Journal of Nuclear Materials 493 (2017) 343-367



Contents lists available at ScienceDirect

Journal of Nuclear Materials

journal homepage: www.elsevier.com/locate/jnucmat



Review

Understanding the reaction of nuclear graphite with molecular oxygen: Kinetics, transport, and structural evolution



Joshua J. Kane ^{a, *}, Cristian I. Contescu ^b, Rebecca E. Smith ^a, Gerhard Strydom ^c, William E. Windes ^a

^a Materials Science & Engineering Department, Energy & Environmental Science and Technology, Idaho National Laboratory, Idaho Falls, ID 83415, USA

^b Materials Science and Technology Division, Oak Ridge National Laboratory, Oak Ridge, TN, USA

^c Reactor Physics Design & Analysis, Nuclear Science and Technology, Idaho National Laboratory, Idaho Falls, ID 83415, USA

HIGHLIGHTS

• Critical review of graphite oxidation relevant to a high-temperature gas-cooled reactor.

• Assesses oxidation in terms of microstructure and its evolution.

• Model is applicable to all nuclear graphites by using a grade independent kinetics model for the graphite-O₂ reaction system.

ARTICLE INFO

Article history: Received 14 December 2016 Received in revised form 19 May 2017 Accepted 2 June 2017 Available online 8 June 2017

Keywords: Graphite Oxidation Intrinsic kinetic model Microstructure Kinetics Mass transport Structural evolution

ABSTRACT

For the next generation of nuclear reactors, HTGRs specifically, an unlikely air ingress warrants inclusion in the license applications of many international regulators. Much research on oxidation rates of various graphite grades under a number of conditions has been undertaken to address such an event. However, consequences to the reactor result from the microstructural changes to the graphite rather than directly from oxidation. The microstructure is inherent to a graphite's properties and ultimately degradation to the graphite's performance must be determined to establish the safety of reactor design. To understand the oxidation induced microstructural change and its corresponding impact on performance, a thorough understanding of the reaction system is needed. This article provides a thorough review of the graphitemolecular oxygen reaction in terms of kinetics, mass and energy transport, and structural evolution: all three play a significant role in the observed rate of graphite oxidation. These provide the foundations of a microstructurally informed model for the graphite-molecular oxygen reaction system, a model kinetically independent of graphite grade, and capable of describing both the observed and local oxidation rates under a wide range of conditions applicable to air-ingress.

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Contents

1.	Terminology	. 345				
2.	2. Prologue					
3.	Introduction	. 346				
	3.1. Nuclear application of graphite	.346				
	3.1.1. Relevant air oxidation scenarios	. 346				
	3.1.2. Oxidation inputs for simulation and design	. 347				
	3.2. Current oxidation kinetics models	. 347				
	3.3. Limitations of current kinetic models	. 347				
4.	Article overview	. 350				
5.	The graphite-oxygen reaction mechanism	. 350				

* Corresponding author. E-mail address: Joshua.kane@inl.gov (J.J. Kane).

http://dx.doi.org/10.1016/j.jnucmat.2017.06.001 0022-3115/Published by Elsevier B.V.

	5.1.	Assumptions of an intrinsic reaction model	350
	5.2.	Reaction mechanism	350
	5.3.	Surface area classifications	353
	5.4.	Oxygen transfer model	353
		5.4.1. Advantages of the oxygen transfer model	354
		5.4.2. Dependence of effective parameters on temperature and oxygen concentration	354
		5.4.3. Changing effective rate constant	354
		5.4.4. Changing effective activation energy	355
	5.5.	Deficiencies of the oxygen transfer model and an alternative stochastic approach	355
6.	Additio	onal considerations for understanding observed oxidation rates	356
	6.1.	Microstructural dependence of graphite-oxygen reaction	356
	6.2.	Effects of gas transport through pores on observed oxidation rates	357
	6.3.	Effects of dynamic pore evolution on effective and observed rates	360
7.	Predict	ting observed rates via intrinsic kinetics and microstructural parameters	360
	7.1.	Equations for describing the observed oxidation rate	360
	7.2.	Structurally dependent oxidation parameters	362
	7.3.	Advantages of a microstructurally dependent oxidation model	363
8.	Researc	ch efforts towards enhancing a microstructurally dependent oxidation model	364
	8.1.	Kinetic models	364
	8.2.	Characterization of microstructural oxidation parameters	364
	8.3.	Non-equimolar gas transport	365
9.	Summa	ary	365
	Acknow	wledgements	365
	Referei	nces	365

Nomenclature

All symbols are listed in order of appearance.						
Symbol	Description	Units/Value	Equation(s)			
φ _n	Thiele modulus: ϕ_n^2 relates the ratio of surface reaction rate to an effective rate of diffusion through a porous material.	Unitless	NA			
\mathbf{k}_0	A rate constant used for a semi-empirical fit of experimental data to a rate law.	Varies	1,2			
E _A	Activation energy	kJ	1,2			
R	Universal gas constant	8.3145 <u>J</u>	1,2			
Т	Temperature	K or °C	1,2,12,13,25,30			
n	Reaction order	Unitless	1,2			
Po	Partial pressure of molecular oxygen gas	Varies	1			
[0 ₂]	Concentration of molecular oxygen gas	mol	2,11-13,19,21-23,25			
x	Stoichiometric coefficient of $CO(g)$. Purposely expressed as seen in Eq. (5) to represent the fraction of $CO(g)$ gaseous product	Unitless	3,21-23,25			
Ce	Carbon edge atom at a {100} and {110} surface	NA	4,5,7,8			
$C_{e}(O_{2})$	Surface dioxyranyl reactive intermediate	NA	4,5,7			
C _e (O)	Surface semiquinone reactive intermediate	NA	4,5,7			
C _b	Carbon atom within basal plane, (001) surface	NA	5,6,8			
C _b (O)	Stable/mobile surface intermediate, epoxy bridge	NA	5-7			
k _{A1}	Reaction rate constant for Eq. (4a)	Kane et al. [29]	4a,11,13			
k _{A2}	Reaction rate constant for Eq. (4b)	Kane et al. [29]	4b,11,13			
k _s ∙k _s *	Reaction rate constant for Eq. (5)	Kane et al. [29]	5,11,13			
k _{Hop}	Reaction rate constant for Eq. (6)	Kane et al. [29]	6			
$\boldsymbol{k}_{\boldsymbol{D}1} \cdot \boldsymbol{k}_{\boldsymbol{D}1}^*$	Reaction rate constant for Eq. (7a)	Kane et al. [29]	7a,10,11,13			
$k_{D2} \cdot k_{D2}^{*}$	Reaction rate constant for Eq. (7b)	Kane et al. [29]	7b,10,11,13			
k _{D3} · k [*] _{D3}	Reaction rate constant for Eq. (7c)	Kane et al. [29]	7c,10,11,13			
k _{NSD}	Reaction rate constant for Eq. (8)	Kane et al. [29]	8			
θ	Surface coverage as defined in Eq. (9)	Unitless	9			
Nc	Carbon molar flux towards the graphite surface	$\frac{mol}{m^2s}$	10-12			
$[\boldsymbol{C_e}(\boldsymbol{O}_2)]$	Surface density of dioxyranyl reactive intermediate	$\frac{mol}{m^2}$	10			
[C _e (O)]	Surface density of semiquinone reactive intermediate	$\frac{mol}{m^2}$	10			
Гe	Surface density of ASA	$\frac{mol}{m^2}$	11,13			
k [″] aff	Effective reaction rate constant for graphite-oxygen reaction normalized to ASA	<u>m</u> 5	12,13,19,2123,25			
N_A, N_B, N_i	Gaseous flux of arbitrary gaseous species A or B or specific gaseous component i	- mol	14-16,20-24,			
C _T	Total gas phase concentration	m-s mol	14,15,20			
D _{AB}	Binary gaseous diffusion coefficient for arbitrary species A and B	$\frac{m^2}{m^2}$	14,15,31			
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