ARTICLE IN PRE

MOLLIQ-04469; No of Pages 7

Journal of Molecular Liquids xxx (2014) xxx-xxx



Contents lists available at ScienceDirect

Journal of Molecular Liquids

journal homepage: www.elsevier.com/locate/molliq



Nanofluid in tilted cavity with partially heated walls

M. Hosseini ^a, M.T. Mustafa ^b, M. Jafaryar ^c, E. Mohammadian ^{d,*}

- ^a Department of Mechanical Engineering, Islamic Azad University, Qaemshahr Branch, Qaemshahr, Mazandaran, Iran
- ^b Department of Mathematics, Statistics and Physics, Qatar University, Doha 2713, Qatar
- ^c Department of Mechanical Engineering, Mazandaran Institute of Technology, Babol, Iran
 - d Department of Mechanical Engineering, Islamic Azad University, Ramsar Branch, Ramsar, Mazandaran, Iran

ARTICLE INFO

Article history:

- Received 28 July 2014
- Received in revised form 6 September 2014 10
- Accepted 29 September 2014
- Available online xxxx 12

- Lattice Boltzmann Method 14
- 15 Nanofluid
- 16 Natural convection
- 17 Square cavity Inclination angle
- 38 19 Heat transfer

32

33

35

36

37

38

39

40

41

42 43

44

45

46 47

48

49 50

51

52 53

54 55

56

ABSTRACT

Lattice Boltzmann Method is applied to investigate the natural convection flow utilizing nanofluids in square en- 20 closure with partially heated walls. The fluid in the cavity is a water-based nanofluid containing different types of 21 nanoparticles: copper (Cu), silver (Ag), alumina (Al₂O₃) and titania (TiO₂). The effective thermal conductivity 22 and viscosity of nanofluid are calculated by the Maxwell-Garnetts (MG) and Brinkman models, respectively. 23 This investigation was compared with other numerical methods and found to be in excellent agreement. Numer- 24 ical results for the flow and heat transfer characteristics are obtained for various values of the nanoparticle vol- 25 ume fraction, Rayleigh numbers and inclination angles together with different kinds of nanofluids. The type of 26 nanofluid is a key factor for heat transfer enhancement. Choosing copper as the nanoparticle proved to have 27 the highest cooling performance for this problem. It is also shown that the Nusselt number is an increasing function of each of the nanoparticle volume fraction and Rayleigh numbers.

© 2014 Published by Elsevier B.V.

1. Introduction

The problem of natural convection in a cavity has been a major topic of research studies due to its occurrence in industrial and technological applications such as chemical vapor deposition instruments (CVD) [1], electronic cooling [2], furnace engineering [3], and solar collectors [4]. Recently, due to the rising demands of modern technology, including chemical production, power station, and microelectronics, there is a need to develop new types of fluids that will be more effective in terms of heat exchange performance. Nanofluids are produced by dispersing the nanometer-scale solid particles into base liquids with low thermal conductivity such as water, ethylene glycol (EG), and oils. [5]. The term "nanofluid" was first coined by Choi [6] to describe this new class of fluids. The materials with nanometer sizes possess unique physical and chemical properties [7]. The presence of the nanoparticles in the fluids noticeably increases the effective thermal conductivity of the fluid and consequently enhances the heat transfer characteristics. Therefore, numerous methods have been taken to improve the thermal conductivity of these fluids by suspending nano/micro-sized particle materials in

Several investigators have experimentally studied flow and thermal characteristics of nanofluids. Especially, in order to understand buoyancy-driven heat transfer of nanofluids in a cavity several

E-mail addresses: M.Hosseini545454@gmail.com (M. Hosseini),

Corresponding author. E.Mohammadian12345@gmail.com (E. Mohammadian). investigations have been theoretically and experimentally conduct- 57 ed. Putra et al. [8] conducted the experiment for observation on the 58 natural convective characteristics of water based on Al₂O₃. They re- 59 ported that natural convective heat transfer in a cavity is decreased 60 with the increment of the volume fraction of nanoparticles. Kim 61 et al. [9] analytically researched the convective instability driven 62 by buoyancy and heat transfer characteristics of nanofluids with theoret- 63 ical models which are used to estimate properties of nanofluids and indi- 64 cated that as the thermal conductivity and shape factor of nanoparticles 65 decrease, the convective motion in a nanofluid sets in easily and their results were similar with Putra et al.'s [8] experimental investigation. 67 Khanafer et al. [10] numerically investigated buoyancy-driven heat trans- 68 fer enhancement in a two-dimensional enclosure utilizing nanofluids. 69 Their paper shows that the Nusselt number for the natural convection 70 of nanofluids is increased with the volume fraction. They reported an en- 71 hancement of heat transfer in horizontal annuli. A theoretical study on a 72 heated cavity was reported by Hwang et al. [11]. They observed that the 73 heat transfer coefficient of Al₂O₃-water nanofluids is reduced when 74 there is an increase in the size of nanoparticles and a decrease in average 75 temperatures. Rashidi et al. [12] studied the effects of magnetic interac- 76 tion number, slip factor and relative temperature difference on velocity 77 and temperature profiles as well as entropy generation in magnetohydro-78 dynamic (MHD) flow of a fluid with variable properties over a rotating 79 disk. Rashidi et al. [13] considered the analysis of the second law of 80 thermodynamics applied to an electrically conducting incompressible 81 nanofluid flowing over a porous rotating disk. Recently several papers 82 were published about nanofluid flow and heat transfer [14-49].

http://dx.doi.org/10.1016/j.molliq.2014.09.051 0167-7322/© 2014 Published by Elsevier B.V.

า

84 85 86 87 88 99 91 92 93 94 95 96 97 98 99 100

Nomenclature	
с	lattice speed
c_i	discrete particle speeds
C_p	specific heat at constant pressure [kJ kg $^{-1}$ K $^{-1}$]
F	external forces
f	density distribution functions
f^{eq}	equilibrium density distribution functions
	internal energy distribution functions
g g ^{eq}	equilibrium internal energy distribution functions
g_y	gravitational acceleration $[m s^{-2}]$
Gr	Grashof number $(=g\beta\Delta TH^3/v^2)$
Н	height/width of the enclosure
k	thermal conductivity
Nu	average Nusselt number
p	pressure [Pa]
Pr	Prandtl number (= v/α)
Ra	Rayleigh number (= $g\beta\Delta TH^3/\alpha\nu$)
T	fluid temperature
(u, v)	velocity components in the (x,y) directions, respectively
w_i	weighting factor
(x, y)	Cartesian coordinates
(X, Y)	dimensionless coordinates
Greek symbols	
α	thermal diffusivity [m ² s ⁻¹]
ϕ	volume fraction
θ	dimensionless temperature
μ	dynamic viscosity [Pa s ⁻¹]
v	kinematic viscosity [m² s]
ρ	fluid density [kg m ⁻³]
$ au_c$	relaxation time for temperature
$ au_{ u}$	relaxation time for flow
β	thermal expansion coefficient [K ⁻¹]
ψ	stream function
γ	inclination angle

Subscripts

c cold
h hot
∞ condition at infinity
nf nanofluid
f base fluid
n solid particles

One of the useful numerical methods that have been used in the recent years is the Lattice Boltzmann Method. Sheikholeslami et al. [50] studied the magnetic field effect on CuO-water nanofluid flow and heat transfer in an enclosure which is heated from below. They found that the effect of Hartmann number and heat source length is more pronounced at high Rayleigh number. Sheikholeslami et al. [51] studied the problem of MHD free convection in an eccentric semi-annulus filled with nanofluid. They showed that Nusselt number decreases with increase of position of inner cylinder at high Rayleigh number. Nanofluid flow and heat transfer have been considered by several authors [52–57].

The main aim of the present study is to identify the ability of Lattice Boltzmann Method (LBM) for solving natural convection flow utilizing nanofluids in a square enclosure with partially heated walls. Different types of nanoparticles such as copper (Cu), silver (Ag), alumina (Al₂O₃) and titania (TiO₂) with water as their base fluid have been considered. The results of LBM are compared with predictions of the finite volume method. The streamline and temperature field and average Nusselt

number for different values of volume fraction, Rayleigh number and 101 inclination angles are also illustrated.

2. Problem definition and mathematical model

2.1. Problem statement 104

103

111

132

The geometry and the coordinate system are schematically shown in 105 Fig. 1. The partially thermally active side walls of the cavity are main- 106 tained at two different but uniform temperatures, namely, T_h and T_c 107 respectively with $T_h > T_c$, and the bottom wall, top wall and remaining 108 parts of the side walls are insulated. In Fig. 1, γ denotes the tilted 109 angle with respect to horizon.

2.2. The Lattice Boltzmann Method

The LB model used here is the same as that employed in [58,59]. 112 The thermal LB model utilizes two distribution functions, f and g, for 113 the flow and temperature fields, respectively. It uses modeling of 114 movement of fluid particles to capture macroscopic fluid quantities 115 such as velocity, pressure, and temperature. In this approach, the 116 fluid domain discretized to uniform Cartesian cells. Each cell holds 117 a fixed number of distribution functions, which represent the num- 118 ber of fluid particles moving in these discrete directions. The D2Q9 119 model was used and values of $w_0 = 4/9$ for $|c_0| = 0$ (for the static 120 particle), $w_{1-4} = 1/9$ for $|c_{1-4}| = 1$ and $w_{5-9} = 1/36$ for $|c_{5-9}| = 121$ $\sqrt{2}$ are assigned in this model.

The density and distribution functions i.e. the f and g, are calculated 123 by solving the Lattice Boltzmann equation (LBE), which is a special 124 discretization of the kinetic Boltzmann equation. After introducing 125 BGK approximation, the general form of the lattice Boltzmann equation 126 with external force is: 127

For the flow field:

$$f_i(x+c_i\Delta t,t+\Delta t) = f_i(x,t) + \frac{\Delta t}{\tau_v} \left[f_i^{eq}(x,t) - f_i(x,t) \right] + \Delta t c_i F_k \qquad (1)$$

For the temperature field:

$$g_i(x + c_i \Delta t, t + \Delta t) = g_i(x, t) + \frac{\Delta t}{\tau_C} \left[g_i^{eq}(x, t) - g_i(x, t) \right]$$
 (2)

where Δt denotes the lattice time step, c_i is the discrete lattice velocity in direction i, F_k is the external force in direction of lattice velocity, and τ_v 133 and τ_C denote the lattice relaxation time for the flow and temperature 134 fields. The kinetic viscosity v and the thermal diffusivity α , are defined 135

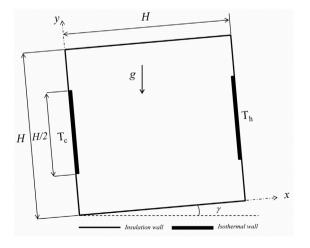


Fig. 1. Geometry of the problem.

Download English Version:

https://daneshyari.com/en/article/5411391

Download Persian Version:

https://daneshyari.com/article/5411391

Daneshyari.com