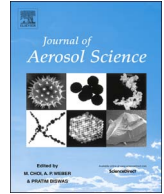




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# Experimental study of cyclone performance for blow-by gas cleaning applications



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## ABSTRACT

The aim of this experimental study is to investigate the separation performances of a new set of small cyclones. The diameter of these cyclones spans the range of 20–45 mm, which is the typical size of these devices when they are used for separating oil mist from blow-by gases in internal combustion engines. To reproduce the flow rates and oil load of combustion engines, we developed a flow bench, with a polydisperse aerosol generator producing engine oil droplets with diameter in a 0.3–10 μm range. Measurements of the aerosol particle concentrations upstream and downstream of the cyclone permitted the determination of the particle collection efficiency, for the six devices that were tested, with flow rates ranging from 20 to 200 NL/min which are typical operating conditions. For the six cyclones, the geometry is normalized and all internal dimensions within the cyclone are proportional to its diameter. With the operating conditions of this study, the annular Reynolds number varied in the range  $1.27 \times 10^3$  to  $12.2 \times 10^3$ . From the measured fractional collection efficiency curves, dimensionless cut-off aerodynamic diameters were determined. These measurements have been compared with available correlations for the determination of this dimensionless diameter as a function of the annular Reynolds number. Different correlations are proposed in this study, for the evaluation of the cut-off diameter and for the shape of the collection efficiency. We were able to establish that the collection efficiency curve dimensionless slope is correlated to a Reynolds number.

## 1. Introduction

Cyclone separators are commonly used in industry to remove solid or liquid particles from a gas stream. These devices are frequently applied to large-scale processes, for both separation and drying applications. Small cyclones have also found various applications, such as personal cyclone samplers applied to environment control. They are also widely used in the automotive industry, particularly in internal combustion engines for the separation of oil mist from blow-by gases. These so-called “blow-by gases” result from leakages between the combustion chamber and the crankcase. These gases flow through the crankcase which contains lubricating oil and the resulting oil mist has to be cleaned up, for pollution control, oil consumption reduction and also to avoid turbo charger oil coking. This is an important feature of crankcase venting systems, and the design of the separation cyclone is of great importance for its collection efficiency: a reduction of the cyclone diameter produces an increase of the collected oil flow, but also results in increased pressure drops.

Various numerical or experimental studies have been carried out to determine the influence of the flow rate and cyclone

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Nomenclature	
$a$	first regression coefficient (dimensionless cut-off aerodynamic diameter), dimensionless
$A_i$	regression coefficient (Lidén & Gudmundsson, 1997), dimensionless
$b$	second regression coefficient (dimensionless cut-off aerodynamic diameter), dimensionless
$B_i$	cyclone dimensional ratios (Lidén & Gudmundsson, 1997), dimensionless
$C_{cmd}$	Cunningham-Millikan-Davies coefficient, dimensionless
$c_o$	ratio of particle mass flow to the air mass flow, dimensionless
$d$	particle geometric diameter, (m)
$d_{ae}$	particle aerodynamic diameter, (m)
$d_{50,MM}$	cut-off diameter evaluated using Muschelknautz's model, see Eq. (3), (m)
$D$	cyclone body diameter, see Fig. 1, (m)
$D_o$	cyclone vortex finder diameter, see Fig. 1, (m)
$D_t$	10 mm tube diameter used in connecting parts, see Fig. 2, (m)
$D_{t,mod}$	$D_{t,mod} = 30$ mm, large tube diameter in improved set-up, see Fig. 20, (m)
$D_p$	particle diffusivity (Mothes and Löffler's model), ( $m^2 s^{-1}$ )
$E$	collection efficiency, dimensionless
$Eu_{in}$	Euler number, see Eq. (16), dimensionless
$f$	wall friction factor in Muschelknautz's model, see Table 1, dimensionless
$H$	height of cyclone inlet slit, see Fig. 1, (m)
$Kn$	Knudsen number, dimensionless
$L$	characteristic cyclone length, (m)
$L_b$	height of cylindrical part of cyclone, see Fig. 1, (m)
$L_c$	height of conical part of cyclone, see Fig. 1, (mm)
$Q_v$	volumetric flow rate, $Nl\ min^{-1}$ (Normal Liter per Minute, Normal conditions being 0 °C and 1.01325 Pa)
$R_{in}$	radial position of the center of the inlet in Muschelknautz's model, see Table 1, (m)
$R_m$	geometric mean radius in Muschelknautz's model, see Table 1, (m)
$Re_R$	cyclone body Reynolds number in Muschelknautz's model, see Table 1, dimensionless
$Re_{ann}$	annular cyclone Reynolds number, dimensionless
$Re$	Reynolds number, dimensionless
$S$	vortex finder length, see Fig. 1, (m)
$S_f$	friction surface in Muschelknautz's model, see Table 1, ( $m^2$ )
$St$	Stokes number, see Eq. (1), dimensionless
$U$	characteristic gas velocity in cyclone, ( $m\ s^{-1}$ )
$u_{in}$	average gas velocity at cyclone inlet, ( $m\ s^{-1}$ )
$v_o$	outlet axial velocity in the vortex finder, in Muschelknautz's model, see Table 1, ( $m\ s^{-1}$ )
$v_{zw}$	“wall axial velocity” in Muschelknautz's model, see Table 1, ( $m\ s^{-1}$ )
$v_{\theta CS}$	“spin velocity near the wall” in Muschelknautz's model, see Table 1, ( $m.s^{-1}$ )
$v_{\theta m}$	“geometrical mean rotational velocity” in Muschelknautz's model, see Table 1, ( $m.s^{-1}$ )
$W$	width of cyclone inlet slit, see Fig. 1, (m)
$W_1$	dimensionless slope, see Eq. (15), dimensionless
$x_{fact,MM}$	correction factor in Muschelknautz's model, see Eq. (3), dimensionless
<i>Greek letters</i>	
$\alpha$	entrance “constriction coefficient” in Muschelknautz's model, see Table 1, dimensionless
$\eta$	collection efficiency, dimensionless
$\kappa_1$	steepness parameter for cyclone efficiency, see Eq. (15), dimensionless
$\mu_g$	gas dynamic viscosity, ( $kg\ m^{-1}\ s^{-1}$ )
$\rho_g$	gas density, ( $kg\ m^{-3}$ )
$\rho_p$	particle density, ( $kg\ m^{-3}$ )
$\xi_b$	cyclone body pressure loss coefficient, based on $v_o$ in Muschelknautz's model, see Table 1, dimensionless
$\xi_o$	outlet tube pressure loss coefficient, based on $v_o$ in Muschelknautz's model, see Table 1, dimensionless
$\xi$	$W/(0.5D)$ in Muschelknautz's model, see Table 1, dimensionless
$\Psi_{50}$	dimensionless cut-off aerodynamic diameter or cut-off parameter, see Eq. (5), dimensionless
<i>Subscripts</i>	
50	at 50% efficiency
in	at the inlet conditions
MM	corresponding to Muschelknautz's model, see Table 1.
ML	corresponding to Mothes & Löffler's model

geometrical parameters on the separation performances. Cut-size diameters which correspond to 50% collection efficiency have been reported in the literature, for a wide range of cyclones, together with theoretical models. Cortés and Gil (2007) proposed a review of these models developed for the evaluation of the cyclone separators collection efficiency. However, it should be noted that currently available studies on small cyclones with liquid aerosol are limited.

In this experimental study, we propose to investigate the collection efficiency performances of a new set of six small cyclones with diameters in the range of 20–45 mm (C-20 to C-45), which are typical of combustion engine crankcase applications where oil droplets polydisperse aerosols are collected. This set of cyclones which are fully homothetic will be referred to as the SFYB family.

## 2. Review of cyclone modeling

### 2.1. Cut-off diameter

Together with the pressure drop, the major characteristic of a cyclone flow is the cut-off diameter  $d_{ae,50}$  that corresponds to a 50%

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