprehensive and large data bank, covering a wide
 range of ternary mixtures containing ILs from open literature sources.
- To develop a novel, accurate and robust intelligent model based on
 LSSVM modeling approach for prediction of viscosity of ternary mix-
- 136 tures containing ILs.
- To evaluate the performance of the developed model for predicting viscosity of ternary mixtures containing ILs using graphical and statistical error analyses.
- 4. To validate the developed model by calculating viscosity of ternary
 mixtures containing ILs as a function of input parameters to see
 whether the proposed model follows the expected physical trends.

- 5. To investigate the applicability domain of the applied model based 143 on the Leverage approach. 144
- 6. To investigate the relative impact of each input parameter on viscosity of ternary mixtures containing ILs using the relevancy factor. 146

2. Data collection

Reliability and robustness of a model/correlation for prediction of a 148 given property strongly depends on the comprehensiveness of the 149 used dataset for its development. In this study, almost all experimental 150 viscosity data of ternary mixtures containing IL data sets, which are 151 available in open literature sources, have been used [57–65]. The prop-152 erties of the studied compounds are summarized in Table 1. The next 153 step is to determine the input variables (independent variables) for 154 model development. Molecular weight (Mw) and boiling point (T_b) of 155 the components as well as the composition of non-IL substances were 156 selected as the input variables to distinguish the diverse species. The 157 viscosity of mixtures containing ILs has been considered as the desirable 158 output. Therefore, the following general relation has been considered 159 for the ternary viscosity of ILs:

$$\mu = f(Mw_i, Tb_i, X_2, X_3). \tag{1}$$

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The used data in this study covers a wide range of IL mixtures, and consequently, the developed model based on these data could be reli-163 able and efficient for predicting viscosity of other IL mixtures. 164

3. Model development

3.1. Least square support vector machine 166

One of the most robust and consistent strategy developed from machine learning community is the Support Vector Machine, which recently has been applied in many fields [33,66,67]. This algorithm as a tool for a set of related supervised learning methods can be employed not only for data analyzing and patterns recognizing, but also for regression analysis. Based on SVM principles, any function f(x) can be expressed as follows [68]: 173

$$f(\mathbf{x}) = \mathbf{w}^T \varphi(\mathbf{x}) + \mathbf{b} \tag{2}$$

where w^T and $\varphi(x)$ are the transposed output layer vector and the kernel 175 function, respectively, and *b* is the bias. The input of the model (*x*) has a dimension of $N \times n$, where *N* and *n* represent the number of data points 176

Component	Molar weight (g/gmol)	Boiling point (K)	Ref.
Water	18.01	373.15	[89]
Ethanol	46.06	352.2	[89]
1-Propanol	60.09	370.3	[89]
Ethyl ethanoate	88.1	350.2	[89]
2-Propanol	60.09	345.55	[89]
1-Methylethyl ethanoate	102.13	361.73	[89]
Ethyl 1,1-dimethylethyl ether	102.17	346.3	[89]
Methanol	32.04	338.0	[89]
1-Octyl-3-methylimidazolium bis [(trifluoromethyl)sulfonyl]imide	475.5	954.0	[65]
1-Butyl-3-methylimidazolium bis [(trifluoromethyl)sulfonyl]imide	419.4	862.4	[65]
1-Ethyl-3-methylimidazolium ethyl sulfate	236.3	712.7	[65]
1,3-Dimethylimidazolium methylsulfate	208.2	666.9	[65]
1-Butyl-3-methylimidazolium methylsulfate	250.3	735.6	[65]

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