



# Thermodynamic performances of a solar driven adsorption system



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## ABSTRACT

This study examines the thermophysical process of a solar driven adsorption cooling system. The data used for the performance study were taken experimentally during the start-up procedure of a solar collector. The generation of high temperatures inside a solar collector adsorption tube is a challenge due to the intermittent nature of solar radiation. In this present study, a solar collector adsorption tube using granular activated carbon (GAC1, GAC2) and methanol is introduced. The proposed system maintains higher adsorption temperatures up to 117.2 °C. The evaporator temperature of the solar adsorption cooling system decreased to −12 °C (sunny day) and 0 °C (sunny-cloudy days), allowing liquid water converted to solid ice. This result showed that a solar collector filled with granular activated carbon and methanol successfully produces ice inside the solar adsorption cooling system throughout the experiment period. A solar-powered pump circulated the melted ice inside the storage chamber during day time and thus decreased the inside temperature of storage chamber to 15 °C and 10 °C for shorter and longer durations, respectively.

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## 1. Introduction

Solar thermal based cooling system is one of the renewable source of cooling with various advantages, such as short installation time and long-life operation, simplicity, without moving parts, silent, safe and non-polluting (Balzani and Reatti, 2005). Solar-driven adsorption cooling systems in recent years have been receiving more attention as a replacement for conventional vapor compression refrigeration cycles driven by electricity. Alghoul et al. (2007) stated that a solid adsorbent (GAC) and liquid adsorbate (ethanol) is the appropriate working pairs for producing ice in a low energy (flat-plate solar collector) based solar adsorption cooling system. The highest COP of a GAC–ethanol based cooling system is found when the regeneration temperature is above 70 °C (Habiba et al., 2014).

This technology is particularly attractive when a high amount of low-temperature heat is available, such as solar thermal energy (Wang and Oliveira, 2006) and weather fluctuations that lead to changes in the cooling load, and the cooling capacity of the system (Alkhair et al., 2015; El-Sharkawya et al., 2014; Habiba et al., 2013).

The major component of a solar adsorption cooling system is the flat-plate solar collector. Alam et al. (2013) stated that the optimization of the cycle time reduces collector size. The collector first absorbs incoming solar radiation and then converts it to thermal

energy that heats up refrigerant fluid flowing through the collector. The whole process is affected by incoming solar radiation, duration of sunlight, and the thermal properties of the collector adsorption tubes, glazing materials, heat insulators, and transparent cover.

Yadav and Bajpai (2012) experimentally investigated the performance of a flat-plate solar collector with evacuated adsorption tubes and found that the solar collector with adsorption tubes has better thermal performance than a flat-plate solar collector without adsorption tubes. The main objective of this study is to develop a solar-driven adsorption cooling system with storage chamber and to investigate its thermal performance under different climatic conditions.

## 2. Materials and methods

### 2.1. Flat-plate adsorption solar collector

The construction of a flat-plate solar collector with polystyrene foam casing, blackened absorber surface, and transparent cover sheets is shown in Fig. 1a and b. The adjustable stand mounted solar collector is inclined toward the horizon of 80 °C (summer) and oriented to the south (Boxwell, 2015). The dimension of the rectangular casing is 1700 × 1000 × 300 × 50 mm and well insulated by 30 mm thick Rockwool. The insulated material provides sealing and reduces heat loss from the back or sides of the collector casing. The thermophysical properties of the insulating materials,

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**Nomenclature**

$A$	area, m <sup>2</sup>	$\varphi$	latitude, °
$T_{amb}$	ambient temperature, °C	$\rho$	density, kg/m <sup>3</sup>
$N$	number of transparent covers	$\varepsilon$	porosity
$\varepsilon_{pl}$	absorber plate emissivity	<b>Subscripts</b>	
$\varepsilon_{gc}$	transparent cover emissivity	sol	solar radiation
$U$	overall heat transfer coefficient, W/m <sup>2</sup> K	be	direct beam
$u$	specific internal energy, J/kg	gr	ground
$\chi^*$	adsorbed phase concentration ratio at equilibrium, kg/kg	sr	sky reflection
$W_o$	maximum adsorption capacity, m <sup>3</sup> /kg	i	ambient air
$q_{sh}$	isosteric heat of adsorption or desorption, J/kg	p	porosity
$C$	specific heat, J/kg·K	at	adsorption tube
$D$	constant in Dubinin-Astakhov equation	p	particle
$h$	specific enthalpy, J/kg	e	evaporator
$L$	latent heat of vaporization, J/kg	c	collector
$m$	mass, kg	D	difference/change
$n$	constant in Dubinin-Astakhov equation	s	solid
$P$	pressure, Pa	gen	generation
$T$	temperature, K	con	condenser or condensation
$V$	volume, m <sup>3</sup>	vp	vapor pressure
$Q$	thermal energy, J	max	maximum
$y$	wetness fraction	min	minimum
$I_T$	incident solar radiation, W/m <sup>2</sup>	ev	evaporator
$t$	time (s)	amb	ambient or atmospheric
$T_w$	initial water temperature, °C	ads	adsorption
$C_w$	specific heat of water, kJ/kg·K	des	desorption
$C_{ice}$	specific heat of ice, kJ/kg·K	f	fluid or liquid
$L_f$	latent heat of ice fusion, kJ/kg	sh	heat of adsorption/desorption
$\delta m_{con}$	differential mass of methanol vapor that flows towards the condenser tube	ap	adsorbed phase
<b>Greek symbols</b>		p	particle
$\varnothing$	diameter, mm	tr	true
$\sigma$	Stefan-Boltzmann constant	<b>Abbreviations</b>	
$\lambda$	wavelength	COP	coefficient of performance
$\omega$	hour angle, °	GAC	granular activated carbon

transparent cover and heat absorbing materials are shown in Table 1.

The collector casing is covered with a high transmittance Plexiglas plate (1940 × 940 × 3 mm). The optical and thermal properties of the Plexiglas made casing retaining the stagnant air layer between the absorber plate and the cover glass. It also reduces the convective losses from the absorber plate and adsorption tube. A 0.5 mm thick aluminium made blackened absorber plate with attached copper made adsorption tubes (Ø40 mm) maximize the radiant energy absorption and transfer the absorbed heat to a working fluid (methanol) at a minimum temperature difference, and minimum radiant emission.

Fig. 1c shows an evacuated copper tube (Ø15 mm) is placed inside a vacuum-sealed adsorption tube and attached to a blackened absorber plate. The space between the bigger and smaller diameter adsorption tube is filled with GAC and methanol. The length of the bigger and smaller diameter adsorption tubes are 1010 mm and 1000 mm, respectively. The adsorption tube is perforated with holes (Ø0.3 mm), is hollow, and the inside space is evacuated. The perforated adsorption tube promotes the state change process of the liquid methanol inside the adsorption tube and eases methanol flow to and from the GAC. The methanol liquid within the adsorption tube heats and turns to vapor when solar radiation falls on the surface of the absorber plate and adsorption tube, and later evacuated through the link tubes. The closed ends of the adsorption tubes placed inside the casing through twelve holes (Fig. 1d).

## 2.2. Condenser

The condenser is an air-cooled heat exchanger which releases heat to the surrounding environment through fins. The methanol vapor (flows from the solar collector adsorption tube during desorption) is liquefied by the influence of natural air flow throughout the condenser and then stored in the storage tank, as shown in Fig. 3a. Later the condensed liquid methanol is gravity-fed to the evaporator using V<sub>3</sub> valve. As shown in Fig. 2a, the heat exchanging surface of the condenser is 900 × 460 mm consisting 80 copper fins (7 × 7 mm).

## 2.3. Evaporator

The evaporator stores the entire condensed methanol received from the condenser storage tank. The heat exchange surface of the evaporator is constructed as a series of six trapezoidal cells as shown in Fig. 2b (the dimensions of the evaporator are 320 × 210 × 100 mm). The evaporator is made of copper sheet and partly immersed in a water tank (Fig. 5), and both the evaporator and water tank are placed in a Rockwool box.

## 2.4. Storage chamber

The dimensions of the storage chamber are 520 × 520 × 320 × 50 mm. The storage chamber maintains lower temperatures during the daytime by circulating melted ice by a

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