



Effect of a real steam turbine on thermoeconomic analysis of combined cycle power plants



Carlo Carcasci ^a, Lorenzo Cosi ^b, Riccardo Ferraro ^b, Beniamino Pacifici ^{c,*}

^a DIEF: Department of Industrial Engineering, University of Florence, Via Santa Marta, 3, Florence, Italy

^b GE Oil&Gas, Florence, Italy

^c Department of Innovation & Information Engineering, Guglielmo Marconi University, Via Plinio, 44, Rome, Italy

ARTICLE INFO

Article history:

Received 9 January 2017

Received in revised form

15 June 2017

Accepted 9 July 2017

Available online 10 July 2017

Keywords:

Combined cycle

Gas turbine

Heat recovery steam generator

Thermoeconomic analysis

Manufacturing cost

Steam turbine

ABSTRACT

The continuing depletion of fossil fuels and the growing restrictions for greenhouse emissions, leads to reprocess wasted heat generated by power plants. For this purpose, Combined Cycles Gas Turbine (CCGT) represent a strong technology to obtain, an increase of performances and competitive costs within global market.

To design the CCGT configuration, energy engineering companies should define and analyze the performances of bottomer cycle, imposing operating parameters of steam turbine and heat recovery boiler. Usually, these plant components are supplied by different manufacturers so the plant could not be globally optimized.

Considering a steam turbines manufacturer as GE Oil&Gas, a high level of components integration, is a chance to optimize globally the bottomer cycle, determining the best machine in terms of efficiency and improving plant productivity. This aim could be obtained through the development of a high level of combination between company simulation codes and energy balance codes.

In this paper, a two-pressure level combined cycle is examined and optimized. The best thermoeconomic configuration is obtained: first, imposing steam turbine efficiency and using literature costs correlations; then, acquiring the efficiency by a steam turbine industrial tool and considering real machines costs. Therefore, two distinct best configurations could be determined and compared.

© 2017 Elsevier Ltd. All rights reserved.

1. Introduction

Nowadays, the continuing depletion of fossil fuels coupled together with emissions restrictions attributable to greenhouse gases, steers to reprocess wasted heat generated by power plants with the aim of enhance global efficiency. One of the technology employed for advancements is the combined cycle power plant. In a progressively competitive market, managed by profits, cutting costs for generating electricity is coming to be crucial, in order to ensure a fast return on investment, however without reducing the power plant reliability and flexibility. Currently, available power-generation combined-cycle plants achieve net plant thermal efficiency typically in the 50–55% LHV range. Further development of gas turbine, high-temperature materials and hot gas path cooling

technology, show promise for near-term future power generation combined-cycle systems, capable of reaching 60% or greater plant thermal efficiency [1].

Often, an energy engineering company should define and to analyze the performances of bottomer steam cycle, imposing the operating parameters of the steam turbine and of the heat recovery boiler. Usually two or more distinct manufacturers fabricate these elements. Due to this, the plant could not be globally optimized, because the energy-balance designer can get the real steam turbine performance and cost only after the entire bottomer cycle is defined.

Considering a steam turbines manufacturer's point of view, as GE Oil&Gas, the integration between a property simulation code and an energy balance code is a chance to evaluate globally the bottomer cycle in order to determine the best plant configuration and to help the final customer to operate properly the plant.

Fig. 1 shows the stream cycle of the process followed to optimize the bottomer plant in the two cases: standard case, using literature costs correlations and a constant value for the efficiency of ST; the

* Corresponding author.

E-mail address: b.pacifici@unimarconi.it (B. Pacifici).

Nomenclature			
A	Final section area, [m ²]	LP	Low pressure
c	Cost, [M\$]	LTE	Low Temperature Economizer
COE	Cost of Energy, [\$/MWh]	O&M	Operating and Maintenance
E	Energy, [kW]	pp	Pinch Point
m	Mass flow, [kg/s]	pump	Pump
p	Pressure, [Pa]	sh	Superheater
T	Temperature, [K]	ST	Steam turbine
x	steam quality, [–]	stack	Stack
W	Power, [kW]	sub	Subcooling
η	Efficiency, [–]	TCR	Total Capital Requirement
		tot	Total
		v	Vapor
<i>Subscript</i>		<i>Acronyms</i>	
app	Approach	BOP	Balance of Plant
bott	Bottomer	C	Compressor
CC	Combined Cycle	CC	Combustion Chamber
Cond	Condenser	CCGT	Combined Cycle Gas Turbine
eco	Economizer	COE	Cost of Energy
eva	Evaporator	GT	Gas Turbine
f	fuel	HP	High Pressure
gas	gas	HRSG	Heat Recovery Steam Generator
HP	High pressure	LTE	Low Temperature Economizer
HRSG	Heat recovery steam generator	LP	Low Pressure
in	Inlet	O&M	Operating and Maintenance Cost
inj	Injection	SPRINT	Spray inter-cooled turbine
is	Iisentropic	ST	Steam Turbine
l	Liquid	T	Turbine/expander
lim	Limit	TEC	Total Equipment Cost

case proposed in this paper, where real parameters of ST costs and efficiency are used.

In the standard case the process will stop at the first cycle, when the bottomer cycle is optimized from a thermodynamic point of view, without considering variation of efficiency and real models of ST. In the new case, first cycle is the same of the previous one, when first attempt of best plant configuration is found, combining the industrial tool with the energy balance code, a new configuration of ST is found. So, is possible to discover new best plant configurations.

A thermodynamic and economic analysis of combined cycle power plants was carried out by several authors [2–23]. Attala et al. [2] have developed a tool aimed at thermo-economic valuation and

optimization of thermal power plants. Roosen et al. [3] considered the optimization of a combined cycle, proceeding with a strict direct cost assessment. Rao and Francuz [4] found and evaluated advanced improvements for combined cycle that will manage to get considerable performance improvements in coal based power systems. Carapellucci and Giordano [5] made a comparison between two different approaches for optimizing CCGTs. Zhu et al. [6] considered the effect of solar addition to describe the combination of solar thermal energy with a natural gas combined-cycle (NGCC) power plant. Tică et al. [7] showed a method to convert a CCGT physical model designed for simulations in an optimization-oriented model, which can be further used with efficient algorithms to improve start-up performances. Ganjehkaviri et al. [8]

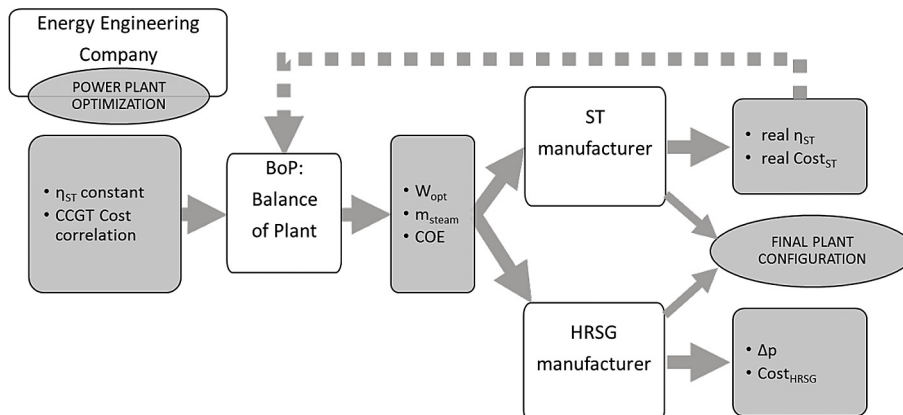


Fig. 1. Stream cycle of the two processes adopted (dashed line is new iterative procedure).

Download English Version:

<https://daneshyari.com/en/article/5475483>

Download Persian Version:

<https://daneshyari.com/article/5475483>

[Daneshyari.com](https://daneshyari.com)