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# Abatement of chromium by adsorption on nanocrystalline zirconia using response surface methodology

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#### 6 ARTICLE INFO ABSTRACT

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#### 32 1. Introduction

UIF fiction (1) was achieved by the proposition of change in the moved by the member of reduced by the moved of the m All living beings including humans require water to survive except in certain ecosystems like hydrothermal vents. Water employed in various sectors is concisely categorized into three categories i.e. industry, agri- culture and domestic. The ever increasing population has resulted in an immense stress on water quantity and quality. The pressure on water resources is further added by increasing population, industrializa- tion and modern agricultural practices. Heavy metal pollution is one of problems retro-grading the aqueous ecosystems. Chromium is one of the metals with applications in various industries such as, electroplating, textile, stainless steel, leather, and paint industries. Higher intake of chromium in human body results in weakening of im- mune system, DNA strand breaks, alteration in cellular signaling path-way, ulcers, allergic dermatitis and ultimate death in many cases [1–3].

 Because of well documented adverse health effects of chromium and its widespread applications, it is mandatory to remove it from industrial effluents prior to discharge. Chemical precipitation, coagulation and flocculation, electro-coagulation, ion exchange, membrane separation, nano-filtration, solvent extraction, reverse osmosis [4–[10\]](#page--1-0), and adsorp- tion [11–[14\]](#page--1-0) are some of the techniques widely reported for the treat- ment of chromium laden aqueous solutions and waters. Each of these techniques has merits but they suffer from certain drawbacks like high operational cost, along with regeneration and need of trained per-sonnel. But adsorption has advantages over other technique due to ease

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Application of nanocrystalline zirconia was investigated for the removal of chromium from aqueous solutions. The 17 nanozirconia was synthesized by 'precipitation method'. The parameters namely initial concentration (5–65 ppm), 18 Q10 pH (0.5 to 10.5), adsorbent dose (2 to 10 g/l) and temperature (298 K to 318 K) were optimized employing central 19 composite design of response surface methodology. The removal of Cr was most affected by pH, followed by an ini- 20 tial concentration and adsorbent dose. Maximum removal  $(\%)$  was achieved at an initial concentration of 20 ppm, 21  $pH = 3$ , adsorbent dose = 4 g/l and 313 K. The experimental data were best fitted in Langmuir's isotherm equation 22 Q11 and the removal followed pseudo second order kinetics. The mechanism of removal was explained by boundary 23 layer diffusion via intraparticle diffusion and was further confirmed by Boyd plot. Thermodynamic parameters 24 revealed that the removal process was spontaneous, endothermic and physiosorptive in nature. Adsorbent was 25 regenerated with hydroxides (0.1 N NaOH, KOH and NH4OH) for further reuse. 26

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in operation, regeneration, high efficiency, low energy input and remov- 56 al of pollutants even at trace concentrations. Various adsorbents like ac- 57 tivated carbon, carbon nanotubes, lignin, chitosan, clay, fly ash, bacteria, Q13 fungi, and nanostructured oxides such as iron oxide and aluminum  $Q14$ oxide [12–23] have been reported for the removal of Cr from aqueous 60 solutions. Present study addresses removal of chromium by adsorption 61 on nanocrystalline zirconia. Zirconia has excellent chemical inertness 62 and is known to be biocompatible with system [\[24\]](#page--1-0). Removal efficiency 63 of the synthesized adsorbent, nanozirconia for removal of Cr was exam- 64 ined and reported. Response surface methodology was used for optimi- 65 zation of experimental parameters and thermodynamic studies for the 66 removal of Cr were also carried out and reported. 67

#### **2. Experimental** 68

#### 2.1. Materials and analytical instruments 69

Potassium dichromate ( $K_2Cr_2O_7$ ) and ammonium hydroxide 70 (NH4OH) were procured from Merck, Mumbai, India. Zirconium 71 oxychloride octahydrate  $(ZrOCl_2·8H_2O)$  was obtained from Himedia, 72 India. Tubular Furnace (IKON, India), Analytical balance (VIBRA), pH 73 meter (IKON, India), X-ray diffractometer (MINIFLEX II, Desktop XRD, Q15 RIGAKU), DTA/TGA (Labsys™ TG–DTA 16, SETARAM Instrumentation), 75 Scanning electron microscope (Quanta 200 f. FEI), Transmission 76 electron microscope (TECNAI G2, FEI), water bath shaker (Narang 77 scientific), and atomic adsorption spectrophotometer (Szhimadzu AA 78 7000) were used in the present studies. The metal was not to the present studies.

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#### 80 2.2. Design of experiments or response surface methodology

 Experiments were designed via response surface methodology (RSM). RSM is a collection of statistical and mathematical tools used to optimize the response governed by several independent variables. It has been useful for modeling and analysis of problems in which a re- sponse of interest is influenced by several variables and its objective is to optimize this response [\[25\].](#page--1-0) Classically, response is optimized by Q16 varying one parameter one at a time and keeping other parameters con- stant. Classical method is time consuming and does not provide the cor- rect picture of quantitative interactions between various parameters. To overcome these drawbacks, RSM is employed to know interaction among various parameters. By taking into account various independent parameters, optimization is achieved through RSM.

Letting this detection of the detection of the method in the set of 93 RSM contains two designs: Box–Behnken design (BBD) and Central 94 composite design (CCD). In BBD, cubic points are taken into consider-95 ation, whereas in CCD, axial points, in addition to cubic points are 96 taken into consideration. It means that BBD has only 3 degrees of free-97 dom  $(-1, 0, +1)$ , whereas CCD system has five degrees of freedom 98 ( $-\alpha$ ,  $-1$ , 0,  $+1$ ,  $+\alpha$ ). In present studies, the four parameters studied 99 were concentration of solution (X1), pH of the solution (X2), dose of 100 adsorbent (X3) and temperature of solution for reaction conditions 101 (X4) at five levels ( $-\alpha$ ,  $-1$ , 0, 1,  $+\alpha$ ) with a significance level of 102 0.05. Here, each parameter is coded by  $-\alpha$ ,  $-1$ , 0, 1, and  $+\alpha$ ,  $-1$ , 0  $103$  and  $+1$  are the minimum, central and maximum coded cubic values 104 respectively. Likewise  $+\alpha$  and  $-\alpha$  represent minimum and maximum 105 coded axial values used in the model, respectively. The value of  $\alpha$  de-106 pends upon the number of process independent variables taken in the 107 design [\[26\]](#page--1-0).

108 The value of  $\alpha$  for orthogonal design is calculated as follows:

 $\alpha = 2$  (number of independent variables/4).

110

Here number of variables was 4. So,

$$
\alpha = 4/4 = 2. \tag{1}
$$

112

The relationship between coded and uncoded variables was obtain-113 ed from the following equation [25]:

**CODED VALUE** = 
$$
X_i - X_n / \Delta X
$$
. (2)

115

Here  $X_i$  is the value of uncoded value of the ith factor,  $X_n$  is the mid-116 way average value of low high, and  $\Delta X$  is the step change.

117 The total number of experiments obtained by operating CCD of RSM in Q17 a MINITAB 16 software was 31. In the experiments, there were 16 factorial

119 points, 8 axial points and 7 replicates [26].

$$
N = 2k + 2k + n_0 = 24 + 2 \times 4 + 7 = 31
$$
\n(3)

121 where N is the total number of experiments, k is the number of factors and  $n_0$  is the number of central runs.

122 On the basis of the results, a second order polynomial is applied to 123 explain the relationship between response and processed variables 124 [\[26\]](#page--1-0) as follows:

$$
Y = \beta_0 + \Sigma \beta_i x_i^2 + \Sigma \beta_{ii} x_i^2 + \Sigma \Sigma \beta_{ij} x_i x_j + \varepsilon_r. \tag{4}
$$

126

Y denotes the predicted response, and i and j take values from 1 to 127 the number of independent process variables.  $\beta_0$ ,  $\beta_i$ ,  $\beta_{ii}$ , and  $\beta_{ii}$  are the 128 offset terms, linear effect, square effect and interaction effect predicted 129 by the method of least squares,  $\epsilon_r$  denotes the error of prediction and 130  $x_i$  and  $x_i$  are coded independent process variables [\[26,27\].](#page--1-0)

#### 2.3. Synthesis of the adsorbent 131

Nanocrystalline zirconia was synthesized by precipitation method 132 [\[28,29\]](#page--1-0). Solution of  $ZrOCl<sub>2</sub>·8H<sub>2</sub>O$  (0.075 M) was prepared in distilled 133 water and was precipitated with 25% ammonia while stirring till its 134 pH reached 10 to 10.5. It resulted in formation of zirconium hydroxide. 135 After complete precipitation, it was filtered and subsequently washed 136 with distilled water to remove chloride from the filtrate which was 137 ascertained by titrating the filtrate with AgNO<sub>3</sub>. After complete removal 138 of chloride, precipitate was dried in an oven at 353 K to 363 K for 24 h. 139 The dried zirconium hydroxide was calcined at 773 K at a heating rate of 140 10 °C/min resulting in the formation of nanocrystalline zirconia as 141 follows [\[28\]:](#page--1-0) 142

$$
ZrOCl_2 \cdot 8H_2O + 2NH_4OH \longrightarrow Zr(OH)_4 + NH_4Cl
$$
 (5)

$$
Zr(OH)_4 \qquad \rightarrow \qquad ZrO_2 + H_2O. \tag{6}
$$

## 147

### 2.4. Batch experiments

Stock solution of Cr(VI) (1000 ppm) was prepared by dissolving 148  $K<sub>2</sub>Cr<sub>2</sub>O<sub>7</sub>$  in distilled water. Experimental conditions with four variables 149 at five degrees of freedom, as suggested by the model were used to per- 150 form the experiments. For adsorption experiments, a known amount of 151 adsorbent, nanozirconia, was added to 50 ml of Cr solution in 100 ml re- 152 agent bottles. The contents were agitated at 90 rpm in a water bath 153 shaker up to equilibrium time, 45 min. pH of the solutions was main- 154 tained by adding 0.1 N NaOH/HCl to the solutions. Isotherm data were 155 obtained by carrying out experiments at different initial concentrations 156 (20 to 70 ppm, pH = 3, dose = 4 g/l, temperature = 293 K to 343 K).  $157$ Thermodynamic parameters were similarly determined by performing 158 experiments at different temperature (293 K to 343 K). 159

After equilibrium, the adsorbent was separated from the solutions 160 by filtration followed by subsequent centrifugation at 6000 rpm for 10 161 min. Residual concentration of Cr in the aliquot was determined by an 162 atomic absorption spectrophotometer (Shimadzu AA7000). All experi- 163 ments were conducted as triplets and the values presented here are 164 average of the three replicates.  $165$ 

The amount of chromium adsorbed per unit mass of the adsorbent 166  $(mg g<sup>-1</sup>)$  was determined by the following expression [\[23\]](#page--1-0): 167

$$
q_e = (C_i - C_e/W) * V \tag{7}
$$

where  $q_e$  is the amount adsorbed on per unit mass of the adsorbent 169  $(mg g<sup>-1</sup>)$  at equilibrium, C<sub>i</sub> and C<sub>e</sub> (both in mg/l) are the initial and the equilibrium concentrations of Cr respectively, and W is the 170 weight of adsorbent (g). Percentage removal of Cu(II) was calculated 171 by applying the following expression [23]: 172

%Removal of metallic ions =  $(C_i-C_e/C_i) * 100$ . (8)

$$
174 \\
$$

#### 2.5. Regeneration batch experiments

For regeneration, the used adsorbent was placed in 1 l chromium so- 175 lution of initial concentration of 50 ppm,  $pH = 2$  and adsorbent dose of 176 5 g/l. Afterwards, the solution was stirred at 350 rpm on magnetic stirrer 177 for 2 h. Chromium loaded adsorbent was isolated by filtration and sub- 178 sequently dried in an oven at 323 K. The used adsorbent was regenerat- 179 ed by taking regenerating agent in a beaker along with used adsorbent 180 viz. chromium loaded nanocrystalline zirconia. It was stirred at 181 350 rpm on magnetic stirrer for 2 h. Afterwards, adsorbents were 182 filtered and dried in an oven. 183

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